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Syngas and Hydrogen Combustion: Ignition and Flame Propagation

Grant Number: DE-FG26-06NT42717

*Development of Comprehensive Detailed and Reduced Reaction Mechanisms for
Syngas and Hydrogen Combustion*

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University Coal Research Contractors Review Conference

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- This project aims to develop the tools necessary for the design of future synthesis-gas and hydrogen (SGH) fueled combustion turbines.
 - Generate a detailed experimental database of SGH combustion at IGCC-like conditions.
 - Investigate fundamental chemical kinetics of $\text{H}_2/\text{CO}/\text{O}_2/\text{N}_2/\text{H}_2\text{O}/\text{CO}_2$ at pressures, temperatures, and concentrations typical of SGH combustion in gas turbines
 - Develop detailed and reduced chemical mechanisms based on this database, capable of predicting NO_x formation during SGH combustion.

- Obtain benchmark experimental data for combustion characteristics of syngas
 - **Conterflow Burner Apparatus**
 - Laminar flame speeds
 - Extinction limits
 - Flame structure
 - **Rapid Compression Machine**
 - Ignition delays at elevated pressures
- Develop comprehensive and computationally-efficient chemical models
 - Assessment of available kinetic mechanisms
 - Theoretical calculations to determine critical rate constants
 - Mechanism optimization
 - Mechanism simplification and reduction

Accomplishments - Year 1

- Autoignition of dry H₂/CO mixtures at elevated pressures in a rapid compression machine.
- Assessment of kinetics of syngas combustion at elevated pressures using global uncertainty analysis methods.
- Reaction kinetics of CO+HO₂ – *ab initio* calculations.
- 3 journal publications and 1 under review.
- Preliminary experimentation on autoignition of wet H₂/CO mixtures at elevated pressures in a rapid compression machine.
- Preliminary experimentation to determine combustion characteristics of wet H₂/CO mixtures in a counterflow configuration.

- Autoignition of Dry H₂/CO Mixtures
 - Characterization of Rapid Compression Machine
 - Ignition Delay Results
 - “Brute Force” Sensitivity Analysis
 - Global Uncertainty Analysis
- Reaction Kinetics of CO+HO₂ → CO₂ + OH: *ab initio* Study and Master Equation Modeling
- Laminar Flame Speeds of Wet H₂/CO Mixtures with Preheat
 - Counterflow Burner Apparatus
 - Preliminary Results
- Conclusions
- Future Work



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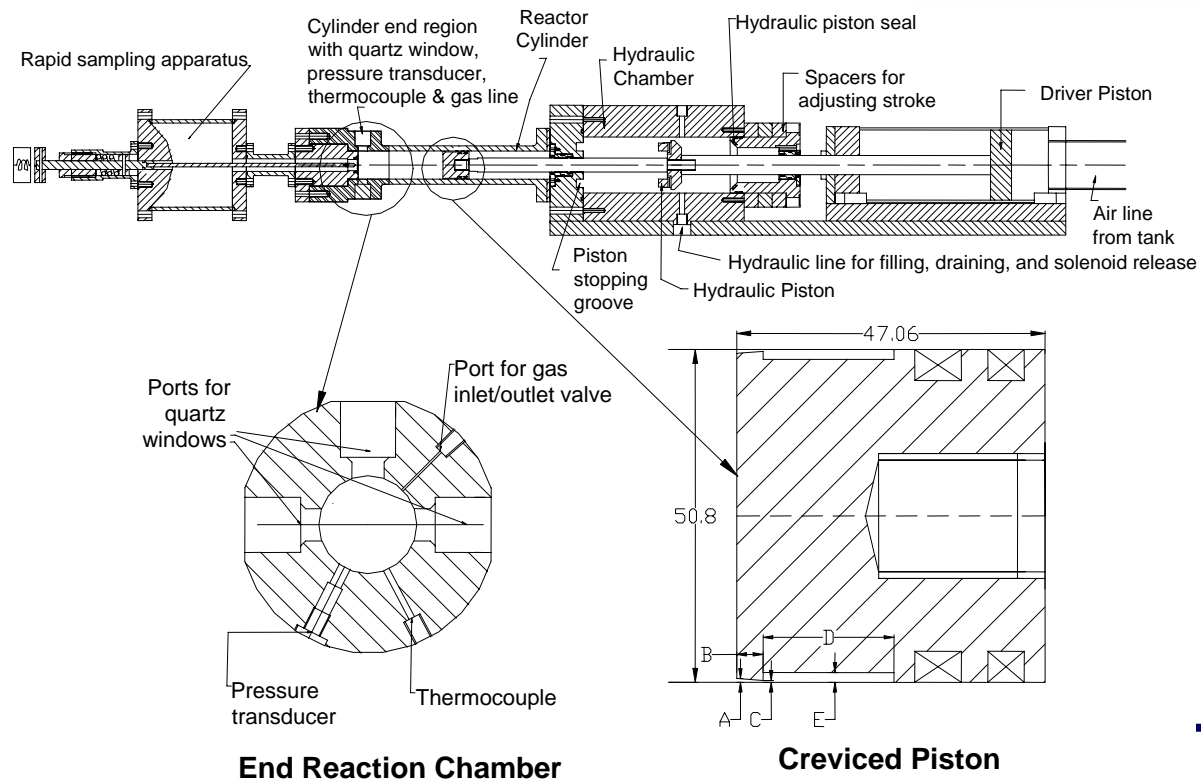
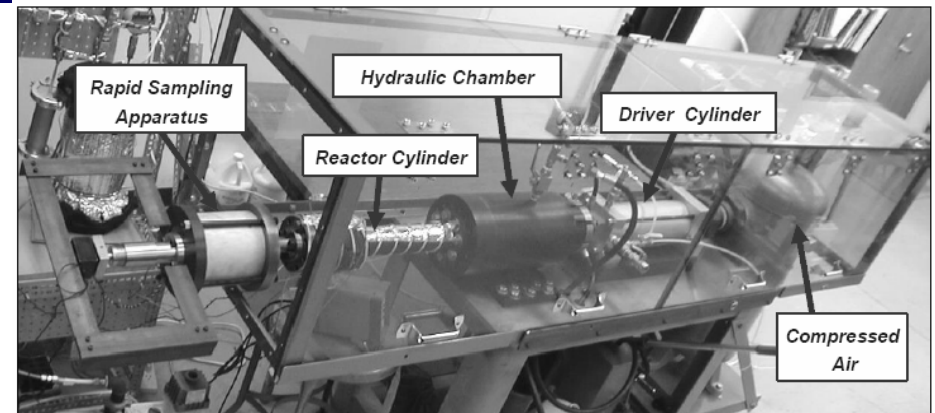
Autoignition of Dry H₂/CO Mixtures



**Combustion
Diagnostics
Laboratory**

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Rapid Compression Machine (RCM)





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Features of the Present RCM

- RCM simulates a single compression stroke of an engine
 - simple and relatively easy to operate
- Adjustable stroke and clearance
- Fast compression (< 30 ms)
- Compressed pressure up to 60 bar
- Temperature – 500 to 1100 K
- Elevated pressure condition is sustained up to 100 ms
- Optimized creviced piston for ensuring homogeneity of reacting mixture
- Optically accessible
- GC/MS and a fast sampling apparatus for species measurement
- Direct measurement of ignition delay
- Study of low-to-intermediate temperature chemistry



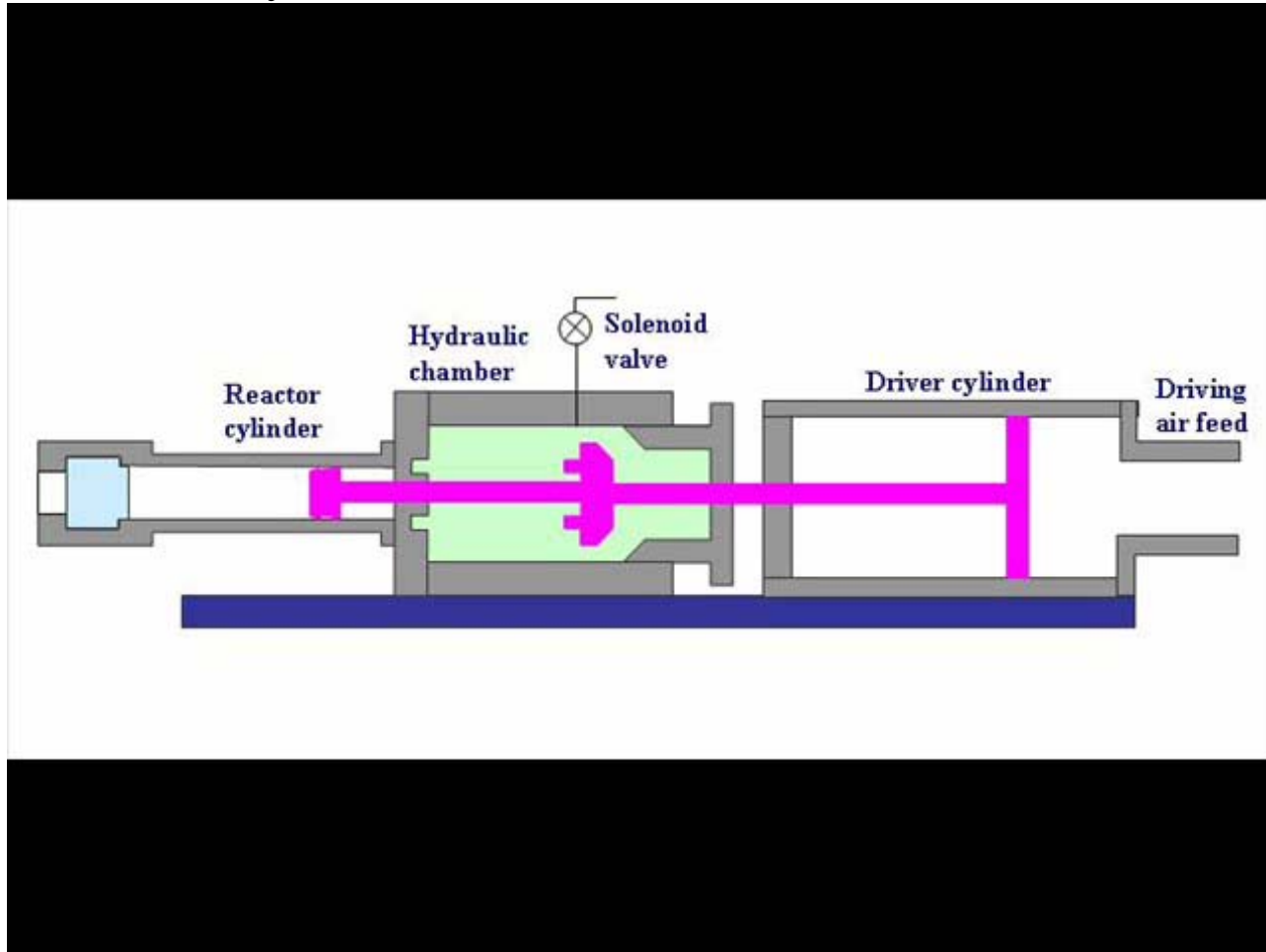


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RCM Operation

- Pneumatically driven
- Hydraulically actuated and stopped

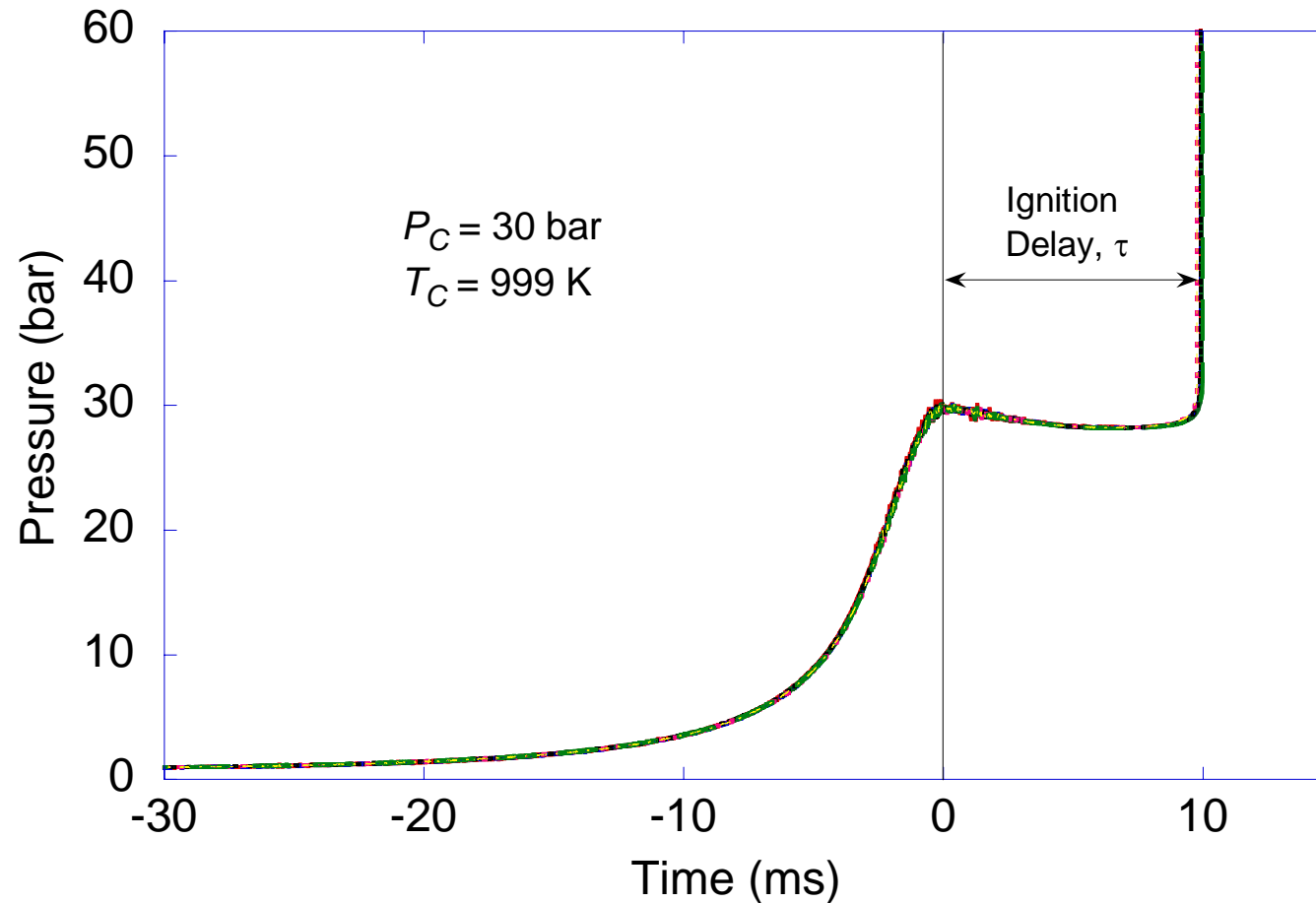




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Reproducibility



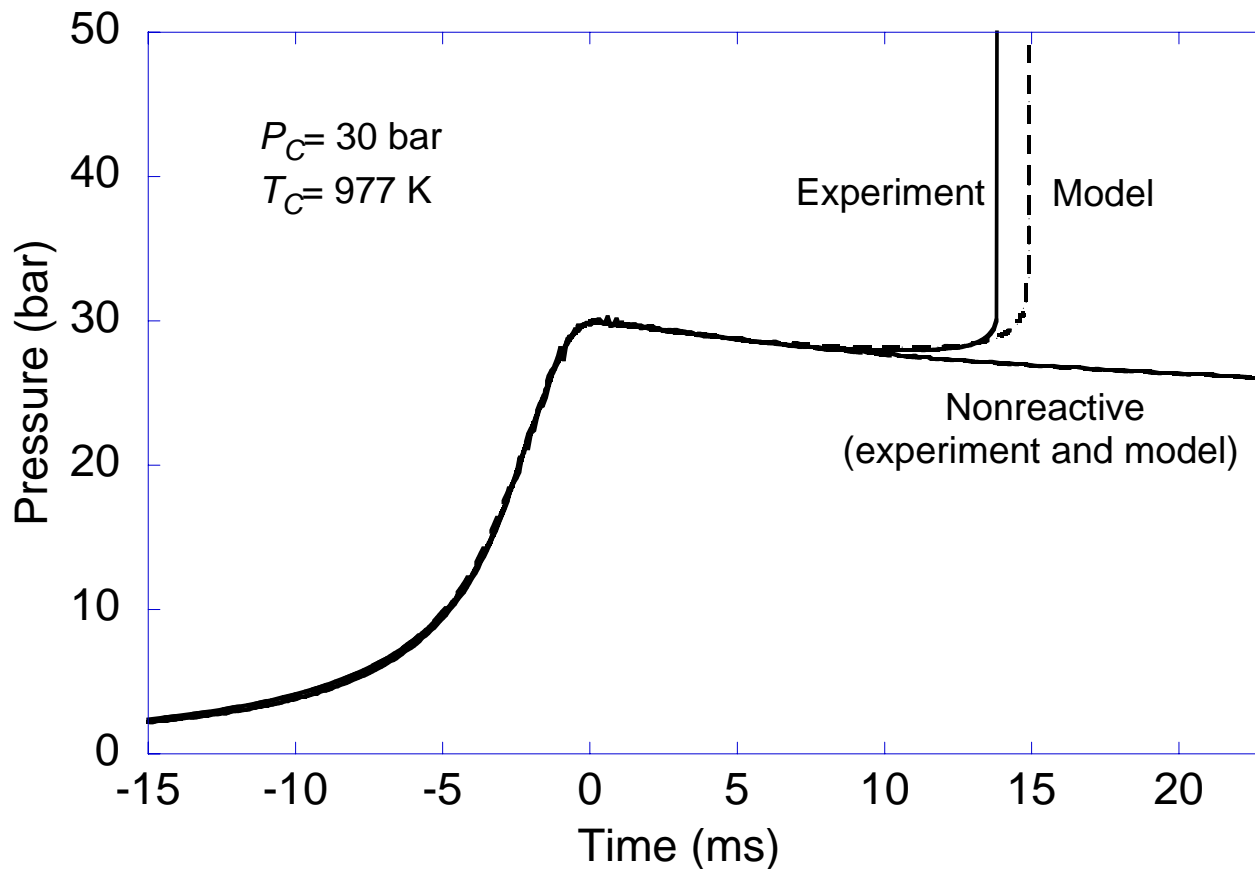
Molar composition: $H_2/CO/O_2/N_2/Ar = 9.375/3.125/6.25/18.125/63.125$

Initial conditions – $T_0 = 298.7$ K and $P_0 = 661$ Torr



Comparison of RCM Experiment and Model

Simulation using CHEMKIN and SENKIN – with volume specified as a function of time in a homogeneous adiabatic system.





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Dry H₂/CO Experiments – Specifications

- Temperature (T_C): 950 – 1100K
- Equivalence ratio (ϕ): 0.36 – 1.6
- Pressure (P_C): 15 – 50 bar
- $R_{CO} = [CO]/([H_2] + [CO])$: 0 – 0.80

Mixture #	ϕ	R_{CO}	H ₂	CO	O ₂	N ₂	Ar
1	1.0	0	12.5%	0%	6.25%	18.125%	63.125%
2	1.0	0.25	9.375%	3.125%	6.25%	18.125%	63.125%
3	1.0	0.50	6.25%	6.25%	6.25%	18.125%	63.125%
4	1.0	0.65	4.375%	8.125%	6.25%	18.125%	63.125%
5	1.0	0.80	2.5%	10%	6.25%	18.125%	63.125%
6	0.36	0.25	6.667%	2.222%	12.345%	14.418%	64.348%
7	0.72	0.25	6.667%	2.222%	6.173%	21.586%	63.352%
8	1.0	0.25	6.667%	2.222%	4.444%	23.600%	63.067%
9	1.3	0.25	6.667%	2.222%	3.419%	24.782%	62.910%
10	1.6	0.25	6.667%	2.222%	2.777%	25.511%	62.823%



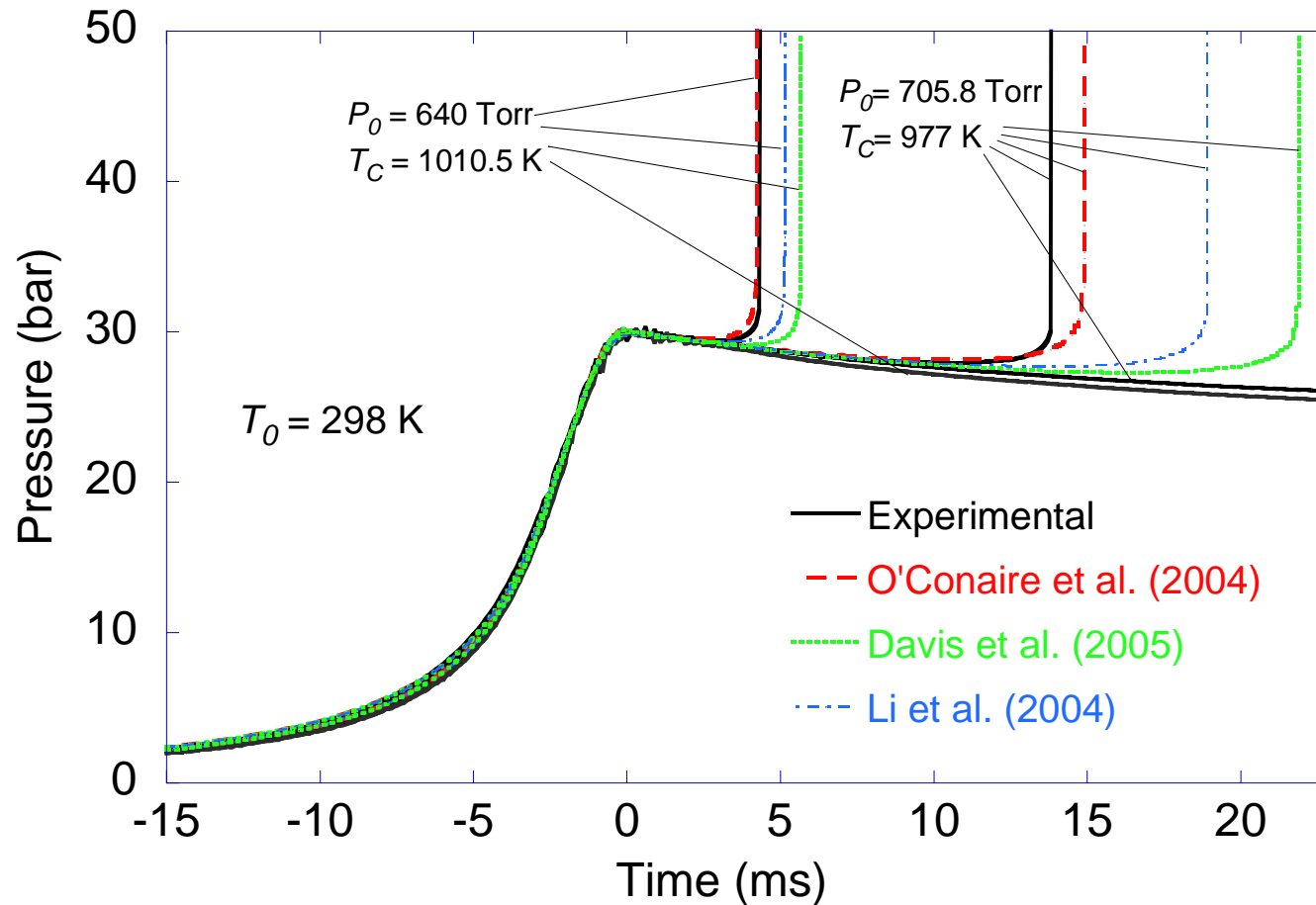


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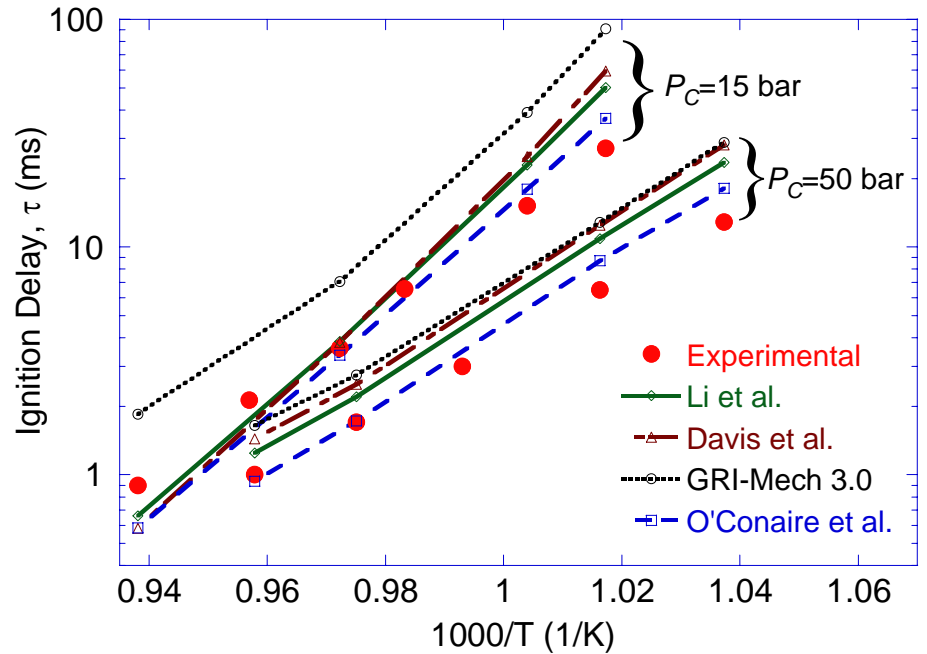
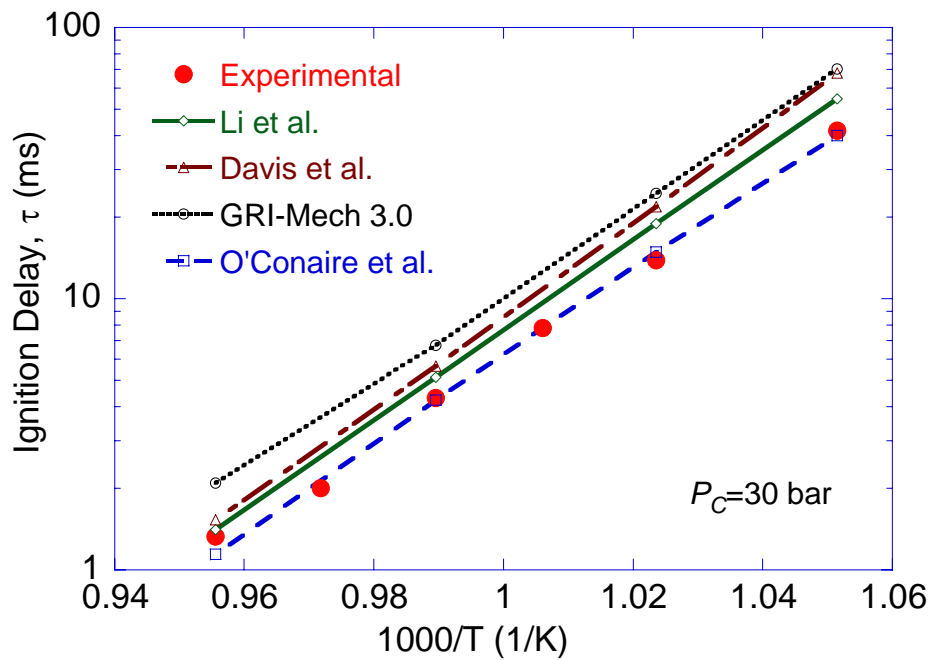
Hydrogen Ignition Delay (1)

- Stoichiometric hydrogen mixtures ($H_2/O_2/N_2/Ar = 2/1/2.9/10.1$)



Hydrogen Ignition Delay (2)

- $H_2/O_2/N_2/Ar = 12.5/6.25/18.125/63.125$

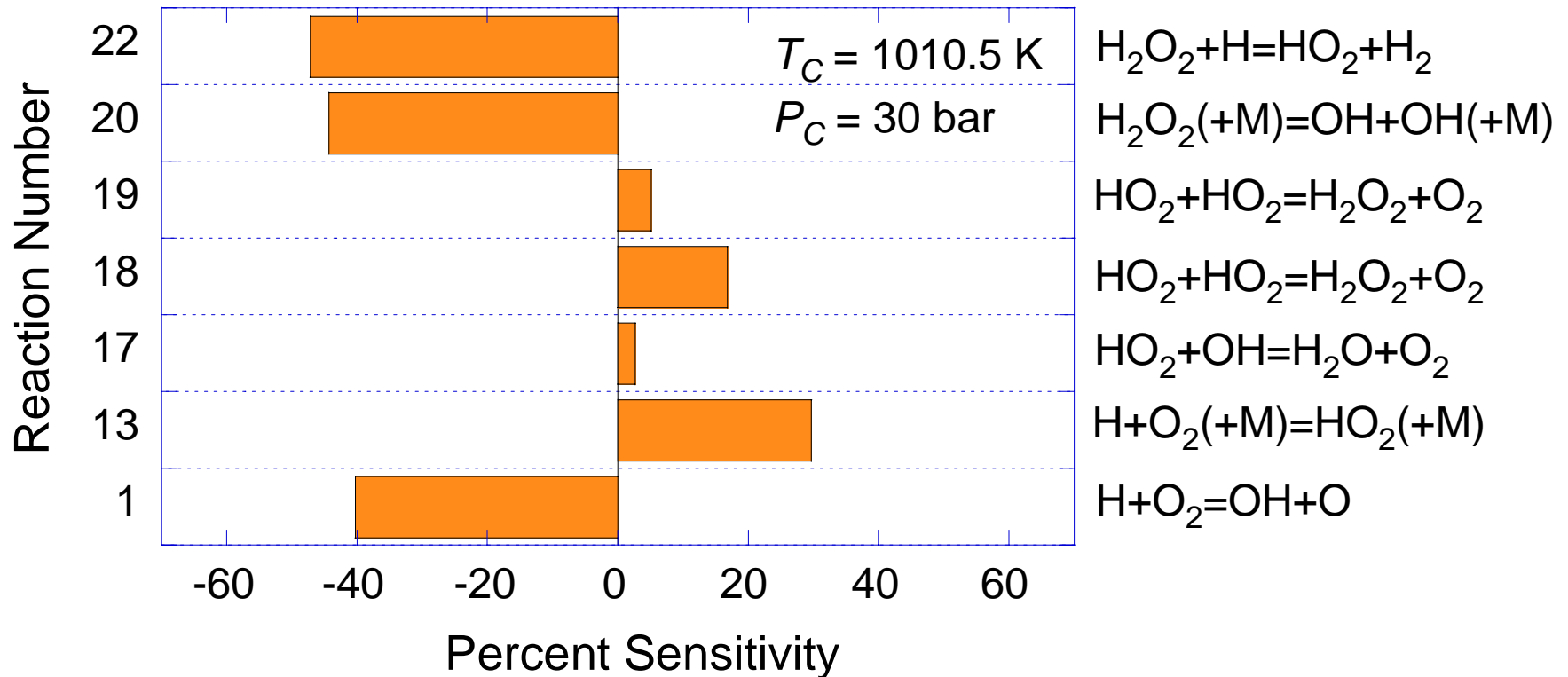




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“Brute Force” Sensitivity Analysis



Reactions involving formation and consumption of HO_2 and H_2O_2 are important.

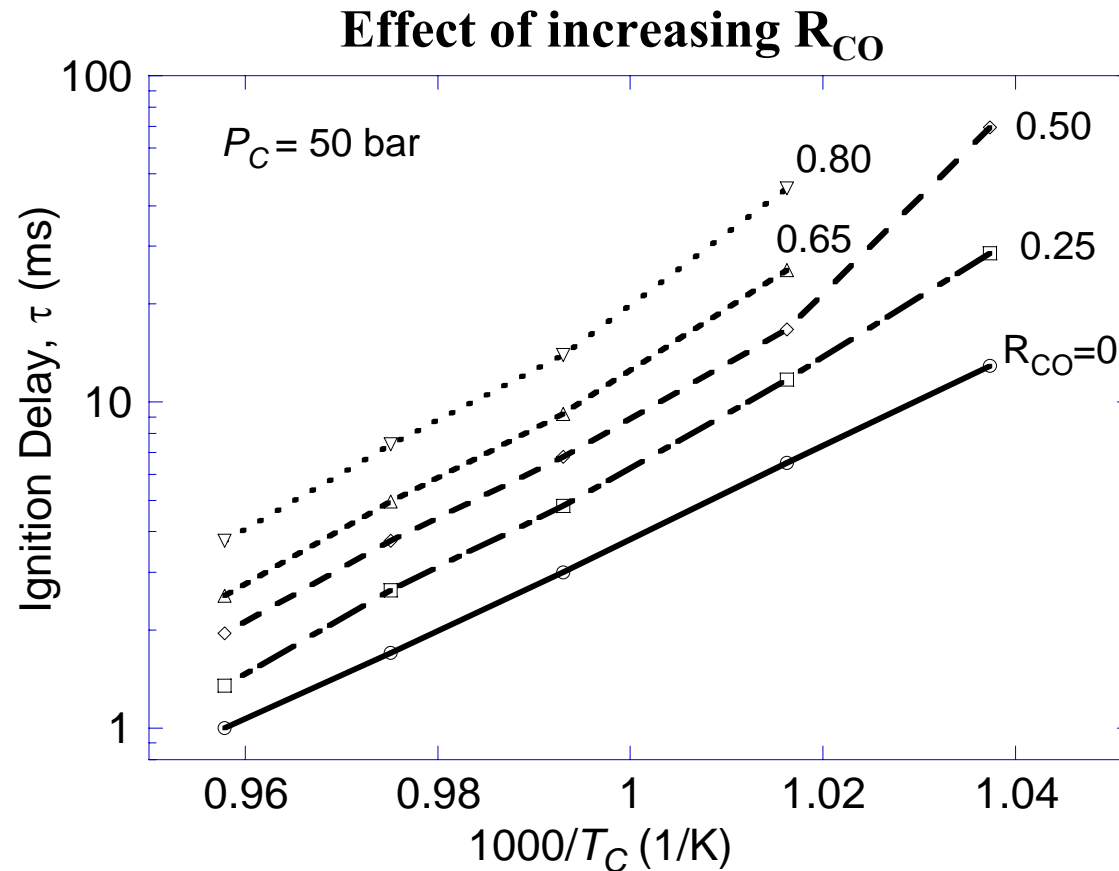




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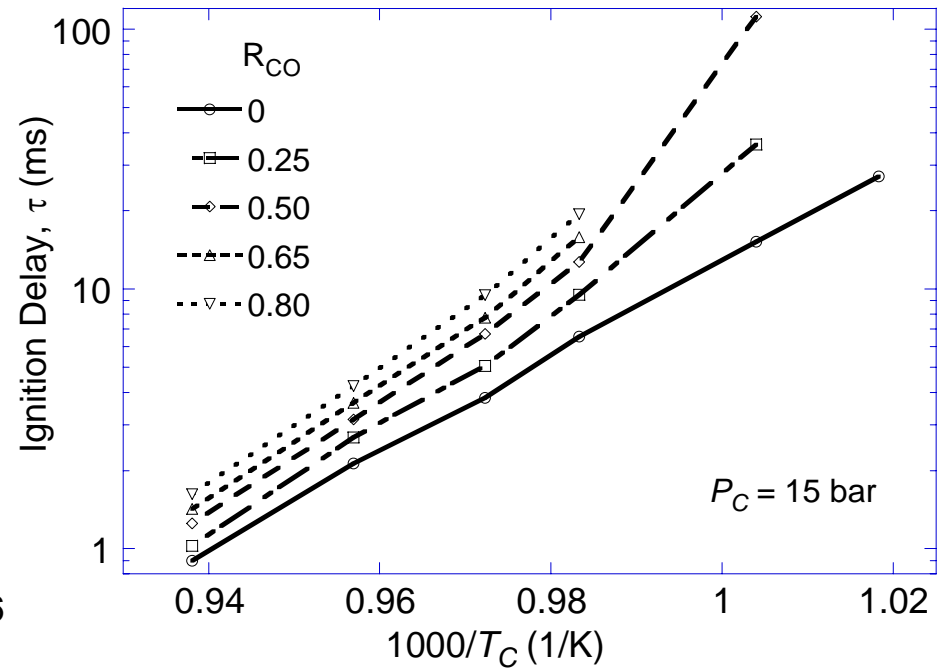
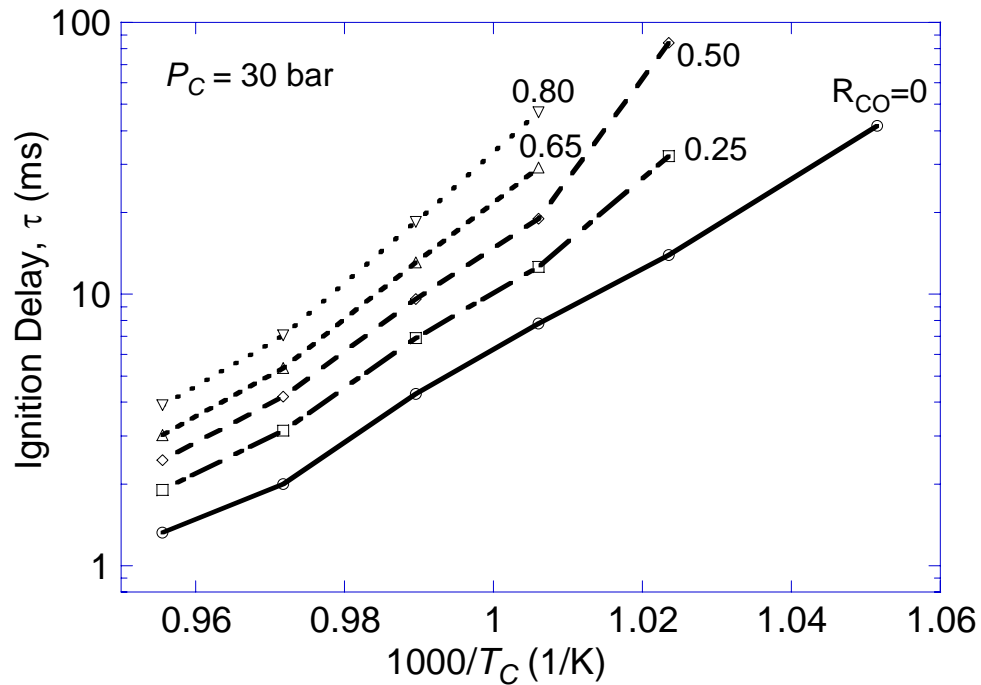
H₂/CO Ignition Delay (1)



Replacement of even small amounts of H₂ with CO leads to an inhibition of autoignition.



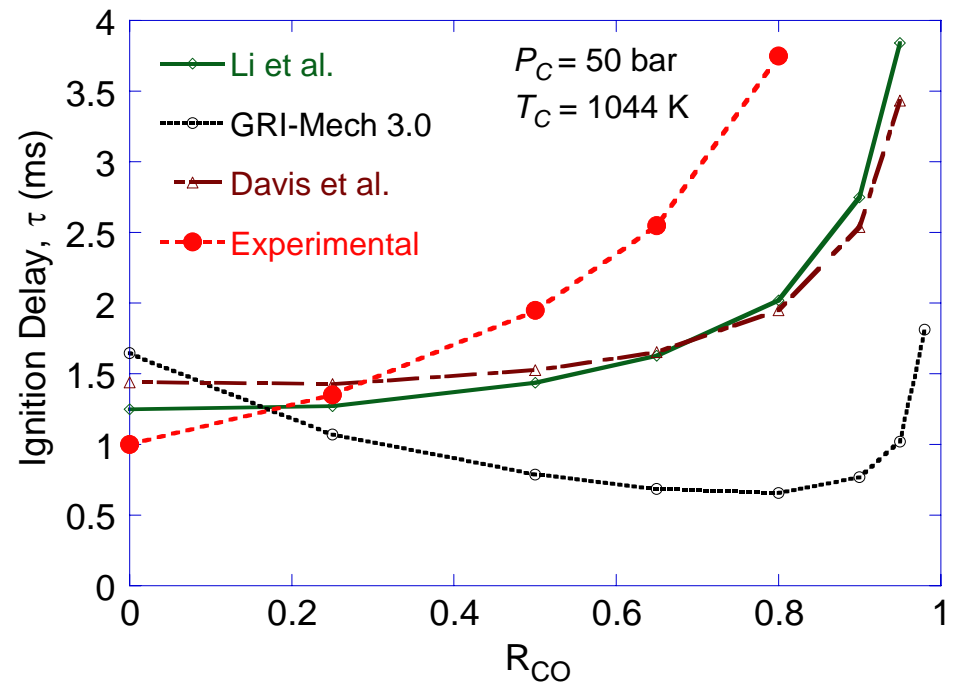
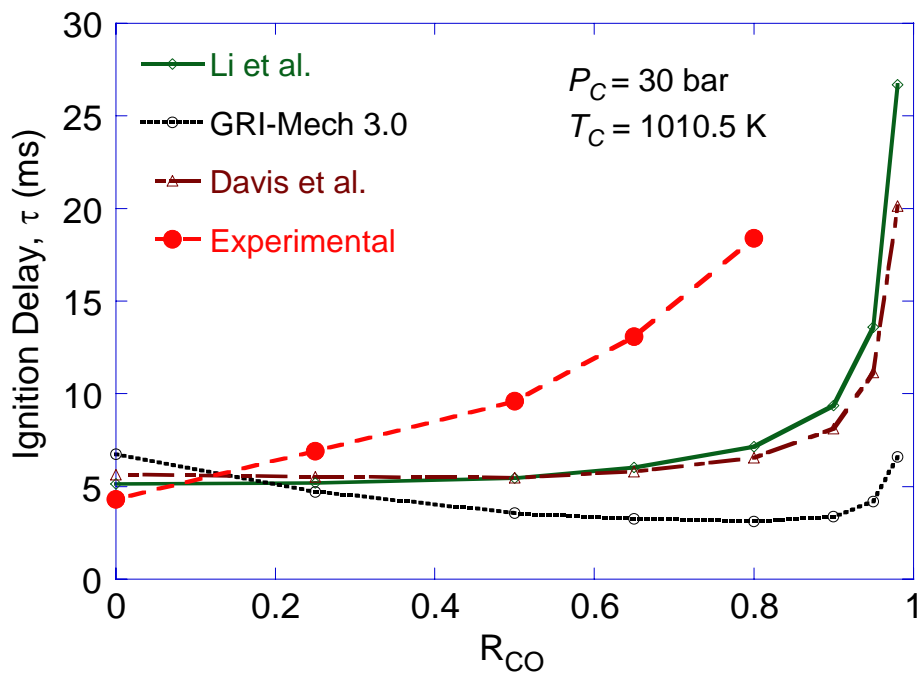
H₂/CO Ignition Delay (2)



The inhibition effect of CO addition is seen to be much more pronounced at higher pressures.

H₂/CO Ignition Delay (3)

- Existing mechanisms fail to describe the inhibition effect of CO addition.
- From mechanisms, inhibition effect of CO is not observed until it constitutes 80% of the total fuel mole fraction.



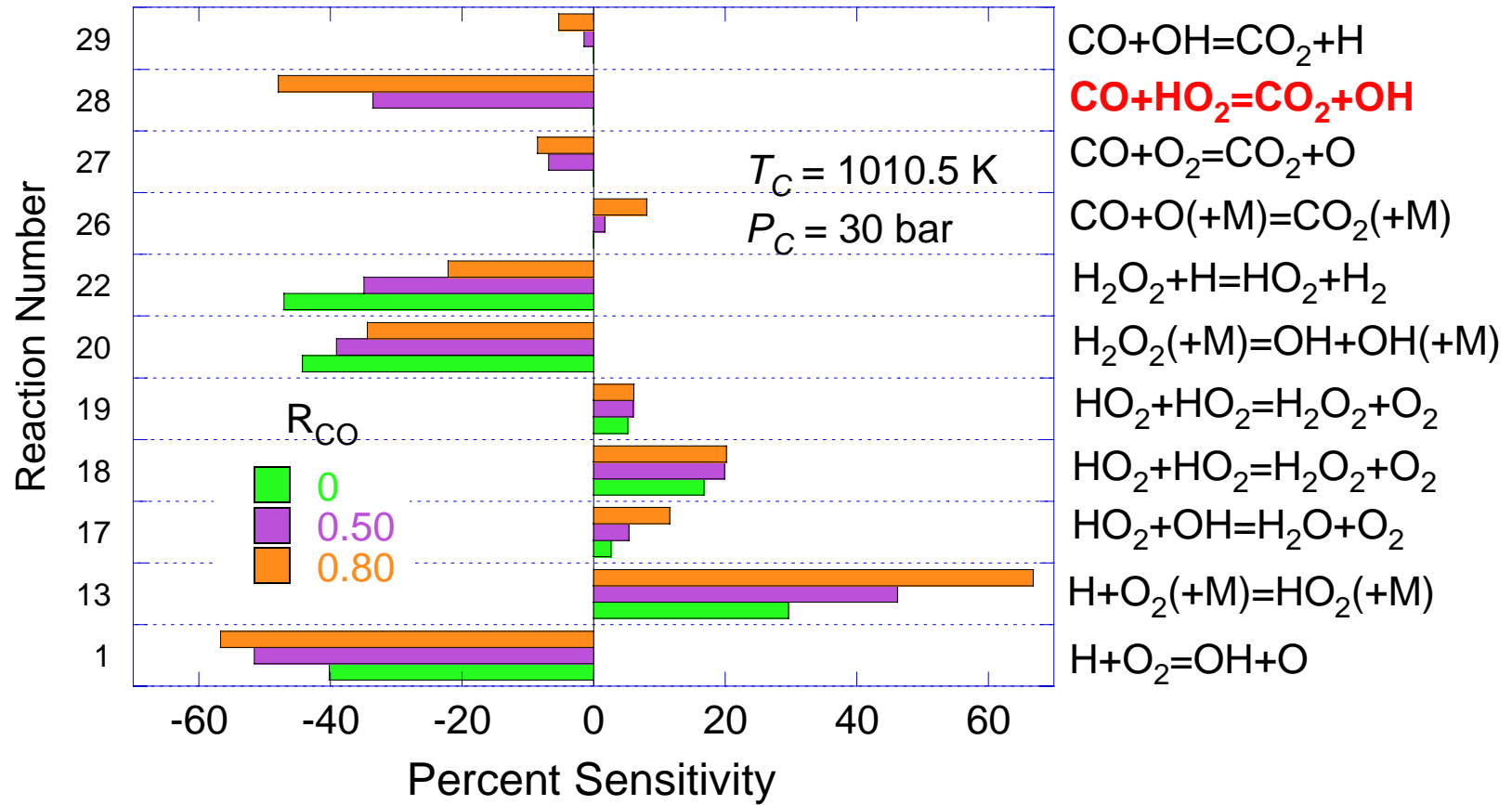
$$(H_2 + CO)/O_2/N_2/Ar = 12.5/6.25/18.125/63.125$$



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“Brute Force” Sensitivity Analysis



$\text{CO} + \text{HO}_2 = \text{CO}_2 + \text{OH}$ appears to be the primary reaction responsible for the mismatch of experimental and calculated ignition delays.





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Global Uncertainty Analysis

- “Brute force” local sensitivity analysis is a useful linear analysis, but this cannot reveal interactions between kinetic parameter values.
- Uncertainties have to be assigned to all relevant parameters and the response to variations within the assigned ranges must be tested.
- Global, non-linear, uncertainty analysis which simultaneously considers variations in all kinetic parameters is required to interpret the origins of the discrepancy (e.g. Morris-one-at-a-time and Monte-Carlo methods).

in collaboration with Prof. J. F. Griffiths, University of Leeds



Morris Analysis (1)

- The overall importance ranking of reactions is determined by the absolute mean perturbation of the predicted ignition delay across all simulations when rate parameters are varied in a prescribed way within their ranges of uncertainty.
- The standard deviation reflects non-linear effects, i.e. the extent to which the sensitivity of the ignition delay may change if other parameters are adjusted.

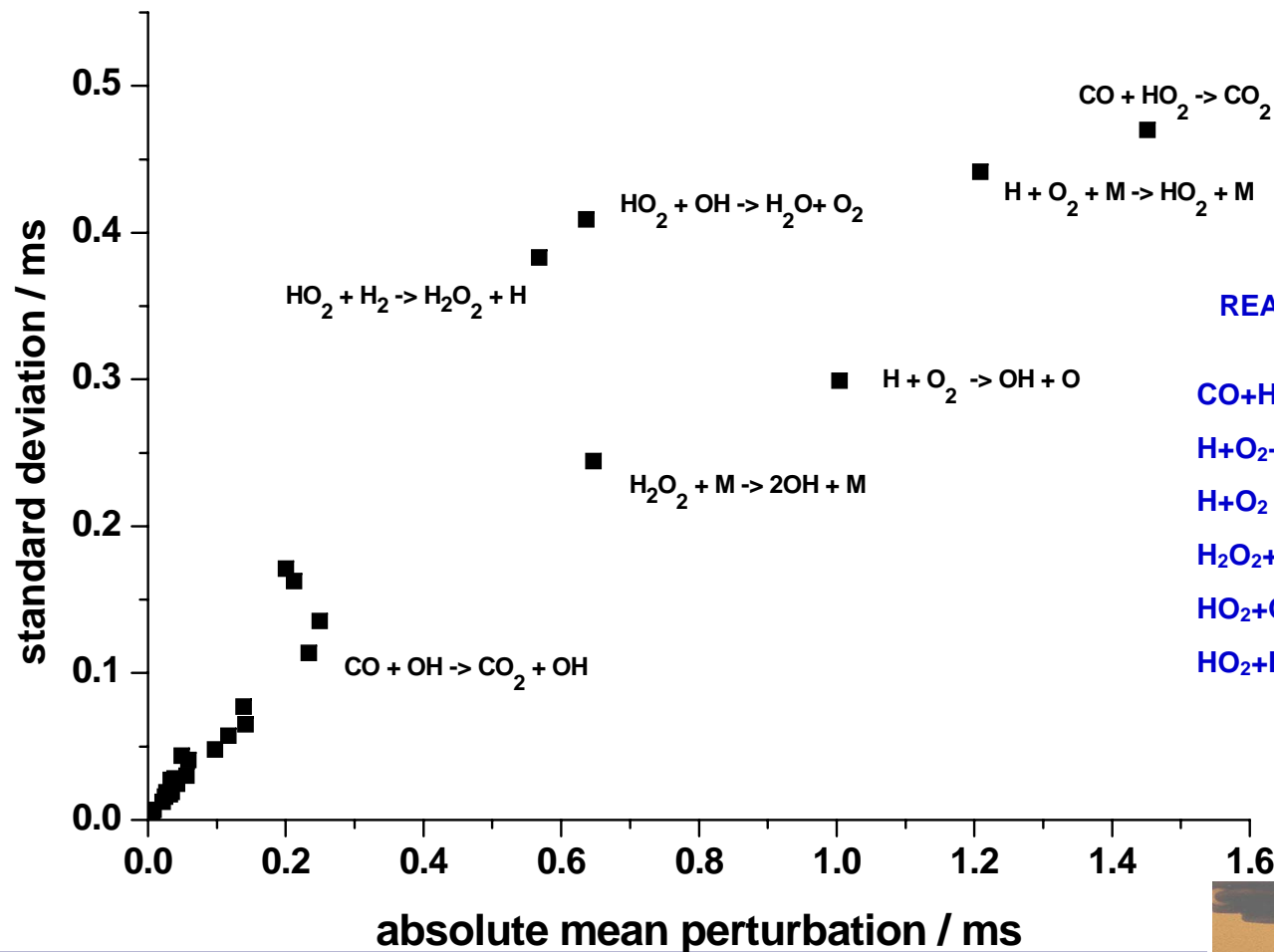


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Morris Analysis (2)

0.8CO + 0.20H₂ at 50 bar and 1040 K using 76 irreversible reaction scheme (Davis *et al.*, 2005)



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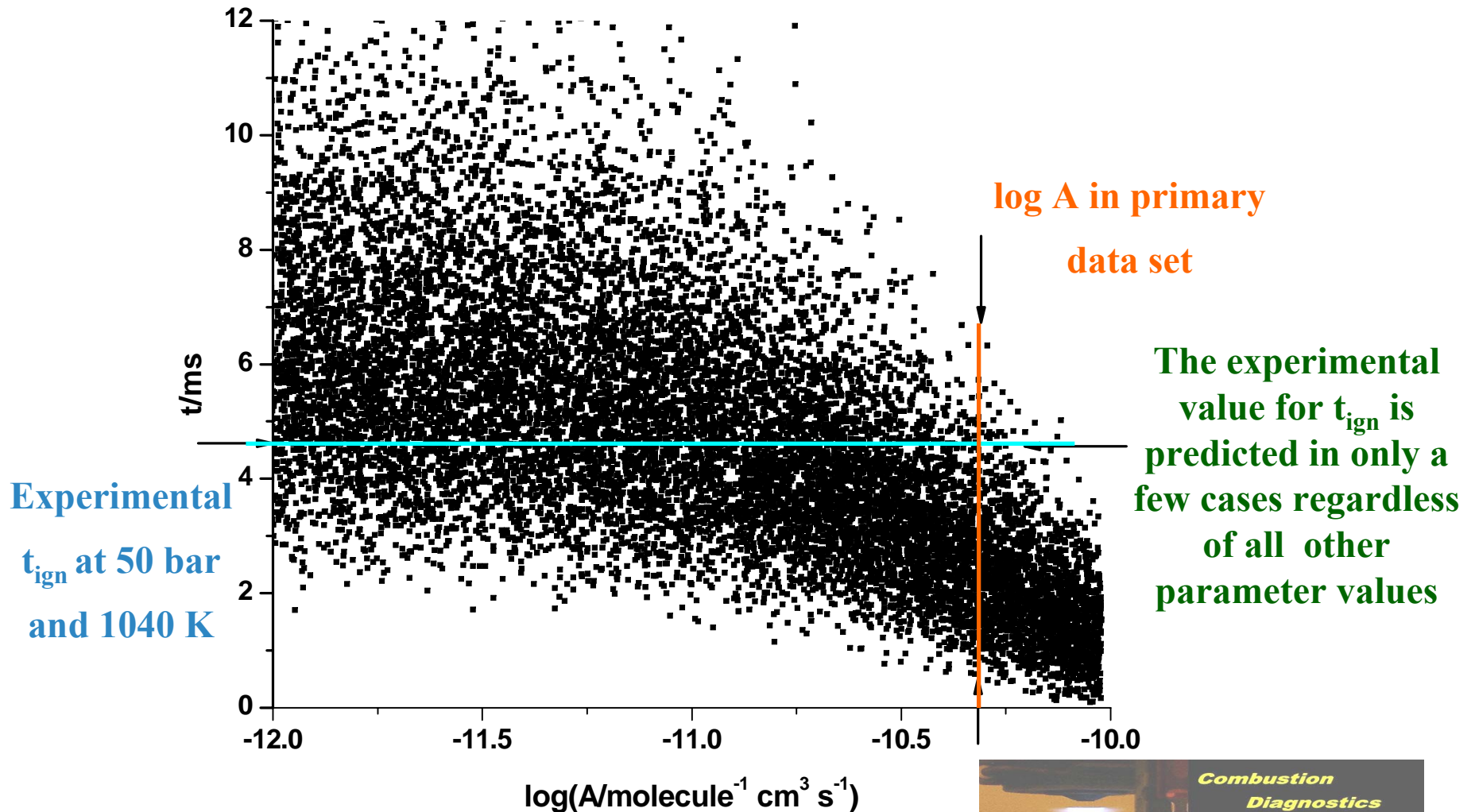


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Monte Carlo Analysis (1)

Significance of k of $\text{CO} + \text{HO}_2$ in predicting ignition delay



This is why we think k for $\text{CO} + \text{HO}_2$ is wrong.



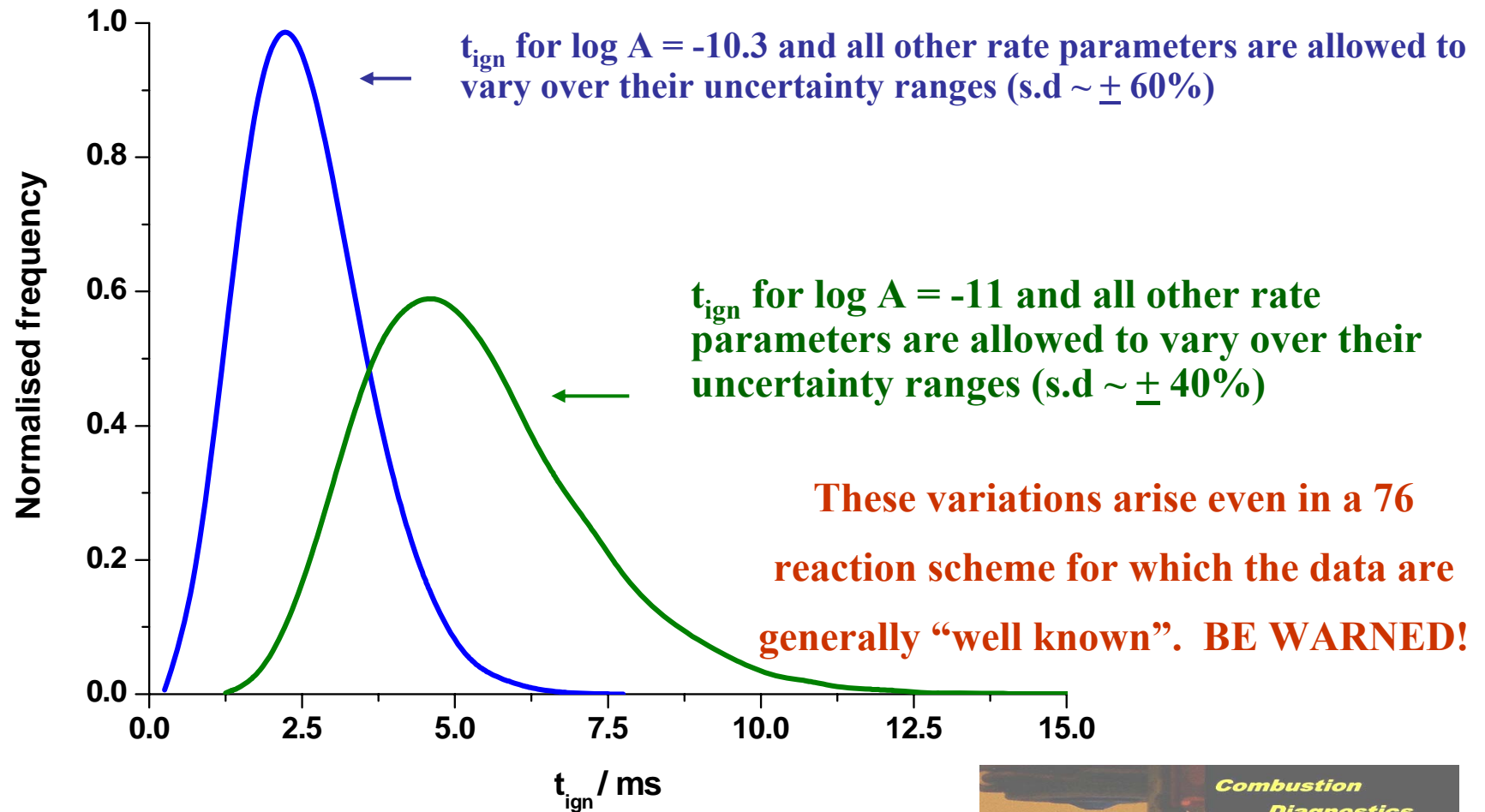


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Monte Carlo Analysis (2)

Relationship of various values of k of $\text{CO}+\text{HO}_2$ with predicted ignition delays



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Conclusions from Global Uncertainty Analysis

- The currently accepted parameter values for $\text{CO} + \text{HO}_2$ are obviously not right.
- $\text{Log } A < -11$ would fix it but the present analysis does not permit us to do more than indicate that the overall reaction rate is too fast.
- This constraint arises from the uncertainty in other rate parameters that gives the scatter in the predicted ignition delays – which is problem for any model validation using ignition delay data.
- Corrected parameters cannot be generated for this reaction solely from ignition delay evaluations
- Direct experimental or theoretical approaches are required to determine the rate parameters.





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Reaction Kinetics of

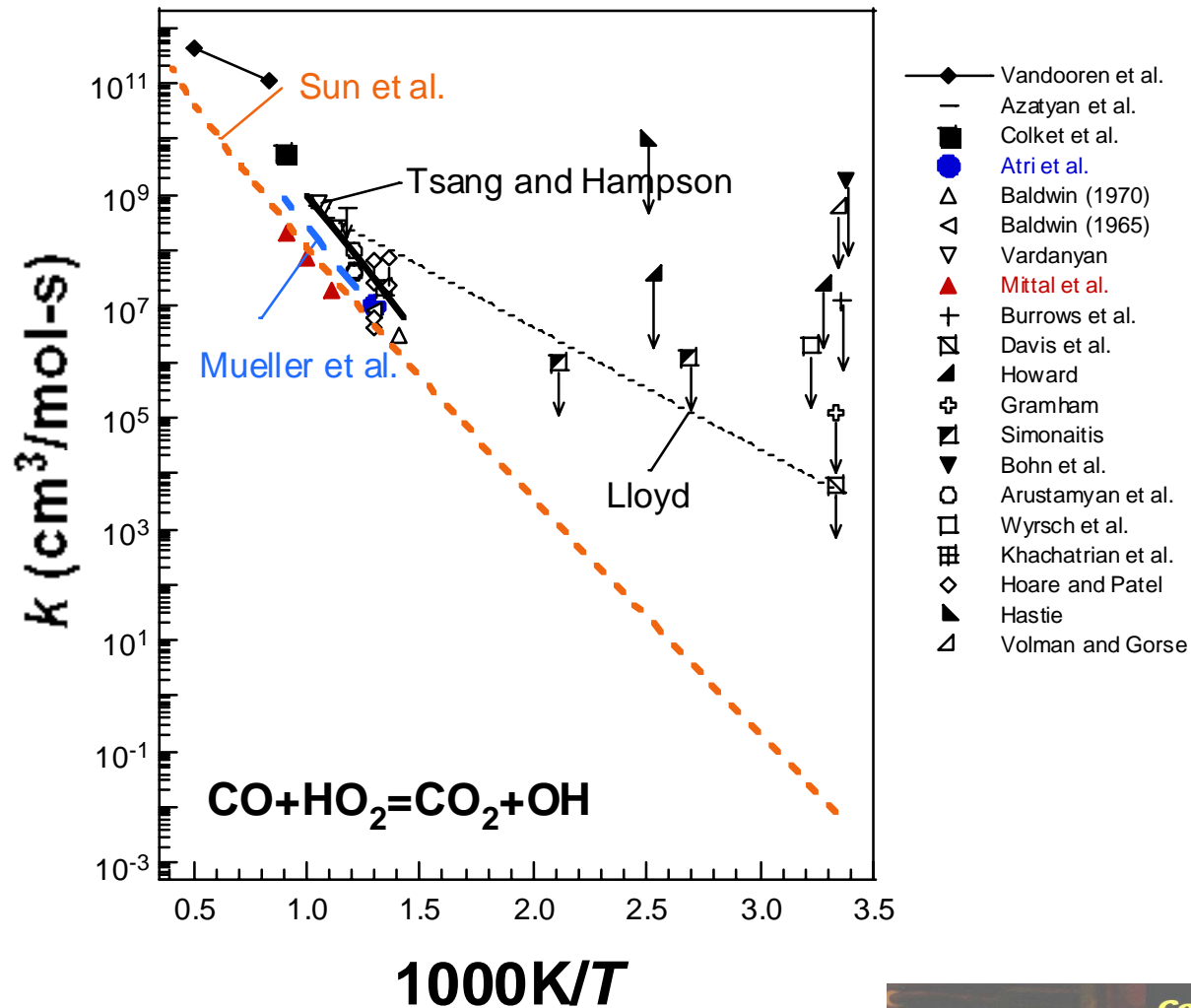


ab initio Study and Master Equation Modeling





Motivation (1)



Motivation (2)

- Prior theoretical efforts are insufficient to ensure an accurate rate coefficient.
- In all cases, the hindered internal rotations in the HOOC•O adduct and the critical geometries were inadequately treated.
- The complexity of the potential energy surface due to the *trans*- and *cis*-conformers and their mutual isomerization was not considered.
- In addition, the calculations of the potential energy barriers may not be sufficiently reliable to obtain accurate rate constant values.



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Approach

- A more detailed analysis of the potential energy surface of $\text{CO} + \text{HO}_2$ reaction using several high-level quantum chemistry methods.
- Our best estimates for the saddle point energies are then incorporated in transition state theory simulations that consider the full complexity of the hindered rotational motions.
- Furthermore, the possibility of collisional stabilization and the dissociation of the adduct back to $\text{CO} + \text{HO}_2$ along the *trans* pathway is examined via master equation simulations.



- CCSD(T)/CBS energy (Halkier, 1998)

$$E_{\text{CCSD(T)/CBS}} \approx E_{\text{CCSD(T)/cc-pVQZ}} + \frac{27}{37} \times \left[E_{\text{CCSD(T)/cc-pVQZ}} - E_{\text{CCSD(T)/cc-pVTZ}} \right]$$

Basis set correction

- FCC/CBS energy (He, 2000)

$$E_{\text{FCC/CBS}} \approx E_{\text{CCSD(T)/CBS}} + \frac{1}{5} \times \left[E_{\text{CCSD(T)/cc-pVTZ}} - E_{\text{CCSD/cc-pVTZ}} \right]$$

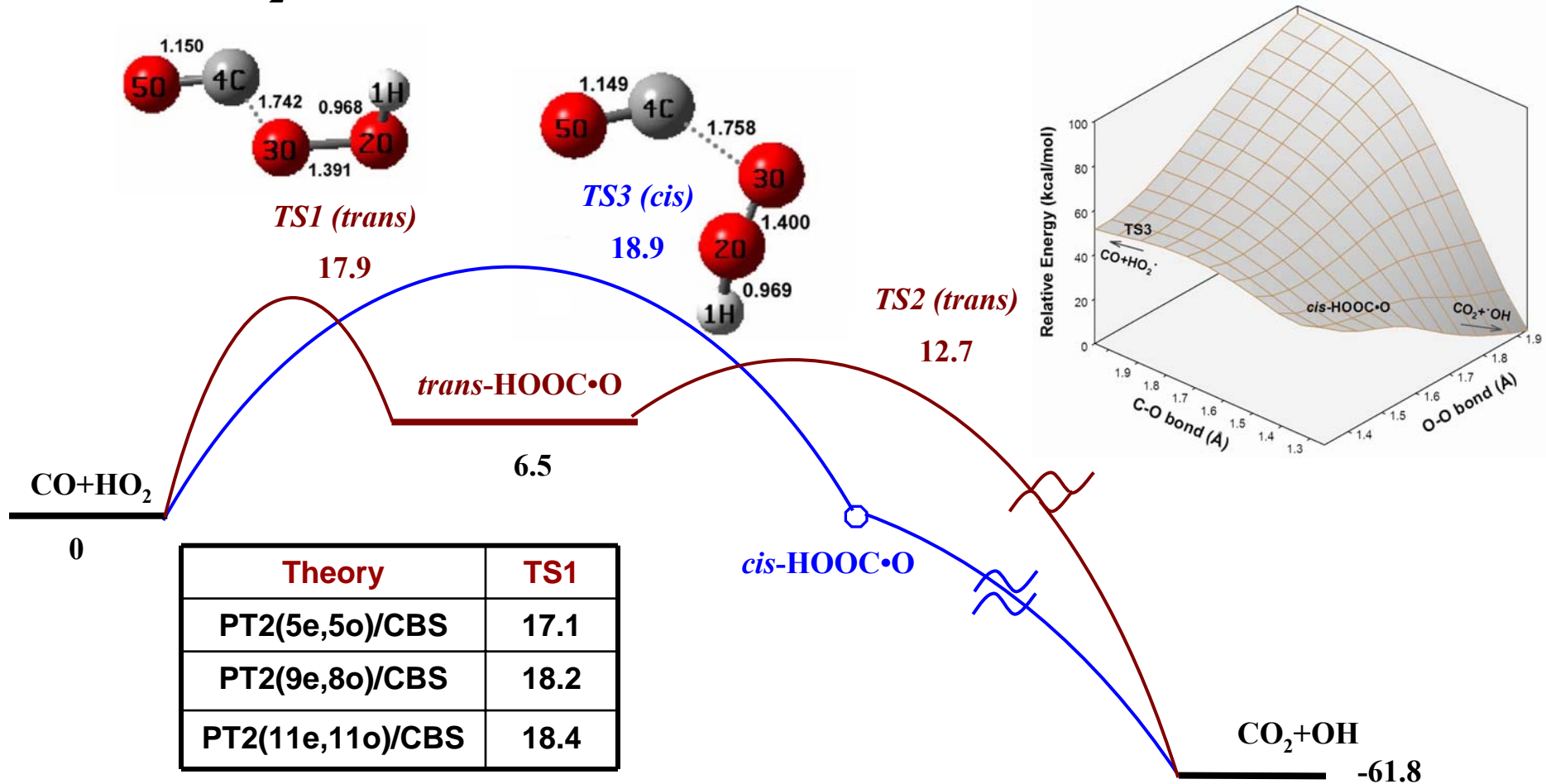
Configuration Interaction truncation error

- Energies (kcal/mol) at 0 K relative to CO + HO₂•

Products/ transition state	G3B3	CCSD(T)/ cc-pVTZ	CCSD(T)/ cc-pVQZ ^a	CCSD(T)/ CBS	FCC/CBS	Literature value
CO ₂ +OH	-63.3	-59.9	-61.0	-61.8	-61.7	-61.6±0.1
HOOC•O	6.3	8.1	7.2	6.5	6.0	
TS1	18.3	18.8	18.3	17.9	17.3	
TS2	12.0	14.4	13.4	12.7	11.8	
TS3	19.3	19.9	19.3	18.9	18.2	
TS4	15.5	17.2	16.4	15.8	15.3	
HC•O+O ₂	33.3	33.1	33.7	34.1	34.0	33.6±0.1

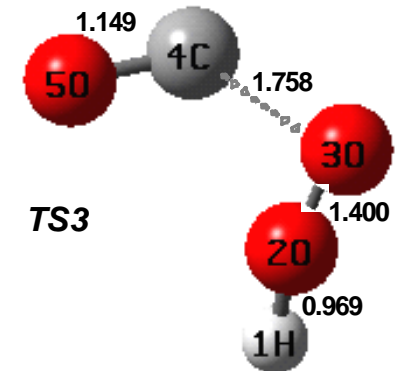
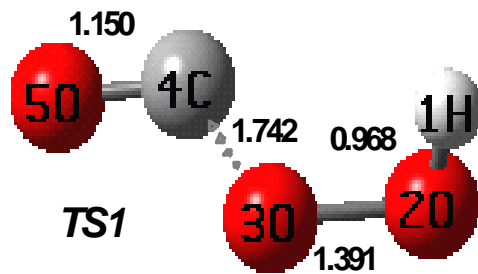
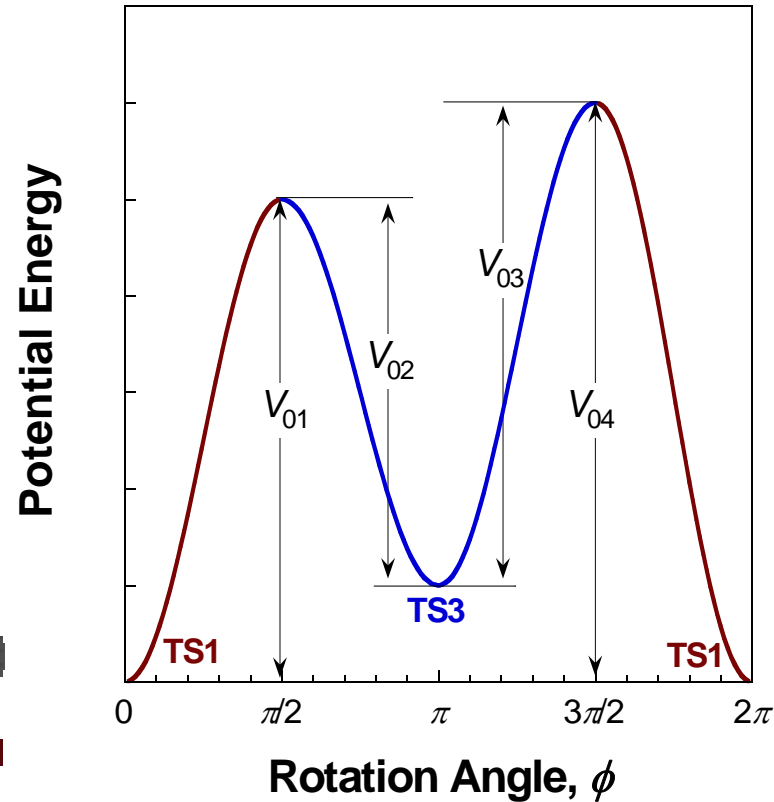
Potential Energy Surface

- CO+HO₂→products (CCSD(T)/CBS//CCSD(T)/cc-pVTZ, kcal/mol)



Internal Rotation

- Asymmetric characteristics
- TS1 ↔ TS3



$$Q_b(T) = \frac{1}{2\pi} \left(\frac{\pi k_B T}{B} \right)^{1/2} \sum_{i=1}^4 \int_{(i-1)\pi/2}^{i\pi/2} d\phi e^{-V/k_B T}$$

Density of States

- Hindered internal rotation contributions

$$\rho_b(E) = \rho_{b1}(E) + \rho_{b2}(E) + \rho_{b3}(E) + \rho_{b4}(E)$$

$$\rho_{b1}(E) = \begin{cases} \frac{\kappa \left(\sqrt{\frac{E}{V_{01}}} \right)}{2\pi\sqrt{BV_{01}}} & \text{for } 0 < E < V_{01} \\ \frac{\kappa \left(\sqrt{\frac{V_{01}}{E}} \right)}{2\pi\sqrt{BE}} & \text{for } E > V_{01} \end{cases}$$

$$\rho_{b2}(E) = \begin{cases} \frac{\kappa \left(\sqrt{\frac{E - (V_{01} - V_{02})}{V_{02}}} \right)}{2\pi\sqrt{BV_{02}}} & \text{for } 0 < E - (V_{01} - V_{02}) < V_{02} \\ \frac{\kappa \left(\sqrt{\frac{V_{02}}{E - (V_{01} - V_{02})}} \right)}{2\pi\sqrt{B[E - (V_{01} - V_{02})]}} & \text{for } E - (V_{01} - V_{02}) > V_{02} \end{cases}$$

$$\rho_{b3}(E) = \begin{cases} \frac{\kappa \left(\sqrt{\frac{E - (V_{01} - V_{02})}{V_{03}}} \right)}{2\pi\sqrt{BV_{03}}} & \text{for } 0 < E - (V_{01} - V_{02}) < V_{03} \\ \frac{\kappa \left(\sqrt{\frac{V_{03}}{E - (V_{01} - V_{02})}} \right)}{2\pi\sqrt{B[E - (V_{01} - V_{02})]}} & \text{for } E - (V_{01} - V_{02}) > V_{03} \end{cases}$$

$$\rho_{b4}(E) = \begin{cases} \frac{\kappa \left(\sqrt{\frac{E}{V_{04}}} \right)}{2\pi\sqrt{BV_{04}}} & \text{for } 0 < E < V_{04} \\ \frac{\kappa \left(\sqrt{\frac{V_{04}}{E}} \right)}{2\pi\sqrt{BE}} & \text{for } E > V_{04} \end{cases}$$

- Total density of states

$$\rho(E) = \int_0^E \rho_b(E) \rho_{\text{rot}}(E - \epsilon) d\epsilon$$



- At lower level approximation

$$I^{(2,n)} = \frac{I_L^{(1,n)} I_R^{(1,n)}}{I_L^{(1,n)} + I_R^{(1,n)}}$$

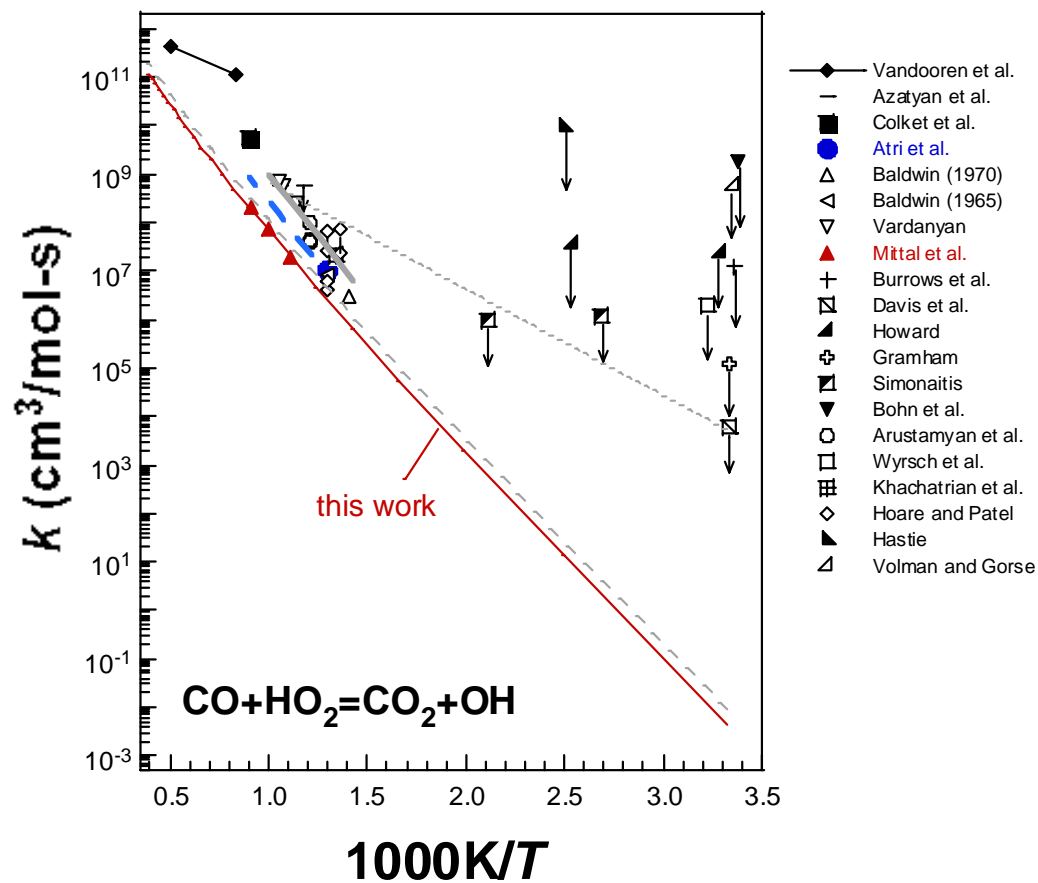
- At higher level approximation (East and Radom, 1997)

$$I^{(3,4)} = I^{(1,1)} - \sum_{i=1}^3 \left[\frac{(\alpha_{ij} U)^2}{m_L + m_R} + \frac{\beta_i^2}{I_i} \right]$$

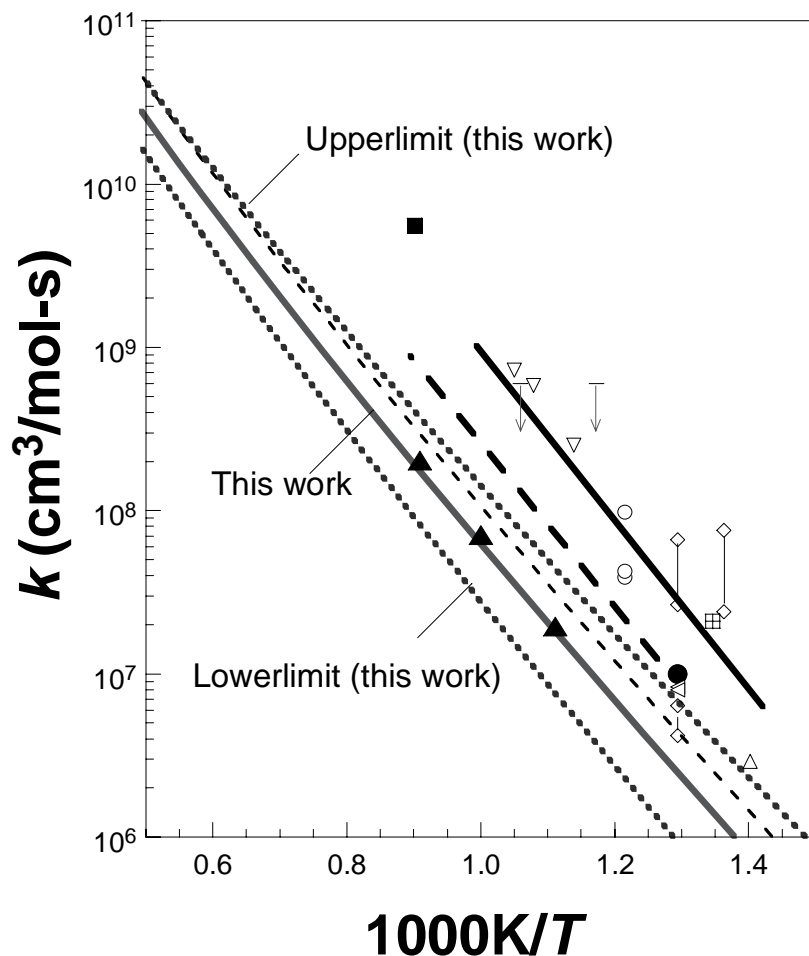


- Effects of internal rotor and I treatment on k ($\text{cm}^3/\text{mol}\cdot\text{s}$)

$T(\text{K})$	Harmonic oscillator	Free rotor with $I^{(3,4)}$	Hindered rotor		
			$I^{(2,1)}$	$I^{(2,3)}$	$I^{(3,4)}$
500	2.1×10^3	3.8×10^4	2.9×10^3	1.5×10^3	1.7×10^3
1000	5.6×10^7	6.1×10^8	1.1×10^8	6.3×10^7	6.5×10^7
1500	2.6×10^9	2.1×10^{10}	5.5×10^9	3.4×10^9	3.2×10^9
2000	2.2×10^{10}	1.4×10^{11}	4.7×10^{10}	2.9×10^{10}	2.7×10^{10}
2500	8.8×10^{10}	4.6×10^{11}	1.9×10^{11}	1.2×10^{11}	1.1×10^{11}



- No pressure dependence up to 500 atm.
- Supports the notion advanced in RCM studies that the literature rate values are too large.



Sources of Uncertainty:

- TS1, TS3 barrier: ± 1 kcal/mol
- Internal rotation barrier: ± 1 kcal/mol
- State counting: 50%

Rate constant Uncertainty:

- 300 K, a factor of 8;
- 1000 K, a factor of 2;
- 2000 K, a factor of 1.7.

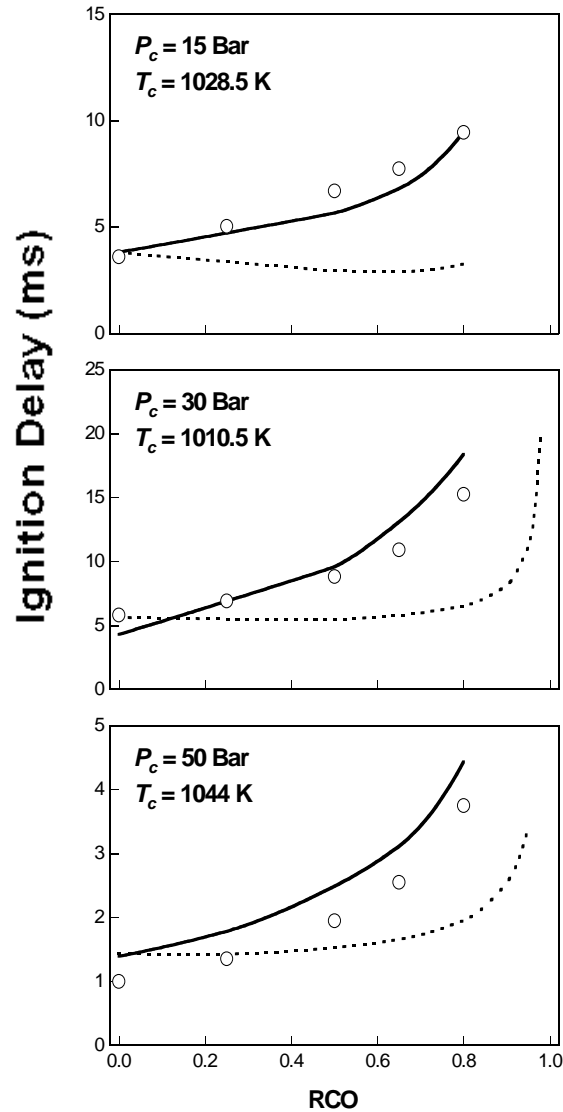
- The error bars reject almost all of the rate values reported in earlier studies.



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Modeling vs. RCM Experiments



Molar composition: $(H_2+CO)/O_2/N_2/Ar$
 $=12.5/6.25/18.125/63.125$.

- Dashed lines: Model of Davis *et al.* (2005)

- Solid lines: updated model.

1. $CO+HO_2=CO_2+OH$ (this work)
2. $CO+OH=CO_2+H$ (Joshi and Wang)
3. $HO_2+OH=H_2O+O_2$ (Sivaramakrishnan *et al.*)



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Summary

- The current theoretical analysis supports lower rate value for $\text{CO} + \text{HO}_2 = \text{CO}_2 + \text{OH}$.
- Recommended rate expression:

$$k(\text{cm}^3/\text{mol}\cdot\text{s}) = 1.57 \times 10^5 T^{2.18} e^{-9030/T}$$

$$(300 \leq T \leq 2500 \text{ K}, P \leq 500 \text{ atm})$$





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*Laminar Flame Speeds of
Wet H₂/CO Mixtures with Preheat*

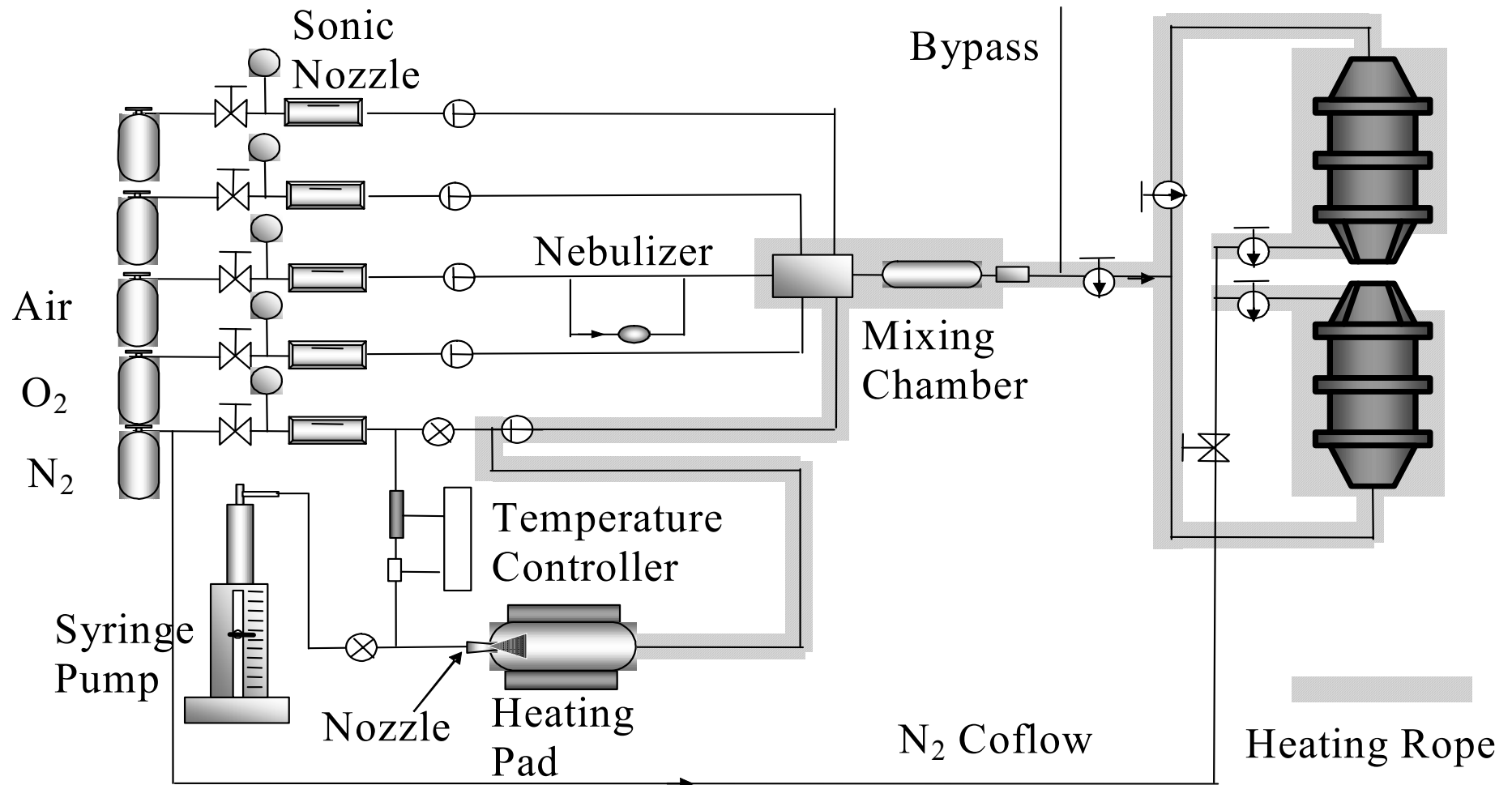




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Counterflow Twin-Flame Configuration

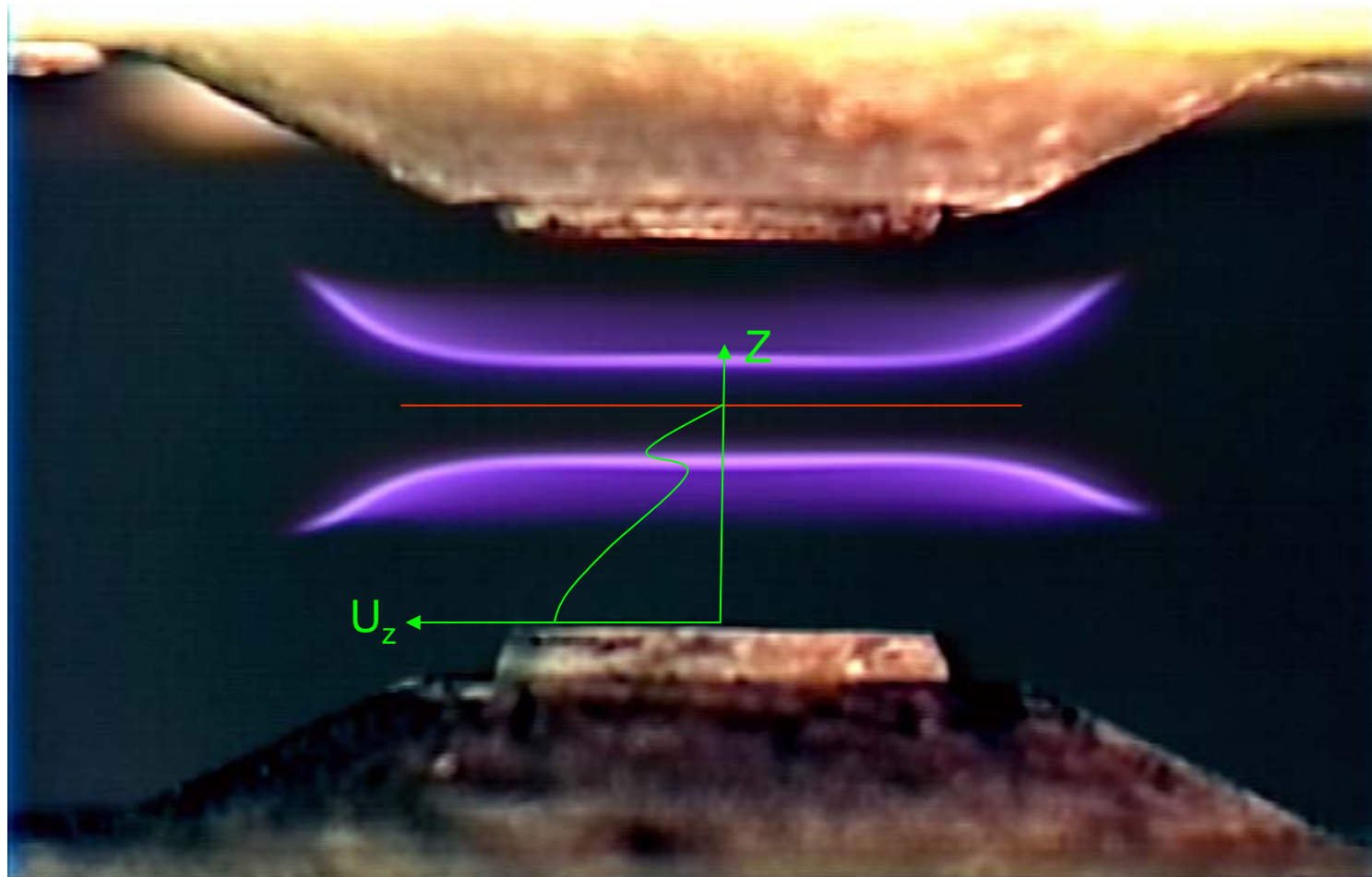




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Counterflow Twin Flames

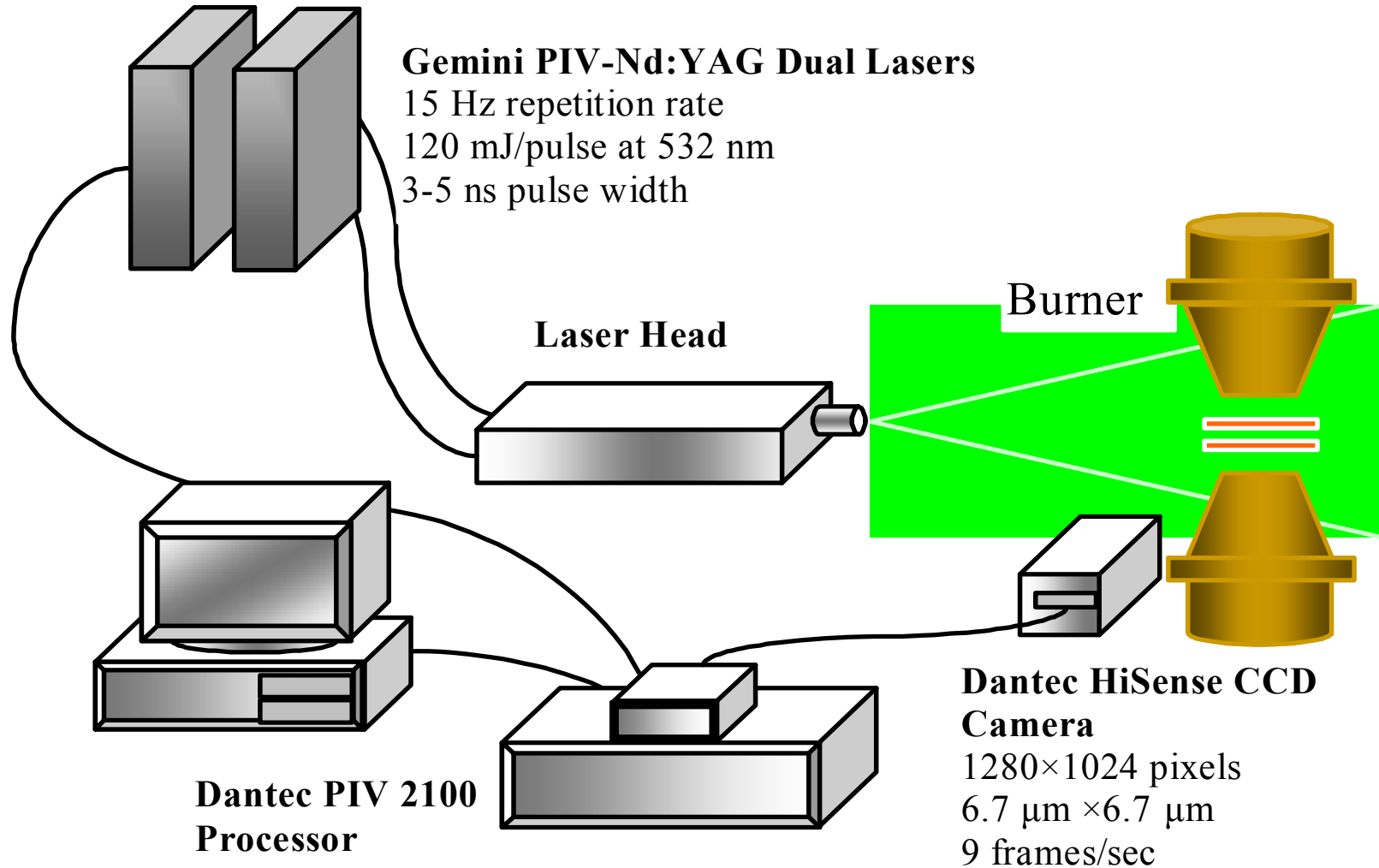




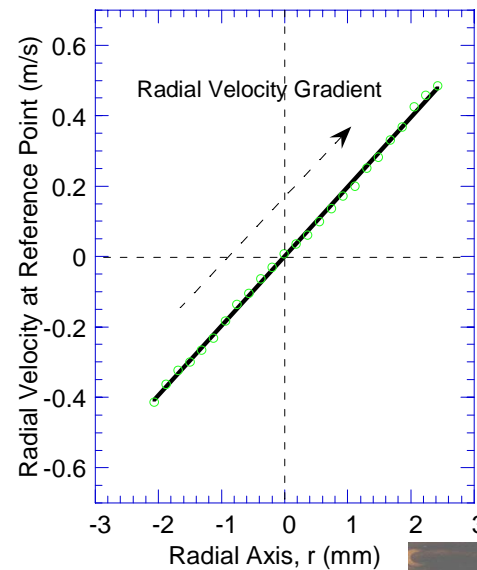
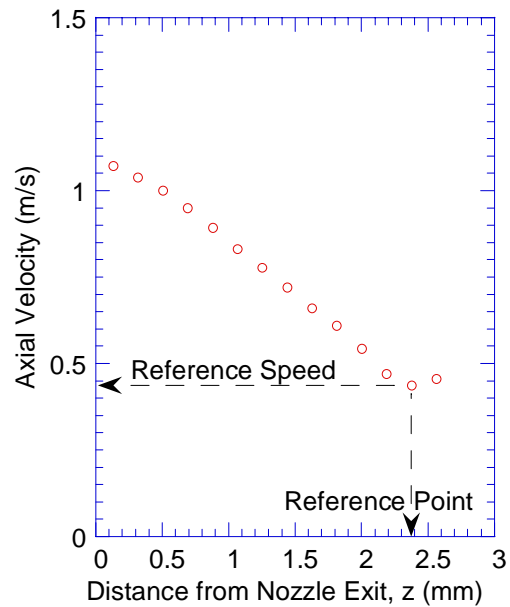
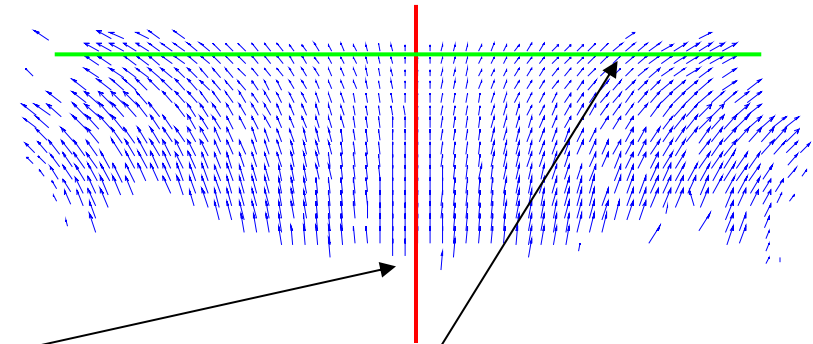
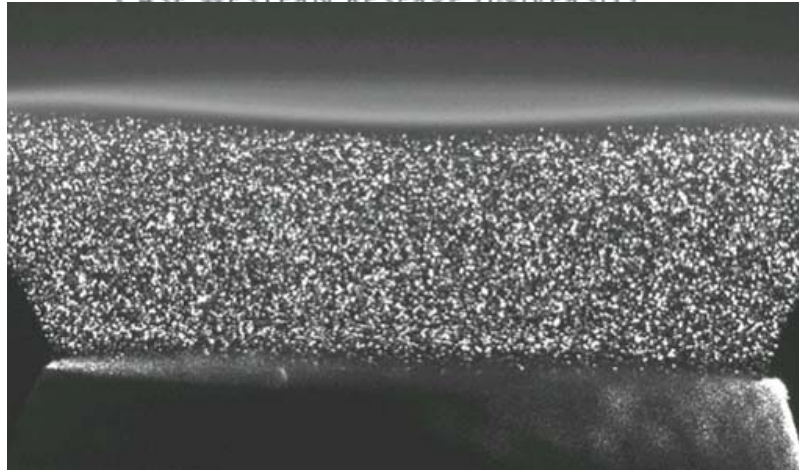
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DPIV System for Velocity Measurement



DPIV Measurement



→ stretch rate, K

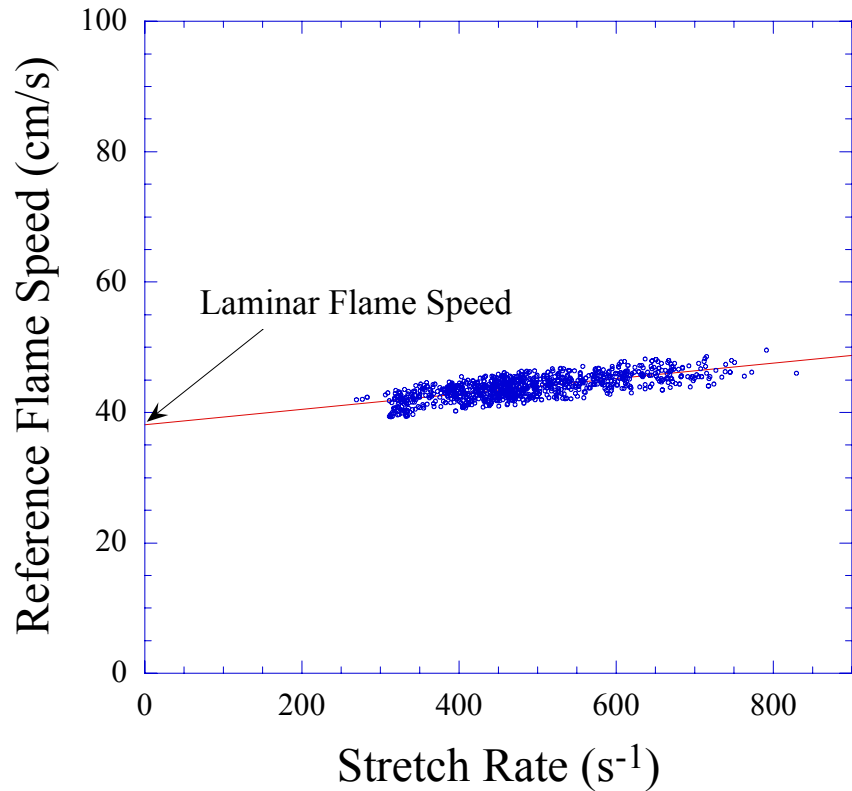


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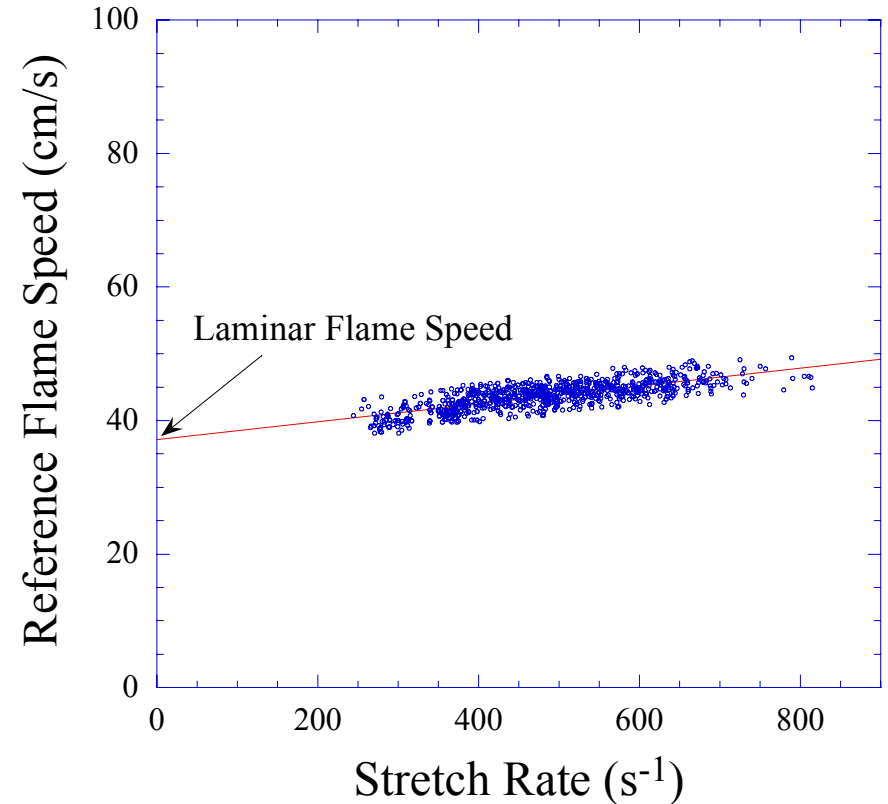
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Linear Extrapolation

$\phi=0.7, R_{CO}=0.95, \xi_{H_2O}=15\%, T_u=323\text{ K}$



$\phi=0.7, R_{CO}=0.95, \xi_{H_2O}=25\%, T_u=323\text{ K}$



$$\xi_{H_2O} = [H_2O] / ([H_2] + [CO] + [H_2O])$$





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Effect of Water Addition on Flame Propagation

Fixed Volumetric Flow Rate

$\phi=0.7$, $R_{CO}=0.75$, $T_u=323$ K

$\xi_{H_2O}=0\%$



$\xi_{H_2O}=25\%$



laminar flame speed decreases with increasing ξ_{H_2O}

Fixed Volumetric Flow Rate

$\phi=1.3$, $R_{CO}=0.95$, $T_u=323$ K

$\xi_{H_2O}=0\%$



$\xi_{H_2O}=25\%$



laminar flame speed increases with increasing ξ_{H_2O}



Combustion
Diagnostics
Laboratory

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Conclusions

- Need comprehensive detailed and reduced mechanisms for syngas and hydrogen combustion.
- Discrepancies between simulations and the newly obtained experimental data are discussed.
- Comparison of experimental and computational results will enable the re-evaluation and optimization of current mechanisms.
- The lack of accurate/meaningful experimental data has in the past hampered the progress in the development of kinetic mechanism.
 - Need extensive benchmark data of high fidelity.



- Obtain detailed experimental data for combustion characteristics of SGH mixtures using rapid compression machine and counterflow burner.
 - Effects of CO₂ and H₂O addition on the autoignition of H₂/CO mixtures.
 - Measurements of laminar flame speeds and strain-induced extinction limits of premixed SGH flames.
- Assess kinetic mechanism against the newly acquired experimental data, thereby enabling re-evaluation and optimization of rate constants and mechanism.
- Conduct *ab initio* quantum chemistry calculation and master equation modeling for certain key reactions, including HO₂+HO₂→H₂O₂+O₂ and HO₂+OH→H₂O+O₂.
 - Notable influence on SGH oxidation rates under high-pressure, low-to-intermediate temperature conditions.
 - Complex temperature and pressure dependences that cannot be easily resolved through mechanism optimization.



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