

US EPA ARCHIVE DOCUMENT

**Table A-1**  
**GHG Emission Summary**  
**Formosa Plastic Corporation, Texas**  
**2012 Expansion Project: Gas Turbines**  
**March 2014**

Source Name	Operating Scenario	EPN	Detailed Calculations in	GHG Mass Emissions (tpy)	CO <sub>2</sub> e (tpy)
Gas Turbine 1	Firing 100% Natural Gas	7K	Table A-2	463,071	463,540
Gas Turbine 2		7L		463,071	463,540
Duct Firing, Unit 1 [1]	Firing 100% Natural Gas	7K	Table A-3	61,449	61,511
	Firing 100% OL Tail Gas		Table A-4	53,041	53,103
	Firing 100% Hydrogen [2]		N/A	0	0
Duct Firing, Unit 2 [1]	Firing 100% Natural Gas	7L	Table A-3	61,449	61,511
	Firing 100% OL Tail Gas		Table A-4	53,041	53,103
	Firing 100% Hydrogen [2]		N/A	0	0
<b>Subtotal Total, Combined Cycle Units [3] =</b>				<b>1,049,040</b>	<b>1,050,103</b>
Turbine Startup, Fuel Line Maintenance [4]	Startup, Maintenance	7K-NGVENT, 7L-NGVENT	Table A-5	1.24	29.9
Fugitive Components [4]	N/A	NG-FUG	Table A-6	20.90	506.1
SF <sub>6</sub> Electrical Insulation [4]	N/A	SF6-FUG	Table A-7	<0.01	28.2
<b>Total =</b>				<b>1,049,062</b>	<b>1,050,667</b>

Notes:

[1] The duct burners may fire up to 100% heat input on any listed fuel or any combination thereof.

[2] Combustion of 100% hydrogen fuel stream in the duct burners does not result in any GHG emissions (carbon content is zero).

[3] Total GHG emissions are calculated as the maximum emissions from duct burner firing on any one of the three fuel types, plus GHG emission contributions from the Gas turbines.

[4] FPC TX Requests that No Emission Limit be established for this source.

Compliance will be assured with the design/work practice standard as specified in the permit.

**Table A-2**  
**GHG Emission Calculations - Natural Gas Combustion - Gas Turbines**  
**Formosa Plastic Corporation, Texas**  
**2012 Expansion Project: Gas Turbines**  
**March 2014**

**GHG Emissions Contribution From Natural Gas Fired Combustion Turbines:**

EPN	Average Heat Input (MMBtu/hr)	Annual Heat Input (MMBtu/yr)	Pollutant	Emission Factor (kg/MMBtu) <sup>1</sup>	GHG Mass Emissions <sup>2</sup> (tpy)	Global Warming Potential <sup>3</sup>	CO <sub>2</sub> e (tpy)
7K	997	8,733,720	CO <sub>2</sub>	53.02	463,062	1	463,062
			CH <sub>4</sub>	1.0E-03	8.73	25	218.3
			N <sub>2</sub> O	1.0E-04	0.87	298	260.3
			<b>Totals</b>	<b>463,071</b>			<b>463,540</b>
7L	997	8,733,720	CO <sub>2</sub>	53.02	463,062	1	463,062
			CH <sub>4</sub>	1.0E-03	8.73	25	218.3
			N <sub>2</sub> O	1.0E-04	0.87	298	260.3
			<b>Totals</b>	<b>463,071</b>			<b>463,540</b>
<b>Total for 2 Turbines</b>				<b>926,143</b>			<b>927,081</b>

Notes:

1. CO<sub>2</sub> GHG factor from Table C-1 of 40 CFR 98 Mandatory Greenhouse Gas Reporting (GHG MRR). CH<sub>4</sub> and N<sub>2</sub>O GHG factors based on Table C-2 of GHG MRR.
2. CO<sub>2</sub> emissions based on 40 CFR Part 98, Subpart C, Equation C-1.
3. Global Warming Potential factors based on Table A-1 of 40 CFR 98 Mandatory Greenhouse Gas Reporting.

Sample Calculation, CO<sub>2</sub>:

$$\text{GHG Mass Emissions (metric ton/yr)} = 0.001 \times 8733720 \text{ (MMBtu/yr)} \times 53.02 \text{ kg/MMBtu} = 463062$$

$$\text{CO}_2\text{e (metric ton/yr)} = 463062 \text{ (tpy)} \times 1 = 463062$$

**Table A-3**  
**GHG Emission Calculations - Duct Burners Natural Gas Combustion**  
**Formosa Plastic Corporation, Texas**  
**2012 Expansion Project: Gas Turbines**  
**March 2014**

GHG Emissions Contribution From Natural Gas Fired Combustion:					Emissions per Unit			
Source Type	Average Heat Input/Unit (MMBtu/hr)	Annual Avg Heat Input, Each Unit (MMBtu/yr)	Pollutant	Emission Factor (kg/MMBtu) <sup>1</sup>	GHG Mass Emissions <sup>2</sup> (metric ton/yr)	Global Warming Potential <sup>3</sup>	CO <sub>2</sub> e (metric ton/yr) (tpy)	
Turbine 1 Duct Burners	120	1,051,200	CO <sub>2</sub>	53.02	55,735	1	55,735	61,447
			CH <sub>4</sub>	1.0E-03	1.05	25	26.3	29.0
			N <sub>2</sub> O	1.0E-04	0.11	298	31.3	34.5
				<b>Totals</b>	<b>55,736</b>		<b>55,792</b>	<b>61,511</b>
Turbine 2 Duct Burners	120	1,051,200	CO <sub>2</sub>	53.02	55,735	1	55,735	61,447
			CH <sub>4</sub>	1.0E-03	1.05	25	26.3	29.0
			N <sub>2</sub> O	1.0E-04	0.11	298	31.3	34.5
				<b>Totals</b>	<b>55,736</b>		<b>55,792</b>	<b>61,511</b>
Total, All Natural Gas Duct Firing					<b>111,472</b>		<b>111,584</b>	<b>123,022</b>

Notes:

1. CO<sub>2</sub> GHG factor from Table C-1 of 40 CFR 98 Mandatory Greenhouse Gas Reporting (GHG MRR). CH<sub>4</sub> and N<sub>2</sub>O GHG factors based on Table C-2 of GHG MRR.
2. CO<sub>2</sub> emissions based on 40 CFR Part 98, Subpart C, Equation C-1.
3. Global Warming Potential factors based on Table A-1 of 40 CFR 98 Mandatory Greenhouse Gas Reporting.

Sample Calculation, CO<sub>2</sub>:

GHG Mass Emissions (metric ton/yr) = 0.001 x 1051200 (MMBtu/yr) x 53.02 kg/MMBtu = 55735

CO<sub>2</sub>e (metric ton/yr) = 55735 (metric ton/yr) x 1 = 55734.6

**Table A-4**  
**GHG Emission Calculations - OL Tail Gas Combustion**  
**Formosa Plastic Corporation, Texas**  
**2012 Expansion Project: Gas Turbines**  
**March 2014**

**Olefins (OL) Tail Gas Data:**

Variable	Value	Units	Reference
Net Heating Value (LHV)	624	Btu/scf	Formosa Design Specification
Carbon Content (Annual Avg)	0.677	kg C/kg	Formosa Design Specification
Molecular Weight (Annual Avg)	9.77	kg/kg-mol	Formosa Design Specification

**GHG Emissions Contribution from OL Tail Gas Combustion:**

Source Type	Average Heat Input/Unit (MMBtu/hr)	Annual Average Fuel Gas Usage/Unit <sup>1</sup> (MMscf/hr)	Annual Average Fuel Use, Each Unit (scf/yr)	Annual Average Heat Input, Each Unit (MMBtu/yr)	Pollutant	Emission Factor (kg/MMBtu) <sup>2</sup>	GHG Mass Emissions <sup>3</sup> (metric ton/yr)	Global Warming Potential <sup>4</sup>	CO <sub>2</sub> e (metric ton/yr)	CO <sub>2</sub> e (tpy)		
Turbine 1 Duct Burners	120	0.192	1.68E+09	1.05E+06	CO <sub>2</sub>		48,109	1	48,109	53,040		
					CH <sub>4</sub>	1.0E-03	1.05	25	26.28	29		
					N <sub>2</sub> O	1.0E-04	0.11	298	31.33	35		
						<b>Totals</b>	<b>48,110</b>		<b>48,166</b>	<b>53,103</b>		
Turbine 2 Duct Burners	120	0.192	1.68E+09	1.05E+06	CO <sub>2</sub>		48,109	1	48,109	53,040		
					CH <sub>4</sub>	1.0E-03	1.05	25	26.28	29		
					N <sub>2</sub> O	1.0E-04	0.11	298	31.33	35		
						<b>Totals</b>	<b>48,110</b>		<b>48,166</b>	<b>53,103</b>		
<b>Total, All OL Tail Gas Combustion</b>							<b>96,220</b>		<b>96,333</b>	<b>106,207</b>		

Notes:

1. Fuel use calculated as: MMscf/hr = Firing rate (MMBtu/hr) / HHV (Btu/scf)

2. CH<sub>4</sub> and N<sub>2</sub>O GHG factors based on Table C-2 of 40 CFR 98 Mandatory Greenhouse Gas Reporting.

CH<sub>4</sub> and N<sub>2</sub>O emissions based on 40 CFR Part 98, Subpart C, Equation C-8.

3. CO<sub>2</sub> emissions based on 40 CFR Part 98, Subpart C, Equation C-5.

4. Global Warming Potential factors based on Table A-1 of 40 CFR 98 Mandatory Greenhouse Gas Reporting.

Sample Calculation: Duct Burners Turbine 1 - CO<sub>2</sub>:

GHG Mass Emissions (metric ton/yr) = (44/12) x 1.68E+09 (scf/yr) x 0.677 kg C/kg x 9.77 kg/kg-mol / 849.5 scf/kg-mole @ std cond. x 0.001 = 4.81E+04

CO<sub>2</sub>e (metric ton/yr) = 4.81E+04 (metric ton/yr) x 1 = 4.81E+04

**Table A-4A**  
**GHG Emission Calculations - Duct Burners OL Tail Gas Combustion**  
**Formosa Plastic Corporation, Texas**  
**2012 Expansion Project: Gas Turbines**  
**March 2014**

**OL Tail Gas Composition**

Compound	Molecular Weight (lb/lbmol)	Lower Heating Value, LHV (Btu/lb)	Lower Heating Value, LHV (Btu/scf)	Molar Composition (mol %) [1]	Component Lower Heating Value, LHV (Btu/scf)	Number of carbons	Component Carbon Mass (lbC/lbmol)	Fuel Carbon Mass (lbC/lbmol)	Component Mass per Lbmol Gas (lb)	carbon content (lbC/lb)
Hydrogen	2.016	51,571	274	45.00%	123.44	0	0	0.000	0.907	<b>0.677</b>
Methane	16.04	21,504	910	55.00%	500.55	1	12	6.600	8.822	
Ethane	30.07	20,429	1,621	0.000050%	0.00	2	24	0.000	0.000	
Propane	44.09	19,923	2,318	0.000010%	0.00	3	36	0.000	0.000	
Carbon Monoxide	28.01	321	323	0.1500%	0.485	1	12	0.018	0.042	
Carbon Dioxide	44.009	0	0	0.0050%	0.000	1	12	0.001	0.002	

Gross heating  
value = 624  
Btu/scf

MW = 9.77  
lb/lbmol

Notes:

[1] Composition is representative and may vary. Estimated composition used for emission calculation purposes only.

**Table A-5**  
**GHG Emission Calculations -**  
**Gaseous Fuel Venting During Turbine Startup and**  
**Fuel Line Maintenance, EPNs 7K-NGVENT, 7L-NGVENT**  
**Formosa Plastic Corporation, Texas**  
**2012 Expansion Project: Gas Turbines**  
**March 2014**

Location	Initial Conditions			Final Conditions			Annual Frequency of Event	CO <sub>2</sub> <sup>3</sup>	CH <sub>4</sub> <sup>4</sup>	Total, both Turbines
	Volume <sup>1</sup> (ft <sup>3</sup> )	Press. (psig)	Temp. (°F)	Press. (psig)	Temp. (°F)	Volume <sup>2</sup> (scf)		Annual (tpy)	Annual (tpy)	Annual (tpy)
Turbine Startup	75.0	300	90	0	68	1,635	30	0.0336	0.98	
Fuel Line Maintenance	20.0	300	90	0	68	436	24	0.00718	0.210	
GHG Mass-Based Emissions								0.0408	1.19	1.24
Global Warming Potential <sup>5</sup>								1	25	
CO <sub>2</sub> e Emissions								0.0408	29.9	29.9

## Notes:

- Initial volume is calculated by multiplying the cross-sectional area by the length of pipe using the following formula:  $V_i = \pi * [(diameter\ in\ inches/12)/2]^2 * length\ in\ feet = ft^3$
  - Final volume calculated using ideal gas law  $[(PV/ZT)_i = (PV/ZT)_f]$ .  $V_f = V_i * (P_i/P_f) * (T_f/T_i) * (Z_f/Z_i)$ , where Z is estimated using the following equation:  $Z = 0.9994 - 0.0002P + 3E-08P^2$ .
  - $CO_2$  emissions based on vol% of  $CO_2$  in natural gas 1.20% from natural gas analysis
  - $CH_4$  emissions based on vol% of  $CH_4$  in natural gas 96.6% from natural gas analysis
  - Global Warming Potential factors based on Table A-1 of 40 CFR 98 Mandatory Greenhouse Gas Reporting

#### *Example calculation:*

<i>1635 scf Nat Gas</i>	<i>0.012 scf CO<sub>2</sub></i>	<i>lbmole</i>	<i>44 lb CO<sub>2</sub></i>	<i>ton =</i>	<i>=</i>	<i>0.0336</i>	<i>ton/yr CO<sub>2</sub></i>
<i>yr</i>	<i>scf Nat Gas</i>	<i>385 scf</i>	<i>lbmole</i>	<i>2000 lb</i>			

**Table A-6**  
**GHG Emission Calculations - Fugitive Component Emissions**  
**Formosa Plastic Corporation, Texas**  
**2012 Expansion Project: Gas Turbines**  
**March 2014**

**GHG Emissions Contribution From Fugitive Piping Components:**

EPN	Source Type	Fluid State	Count	Emission Factor <sup>1</sup> scf/hr/comp	CO <sub>2</sub> Content (vol %)	CH <sub>4</sub> Content (vol %)	CO <sub>2</sub> (tpy)	Methane (tpy)	Total (tpy)
NG-FUG	Valves	Gas/Vapor	600	0.121	1.20%	96.6%	0.436	12.80	
	Flanges	Gas/Vapor	2400	0.017			0.245	7.19	
	Relief Valves	Gas/Vapor	5	0.193			5.80E-03	1.70E-01	
	Sampling Connections	Gas/Vapor	10	0.031			1.86E-03	5.46E-02	
	Compressors	Gas/Vapor	3	0.002			3.60E-05	1.06E-03	
<b>GHG Mass-Based Emissions</b>							0.689	20.2	<b>20.9</b>
<b>Global Warming Potential<sup>2</sup></b>							1	25	
<b>CO<sub>2</sub>e Emissions</b>							0.69	505.4	<b>506.1</b>

Notes:

1. Emission factors from Table W-1A of 40 CFR 98 Mandatory Greenhouse Gas Reporting
2. Global Warming Potential factors based on Table A-1 of 40 CFR 98 Mandatory Greenhouse Gas Reporting.

*Example calculation:*

600 valves	0.121 scf gas	0.012 scf CO <sub>2</sub>	lbmol	44.01 lb CO <sub>2</sub>	8760 hr	ton	0.44	ton/yr
	hr * valve	scf gas	385 scf	lbmol	yr	2000 lb		

**Table A-7**  
**GHG Emission Calculations - Electrical Equipment Insulated with SF<sub>6</sub>**  
**Formosa Plastic Corporation, Texas**  
**2012 Expansion Project: Gas Turbines**  
**March 2014**

EPN	Insulated SF <sub>6</sub> Circuit Breaker Capacity (pounds)	Annual Leak Rate, wt %	Annual Leak Rate (tpy)	Global Warming Potential <sup>1</sup>	Estimated Annual CO <sub>2</sub> e Emission Rate (tpy)
SF6-FUG	495	0.50%	1.24E-03	22,800	28.2

Notes:

1. Global Warming Potential factors based on Table A-1 of 40 CFR 98 Mandatory Greenhouse Gas Reporting.