



Accelerating Design of Batteries Using Computer-Aided Engineering Tools



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Outline

- Motivation for Battery Computer-Aided Engineering (CAE)
- Multi-Physics Modeling at Various Scales
- NREL Modeling Approach (MSMD)
- Results
 - Impact of Cell Tab Locations
 - Impact of Cell Aspect Ratio
- Conclusions

Motivation for Battery Design Tools

Cell/battery development process for testing new materials in multiple cell sizes, in multiple pack designs, and over many months is extremely time consuming, expensive, and ad hoc

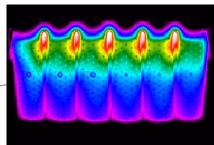
• Large cells/batteries suffer from heat, current, and stress issues not present in small configurations

CAE processes offer a methodology to shorten design cycle and optimize batteries for thermal uniformity, safety, long life, and low cost

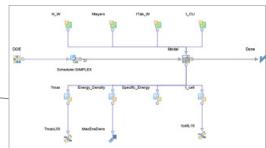
- Proven examples from automotive and aerospace
- Robust design, 6-sigma, design optimization,...

Requirements for large battery CAE:

- Efficient mathematical models (desktop PC)
- Capture correct physics and 3-D geometry



Thermal Image of Gen I Toyota Prius Module

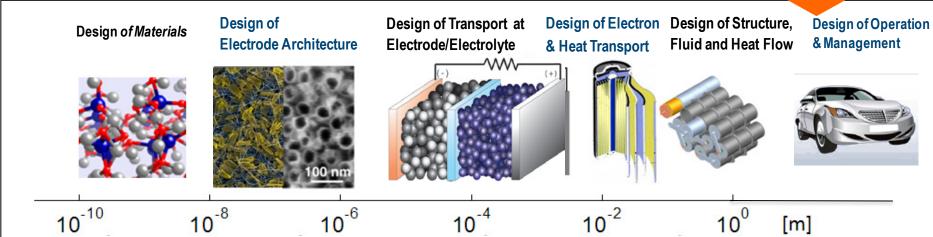


Process Integration, Design & Optimization (PIDO) Software

Multi-Scale Physics in Li-Ion Battery

"Requirements" are usually defined in a macroscale domain and in terms of:

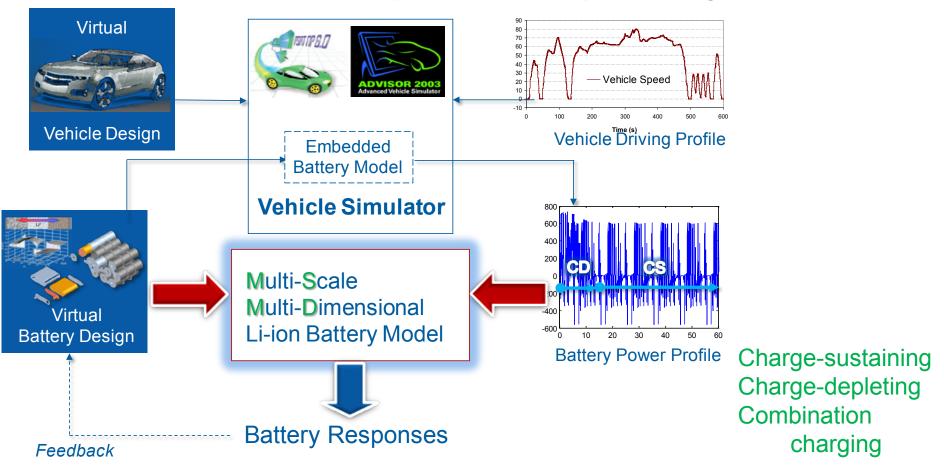
Performance
Life
Cost
Safety



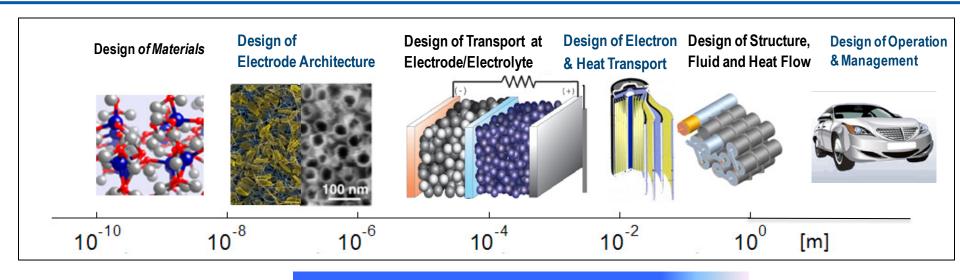
- Wide range of length and time-scale physics
- Design improvements required at different scales
- Need for better understanding of interaction among different-scale physics

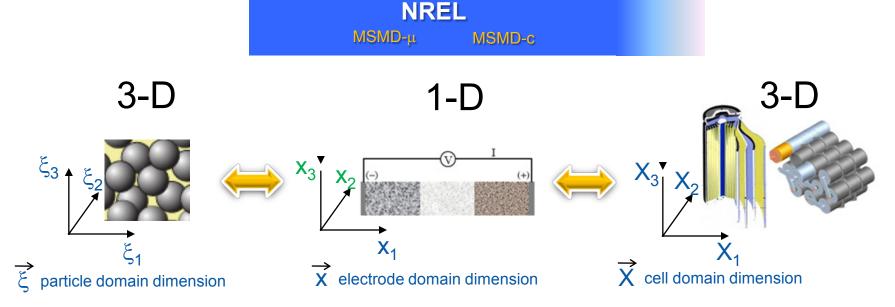
Virtual Integrated Design Battery Pack and Vehicle Simulations

Integrated design approach using a vehicle simulation tool with a battery pack simulation tool that has details of cell-level model embedded in it would be a powerful technique to design batteries



NREL's Multi-Scale Multi-Dimensional (MSMD) Model Efficient representation of 3-D electrochemical/thermal physics

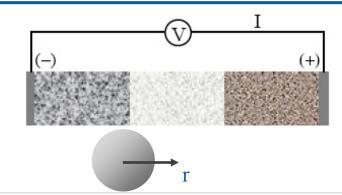




Electrode-Scale Performance Model in the NREL MSMD Model

Charge Transfer Kinetics at Reaction Sites

$$\begin{split} j^{Li} &= a_s i_o \left\{ \exp \left[\frac{\alpha_a F}{RT} \eta \right] - \exp \left[-\frac{\alpha_c F}{RT} \eta \right] \right\} \\ i_0 &= k (c_e)^{\alpha_a} (c_{s, \max} - c_{s, e})^{\alpha_a} (c_{s, e})^{\alpha_c} \quad \eta = (\phi_s - \phi_e) - U \end{split}$$



Species Conservation

$$\begin{split} &\frac{\partial c_s}{\partial t} = \frac{D_s}{r^2} \frac{\partial}{\partial r} \left(r^2 \frac{\partial c_s}{\partial r} \right) \\ &\frac{\partial \left(\mathcal{E}_e c_e \right)}{\partial t} = \nabla \cdot \left(D_e^{\it eff} \nabla c_e \right) + \frac{1 - t_+^o}{F} \, j^{\rm Li} - \frac{\mathbf{i}_e \cdot \nabla t_+^o}{F} \end{split}$$

Charge Conservation

$$\begin{split} &\nabla \cdot \left(\sigma^{\mathit{eff}} \nabla \phi_{\mathit{s}} \right) - j^{\mathrm{Li}} = 0 \\ &\nabla \cdot \left(\kappa^{\mathit{eff}} \nabla \phi_{\mathit{e}} \right) + \nabla \cdot \left(\kappa^{\mathit{eff}}_{\mathit{D}} \nabla \ln c_{\mathit{e}} \right) + j^{\mathrm{Li}} = 0 \end{split}$$

- Pioneered by Newman group (Doyle, Fuller, and Newman 1993)
- Captures *lithium diffusion dynamics* and *charge transfer kinetics*
- Predicts current/voltage response of a battery
- Provides design guide for thermodynamics, kinetics, and transport across electrodes

Energy Conservation

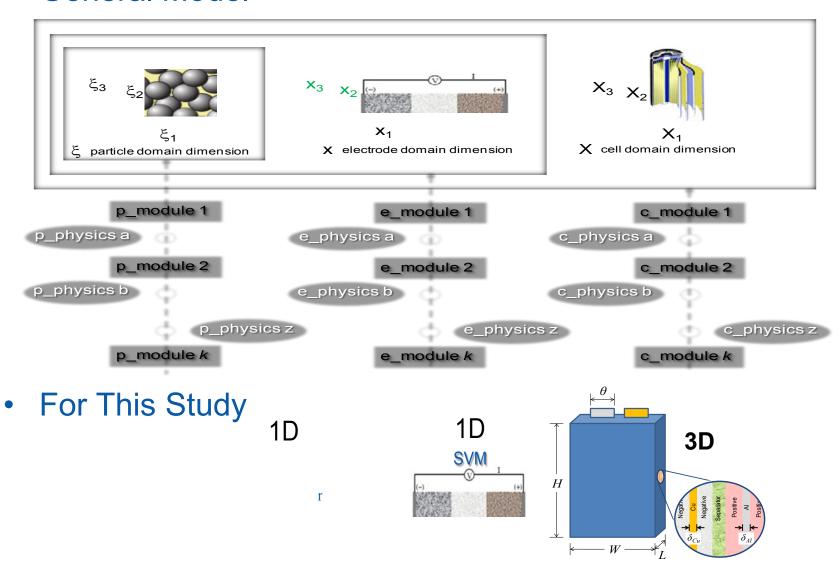
$$\rho c_{p} \frac{\partial T}{\partial t} = \nabla \cdot (k \nabla T) + q'''$$

$$q''' = j^{Li} \left(\phi_{s} - \phi_{e} - U + T \frac{\partial U}{\partial T} \right) + \sigma^{eff} \nabla \phi_{s} \cdot \nabla \phi_{s} + \kappa^{eff} \nabla \phi_{e} \cdot \nabla \phi_{e} + \kappa^{eff}_{D} \nabla \ln c_{e} \cdot \nabla \phi_{e}$$

Difficult to resolve *heat* and *electron current* transport

Modularized Hierarchy of Model Structure in NREL's MSMD Approach

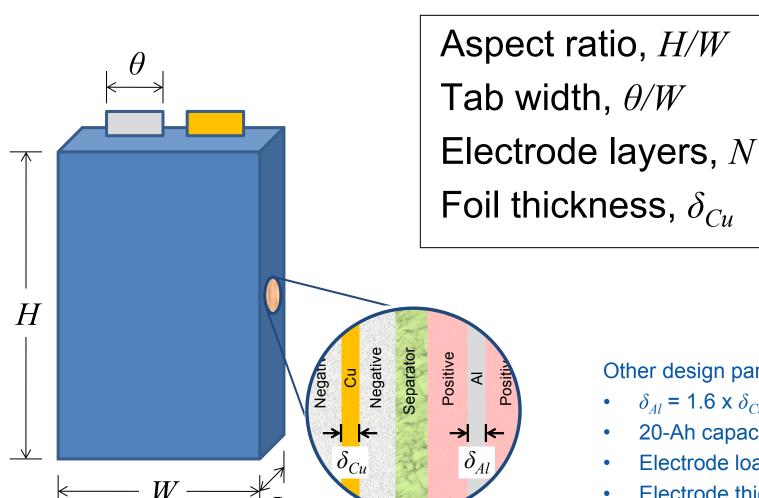
General Model



Results: Impact of Tab Location—Importance of Multi-Physics Interaction 30 mm Comparison of two 40-150 mm Ah flat-cell designs 2 min 5C discharge working potential working potential > Larger over-potential This cell is cycled promotes faster discharge more uniformly, can reaction therefore use less > Converging current 3.1 🔄 active material (\$) causes higher potential and is expected to 3.08 · 150 drop along the collectors have longer life. 100 0 0 0 Y(mm) Y(mm) X(mm) electrochemical electrochemical current production current production SOC SOC X(mm) Y(mm) 0 0 150 X(mm) 100 0 0 Y(mm) X(mm) X(mm) temperature temperature ➤ High temperature promotes faster electrochemical reaction ➤ Higher localized reaction causes more heat 50 100 0 0 Y(mm) X(mm) X(mm) generation

nickel-cobalt-aluminum (NCA) cathode and graphite anode

Macroscopic Parameters for Design



Other design parameters fixed:

- δ_{Al} = 1.6 x δ_{Cu}
- 20-Ah capacity
- Electrode loadings
- Electrode thicknesses (Typical tradeoff between power & energy does not arise in this study)

Design Impact of Alternative Aspect Ratio

1. Nominal Design

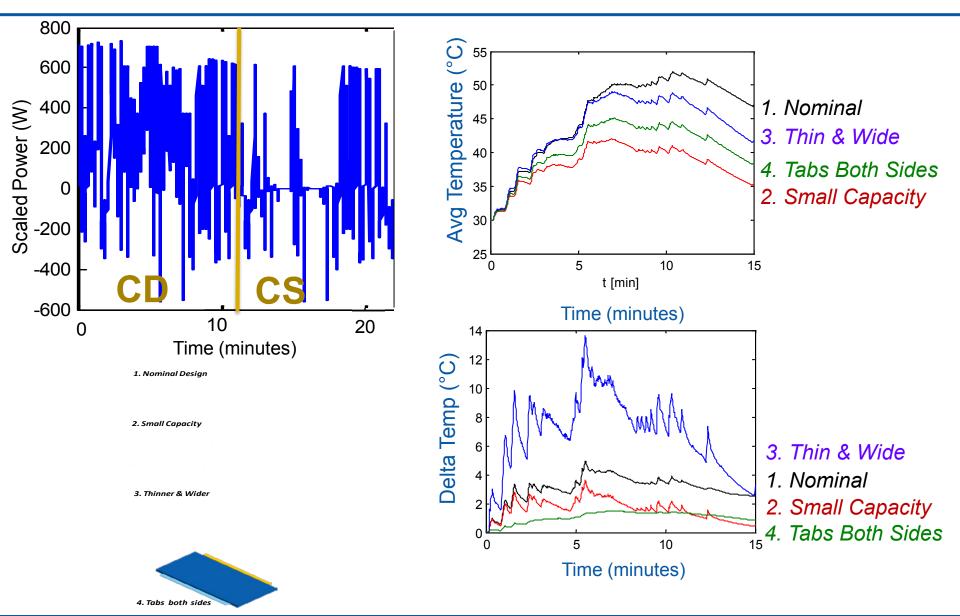
2. Small Capacity

3. Thinner & Wider

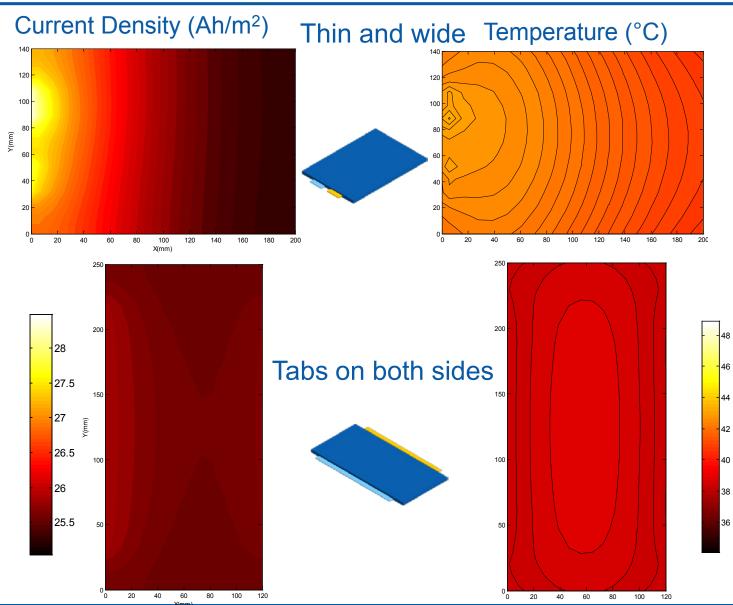
4. Tabs both sides

- 140 x 100 x 15 mm³
- Tabs on the same side
- 20 Ah
- Nominal area and thickness
- 3 x (140 x 100 x 5) mm³
- Same tab design
- 3 x 6.67 Ah
- Same electrode area/stack layer
- 1/3 thickness
- ~ 3x surface area
- 200 x 140 x 7.5 mm³
- Same tabs
- 20 Ah
- 2x electrode area/stack layer
- 1/2 thickness
- ~ 2x surface area
- 250 x 120 x 7 mm³
- Wide-counter tab design
- 20 Ah
- ~2x electrode area/stack layer
- ~1/2 thickness
- ~2x surface area

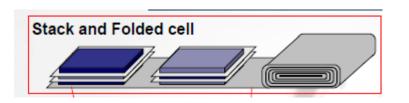
Results: Impact of Aspect Ratio



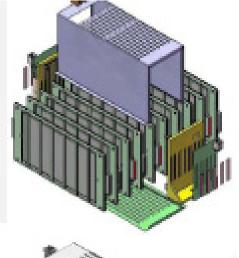
Imbalance Between 20-Ah Designs



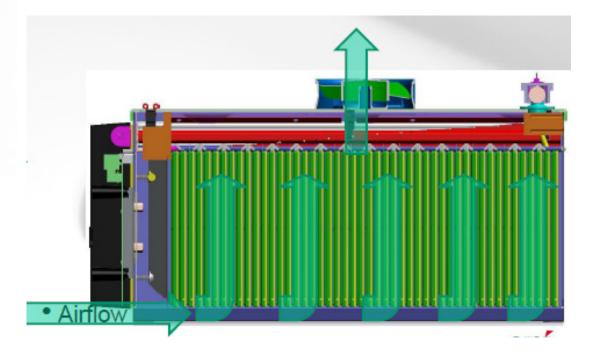
Cell to Pack Modeling Essential for Proper Thermal and Electrical Operations











Summary

- Non-uniform battery physics, which is more probable in largeformat cells, can cause unexpected performance and life degradations in lithium-ion batteries.
- Computer-aided engineering could investigate various design options quickly before fabrication and testing.
- A Multi-Scale Multi-Dimensional model was used for evaluating large-format prismatic automotive cell designs by integrating microscale electrochemical processes and macro-scale transports.
- A thin-form factor prismatic cell with wide counter tab design would be preferable to manage cell internal heat and electron current transport, and consequently to achieve uniform electrochemical kinetics over a system.
- Engineering questions to be addressed in the future using 3-D modeling include:
 - -What is the optimum form-factor and size of a cell?
 - Where are good locations for tabs or current collectors?
 - How different are externally proved temperature and electric signals from nonmeasurable cell internal values?
 - Where is the effective place for cooling? What should the heat-rejection rate be?

Thank You!

