

High-Temperature Vaporization Behavior of Oxides II. Oxides of Be, Mg, Ca, Sr, Ba, B, Al, Ga, In, Tl, Si, Ge, Sn, Pb, Zn, Cd, and Hg

R. H. Lamoreaux and D. L. Hildenbrand

SRI International, Menlo Park, California 94025

and
L. Brewer

Department of Chemistry, University of California, Berkeley, California 94720

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In order to assess the high-temperature vaporization behavior and equilibrium gas phase compositions over the condensed oxides of Be, Mg, Ca, Sr, Ba, B, Al, Ga, In, Tl, Si, Ge, Sn, Pb, Zn, Cd, and Hg, the relevant thermodynamic and molecular constant data have been compiled and critically evaluated. Selected values of the Gibbs energy functions of condensed and vapor phases are given in the form of equations valid over wide temperature ranges, along with the standard entropies and enthalpies of formation. These data were used to generate plots of equilibrium partial pressures of vapor species as functions of temperature for representative environmental conditions ranging from reducing to oxidizing. The calculated partial pressures and compositions agree, for the most part, with experimental results obtained under comparable conditions. Maximum vaporization rates have been calculated using the Hertz-Knudsen equation. Literature references are given.

Key words: critically reviewed data; enthalpy increment; enthalpy of formation; entropy; Gibbs energy function; high temperature; oxide; partial pressure; thermodynamic data; vaporization; vaporization rate.

Contents

1. Introduction	420	n. Pb-O System	437
1.1. Background	420	o. Zn-O System	438
2. Properties of Individual Systems	421	p. Cd-O System	439
2.1. Data Evaluation, Units, and Symbols	421	q. Hg-O System	439
2.2. Thermodynamic Data and Vaporization Equilibria	421	3. High-Temperature Equilibria and Reaction Rates	441
a. Be-O System	426	3.1 Mathematics of Vaporization Calculations	441
b. Mg-O System	426	3.2 Vaporization Rate Calculations	442
c. Ca-O System	428	4. Acknowledgments	442
d. Sr-O System	428	5. References	442
e. Ba-O System	430		
f. B-O System	431		
g. Al-O System	431		
h. Ga-O System	432		
i. In-O System	432		
j. Tl-O System	432		
k. Si-O System	435		
l. Ge-O System	435		
m. Sn-O System	436		

List of Tables

1. Melting temperatures and enthalpies of fusion of oxide phases	421
2. Gibbs energy function equation parameters	422
3. Values of $\Delta_f H_{298}^\circ/R$, S_{298}°/R , and $(H_T^\circ - H_{298}^\circ)/R$	424
4. Sources of data in Tables 1-3	425

List of Figures

1. BeO vaporization in 10^{-15} bar O_2	427
2. BeO congruent vaporization	427
3. BeO vaporization in 0.2 bar O_2	427
4. BeO maximum vaporization rates	427
5. MgO vaporization in 10^{-15} bar O_2	427

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6. MgO congruent vaporization	427	and vaporization of Tl-Tl ₂ O mixture above 731 K	434
7. MgO vaporization in 0.2 bar O ₂	428	38. Tl ₂ O congruent vaporization	434
8. MgO maximum vaporization rates	428	39. Tl ₂ O ₃ vaporization below 1060 K and TlO vaporization above 1060 K in 0.2 bar O ₂	434
9. CaO vaporization in 10 ⁻¹⁵ bar O ₂	428	40. Maximum vaporization rates of thallium oxides	434
10. CaO congruent vaporization	428	41. SiO ₂ vaporization in 10 ⁻¹⁵ bar O ₂	435
11. CaO vaporization in 0.2 bar O ₂	429	42. SiO ₂ congruent vaporization	435
12. CaO maximum vaporization rates	429	43. SiO ₂ vaporization in 0.2 bar O ₂	435
13. SrO vaporization in 10 ⁻¹⁵ bar O ₂	429	44. SiO ₂ maximum vaporization rates	435
14. SrO congruent vaporization	429	45. GeO ₂ vaporization in 10 ⁻¹⁵ bar O ₂ below 1210 K and vaporization of Ge-GeO ₂ mixture above 1210 K	436
15. SrO vaporization in 0.2 bar O ₂	429	46. GeO ₂ congruent vaporization	436
16. SrO maximum vaporization rates	429	47. GeO ₂ vaporization in 0.2 bar O ₂	436
17. BaO vaporization in 10 ⁻¹⁵ bar O ₂	430	48. GeO ₂ maximum vaporization rates	436
18. BaO congruent vaporization	430	49. SnO ₂ vaporization in 10 ⁻¹⁵ bar O ₂ below 1163 K and vaporization of Sn-SnO ₂ mixture above 1163 K	437
19. BaO vaporization in 0.2 bar O ₂	430	50. SnO ₂ congruent vaporization	437
20. BaO maximum vaporization rates	430	51. SnO ₂ vaporization in 0.2 bar O ₂	437
21. B ₂ O ₃ vaporization in 10 ⁻¹⁵ bar O ₂ below 1923 K and vaporization of B-B ₂ O ₃ mixture above 1923 K	431	52. SnO ₂ maximum vaporization rates	437
22. B ₂ O ₃ congruent vaporization	431	53. PbO vaporization in 10 ⁻¹⁵ bar O ₂ below 905 K and vaporization of Pb-PbO mixture above 905 K	438
23. B ₂ O ₃ vaporization in 0.2 bar O ₂	431	54. PbO congruent vaporization	438
24. B ₂ O ₃ maximum vaporization rates	431	55. PbO vaporization in 0.2 bar O ₂	438
25. Al ₂ O ₃ vaporization in 10 ⁻¹⁵ bar O ₂ below 2230 K and vaporization of Al-Al ₂ O ₃ mixture above 2230 K	432	56. PbO maximum vaporization rates	438
26. Al ₂ O ₃ congruent vaporization	432	57. ZnO vaporization in 10 ⁻¹⁵ bar O ₂	438
27. Al ₂ O ₃ vaporization in 0.2 bar O ₂	432	58. ZnO congruent vaporization	439
28. Al ₂ O ₃ maximum vaporization rates	432	59. ZnO vaporization in 0.2 bar O ₂	439
29. Ga ₂ O ₃ vaporization in 10 ⁻¹⁵ bar O ₂ below 1446 K and vaporization of Ga-Ga ₂ O ₃ mixture above 1446 K	433	60. ZnO maximum vaporization rates	439
30. Ga ₂ O ₃ congruent vaporization	433	61. CdO vaporization in 10 ⁻¹⁵ bar O ₂	439
31. Ga ₂ O ₃ vaporization in 0.2 bar O ₂	433	62. CdO congruent vaporization	440
32. Ga ₂ O ₃ maximum vaporization rates	433	63. CdO vaporization in 0.2 bar O ₂	440
33. In ₂ O ₃ vaporization in 10 ⁻¹⁵ bar O ₂ below 1239 K and vaporization of In-In ₂ O ₃ mixture above 1239 K	433	64. CdO maximum vaporization rates	440
34. In ₂ O ₃ congruent vaporization	433	65. HgO vaporization in 10 ⁻¹⁵ bar O ₂	440
35. In ₂ O ₃ vaporization in 0.2 bar O ₂	434	66. HgO congruent vaporization	440
36. In ₂ O ₃ maximum vaporization rates	434	67. HgO vaporization in 0.2 bar O ₂	440
37. Tl ₂ O vaporization in 10 ⁻¹⁵ bar O ₂ below 731 K		68. HgO maximum vaporization rates	441

1. Introduction

1.1. Background

Oxide materials are used or encountered in a wide variety of high-temperature applications where vaporization rates and thermodynamic stabilities are often limiting factors. The efficient design and operation of high-temperature devices and processes requires reliable information about the stability and volatility of these oxides so that vaporization losses and component lifetimes can be predicted.

Despite continuing research efforts and the use of increasingly sophisticated techniques, there are still many gaps in our knowledge and understanding of the detailed vaporization thermodynamics of metal oxide systems. This puts a premium on critical review of the literature and selection of the necessary thermodynamic data. However, even in

cases where most of the requisite data are compiled, the user must resort to a significant amount of additional calculations, sometimes unfamiliar, in order to evaluate vapor composition and vaporization behavior for specific environmental conditions. Thus we perceive a definite need for critically evaluated data, presented in a format that gives users ready access to the detailed vaporization chemistry and equilibrium partial pressures of the various species. To this end, we present graphs of species partial pressures as functions of temperature under representative reducing, neutral, and oxidizing environments. We also give equations for calculating partial pressures and maximum vaporization rates for arbitrary conditions of temperature and oxygen potential.

The present work is the second publication in a program sponsored by the Office of Standard Reference Data of the National Bureau of Standards to provide critically re-

viewed thermodynamic data of oxides, along with overviews of their high-temperature vaporization phenomena. The previous article (Lamoreaux and Hildenbrand, 1984) on alkali metal oxide systems discussed the scope of the program, the relevant literature, methods of data evaluation, and the mathematics of vaporization calculations. This article covers oxide systems of the elements Be, Mg, Ca, Sr, Ba, B, Al, Ga, In, Tl, Si, Ge, Sn, Pb, Zn, Cd, and Hg.

Readers should note that revised JANAF Thermodynamic Tables (Chase *et al.*, 1985), the final CODATA Key Values for Thermodynamics, and the CODATA Thermodynamic Tables (Garvin *et al.*, 1987) have been in preparation in the same time period as the present work and should appear concurrently. The minor differences in selected values of thermodynamic properties are immaterial to the purpose of this paper.

2. Properties of Individual Systems

2.1. Data Evaluation, Units, and Symbols

Molecular constants cited in the text are internuclear distances r in nm, vibrational wavenumbers ω in cm^{-1} , the molecular symmetry number σ , electronic state quantum weights g_i , and excited electronic state term values T_e in cm^{-1} . Thermodynamic quantities are expressed in dimensionless units, e.g., S°/R , G°/RT , or in kelvin units, e.g., $\Delta H^\circ/R$, $\Delta G^\circ/R$. The symbols K and kK, where $1 \text{ kK} = 10^3 \text{ K}$, are used to represent kelvin units. Values of R used in the present work are $1.98719 \text{ cal/mol K}$ and 8.3144 J/mol K . The standard state pressure was taken as 1 atm ($1.01325 \times 10^5 \text{ Pa}$), although the unit for computed vaporization partial pressures is the bar (10^5 Pa).

The thermodynamic symbols used in the present work are the following:

$\Delta_f H_{298}^\circ/R$	The standard molar enthalpy of formation at 298.15 K divided by the molar gas constant. Units = kelvins.
$(H_{298}^\circ - H_0^\circ)/R$	The standard molar enthalpy increment between 0 and 298.15 K divided by the molar gas constant. Units = kelvins.
$-(G_T^\circ - H_{298}^\circ)/RT$	The standard molar Gibbs energy function divided by the molar gas constant.
S_T°/R	The standard molar entropy at T K divided by the molar gas constant.
$T_{\text{us}}, \Delta_{\text{us}} H^\circ/R$	Solid-phase transition temperature and standard molar enthalpy of transition divided by the molar gas constant.
$T_{\text{fus}}, \Delta_{\text{fus}} H^\circ/R$	Melting temperature and standard molar enthalpy of fusion divided by the molar gas constant.

2.2. Thermodynamic Data and Vaporization Equilibria

Selected values of thermochemical properties of the relevant chemical species involved in the high-temperature vaporization equilibria are shown in Tables 1–3. Table 1 lists the reported melting points and enthalpies of fusion of high-temperature oxide phases. Table 2 presents Gibbs energy functions fit to the equation

$$-(G_T^\circ - H_{298}^\circ)/RT = A + BT + CT^2 + DT^3 + ET^4 \quad (1)$$

Values of $\Delta_f H_{298}^\circ/R$, S_{298}°/R , and $(H_{298}^\circ - H_0^\circ)/R$ are presented in Table 3.

After careful review and comparison of the literature, Vols. 2 and 3 of the IVTAN compilation (Glushko *et al.*, 1978, 1979a, 1981, 1983) and recent JANAF (Stull *et al.*, 1971) supplements (Chase *et al.*, 1974, 1975, 1978, 1982, and dated individual issues) were chosen as the primary sources of data for the oxides of Be, Mg, Ca, Sr, Ba, B, Al, Ga, In, Tl, Si, Ge, Sn, and Pb. This choice was due to the uniform coverage of the recent literature and to the thoroughness of the reviews presented; agreement of recent JANAF issues with the IVTAN selected values is excellent. Other literature examined included reviews cited in the first paper (Brewer, 1953; Coughlin, 1954; Kelley, 1960; Schick, 1960; Ackermann and Thorn, 1961; Brewer and Rosenblatt, 1961; Kelley and King, 1961; Olette and Ancy-Moret, 1963; Wicks and Block, 1963; Brewer and Rosenblatt, 1969; Barin and Knacke, 1973; Samsonov *et al.*, 1978) and the 1982 NBS compilation (Wagman *et al.*, 1982). As described below, data from the selected sources were supplemented by our own analyses for a few of the minor gaseous species not

Table 1. Melting temperatures and enthalpies of fusion of oxide phases^a

	T_{fus} (K)	$\Delta_{\text{fus}}H/R$ (kK)
BeO	2851 ± 12	10.3 ± 0.7
MgO	3100 ± 25	9.3 ± 0.7
CaO	2900 (-50,+300)	6.3 ± 0.6
SrO	2930 ± 30	8.4 ± 0.8
BaO	2290 ± 30	7.1 ± 0.7
B ₂ O ₃	723 ± 1	2.95 ± 0.02
Al ₂ O ₃	2327 ± 4	13.40 ± 0.36
Ga ₂ O ₃	2080 ± 20	12.0 ± 2.4
In ₂ O ₃	2186 ± 10	12.6 ± 1.2
Tl ₂ O	852 ± 10	3.64 ± 0.12
Tl ₂ O ₃	1107 ± 10	6.37 ± 1.20
SiO ₂ (qu)	1726 ± 10	0.9 ± 0.1
SiO ₂ (cr)	1996 ± 5	1.15 ± 0.25
GeO ₂	1388 ± 3	2.07 ± 0.3
SnO	1250 ± 30	3.33 ± 0.6
SnO ₂	1903 ± 10	2.81 ± 0.6
PbO	1160 ± 10	3.08 ± 0.05
ZnO	2242 ± 25	
CdO	>1500	

^aSee Table 4 for references.

Table 2. Gibbs energy function equation parameters (Continued)

	$(G^{\circ}T-H^{\circ}298)/RT = A + BT + CT^2 + DT^3 + ET^4$					T range, K
	A	10^3B	10^6C	10^9D	$10^{12}E$	
Tl ₂ O(g)	39.860 34.842	-17.750 8.350	48.76 -2.4334	-44.064 0.4584	14.375 -0.03765	298-1000 1000-3000
Tl ₂ O ₃ (s)	23.752 13.305	-39.353 15.999	107.127 -2.626	-96.004	31.16	298-1000 1000-1107
Tl ₂ O ₃ (l)	-0.743	40.917	-18.715	5.250	-0.627	1107-2000
Si(s)	3.101 1.052	-7.304 3.254	19.833 -0.7263	-17.696 0.0850	5.73	298-1000 1000-1687
Si(l)	-8.152	13.849	-5.0426	0.961	-0.07316	1687-3600
Si(g)	20.984 19.039 19.959	-7.130 3.32 1.9552	19.901 -1.0484 -0.2806	-18.28 0.2128 0.01899	6.03 -0.0185	298-1000 1000-3000 3000-3600
SiO(g)	26.584 23.682	-10.123 4.7876	27.756 -1.2880	-24.936 0.2291	8.113 -0.01797	298-1000 1000-3000
SiO ₂ (qu.)	6.947 1.394	-16.833 9.002	44.87 -2.166	-38.893	12.413	298-1000 1000-1726
SiO ₂ (cr.)	7.605 1.937	-19.79 8.590	51.495 -1.935	-44.403 0.225	13.91	298-1000 1000-1996
SiO ₂ (l)	2.120	7.6492	-1.2588	0.0998		1996-3000
SiO ₂ (g)	29.295 24.696	-15.684 7.467	42.55 -1.898	-37.810 0.3194	12.21 -0.0238	298-1000 1000-3000
Si ₂ (g)	28.845 25.520	-11.627 5.589	31.790 -1.3680	-28.374 0.210	9.206 -0.01386	298-1000 1000-3000
Si ₂ O ₂ (g)	40.398 33.340	-26.536 10.626	71.564 -2.860	-65.861 0.509	22.009 -0.040	298-1000 1000-3000
Si ₃ (g)	34.400 29.042	-10.44 9.140	53.630 -2.788	-49.616 0.5832	16.862 -0.05276	298-1000 1000-3000
Ge(s)	5.484 2.896	-15.1302 1.8154	43.7517 1.6677	-48.3508 -1.5224	20.0263 0.3924	298-700 700-1210.4 1210.4-3200
Ge(l)	-5.426	15.1874	-6.5705	1.4859	-0.13343	298-1000
Ge(g)	21.363 18.485	-10.534 4.992	29.285 -1.8107	-26.974 0.3906	8.883 -0.0351	298-1000 1000-3200
GeO(g)	28.117 25.086	-10.587 5.008	29.000 -1.385	-26.066 0.251	8.48 -0.020	298-1000 1000-3000
GeO ₂ (s)	7.621 118.948	-23.827 -403.336	63.421 538.497	-57.714 -313.567	19.138 68.097	298-1000 1000-1388
GeO ₂ (l)	-7.387	21.608	-8.362	1.844	-0.167	1388-3000
GeO ₂ (g)	30.914 26.045	-16.700 7.971	45.425 -2.142	-40.53 0.3796	13.12 -0.0298	298-1000 1000-3000
Ge ₂ (g)	32.229 28.103	-15.564 7.132	43.747 -2.398	-40.584 0.4977	13.465 -0.0437	298-1000 1000-3000
Ge ₂ O ₂ (g)	40.990 33.146	-28.642 12.193	77.350 -3.875	-71.242 0.830	23.759 -0.079	298-1000 1000-2000
Ge ₃ O ₃	55.839 41.917	-48.258 22.959	130.774 -9.814	-121.600 3.022	40.908 -0.420	298-1000 1000-2000
Sn(s)	9.860	-34.0554	110.534	-151.014	79.2152	298-505.12
Sn(l)	1.684 4.201	14.256 6.483	-11.690 -2.3645	5.627 0.5071	-1.122 -0.0450	505.12-1400 1400-3000
Sn(g)	21.052 18.77	-6.998 3.667	18.881 -0.7262	-16.378 0.0646	5.221	298-1000 1000-3000
SnO(s)	10.425 4.990	-30.8313 4.5034	89.3685 1.9568	-99.1119 -2.0117	41.2146 0.5137	298-700 700-1250
SnO(l)	-3.168	19.3711	-9.1257	2.5224	-0.2917	1250-2000
SnO(g)	29.148 26.025	-10.96 5.173	30.054 -1.461	-27.070 0.2692	8.816 -0.0217	298-1000 1000-3000
SnO ₂ (s)	8.410 2.201	-21.510 9.676	57.480 -2.092	-50.560 0.236	16.203	298-1000 1000-1903
SnO ₂ (l)	-1.715	13.943	-3.931	0.6916	-0.0523	1903-3000

Table 2. Gibbs energy function equation parameters (Continued)

	$(G^{\circ}T-H^{\circ}298)/RT = A + BT + CT^2 + DT^3 + ET^4$					T range, K
	A	10^3B	10^6C	10^9D	$10^{12}E$	
SnO ₂ (g)	32.251 27.190	-17.54 8.322	47.834 -2.301	-42.85 0.4159	13.90 -0.033	298-1000 1000-3000
Sn ₂ (g)	32.827 28.634	-12.85 7.03	34.68 -1.967	-30.297 0.3357	9.65 -0.0245	298-1000 1000-3000
Sn ₂ O ₂ (g)	35.752	6.440	1.070	-1.011	0.171	298-3000
Sn ₃ O ₃ (g)	44.474	0.177	14.80	-7.926	1.264	298-3000
Sn ₄ O ₄ (g)	51.729	6.476	9.775	-5.144	0.772	298-3000
Pb(s)	9.762	-17.085	49.44	-54.63	22.66	298-600.65
Pb(l)	4.814	8.045	-3.983	1.191	-0.1493	600.65-2200
Pb(g)	21.847 19.914	-6.85 3.308	19.007 -1.080	-17.354 0.2288	5.70 -0.0197	298-1000 1000-3000
PbO(red)	11.492	-28.7693	82.3965	-89.2160	36.1111	298-762
PbO(yel)	6.081	4.9700	1.5284	-1.8198	0.4842	762-1160
PbO(l)	-1.494	19.2561	-9.2613	2.6476	-0.3178	1160-2000
PbO(g)	30.128 26.949	-11.204 5.276	30.750 -1.5062	-27.740 0.2792	9.040 -0.0225	298-1000 1000-3000
PbO ₂ (s)	10.231	-15.016	41.48	-33.24	9.446	298-1200
PbO ₂ (g)	33.462 28.252	-18.196 8.606	49.746 -2.440	-44.714 0.450	14.536 -0.0364	298-1000 1000-3000
Pb ₂ (g)	34.777 31.381	-12.426 5.687	34.43 -1.6535	-31.38 0.3116	10.30 -0.02454	298-1000 1000-3000
Pb ₂ O ₂ (g)	35.958	4.176	7.238	-4.146	0.658	298-3000
Pb ₂ O ₃ (s)	24.026	-48.4163	129.197	-117.502	39.0413	298-1000
Pb ₃ O ₃ (g)	44.777	6.271	10.844	-6.210	0.985	298-3000
Pb ₃ O ₄ (s)	26.958	-20.333	64.277	-45.386	11.00	298-1500
Pb ₄ O ₄ (g)	50.677	8.367	14.449	-8.274	1.312	298-3000
Pb ₅ O ₅ (g)	54.313	10.462	18.055	-10.338	1.639	298-3000
Pb ₆ O ₆ (g)	62.478	12.557	21.661	-12.401	1.966	298-3000
Zn(s)	5.763	-6.350	15.47	-8.73		298-692.73
Zn(l)	1.150	9.66	-4.862	1.132		692.73-1200
Zn(g)	19.791 18.184	-4.396 3.2905	12.606 -1.0522	-10.378 0.2166	3.000 -0.01932	298-1200 1200-3000
ZnO(s)	8.676 3.215	-29.783 5.346	86.988 -0.145	-98.618 -0.494	42.157 0.123	298-693 693-2000
ZnO(g)	28.337 25.163	-11.610 5.166	31.807 -1.4237	-28.827 0.2511	9.43 -0.01924	298-1000 1000-3000
Cd(s)	5.195	10.13	-40.49	74.52	-45.76	298-594.26
Cd(l)	2.511	10.22	-5.823	1.538		594.26-1100
Cd(g)	20.748 19.318	-5.4625 2.349	15.305 -0.035	-13.216 -0.263	4.055 0.064	298-1100 1100-2000
CdO(s)	6.887	-5.035	16.921	-12.132	2.97	298-1500
CdO(g)	29.305 26.054	-11.443 5.467	31.53 -1.6246	-28.494 0.3137	9.29 -0.0266	298-1000 1000-3000
Hg(l)	10.797	-14.507	41.32	-43.32	16.75	298-800
Hg(g)	21.798 19.906	-6.845 3.195	18.997 -0.9736	-17.344 -0.1891	5.697 -0.01585	298-1000 1000-3000
HgO(s)	10.251	-15.674	42.5	-37.73	12.18	298-1000
HgO(g)	27.982	2.237	1.41	-0.8606	0.1332	298-2900

^aSee Table 4 for references.

Table 3. Values of $\Delta_f H^\circ_{298/R}$, $S^\circ_{298/R}$, and $(H^\circ_{298}-H^\circ_0)/R$ ^a

	$\Delta_f H^\circ_{298/R}$ (kK)	$S^\circ_{298/R}$	$(H^\circ_{298}-H^\circ_0)/R$ (kK)
O(g)	29.97 ± 0.01	19.3578 ± 0.0001	0.8092
O ₂ (g)		24.660 ± 0.004	1.0440
O ₃ (g)	17.1 ± 0.2	28.73 ± 0.01	1.2468
Be(α)		1.143 ± 0.006	0.2345
Be(g)	39.0 ± 0.6	16.3770 ± 0.0001	0.74538
BeO(s)	-73.29 ± 0.3	1.656 ± 0.005	0.3412
BeO(g)	16.1 ± 1.	23.756 ± 0.05	1.0449
Be ₂ O(g)	-4.5 ± 0.3	27.403 ± 0.3	1.3459
Be ₂ O ₂ (g)	-46.3 ± 3.	30.19 ± 0.3	1.4697
Be ₃ O ₃ (g)	-123. ± 4.	34.045 ± 0.3	1.819
Be ₄ O ₄ (g)	-198. ± 5.	35.644 ± 0.3	1.9044
Be ₅ O ₅ (g)	-265. ± 15.	(36.07) ± 0.3	2.290
Be ₆ O ₆ (g)	-330. ± 15.	(41.26) ± 0.5	2.583
Mg(s)		3.931 ± 0.01	0.6014
Mg(g)	17.7 ± 0.1	17.8651 ± 0.0001	0.74538
MgO(s)	-72.34 ± 0.04	3.24 ± 0.02	0.6206
MgO(g)	7.0 ± 3.	25.637 ± 0.01	1.0715
Mg ₂ (g)	34.7 ± 0.3	29.33 ± 0.05	1.2409
Ca(s)		5.003 ± 0.04	0.689
Ca(g)	21.4 ± 0.1	18.6154 ± 0.0004	0.74538
CaO(s)	-76.384 ± 0.1	4.582 ± 0.02	0.812
CaO(g)	5.3 ± 2.	26.412 ± 0.05	1.077
CaO ₂ (s)	-79.6 ± 0.3	(7.8) ± 0.3	
Ca ₂ (g)	41.6 ± 0.4	30.842 ± 0.2	1.316
Sr(s)		6.70 ± 0.02	0.7902
Sr(g)	19.8 ± 0.5	19.7886 ± 0.0002	0.74538
SrO(s)	-71.0 ± 0.1	6.668 ± 0.06	1.042
SrO(g)	-0.2 ± 3.	27.656 ± 0.002	1.0873
SrO ₂ (s)	-77. ± 2.	(11.) ± 0.5	
Sr ₂ (g)	37.3 ± 0.6	33.493 ± 0.6	1.3237
Sr ₂ O(g)	-25.4 ± 3.	34.1 ± 1.	1.535
Ba(s)		7.517 ± 0.08	0.8311
Ba(g)	21.9 ± 1.	20.4627 ± 0.0001	0.74538
BaO(s)	-65.9 ± 0.3	8.66 ± 0.05	1.198
BaO(g)	-15.4 ± 1.	28.306 ± 0.05	1.084
Ba ₂ (g)	41.9 ± 0.8	35.015 ± 0.6	1.3172
Ba ₂ O(g)	-29. ± 5.	34.8 ± 1.	1.429
Ba ₂ O ₂ (g)	-72. ± 5.	38.3 ± 1.	1.882
B(s)		0.710 ± 0.01	0.1470
B(g)	67.9 ± 0.5	18.441 ± 0.001	0.7603
BO(g)	1.2 ± 1.	24.458 ± 0.003	1.0433
BO ₂ (g)	-39.0 ± 2.	27.665 ± 0.01	1.2956
B ₂ (g)	99.8 ± 4.	24.291 ± 0.1	1.0598
B ₂ O(g)	33. ± 12.	27.20 ± 0.50	1.4172
B ₂ O ₂ (g)	-55.5 ± 1.	30.015 ± 0.2	1.6112
B ₂ O ₃ (s)	-153.17 ± 0.17	6.491 ± 0.04	1.1187
B ₂ O ₃ (g)	-100.5 ± 0.5	34.371 ± 0.5	1.7341
Al(s)		3.405 ± 0.01	0.5490
Al(g)	39.60 ± 0.3	19.7782 ± 0.0001	0.8322
AlO(g)	8.1 ± 1.	26.25 ± 0.01	1.0568
AlO ₂ (g)	-10.4 ± 4.	(30.27) ± 1.	1.4483
Al ₂ (g)	59.0 ± 2.5	28.075 ± 0.03	1.1808
Al ₂ O(g)	-17.5 ± 2.	30.33 ± 0.4	1.5288
Al ₂ O ₂ (g)	-47.5 ± 4.	(33.78) ± 1.5	1.7462
Al ₂ O ₃ (s)	-201.54 ± 0.15	6.127 ± 0.01	1.2047
Ga(s)		4.993 ± 0.04	0.675

Table 3. Values of $\Delta_f H^\circ_{298/R}$, $S^\circ_{298/R}$, and $(H^\circ_{298}-H^\circ_0)/R$ (Continued)

	$\Delta_f H^\circ_{298/R}$ (kK)	$S^\circ_{298/R}$	$(H^\circ_{298}-H^\circ_0)/R$ (kK)
Ga(g)	32.7 ± 0.5	20.3180 ± 0.0002	0.7879
GaO(g)	17.7 ± 3.	27.749 ± 0.006	1.0734
Ga ₂ O(g)	-11.46 ± 1.	34.21 ± 0.4	1.4712
Ga ₂ O ₃ (s)	-131.2 ± 0.5	10.216 ± 0.04	1.750
In(s)		6.934 ± 0.03	0.7950
In(g)	28.9 ± 0.1	20.8878 ± 0.0001	0.7455
InO(g)	20.5 ± 3.	28.76 ± 0.06	1.081
In ₂ O(g)	-5.17 ± 2.	35.91 ± 0.4	1.5087
In ₂ O ₃ (s)	-111.4 ± 0.2	13.00 ± 0.4	2.0807
Tl(s)		7.734 ± 0.02	0.8217
Tl(g)	21.7 ± 0.2	21.7522 ± 0.0001	0.74538
TlO(g)	23.6 ± 5.	29.76 ± 1.	1.0904
Tl ₂ O(s,l)	-20.1 ± 0.2	17.56 ± 1.	1.816
Tl ₂ O(g)	3.7 ± 1.	37.85 ± 0.6	1.554
Tl ₂ O ₃ (s)	-46.5 ± 0.5	19.244 ± 1.	2.4295
Si(s)		2.262 ± 0.01	0.3869
Si(g)	54.2 ± 1.	20.1903 ± 0.0001	0.9081
SiO(g)	-11.9 ± 0.6	25.437 ± 0.002	1.0482
SiO ₂ (qu)	-109.53 ± 0.1	4.99 ± 0.02	0.8318
SiO ₂ (g)	-38.7 ± 1.	27.496 ± 0.1	1.268
Si ₂ (g)	67.9 ± 2.	27.625 ± 0.1	1.1141
Si ₂ O ₂ (g)	-43.22 ± 2.	37.3 ± 3.	1.835
Si ₃ (g)	74. ± 3.	32.3 ± 0.60	1.6783
Ge(s)		3.74 ± 0.02	0.5576
Ge(g)	44.7 ± 0.4	20.181 ± 0.001	0.8998
GeO(g)	-4.5 ± 0.5	26.915 ± 0.005	1.0562
GeO ₂ (tet)	-69.78 ± 0.1	4.776 ± 0.02	0.8696
GeO ₂ (g)	-13. ± 2.	29.00 ± 0.1	1.354
Ge ₂ (g)	58. ± 1.	30.508 ± 0.001	1.3983
Ge ₂ O ₂ (g)	-33. ± 2.	37.6 ± 1.5	1.900
Ge ₃ O ₃ (g)	-59.6 ± 2.	50.2 ± 2.5	3.250
Sn(s)		6.156 ± 0.01	0.7605
Sn(g)	36.23 ± 0.1	20.2517 ± 0.0004	0.7475
SnO(s)	-33.76 ± 0.02	6.876 ± 0.035	1.0507
SnO(g)	2.6 ± 0.6	27.904 ± 0.005	1.0663
SnO ₂ (s)	-69.47 ± 0.02	5.895 ± 0.01	1.0084
SnO ₂ (g)	-5. ± 6.	30.248 ± 0.5	1.4186
Sn ₂ (g)	49.6 ± 1.	31.352 ± 0.1	1.235
Sn ₂ O ₂ (g)	-29. ± 2.	37.7 ± 3.	
Sn ₃ O ₃ (g)	-61. ± 3.	45.6 ± 4.	
Sn ₄ O ₄ (g)	-95. ± 3.	54.4 ± 4.	
Pb(s)		7.794 ± 0.035	0.8263
Pb(g)	23.48 ± 0.1	21.080 ± 0.001	0.74538
PbO(red)	-26.29 ± 0.06	8.16 ± 0.02	1.1095
PbO(g)	8.2 ± 1.	28.857 ± 0.003	1.0778
PbO ₂ (g)	0.8 ± 6.	31.39 ± 0.1	1.4735
PbO ₂ (s)	-33.1 ± 0.3	8.635 ± 0.02	1.3184
Pb ₂ (g)	35.9 ± 0.3	33.383 ± 0.1	1.270
Pb ₂ O ₂ (g)	-15. ± 3.	37.3 ± 3.	
Pb ₂ O ₃ (s)	-59.1 ± 0.4	18.27 ± 0.25	2.5113
Pb ₃ O ₃ (g)	-38. ± 4.	47.5 ± 4.	
Pb ₃ O ₄ (s)	-86.4 ± 0.8	25.49 ± 0.3	3.6308
Pb ₄ O ₄ (g)	-68. ± 6.	54.2 ± 5.	
Pb ₅ O ₅ (g)	-93. ± 6.	58.8 ± 6.	
Pb ₆ O ₆ (g)	-119. ± 6.	67.8 ± 6.	

Table 3. Values of $\Delta H^\circ_{298}/R$, S°_{298}/R , and $(H^\circ_{298}-H^\circ_0)/R$. (Continued)

	$\Delta H^\circ_{298}/R$ (K)	S°_{298}/R	$(H^\circ_{298}-H^\circ_0)/R$ (K)
Zn(s)		5.017 ± 0.02	0.6804
Zn(g)	15.69 ± 0.02	19.3494 ± 0.0002	0.74538
ZnO(s)	-42.15 ± 0.03	5.25 ± 0.05	0.8339
ZnO(g)	10.9 ± 1.	26.95 ± 0.3	1.082
Cd(s)		6.230 ± 0.02	0.7513
Cd(g)	13.45 ± 0.08	20.1623 ± 0.0001	0.74538
CdO(s)	-31.04 ± 0.1	6.59 ± 0.20	1.011
CdO(g)	15.6 ± 1.	(28.014) ± 0.1	1.104
Hg(l)		9.13 ± 0.01	1.1236
Hg(g)	7.382 ± 0.005	21.0310 ± 0.0002	0.74542
HgO(s)	-10.92 ± 0.01	8.45 ± 0.04	1.0965
HgO(g)	11.2 ± 1.0	28.86 ± 0.3	1.082

^aSee Table 4 for references.

included in the major compilations. In all cases, the thermodynamic values selected reproduce, within experimental uncertainty, the vapor pressure measurements considered reliable.

In reviewing the available tabulations of thermodynamic functions for gaseous atoms, it was discovered that heat capacity, Gibbs energy function, entropy, and enthalpy increment values for many elements are in error because they are based on only the observed electronic levels, e.g., as listed by Moorc (1949, 1952, 1958), and do not include unobserved low-lying levels, which can contribute significantly. Although this problem was not severe for the elements covered in this paper, it should be noted that the equations for Gibbs energy functions given for gaseous atoms in Table 2 are consistent with new calculations that take into account more recent spectroscopic data and estimates of missing low-lying electronic levels (Brewer, 1983). The equations given for $-(G^\circ_T - H^\circ_{298})/RT$ represent the tabulated values within typical limits of ± 0.01 over their applicable temperature ranges. The equations were derived by fitting tabular data and are not direct integrations of heat capacity equations. Because of the nature of the polynomial fits, values derived by differentiating these equations do not represent thermodynamic properties, e.g., heat capacities, accurately.

Data sources for each of the selected values are in any case summarized in Table 4, and more complete discussions of data sources are given below, when necessary.

The calculated partial pressures of major gaseous species in equilibrium with stable condensed oxide phases are shown below as plots of $\log P$ vs $1/T$ for several representative vaporization conditions. The particular conditions are 0.2 bar O_2 , representing oxidizing conditions, congruent vaporization, representing neutral vaporization, and either 10^{-15} bar O_2 or the O_2 pressure of the metal-metal oxide equilibria, representing reducing conditions. The metal-metal oxide equilibrium O_2 pressure was chosen when it exceeded 10^{-15} bar. The maximum vaporization rates calculated by the Hertz-Knudsen equation are also shown in plots below.

TABLE 4. Sources of data in Tables 1 through 3^a

	$-(G^\circ_T - H^\circ_{298})/RT$ $S^\circ_{298} \cdot H^\circ_{298} - H^\circ_0$	$\Delta_r H^\circ_{298}$	T_{fus}
O(g)	6,25	7	
O ₂ (g)	6,25		
O ₃ (g)	25	25	
Be(α)	1(2),7,8,9,14		
Be(g)	1,2,7,8,10,14	7,8,1,9,14	
BeO(s)	1,5,7(9),14	7,1,5,9,14	1
BeO(g)	1,5,14	1,5,14	
Be ₂ O(g)	1	1	
Be ₂ O ₂ (g)	1	1	
Be ₃ O ₃ (g)	1	1	
Be ₄ O ₄ (g)	1	1	
Be ₅ O ₅ (g)	2	b	
Be ₆ O ₆ (g)	2,14	b	
Mg(s)	2(1),7,8,14		2
Mg(g)	1,8,2,7,9,10,14	7,1,2(8),9,14	
MgO(s)	1,5,7,9,14	7,1,5,9,14	1,19
MgO(g)	5,1,14	5,1,14	
Mg ₂ (g)	5(1)	5(1)	
Ca(s)	1,7,2,8,9,14		1
Ca(g)	1,2,7,8,9,10,14	7,11,1,8,9,14	
CaO(s)	1(4),7,14	7,1,4,9,14	1
CaO(g)	5,1,14	5,1,14	
CaO ₂ (s)		26(9)	
Ca ₂ (g)	5(1),14	5(1),14	
Sr(s)	1(2),(9,14)		1
Sr(g)	1,3(8),9,10,14	11(1,9,14)	
SrO(s)	1,4(9,14)	1,4,9,14	1
SrO(g)	1,4,14	27,4(9),14	
SrO ₂ (s)		12(9)	
Sr ₂ (g)	1	1	
Sr ₂ O(g)	1	b	
Ba(s)	1,4,9,14		1
Ba(g)	10,1,4,9,10,14	8,11(1,3,9,14)	
BaO(s)	1,4(9,14)	1,4(9),14	1
BaO(g)	1,4,14	1(4),14	
Ba ₂ (g)	1	1	
Ba ₂ O(g)	b	b	
Ba ₂ O ₂ (g)	b	b	
B(s)	13,1,7,8,9,14		13
B(g)	13,1,7,8,9,10,14	11,1,7,9(13)	
BO(g)	1,2,9,14	1,2,14	
BO ₂ (g)	1,2,9,14	1	
B ₂ (g)	1,13	13,1	
B ₂ O(g)	1,2,14	1	
B ₂ O ₂ (g)	1(2),(9)	1,2(9)	
B ₂ O ₃ (s)	1,3,7,9,14	1,3,7,9,14	1
B ₂ O ₃ (g)	1,3(9)	1,3,7,9	
Al(s)	28,1,7,8,9,14,17		28
Al(g)	17,1,7,8,10,14	28,1,7,8,14,17	
AlO(g)	17(1)	17,1	
AlO ₂ (g)	17(1)	17(1)	
Al ₂ (g)	1	1	
Al ₂ O(g)	17(1)	17(1)	
Al ₂ O ₂ (g)	17,1	17,1	
Al ₂ O ₃ (s)	17,1,7,9,14	7,17,1,9,14	1,19
Ga(s)	1,22,8,9,14		1
Ga(g)	1,8(9),10,14	1,8(9),14	
GaO(g)	1,9	1	
Ga ₂ O(g)	1	1	
Ga ₂ O ₃ (s)	1,9,14	1,9,14	1
In(s)	1,8(9),14		1
In(g)	8,1,9,10,14	1,8,9,14	
InO(g)	1	1	
In ₂ O(g)	1	1	
In ₂ O ₃ (s)	1	1,9	1
Tl(s)	8,1,9,14		1
Tl(g)	8,1,9,10,14	8,11,1,9,14	
TlO(g)	1	1	
Tl ₂ O(s)	1	1(14)	1

TABLE 4. (continued)

	$-(G^\circ T - H_{298}^\circ)/T$	$\Delta_f H_{298}^\circ$	T_{fus}
	$S_{298}^\circ, H_{298}^\circ - H_0^\circ$		
Tl ₂ O(g)	1(14)	1	
Tl ₂ O ₃ (s)	1(14)	1(14)	1
Si(s)	21,26,8,14,16		21
Si(g)	16,2,7,8,9,10,14	2,7,16	
SiO(g)	16,2,9,14	16(2),9,14	
SiO ₂ (qu)	^b	7,2,9,14,16	19,2
SiO ₂ (cr)	^b		16,2
SiO ₂ (g)	16,2,14	16,2,9,14,	
Si ₂ (g)	16,2,9,14	16	
Si ₂ O ₂ (g)	^b	^b	
Si ₃ (g)	23,2,14,16	8,2,14,16	
Ge(s)	8,16,7,9,14		16
Ge(g)	16,8,9,10,14	16(8,9,14)	
GeO(g)	12,16(9)	12,16(9)	
GeO ₂ (s)	16,7,14	7,14,16	16
GeO ₂ (g)	16	16	
Ge ₂ (g)	16,9	16	
Ge ₂ O ₂ (g)	^b	^b	
Ge ₃ O ₃ (g)	^b	^b	
Sn(s)	8,16,7,9,14		16
Sn(g)	8,16,9,10,14	7,16,8(9),14,16	
SnO(s)	16,7(9),14	16(7,9,14)	16
SnO(g)	16,9	16(9)	
SnO ₂ (s)	16(7,9,14)	16(7,9,14)	16
SnO ₂ (g)	16	16	
Sn ₂ (g)	16,18	18,16	
Sn ₂ O ₂ (g)	^b	^b	
Sn ₃ O ₃ (g)	^b	^b	
Sn ₄ O ₄ (g)	^b	^b	
Pb(s)	16,7,8,9,14		16
Pb(g)	16,10(2,8,9,14)	7,8,9,14,16	
PbO(red)	16,3,9,14	3,16,9,14	
PbO(yel)	16,3,14	16,2,20	16
PbO(g)	16,3,14	3,16,14	
PbO ₂ (s)	3,14,16	3,16,14	
PbO ₂ (g)	16	16	
Pb ₂ (g)	16,18	18,16	
Pb ₂ O ₂ (g)	^b	^b	
Pb ₂ O ₃ (s)	16,9	16	
Pb ₃ O ₃ (g)	^b	^b	
Pb ₃ O ₄ (s)	3,9,14,16	3,16,9,14	
Pb ₄ O ₄ (g)	^b	^b	
Pb ₅ O ₅ (g)	^b	^b	
Pb ₆ O ₆ (g)	^b	^b	
Zn(s)	15(8),(14)		15
Zn(g)	15,8,10,14	7,8,9,14,15	
ZnO(s)	7,14	7(9),14	20

a. Be-O System

The only high-temperature solid phase is the oxide, BeO. Under neutral and reducing conditions, vaporization takes place primarily by decomposition to Be atoms and oxygen species. BeO, Be₂O₂, Be₃O₃, Be₄O₄, and Be₅O₅ are the principal vapor species under oxidizing conditions. Partial pressures of major vapor species and calculated maximum vaporization rates are shown in Figs. 1-4.

Be₅O₅(g), Be₆O₆(g) thermodynamic data—the enthalpy of formation was calculated by the third-law method using the mass spectrometric data of Chupka, Berkowitz, and Giese (1959) and of Theard and Hildenbrand (1964).

TABLE 4. (continued)

	$-(G^\circ T - H_{298}^\circ)/T$	$\Delta_f H_{298}^\circ$	T_{fus}
	$S_{298}^\circ, H_{298}^\circ - H_0^\circ$		
ZnO(g)	^b	^b	
Cd(s)	8,14		8
Cd(g)	8,7,10,14	8,7,14	
CdO(s)	14,7	7,14	20
CdO(g)	^b	^b	
Hg(l)	8,2,14		
Hg(g)	2,8,7,10,14	7,2,8,14	
HgO(s)	2,7,14	7,2,14	
HgO(g)	^b	^b	

References to Table 4

- ¹(Glushko *et al.*, 1981).
- ²(Stull *et al.*, 1971).
- ³(Chase *et al.*, 1974).
- ⁴(Chase *et al.*, 1975).
- ⁵(Chase *et al.*, 1978).
- ⁶(Chase *et al.*, 1982).
- ⁷(COA, 1978).
- ⁸(Hultgren and Desai, 1973).
- ⁹(Wagman *et al.*, 1982).
- ¹⁰(Brewer, 1983).
- ¹¹(Brewer, 1977).
- ¹²(Brewer and Rosenblatt, 1969).
- ¹³(Stull *et al.*, 1971, 31 March 1979 unbound supplement).
- ¹⁴(Pankratz, 1982).
- ¹⁵(Stull *et al.*, 1971, 31 December 1978 unbound supplement).
- ¹⁶(Glushko *et al.*, 1979a).
- ¹⁷(Stull *et al.*, 1971, 31 December 1979 unbound supplement). JANAF issued two sets of supplements on Al-O species dated 1979; the later set, with references to literature as late as 1982, is cited.
- ¹⁸(Balasubramanian and Pitzer, 1983).
- ¹⁹(Hlavac, 1982).
- ²⁰(Shunk, 1969).
- ²¹(Desai, 1986a).
- ²²(Amitin *et al.*, 1984).
- ²³(Brewer, 1984).
- ²⁴(Richet *et al.*, 1982).
- ²⁵(Glushko *et al.*, 1978).
- ²⁶(Glushko *et al.*, 1979b).
- ²⁷(Murad, 1981).
- ²⁸(Desai, 1986b).

^a References without parentheses are in essential agreement; those in parentheses differ from the chosen value by a significant portion of the stated uncertainty. The sources of the selected data are in boldface.

^b See text.

b. Mg-O System

The only high-temperature solid phase is the oxide, MgO. In neutral and reducing atmospheres, vaporization takes place by dissociation to give gaseous oxygen species and Mg(g); the MgO(g) partial pressure is comparable to that of Mg(g) in oxidizing atmospheres. Partial pressures of major vapor species and calculated maximum vaporization rates are shown in Figs. 5-8. As can be seen from the graphs, MgO is especially volatile at high temperatures under reducing conditions. This has important practical consequences in pointing out the instability and limited usefulness of magnesia-based refractories in hydrogen-containing or otherwise

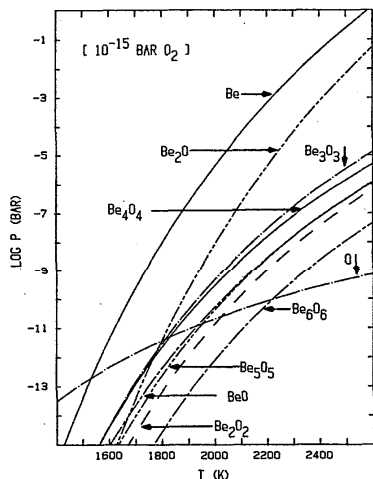


FIG. 1. BeO vaporization in 10^{-15} bar O_2 .

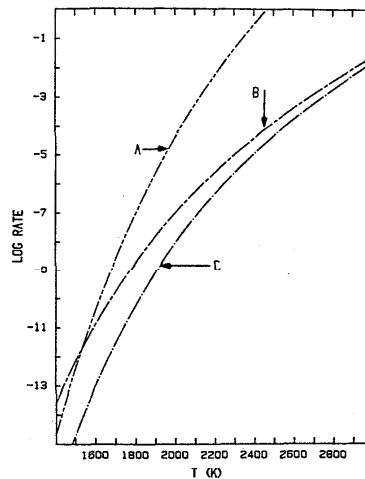


FIG. 4. BeO maximum vaporization rates. A— 10^{-15} bar O_2 ; B—congruent vaporization; C—0.2 bar O_2 .

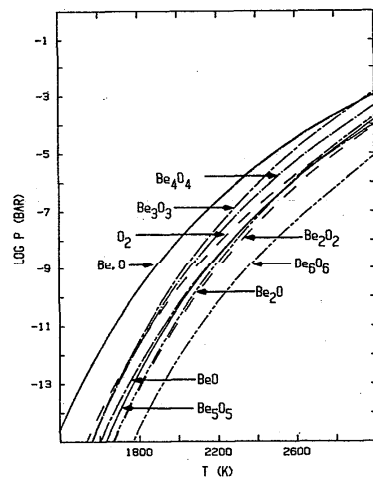


FIG. 2. BeO congruent vaporization.

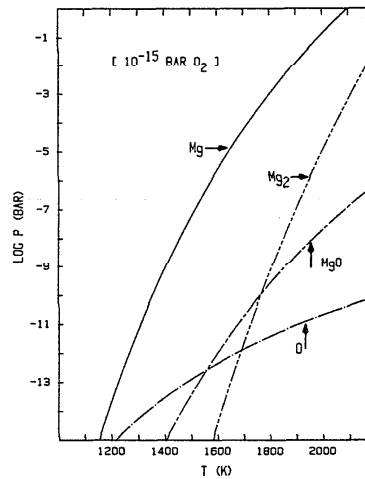


FIG. 5. MgO vaporization in 10^{-15} bar O_2 .

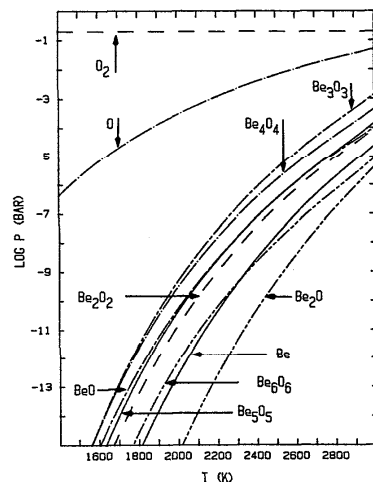


FIG. 3. BeO vaporization in 0.2 bar O_2 .

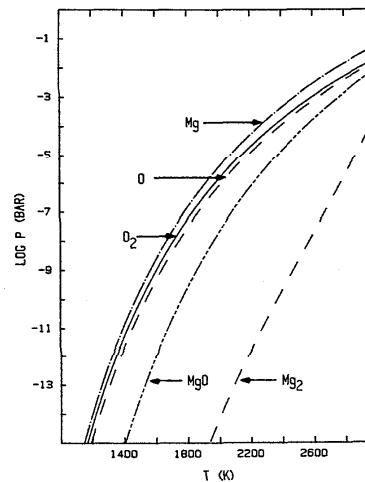


FIG. 6. MgO congruent vaporization.

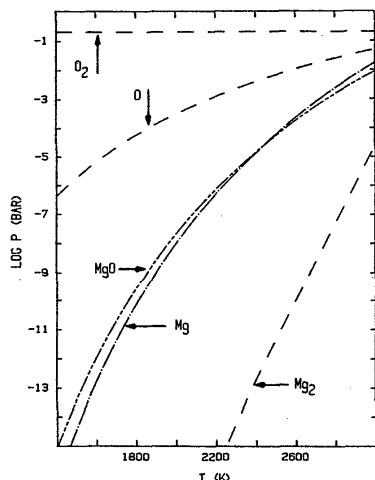
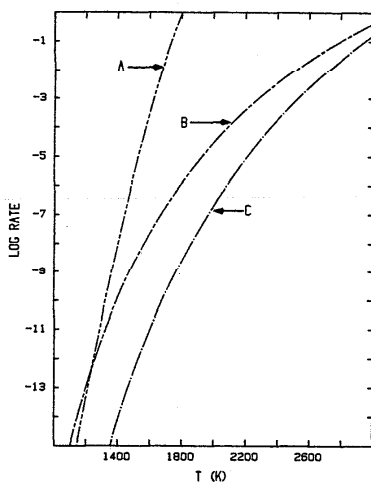
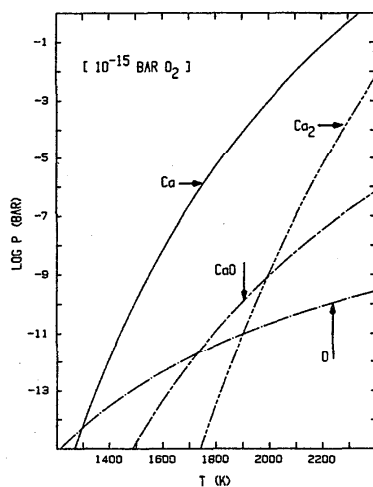
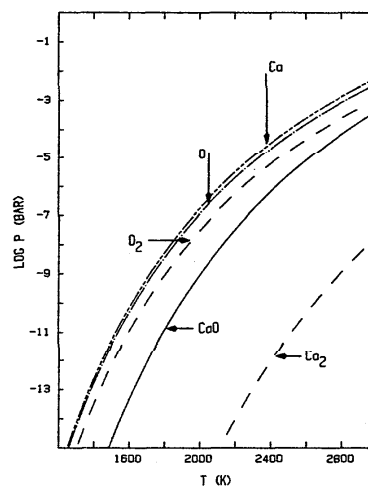
FIG. 7. MgO vaporization in 0.2 bar O_2 .FIG. 8. MgO maximum vaporization rates. A— 10^{-15} bar O_2 ; B—congruent vaporization; C—0.2 bar O_2 .FIG. 9. CaO vaporization in 10^{-15} bar O_2 .

FIG. 10. CaO congruent vaporization.

reducing atmospheres. The same is true of several of the other alkaline earth oxides.

c. Ca-O System

The only high-temperature solid phase is the oxide, CaO. The equilibrium oxygen pressure of the peroxide, CaO_2 , exceeds 0.2 bar at temperatures above about 300 K (Vannerberg, 1962). Vaporization takes place primarily by dissociation to Ca(g) and oxygen under neutral and reducing conditions; CaO(g) is the primary vapor phase product in oxidizing atmospheres. Partial pressures of major vapor species and calculated maximum vaporization rates are shown in Figs. 9–12.

d. Sr-O System

$SrO(s)$ is the stable high-temperature condensed phase under neutral and reducing conditions. $SrO_2(s)$ is stable in oxidizing atmospheres at lower temperatures; the O_2 pressure over $SrO_2(s)$ reaches 0.2 bar at about 800 K (Vannerberg, 1962). Vaporization takes place primarily by dissociation to Sr(g), SrO(g), and oxygen species under neutral and oxidizing conditions, while sublimation to SrO(g) dominates in oxidizing atmospheres. The calculated neutral vapor composition is consistent with the observation of Kaufman *et al.* (1965) from electric deflection experiments that the vapor at 2500 K contains about 5 mol % molecular SrO. Partial pressures of major vapor species and calculated maximum vaporization rates are shown in Figs. 13–16.

$Sr_2O(g)$ thermodynamic data—although Sr_2O is not a major species and is not listed in the IVTAN or JANAF compilations, the results of Drowart *et al.* (1964) indicate that it should be included for completeness. Therefore, their estimated molecular constants were adopted and used to evaluate thermodynamic functions: $\angle Sr-O-Sr = 180^\circ$, $r(Sr-O) = 0.192$ nm, vibrational fundamentals of 256, 233 (doubly degenerate), and 888 cm^{-1} , an electronic ground state degeneracy of 3, and no excited electronic states. The enthalpy of formation of $Sr_2O(g)$ was derived from a third-

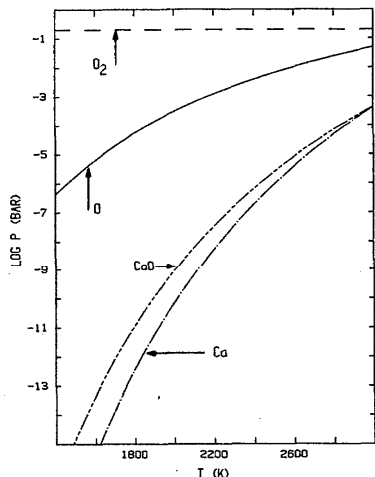


FIG. 11. CaO vaporization in 0.2 bar O₂.

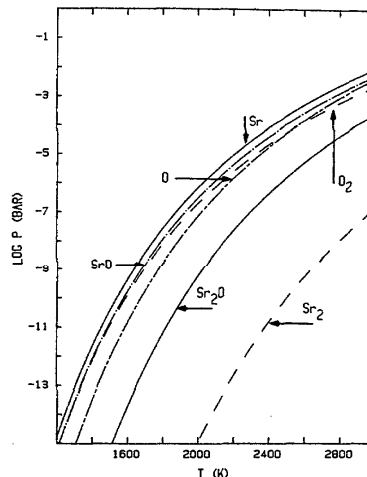


FIG. 14. SrO congruent vaporization.

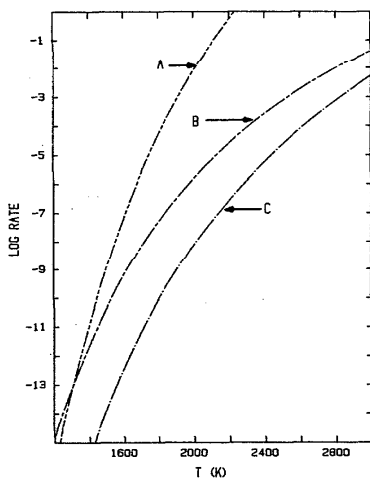


FIG. 12. CaO maximum vaporization rates. A—10⁻¹⁵ bar O₂; B—congruent vaporization; C—0.2 bar O₂.

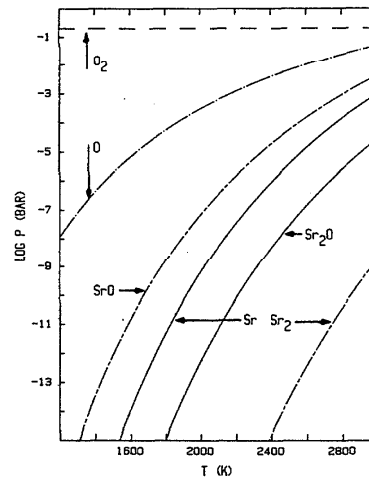


FIG. 15. SrO vaporization in 0.2 bar O₂.

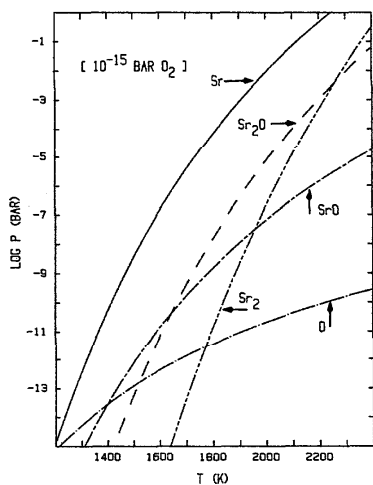


FIG. 13. SrO vaporization in 10⁻¹⁵ bar O₂.

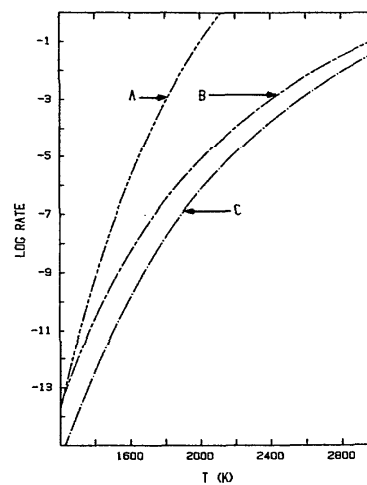


FIG. 16. SrO maximum vaporization rates. A—10⁻¹⁵ bar O₂; B—congruent vaporization; C—0.2 bar O₂.

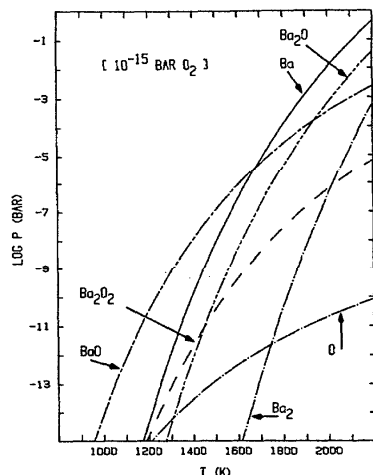
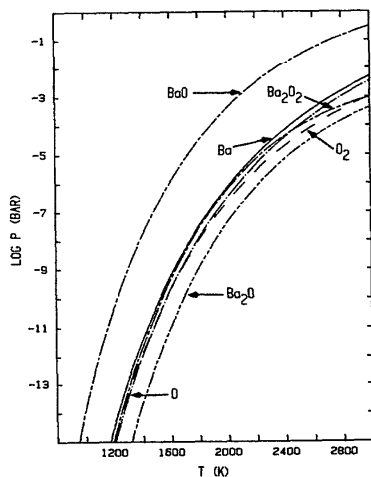
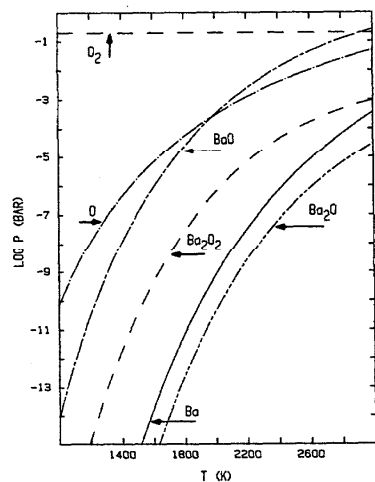
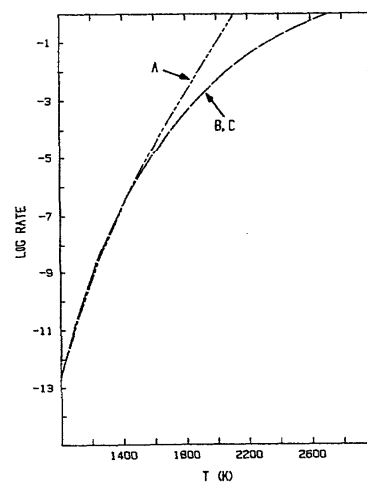
FIG. 17. BaO vaporization in 10^{-15} bar O_2 .

FIG. 18. BaO congruent vaporization.

FIG. 19. BaO vaporization in 0.2 bar O_2 .FIG. 20. BaO maximum vaporization rates. A— 10^{-15} bar O_2 ; B—congruent vaporization; C—0.2 bar O_2 .

law treatment of the equilibrium data of Drowart *et al.* (1964) using these calculated functions. As can be seen in the graphs, Sr_2O is a minor feature of the vaporization chemistry under each of the environmental conditions.

$CaO_2(s)$ thermodynamic data—the enthalpy of formation was recalculated by (Garvin *et al.*, 1987) from the experimental data cited by Glushko *et al.* (1979b).

e. Ba-O System

$BaO(s)$ is the condensed phase stable at high temperatures under neutral and reducing conditions. In oxidizing atmospheres $BaO_2(s)$ is stable at low temperatures; the O_2 pressure over $BaO_2(s)$ reaches 0.2 bar at about 1000 K (Vannerberg, 1962; Kedrovskii *et al.*, 1967).

The calculated vaporization equilibria shown in Figs. 17–19 indicate that $BaO(g)$ is the principal product for vaporization under oxidizing and neutral conditions, but that $Ba(g)$ becomes important at high temperatures under reducing conditions. It should be pointed out that our calculated neutral vapor composition differs appreciably from the reported results of four separate mass spectrometric studies (Inghram *et al.*, 1955; Newbury *et al.*, 1968; Semenov *et al.*, 1972; Hilpert and Gerads, 1975) in that the latter indicate almost comparable BaO and Ba partial pressures at 1500 to 1800 K. Recent mass spectrometric investigation in our own laboratory (Lamoreaux and Hildenbrand, 1983), however, show that under neutral conditions the ratio $p(BaO)/p(Ba) > 100$, so that, as suspected, some reduction of BaO was occurring in the earlier work. The calculated maximum vaporization rate is shown in Fig. 20.

Here again, the major compilations do not include data for the species Ba_2O_2 and Ba_2O , but they are included here for completeness since they have been observed; molecular constants were selected as noted below. The enthalpies of formation for these species were chosen so as to be consistent with the neutral composition inferred from our mass spectra at low ionizing energy.

$Ba_2O(g)$ thermodynamic data—the Gibbs energy functions were calculated using the approximate molecular

constants of Kudin (1981): $r(\text{Ba-O}) = 0.231$ nm, $\angle\text{Ba-O-Ba} = 180^\circ$, electronic ground state degeneracy = 3, no excited electronic states, and vibrational fundamentals of 500, 280(2), and 720 cm^{-1} .

Ba_2O_2 thermodynamic data—the Gibbs energy functions were calculated using the matrix isolation spectroscopy results of Ault and Andrews (1975) for the planar rhombic molecule with a derived O-Ba-O angle of 102° and observed vibrational fundamentals at 402 and 501 cm^{-1} , and the estimated molecular constants of Kudin (1981): $r(\text{Ba-O}) = 0.21$ nm, vibrational fundamentals 470, 330, 270, and 200 cm^{-1} , electronic ground state degeneracy = 1, and no excited electronic states.

f. B-O System

The stable solid phase is B_2O_3 , with a melting point of 723 K. Vaporization takes place primarily by evolution of $\text{B}_2\text{O}_3(\text{g})$, except that $\text{B}_2\text{O}_2(\text{g})$ becomes important at high temperatures under reducing conditions and $\text{BO}_2(\text{g})$ is important at low temperatures under oxidizing conditions. The calculated vaporization equilibria and vaporization rates are shown in Figs. 21–24. Partial pressures under reducing conditions were calculated for an O_2 partial pressure of 10^{-15} bar up to 2923 K, where the calculated O_2 pressure of the B- B_2O_3 equilibrium reaches this value, and for the O_2 pressure of the B- B_2O_3 equilibrium at higher temperatures. If liquid B_2O_3 is the only condensed phase present, its composition will change during vaporization unless $\text{B}_2\text{O}_3(\text{g})$ evolution dominates; if the liquid composition is changing, the partial pressures indicated are thus strictly applicable only at the start of vaporization.

g. Al-O System

Al_2O_3 is the stable solid phase in this system. The major gaseous aluminum species are Al, AlO, and Al_2O , depending on conditions. Some earlier reviews selected data that indicated a much higher thermodynamic stability for $\text{AlO}_2(\text{g})$, such that this species dominated the vaporization chemistry under oxidizing conditions. We agree with the recent

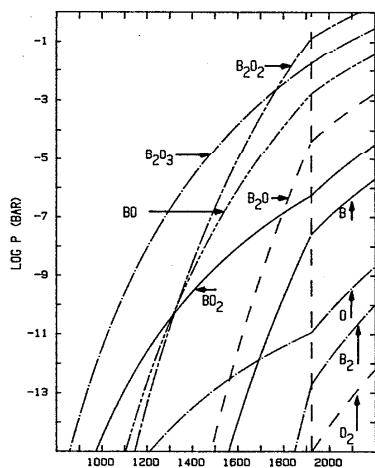


FIG. 21. B_2O_3 vaporization in 10^{-15} bar O_2 below 2923 K and vaporization of B- B_2O_3 mixture above 2923 K.

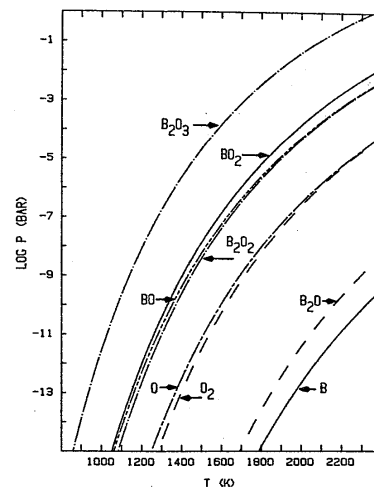


FIG. 22. B_2O_3 congruent vaporization.

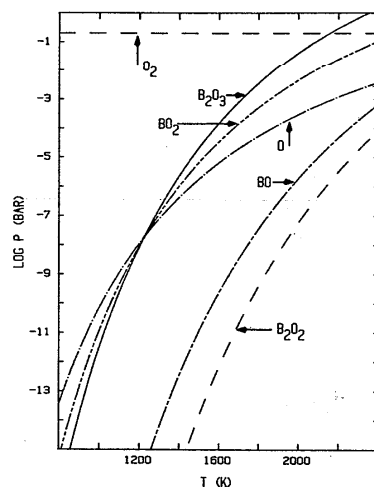


FIG. 23. B_2O_3 vaporization in 0.2 bar O_2 .

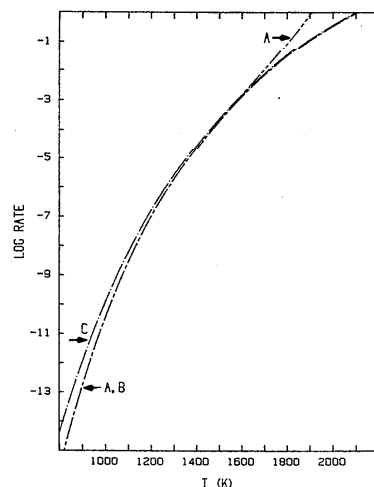


FIG. 24. B_2O_3 maximum vaporization rates. A— 10^{-15} bar O_2 ; B—congruent vaporization; C—0.2 bar O_2 .

IVTAN (Glushko *et al.*, 1981) and JANAF table (Stull *et al.*, 1971, December 31, 1979 unbound supplement) publications that assign a significantly lower stability to $\text{AlO}_2(\text{g})$, based primarily on the studies of Ho and Burns (1980). The calculated vaporization equilibria and maximum vaporization rates are shown in Figs. 25–28. Vaporization under reducing conditions was calculated for an O_2 pressure of 10^{-15} bar of O_2 up to 2230 K, where the calculated O_2 pressure of the Al– Al_2O_3 equilibrium reaches 10^{-15} bar, and for the O_2 pressure of the Al– Al_2O_3 equilibrium above this temperature.

h. Ga–O System

The stable solid phase is Ga_2O_3 . The calculated vaporization equilibria and maximum vaporization rates are shown in Figs. 29–32. Vaporization under reducing conditions was calculated for an O_2 pressure of 10^{-15} bar up to 1446 K, where the O_2 pressure of the Ga– Ga_2O_3 equilibrium reaches this value, and for the O_2 pressure of the Ga– Ga_2O_3 equilibrium at higher temperatures.

i. In–O System

The stable solid phase is In_2O_3 . The calculated vaporization partial pressures and maximum vaporization rates are shown in Figs. 33–36. Partial pressures under reducing conditions were calculated for an O_2 pressure of 10^{-15} bar up to 1239 K, where the O_2 pressure of the In– In_2O_3 equilibrium reaches this value, and for the O_2 pressure of the In– In_2O_3 equilibrium at higher temperatures.

j. Tl–O System

The stable solid oxide phase under neutral and reducing conditions, and in 0.2 atm of O_2 above about 1060 K, is Tl_2O . Tl_2O_3 is the stable phase at lower temperatures under oxidizing conditions. Calculated partial pressures and maximum rates for vaporization processes are shown in Figs. 37–40. Partial pressures over Tl_2O under reducing conditions were calculated for an O_2 pressure of 10^{-15} bar up to 731 K, where the O_2 partial pressure of the Tl– Tl_2O equilibrium

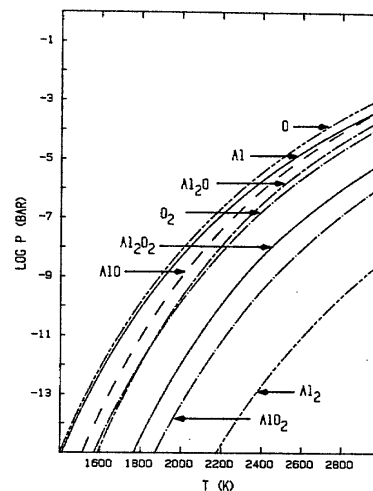


FIG. 26. Al_2O_3 congruent vaporization.

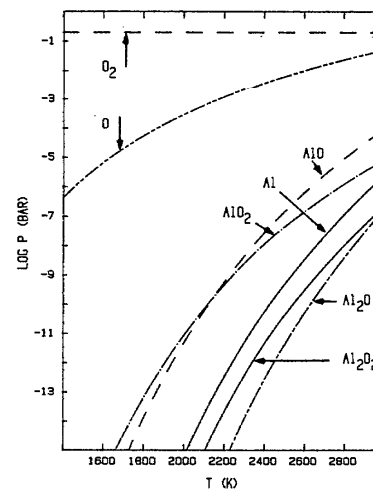


FIG. 27. Al_2O_3 vaporization in 0.2 bar O_2 .

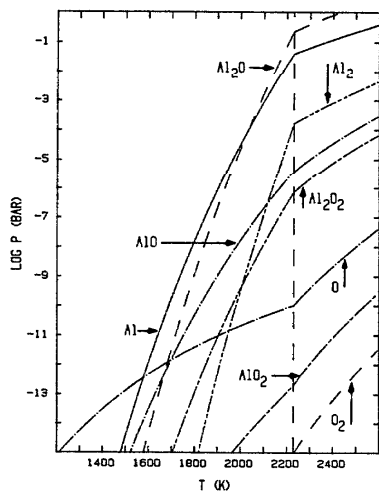


FIG. 25. Al_2O_3 vaporization in 10^{-15} bar O_2 below 2230 K and vaporization of Al– Al_2O_3 mixture above 2230 K.

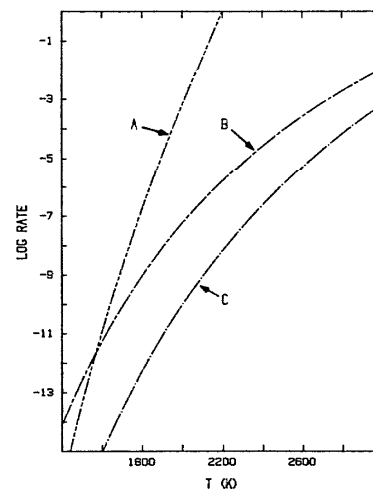


FIG. 28. Al_2O_3 maximum vaporization rates. A— 10^{-15} bar O_2 ; B—congruent vaporization; C—0.2 bar O_2 .

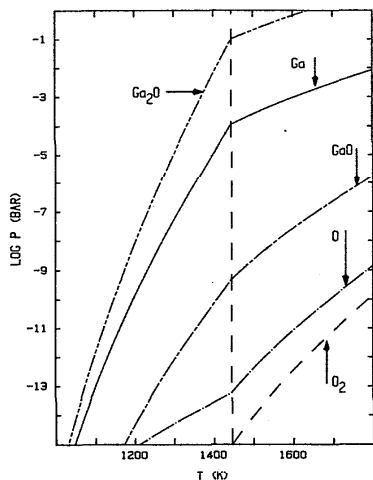


FIG. 29. Ga₂O₃ vaporization in 10⁻¹⁵ bar O₂ below 1446 K and vaporization of Ga-Ga₂O₃ mixture above 1446 K.

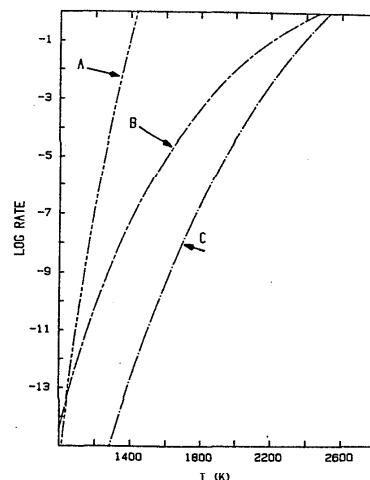


FIG. 32. Ga₂O₃ maximum vaporization rates. A—10⁻¹⁵ bar O₂; B—congruent vaporization; C—0.2 bar O₂.

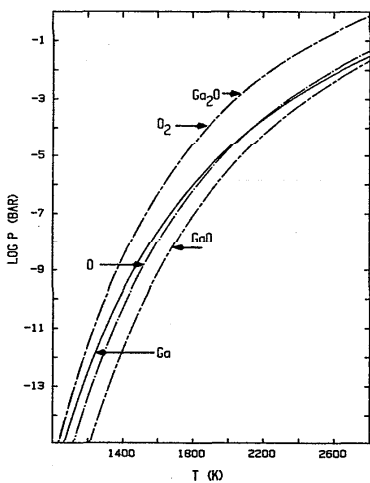


FIG. 30. Ga₂O₃ congruent vaporization.

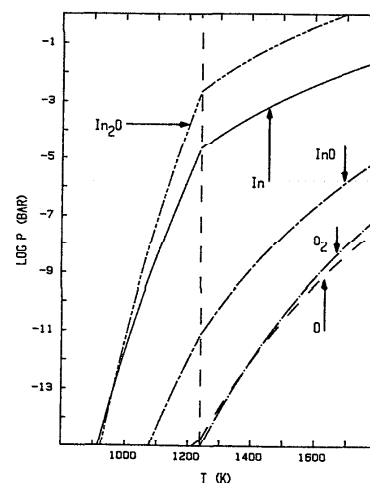


FIG. 33. In₂O₃ vaporization in 10⁻¹⁵ bar O₂ below 1239 K and vaporization of In-In₂O₃ mixture above 1239 K.

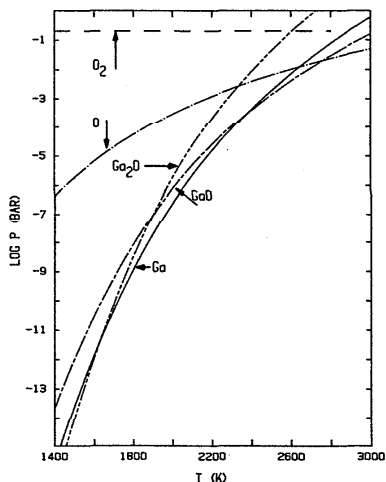


FIG. 31. Ga₂O₃ vaporization in 0.2 bar O₂.

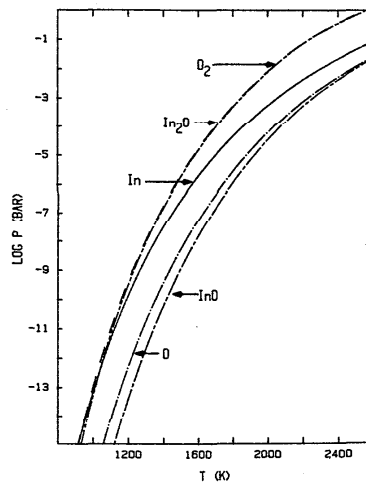
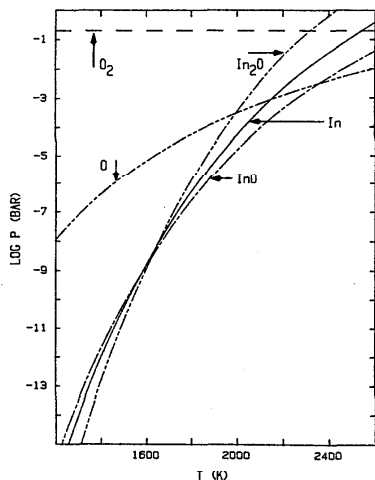
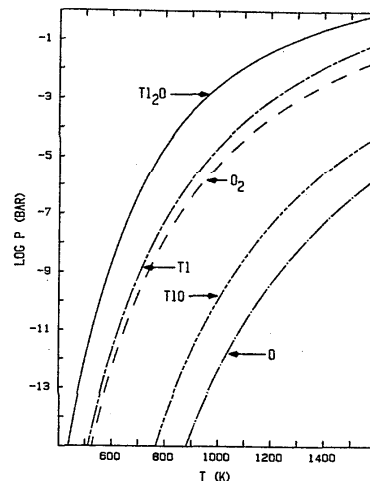
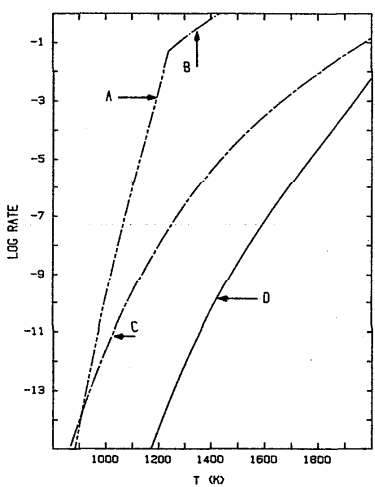
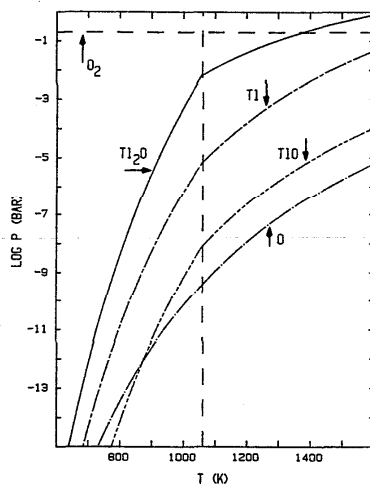
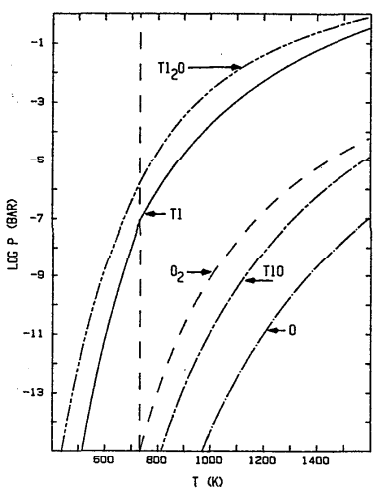
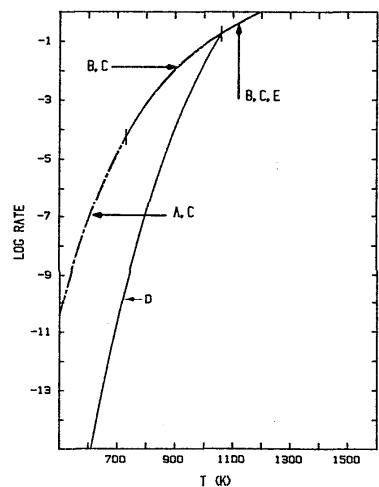


FIG. 34. In₂O₃ congruent vaporization.

FIG. 35. In_2O_3 vaporization in 0.2 bar O_2 .FIG. 38. Tl_2O congruent vaporization.FIG. 36. In_2O_3 maximum vaporization rates. A— 10^{-15} bar O_2 ; B— $\text{In-In}_2\text{O}_3$; C—congruent vaporization; D—0.2 bar O_2 .FIG. 39. Tl_2O_3 vaporization below 1060 K and TlO vaporization above 1060 K in 0.2 bar O_2 .FIG. 37. Tl_2O vaporization in 10^{-15} bar O_2 below 731 K and vaporization of $\text{Tl-Tl}_2\text{O}$ mixture above 731 K.FIG. 40. Maximum vaporization rates of thallium oxides. A— Tl_2O in 10^{-15} bar O_2 ; B— $\text{Tl-Tl}_2\text{O}$ equilibrium vaporization; C— Tl_2O congruent vaporization; D— Tl_2O_3 vaporization in 0.2 bar O_2 ; E— Tl_2O vaporization in 0.2 bar O_2 .

reaches this value, and for the O_2 pressure of the $Tl-Tl_2O$ equilibrium at higher temperatures. Partial pressures for vaporization in 0.2 bar of O_2 were calculated for Tl_2O_3 up to 1060 K, and for Tl_2O at higher temperatures.

k. Si-O System

Calculated partial pressures for vaporization of SiO_2 are shown in Figs. 41–44. $SiO(g)$ is the principal silicon-containing vaporization product under neutral and reducing conditions, while $SiO_2(g)$ is favored under oxidizing conditions below about 2500 K.

SiO_2 (quartz, cristobalite, liquid) thermodynamic data—the CODATA (Cox, 1978) value of the enthalpy of formation of quartz was accepted. Other data were taken from the recent article of Richet *et al.* (1982), which reviewed the available literature.

$Si_2O_2(g)$ thermodynamic data—Gibbs energy functions were calculated using the molecular constants of Khanna *et al.* (1981) for a planar Si–O–Si–O molecule with the terminal atoms lying on opposite sides of the central O–Si bond axis: $\angle Si-O-Si = \angle O-Si-O = 109.5^\circ$, $r(Si-O, \text{terminal}) = 0.174 \text{ nm}$, $r(Si-O, \text{central}) = 0.151 \text{ nm}$, ground electronic state degeneracy = 1, and no excited electronic states. The vibrational fundamentals as measured by infrared and Raman matrix isolation spectroscopy were 1222, 804, 766, 252, and 79 cm^{-1} ; the remaining fundamental at 180 cm^{-1} was calculated by force constant calculations (Khanna *et al.*, 1981). The Gibbs energy functions calculated using these constants are 2.8 K greater than those calculated using the data of Anderson and Ogden (1969) for a molecule with D_{2h} symmetry. The enthalpy of formation was then calculated by the third-law method from the mass spectrometric data of Porter *et al.* (1955) and of Zmbov *et al.* (1973).

l. Ge-O System

The stable condensed phase below 1308 K is tetragonal GeO_2 ; the hexagonal crystal structure is stable from 1308 K to the melting temperature, 1388 K (Glushko *et al.*, 1979a). Calculated partial pressures for vaporization of GeO_2 are shown in Figs. 45–48. GeO is the major germanium-contain-

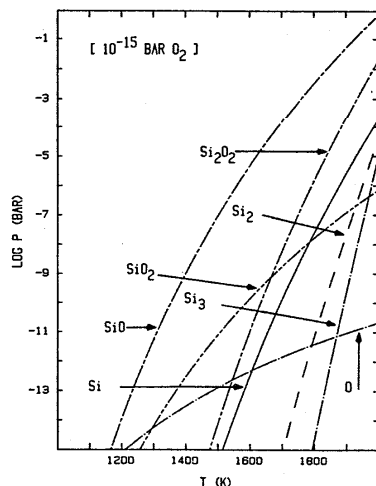


FIG. 41. SiO_2 vaporization in 10^{-15} bar O_2 .

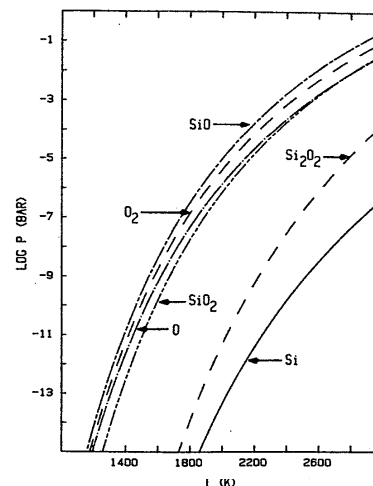


FIG. 42. SiO_2 congruent vaporization.

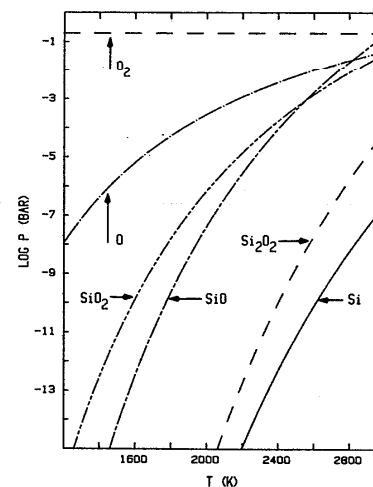


FIG. 43. SiO_2 vaporization in 0.2 bar O_2 .

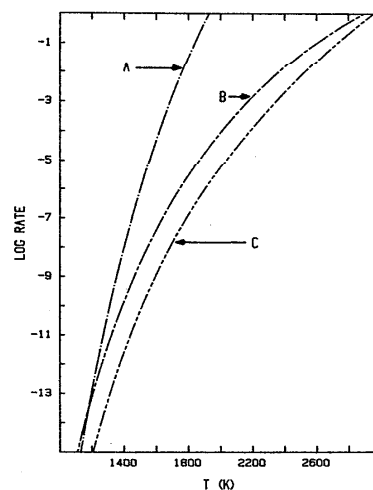


FIG. 44. SiO_2 maximum vaporization rates. A— 10^{-15} bar O_2 ; B—congruent vaporization; C—0.2 bar O_2 .

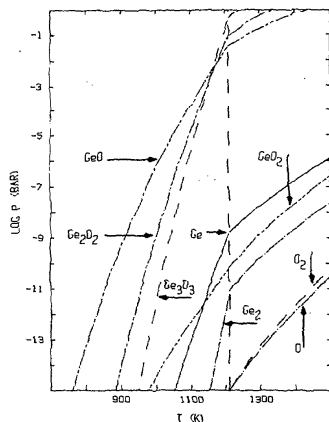


FIG. 45. GeO_2 vaporization in 10^{-15} bar O_2 below 1210 K and vaporization of Ge- GeO_2 mixture above 1210 K.

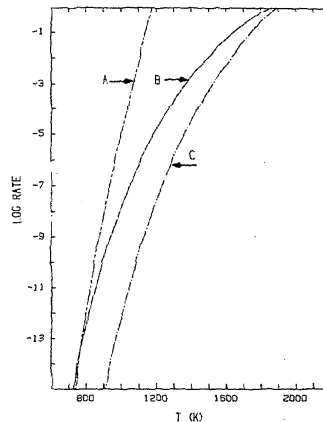


FIG. 48. GeO_2 maximum vaporization rates. A— 10^{-15} bar O_2 ; B—congruent vaporization; C—0.2 bar O_2 .

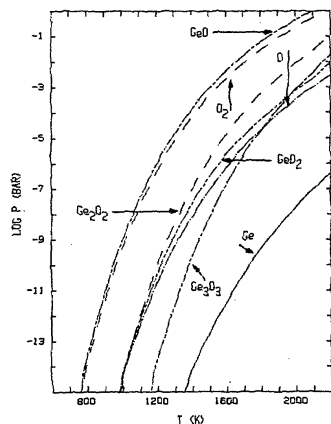


FIG. 46. GeO_2 congruent vaporization.

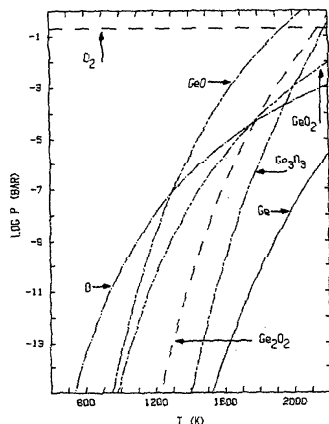


FIG. 47. GeO_2 vaporization in 0.2 bar O_2 .

ing vapor species under most conditions, with the polymeric species Ge_2O_2 and Ge_3O_3 becoming important at higher temperatures under reducing conditions.

$\text{Ge}_2\text{O}_2(\text{g})$ thermodynamic data—Gibbs energy functions were calculated using the molecular data of Ogden and Ricks (1970) which were estimated except for the observed vibrational fundamentals at 601 and 666 cm^{-1} : D_{2h} symmetry, symmetry number = 4, $r(\text{Ge}-\text{O}) = 0.187$ nm, $\angle\text{O}-\text{Ge}-\text{O} = 83^\circ$. The electronic ground state degeneracy was taken as unity, no excited electronic states were considered, and the remaining vibrational fundamentals of 120, 500, 450, and 80 cm^{-1} were estimated by analogy with the alkali metal M_2O_2 species (Lamoreaux and Hildenbrand, 1984). The enthalpy of vaporization was chosen to yield calculated vaporization equilibria consistent with the mass spectrometric data of Drowart *et al.* (1965).

$\text{Ge}_3\text{O}_3(\text{g})$ thermodynamic data—Gibbs energy functions were calculated using the molecular data of Ogden and Ricks (1970), which were estimated except for doubly degenerate vibrational fundamentals at 824 and 438 cm^{-1} : D_{3h} symmetry, symmetry number = 6, $r(\text{Ge}-\text{O}) = 0.185$ nm, $\angle\text{O}-\text{Ge}-\text{O} = 100^\circ$, $\angle\text{Ge}-\text{O}-\text{Ge} = 140^\circ$. The electronic ground state degeneracy was taken to be 1, no excited electronic states were considered, and the remaining vibrational fundamentals were estimated by analogy to Be_3O_3 : 159(2), 70(2), 150, 70(2), and 90 cm^{-1} . The enthalpy of formation was chosen to yield calculated vaporization equilibria in agreement with the mass spectrometric studies of Drowart *et al.* (1965).

m. Sn-O System

The stable condensed phase is SnO_2 . Calculated partial pressures for vaporization of SnO_2 are shown in Figs. 49–52. $\text{SnO}(\text{g})$ is the principal tin-containing vaporization species, with the polymeric species Sn_2O_2 , Sn_3O_3 , and Sn_4O_4 becoming important at higher temperatures under reducing conditions.

$\text{Sn}_2\text{O}_2(\text{g})$ thermodynamic data—because the existing spectroscopic data are insufficient to adequately determine

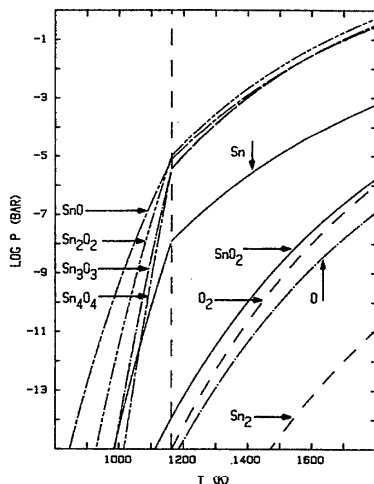


FIG. 49. SnO_2 vaporization in 10^{-15} bar O_2 below 1163 K and vaporization of Sn– SnO_2 mixture above 1163 K.

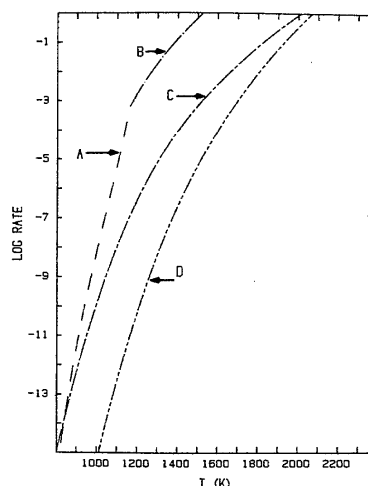


FIG. 52. SnO_2 maximum vaporization rates. A— 10^{-15} bar O_2 ; B—Sn– SnO_2 equilibrium; C—congruent vaporization; D—0.2 bar O_2 .

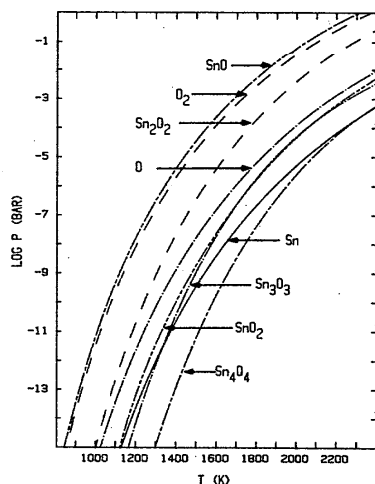


FIG. 50. SnO_2 congruent vaporization.

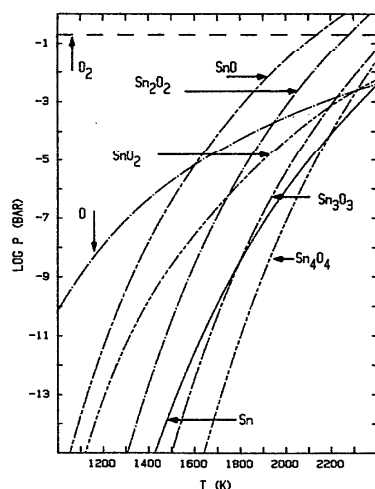


FIG. 51. SnO_2 vaporization in 0.2 bar O_2 .

the molecular constants of $\text{Sn}_2\text{O}_2(\text{g})$, the estimated S_{298}°/R value of Colin *et al.* (1965) was used along with the estimated value $C_p^\circ/R = 2.3$ g-at. derived by analogy to other gaseous compounds to calculate the Gibbs energy functions shown in Table 2. The enthalpy of formation was selected to yield calculated equilibria in agreement with the results of Colin *et al.*; the thermodynamic data presented in Tables 2 and 3 are consistent with observed partial pressures over the temperature range of the mass spectrometer studies.

$\text{Sn}_3\text{O}_3(\text{g})$ thermodynamic data—the data were derived as for $\text{Sn}_2\text{O}_2(\text{g})$, except that the value of C_p°/R was estimated as 2.5/g-at.

$\text{Sn}_4\text{O}_4(\text{g})$ thermodynamic data—the data were derived as for $\text{Sn}_3\text{O}_3(\text{g})$.

n. Pb–O System

The stable condensed oxide phase under neutral and reducing conditions, and in 0.2 atm of O_2 at temperatures above about 800 K, is PbO. Calculated partial pressures for vaporization of PbO are shown in Figs. 53–56. The predominant vapor phase species under neutral and oxidizing conditions are PbO and its polymers Pb_2O_2 , Pb_3O_3 , Pb_4O_4 , Pb_5O_5 , and Pb_6O_6 ; under reducing conditions the predominant vapor species is atomic lead.

Pb_2O_2 , Pb_3O_3 , Pb_4O_4 , Pb_5O_5 , and Pb_6O_6 thermodynamic data—Drowart, Colin, and Exsteen (1965) and Kazenas, Chizhikov, and Tsvetkov (1968) analyzed the vapors over PbO by mass spectroscopy. The thermodynamic properties of the gaseous PbO polymers given in Tables 2 and 3 were derived from the results of Drowart and co-workers, who made measurements to 1200 K and observed all five of these species. Kazenas *et al.* made measurements at temperatures up to 950 K and did not observe the pentamer or hexamer. The enthalpies of formation and entropies at 298 K selected by Drowart *et al.* were accepted for the dimer, trimer, and tetramer; the Gibbs energy functions for these species were derived by assuming that $C_p^\circ/R = 3.0$ /g-at. at all temperatures above 298 K. Although this heat capacity

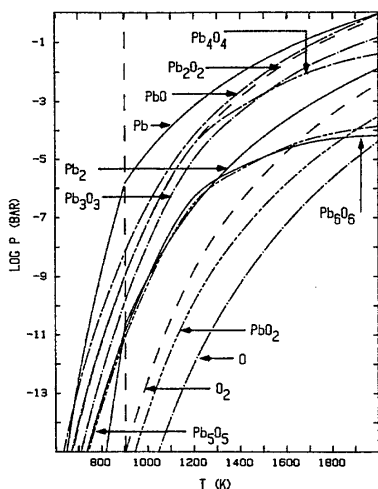


FIG. 53. PbO vaporization in 10^{-15} bar O_2 below 905 K and vaporization of Pb-PbO mixture above 905 K.

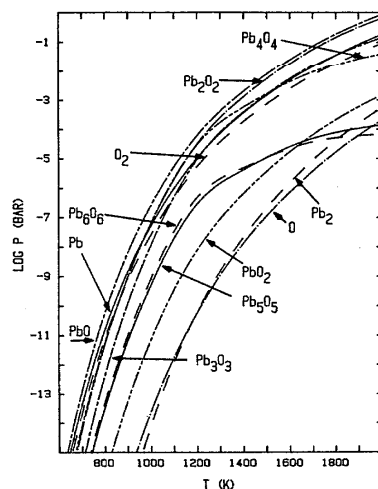


FIG. 54. PbO congruent vaporization.

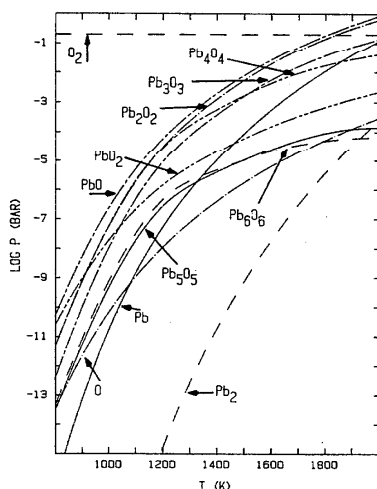


FIG. 55. PbO vaporization in 0.2 bar O_2 .

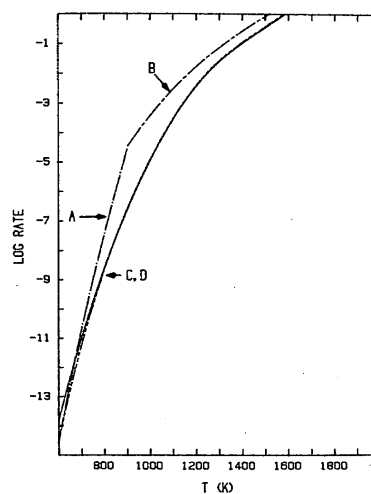


FIG. 56. PbO maximum vaporization rates. A— 10^{-15} bar O_2 ; B—Pb-PbO equilibrium; C—congruent vaporization; D—0.2 bar O_2 .

value seems somewhat large, calculations using the resulting thermodynamic properties are in excellent agreement with Drowart's gas phase equilibria over the temperature range of measurements. Equilibrium data are available for Pb_5O_5 and Pb_6O_6 at only one temperature, 1200 K. The entropy at 298 K for these two species was estimated by extrapolating the values for the monomeric through tetrameric species, and the estimated value $C_p^\circ/R = 3.0$ was used to calculate values of the Gibbs energy functions. The gas phase equilibria at 1200 K were then used to derive values of the enthalpies of formation.

o. Zn-O System

The stable solid phase is ZnO. Vaporization takes place predominantly by dissociation into gaseous Zn and O_2 , and a much smaller amount of $ZnO(g)$. Figures 57-60 show calculated partial pressures for vaporization of ZnO. The Gibbs energy function of gaseous ZnO was calculated using the estimated internuclear distance of Brewer and Rosenb-

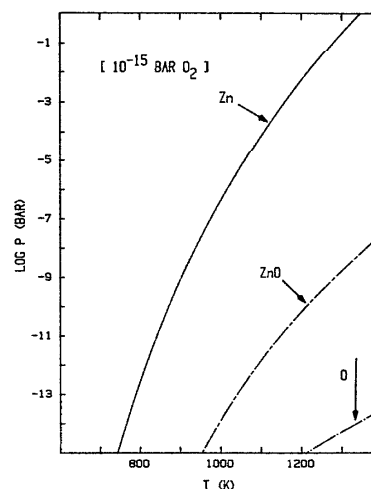


FIG. 57. ZnO vaporization in 10^{-15} bar O_2 .

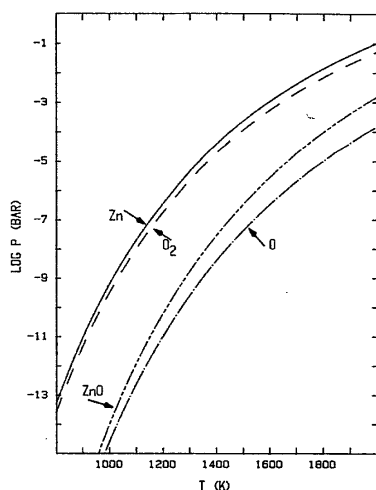
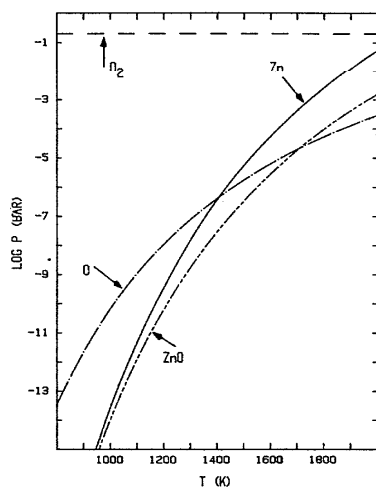
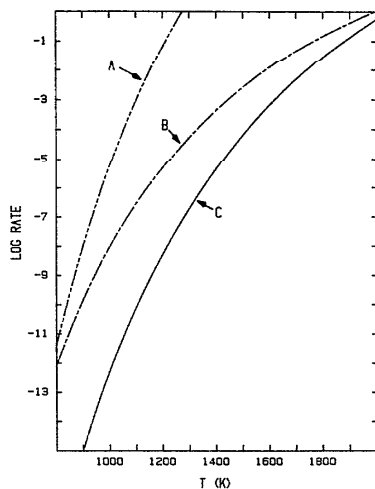
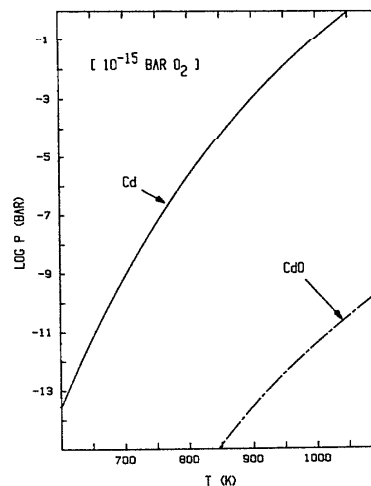


FIG. 58. ZnO congruent vaporization.

FIG. 59. ZnO vaporization in 0.2 bar O₂.FIG. 60. ZnO maximum vaporization rates. A— 10^{-15} bar O₂; B—congruent vaporization; C—0.2 bar O₂.FIG. 61. CdO vaporization in 10^{-15} bar O₂.

latt (1969) for the nondegenerate electronic ground state, $r(\text{Zn-O}) = 0.174$ nm and the value of the vibrational fundamental, 810 cm^{-1} , from the matrix-isolation study of Prochaska and Andrews (1980). The selected value of $\Delta_f H_{298}^\circ/R$ for $\text{ZnO}(\text{g})$, 10.9 ± 1 kK, was derived using the mass spectrometric relative intensity measurements of Grade *et al.* (1982) for the vaporization of $\text{ZnO}(\text{s})$, and is in reasonable accord with the selected value of Pedley and Marshall (1983), 13.1 ± 5 kK.

p. Cd-O System

The stable solid phase is CdO. Vaporization takes place predominantly by dissociation into gaseous Cd and O₂ and a much smaller amount of CdO(g). Figures 61–64 show calculated partial pressures for vaporization of CdO. The Gibbs energy function of CdO(g) was calculated using the estimated internuclear distance of Brewer and Rosenblatt (1969) for the nondegenerate electronic ground state, $r(\text{Cd-O}) = 0.185$ nm. The vibrational fundamental, 719 cm^{-1} , was taken from the matrix-isolation study of Prochaska and Andrews (1980). The selected value of $\Delta_f H_{298}^\circ/R$ for $\text{CdO}(\text{g})$, 15.6 ± 1 kK, was derived from the mass spectrometric relative intensity measurements of Grade and Hirschwald (1982) for the vaporization of $\text{CdO}(\text{s})$, and is in good accord with the selected value of Pedley and Marshall (1983), 15.1 ± 10 kK, and the lower limit found by Behrens and Mason (1981), 13.7 kK.

q. Hg-O System

The stable solid phase is HgO. Vaporization takes place primarily by dissociation into gaseous Hg and O₂ and a smaller amount of HgO(g). Figures 65–68 show calculated partial pressures for vaporization of HgO. The Gibbs energy function of HgO(g) was calculated using the estimated internuclear distance of Brewer and Rosenblatt (1969), 0.195 nm, for the nondegenerate electronic ground state and the vibrational fundamental, 676 cm^{-1} , of Butler *et al.* (1979) determined by matrix-isolation spectroscopy. The calculated values of $-(G_T^\circ - H_{298}^\circ)/RT$ are about 0.1 greater

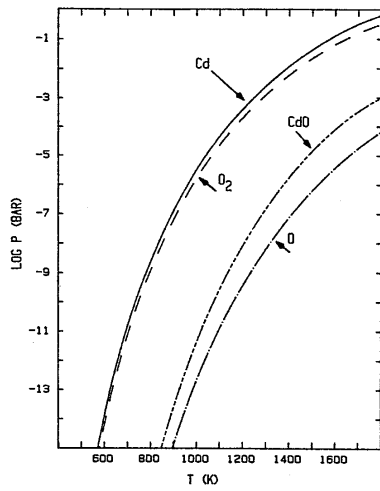


FIG. 62. CdO congruent vaporization.

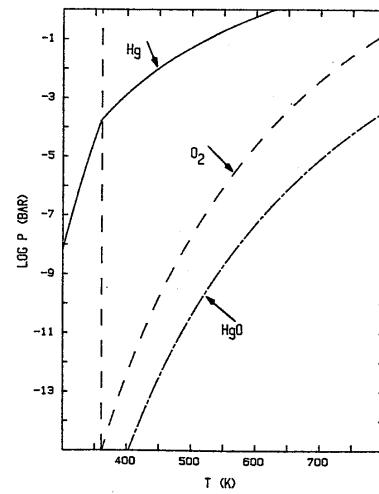
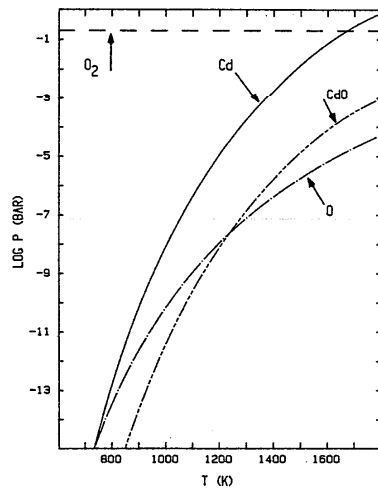
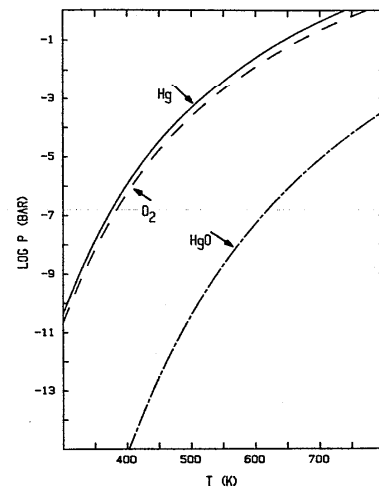
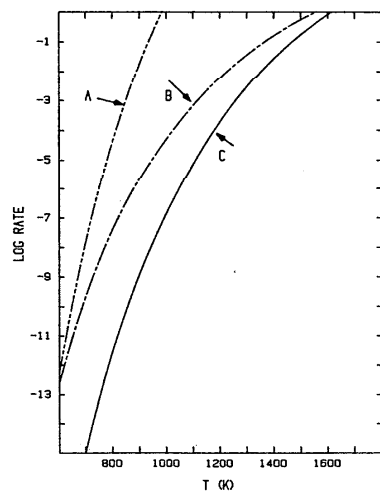
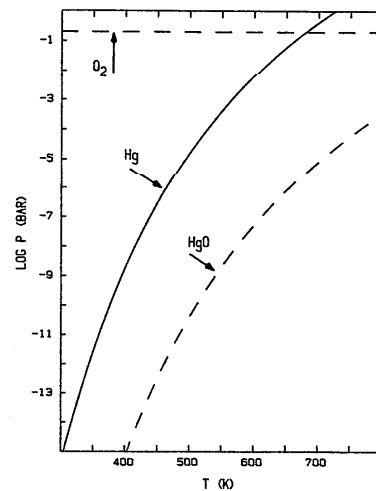
FIG. 65. HgO vaporization in 10^{-15} bar O_2 below 361 K and vaporization of Hg-HgO mixture above 361 K.FIG. 63. CdO vaporization in 0.2 bar O_2 .

FIG. 66. HgO congruent vaporization.

FIG. 64. CdO maximum vaporization rates. A— 10^{-15} bar O_2 ; B—congruent vaporization; C—0.2 bar O_2 .FIG. 67. HgO vaporization in 0.2 bar O_2 .

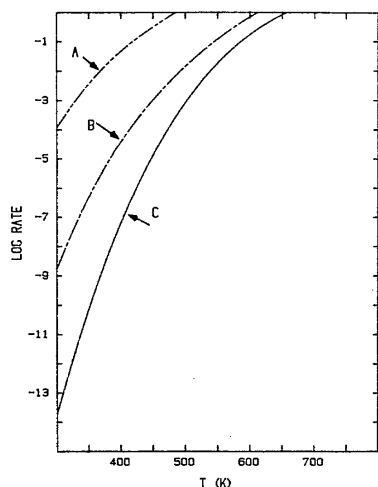


FIG. 68. HgO maximum vaporization rates. A— 10^{-15} bar O_2 ; B—congruent vaporization; C—0.2 bar O_2 .

than those of JANAF (Stull *et al.*, 1971) from 298 to 2000 K. The selected value of $\Delta_r H_{298}^\circ/R$ for HgO(g), 11.2 ± 1 kK, was derived from the mass spectrometric ion intensity ratio measurements of Grade and Hirschwald (1982). JANAF (Stull *et al.*, 1971), and Pankratz (1982) had selected the estimated value 5 ± 8 kK.

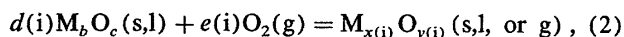
3. High-Temperature Equilibria and Reaction Rates

Calculations using the selected thermochemical data were discussed in the previous paper (Lamoreaux and Hildenbrand, 1984). The basic equations are presented here so that species partial pressures and maximum vaporization rates can be calculated for specific temperatures and oxidation conditions.

3.1. Mathematics of Vaporization Calculations

For many vaporization conditions one or two vapor species are predominant, and calculation of the chemical equilibrium from thermodynamic data is straightforward. Calculations can be more complicated when several species are present in significant quantities. The following procedure is a general method for calculating the equilibrium pressures of vapor species in equilibrium with a condensed phase of known composition.

The chemical species present at equilibrium in the vaporization of a condensed binary oxide can be described mathematically as being formed by linear combination of the vaporizing oxide $M_b O_c$ and oxygen O_2 according to the general reaction for the production of species i ,



where $e(i)$ may be zero, negative, or positive. Possible species include the vaporizing phase $M_b O_c$ (s or l), considered to be species 1, and O_2 (g) as well as the species produced by their linear combination. From mass balance,

$$d(i) = x(i)/b \quad (3)$$

and

$$e(i) = [by(i) - cx(i)]/2b. \quad (4)$$

We define the Gibbs energy of species i at temperature T as

$$G_T^\circ(i)/RT = (G_T^\circ - H_{298}^\circ)/RT + \Delta_r H_{298}^\circ(i)/RT. \quad (5)$$

The Gibbs energy change for the reaction producing species i from $M_b O_c$ (s or l) and O_2 (g), $\Delta_r G_T^\circ(i)$, is given by

$$\begin{aligned} \Delta_r G_T^\circ(i)/RT = & G_T^\circ(i)/RT - d(i) \\ & \times G_T^\circ[M_b O_c (s \text{ or } l)]/RT \\ & - e(i)G_T^\circ[O_2(g)]/RT, \end{aligned} \quad (6)$$

and the equilibrium constant for producing gas species i is

$$\begin{aligned} K(i) = & \exp[-\Delta_r G_T^\circ(i)/RT] \\ = & p(i)/\{a(1)^{d(i)}p[O_2(g)]^{e(i)}\}, \end{aligned} \quad (7)$$

where the pressures $p(i)$ are considered low enough that they are equal to fugacities, and $a(1)$ is the activity of $M_b O_c$. If $M_b O_c$ is a pure condensed phase, its activity is unity, and

$$p(i) = k(i)p(O_2)^{e(i)} \quad (8)$$

for the gas species. If the oxygen pressure is known, the pressure of each species i can be calculated from this equation.

For congruent vaporization, the vapor composition is the same as the condensed phase, and

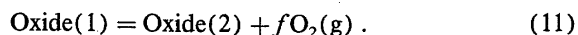
$$\frac{\sum [p(i)x(i)]}{\sum [p(i)y(i)]} = \frac{b}{c}. \quad (9)$$

This leads to the expression

$$\sum \{K(i)p(O_2)^{e(i)}[cx(i) - by(i)]\} = 0, \quad (10)$$

where summation is over the gaseous species present. In practice, this equation is solved for $p(O_2)$ by graphical interpolation or by numerical methods. The value found for $p(O_2)$ is then used in Eq. (8) to find the other partial pressures.

For the above calculations to correspond to equilibrium vaporization, they must be used for vaporization of the condensed oxide phases or phases stable under the particular vaporization conditions. Where more than one oxide phase is a possibility, the stable phase or phases must be determined. Two condensed oxide phases of fixed composition at a given temperature are related by the equilibrium



Oxide(1) is assumed to have the greater oxygen activity. The equilibrium constant for this reaction is

$$K_{eq} = a(2)p(O_2)^f/a(1). \quad (12)$$

If both condensed phases are at equilibrium, their activities are unity, and the pressure of O_2 is given by the equation

$$p_{eq}(O_2) = K_{eq}^{(1/f)}. \quad (13)$$

Oxide (1) is the stable phase for O_2 pressures greater than $p_{eq}(O_2)$, and oxide (2) is stable for O_2 pressures less than $p_{eq}(O_2)$ at the given temperature.

3.2. Vaporization Rate Calculations

Maximum vaporization rates are calculated using the Hertz-Knudsen equation of classical kinetic theory, which applies to free vaporization from an uncontaminated surface at low pressures. For gas species i evolving from the surface, the maximum vaporization rate $dn(i)/dt$ in $\text{mol cm}^{-2} \text{ s}^{-1}$ is

$$\frac{dn(i)}{dt} = \frac{p(i)}{[2\pi M(i)RT]^{1/2}}, \quad (14)$$

where $M(i)$ and $p(i)$ are the gram molecular weight and equilibrium partial pressure of vapor species i , and R and T are the molar gas constant and absolute temperature. Since 1 bar is 10^6 dyn cm^{-2} and R is $8.3144 \times 10^6 \text{ erg mol}^{-1} \text{ deg}^{-1}$, for pressures in bar, this is equivalent to

$$\frac{dn(i)}{dt} = 43.8 \left(\frac{p(i)}{[M(i)T]^{1/2}} \right) \text{ mol cm}^{-2} \text{ s}^{-1}. \quad (15)$$

Calculation of maximum vaporization rates is more difficult for incongruent than for congruent processes. In general, solid-phase activities during the vaporization process are not known, and calculated maximum vaporization rates of oxides that deviate from their original stoichiometry should be considered indicative rather than exact (Beruto *et al.*, 1981). In the present work, maximum vaporization rates have been calculated for incongruent, as well as congruent vaporization. Only initial vaporization rates, for which no condensed phase composition changes have taken place, are considered. Vaporization rates are expressed in terms of the mass of originally present oxide $M_b O_c$ lost as measured by the volatility of metal atoms. The total mass loss thus calculated is

$$\frac{dm}{dt} = 44.3 \left(\frac{M(M_b O_c)}{b} \right) \sum \left(\frac{p(i)x(i)}{[M(i)T]^{1/2}} \right), \quad (16)$$

where dm/dt is the mass loss rate in $\text{g cm}^{-2} \text{ s}^{-1}$, $M_b O_c$ is the formula of the condensed oxide, and $x(i)$ and $M(i)$ are the number of gram atoms of metal per mole and gram molecular weight of gas species i .

Although actual vaporization rates may be lower because of kinetic factors, the calculated maximum vaporization rate is useful as a rough guide to material loss rates. Recent references on maximum vaporization rates include works by Turkdogan (1980) and Beruto *et al.* (1981).

4. Acknowledgments

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 Glushko, V. P., Gurvich, L. V., Bergman, G. A., Veitz, I. V., Medvedev, V. A., Khachkuruzov, G. A., and Yungman, V. S. (1981). *Thermodynamic Data for Individual Substances* (Nauka, Moscow), Vol. 3: The elements B, Al, Ga, In, Tl, Be, Mg, Ca, Sr, and Ba and their compounds.
 Glushko, V. P., Gurvich, L. V., Bergman, G. A., Veitz, I. V., Medvedev, V. A., Khachkuruzov, G. A., and Yungman, V. S. (1983). *Thermodynamic Data for Individual Substances* (Nauka, Moscow), Vol. 4: The elements Cr, Mo, W, V, Nb, Ta, Ti, Zr, Hf, Sc, Y, La, Th, U, Pu, Li, Na, K, Rb, Cs, and their compounds.
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