
**South Coast
Air Quality Management District**

**SOx RECLAIM
WORKING GROUP MEETING**

April 3, 2008

Allocations

- Tier I Allocations (note)
- Tier II Shave Factor = 34.75%
- Tier II = $(1 - 0.3475) \times \text{Tier I}$
= $0.6525 \times \text{Tier I}$

Note: Unadjusted Tier I

Allocations & Emissions

FACILITY	ALLOCATIONS (TPD)**		EMISSIONS (TPD)	
	TIER I	TIER II	2002-03	2005
BP, CARSON	1.31	0.85	2.57	1.86
EXXONMOBIL	0.75	0.78	0.74	0.91
CONOCOP, WILM	1.19	0.45	1.38	1.15
CHEVRON	1.29	0.84	1.41	0.99
TESORO	0.69	0.20	1.02	1
ULTRAMAR	0.30	0.49	0.99	0.86
CONOCOP, CARSON	0.28	0.18	0.69	0.58
BP, WILMINGTON	1.28	0.84	0.41	0.36
CPC	0.33	0.22	0.15	0.28
RHODIA	1.71	1.12	0.78	1.13
OWENS-BROCKWAY	1.01	0.66	0.43	0.2
OTHERS	4.92	3.19	1.13	0.60
TOTAL	15.06*	9.81	11.70	9.92***

* Unadjusted, 41 facilities

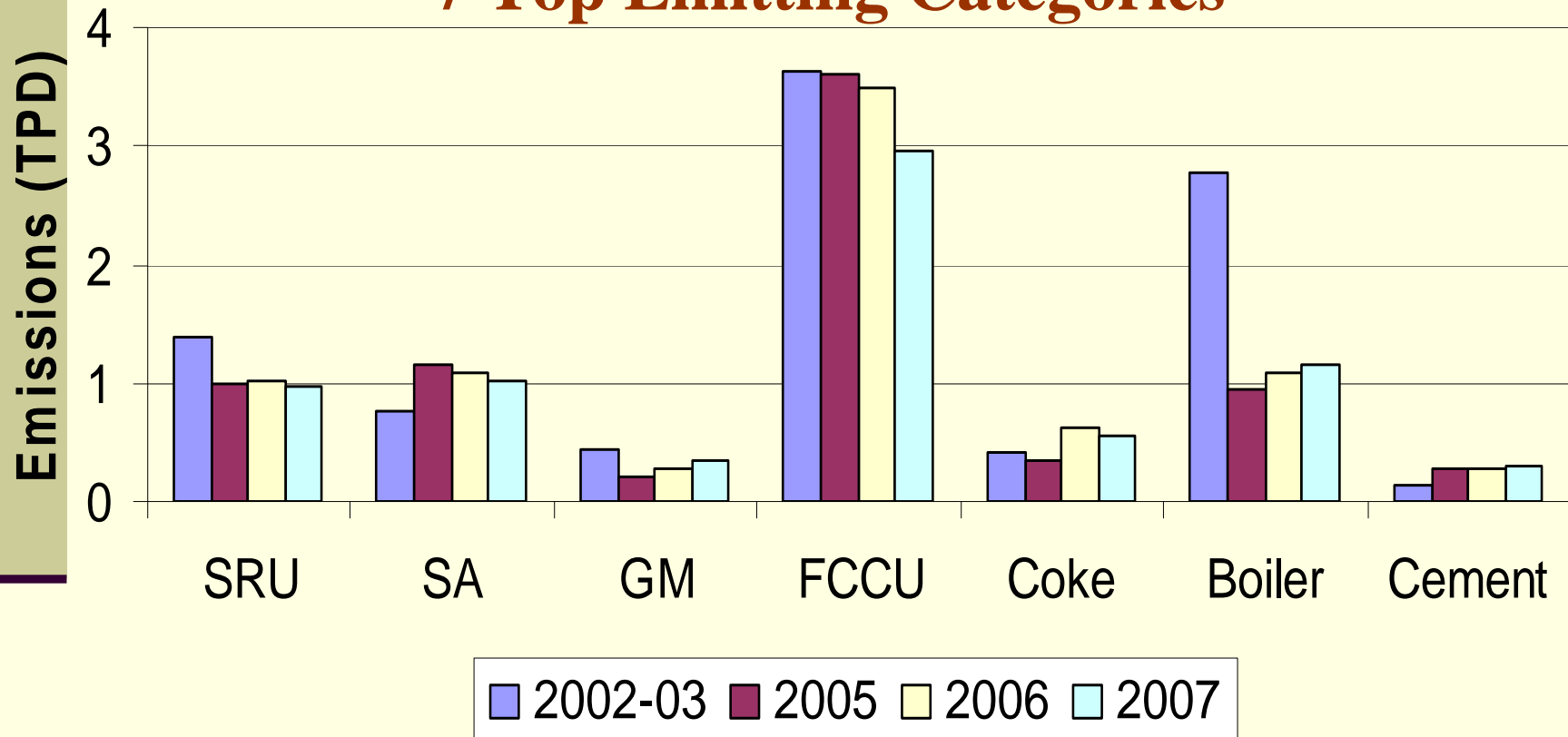
** Not Including Trades

*** 33 facilities

2002 – 2007 Emissions

11 Top Emitting Facilities

7 Top Emitting Categories



Total: 9.6 TPD (2002 with All Boilers/Heaters)

7.5 TPD (2005), 7.9 TPD (2006), 7.3 TPD(2007)

Survey Responses

FCCUs

- **Tier I Level: 13.7 Lbs/Mbarrels**
- 2005 Emission Rates
 - Refinery 1: 7 Lbs/Mbarrels
 - Refinery 2: 11 Lbs/Mbarrels
 - Refinery 3: 17 Lbs/Mbarrels
 - Refinery 4 & 5: 22 Lbs/Mbarrels
 - Refinery 6: 35 Lbs/Mbarrels
- **Current Average: 17.9 Lbs/Mbarrels**

Survey Responses

FCCUs

- SOx Concentrations (0% O₂)
 - Refinery E: 11 ppmv with GRACE DAVISON
 - Refinery D: 12 ppmv with Hydrotreating
 - Refinery A: 18 ppmv with INTERCAT
 - Refinery B: 36 ppmv with GRACE DAVISON
 - Refinery C: 55 ppmv with INTERCAT
 - Refinery F: 58 ppmv with INTERCAT or GRACE *

*Use SOx Reducing Catalysts When Needed. In 2007 Trials Achieved 70%-80% SOx Reduction, 15 ppmv – 23 ppmv SOx Concentrations

Survey Responses

FCCUs

■ Consent Decree Limits*

- 3 Refineries: 25 ppmv, By 2011
- 1 Refinery: 36 ppmv
- 1 Refinery: 50 ppmv

■ All Refineries Operate At Below Limits Required By Consent Decree

* Limits are 365-day averages. At one refinery, limit is for FCCU and waste heat boiler, including start-up, shut-down, malfunction

Survey Responses

FCCUs – SO_x Reducing Catalysts

- Pickup Factor = 4.0 – 7.5 Lbs SO_x Per Pound of Catalyst*
- Control Efficiency = 70% - 80%
- Emission Rate = ~ 20 Lbs/Mbarrels
- Costs: \$6 - \$8 Per Pound Catalyst
- CE = \$2,000 - \$3,500 Per Ton SO_x

* Based on reported data from 2 refineries

Survey Responses

FCCUs – Wet Scrubber/Wet ESP

- Wet Scrubber/Wet ESP for PM₁₀ & SO_x
- Estimated Impacts
 - SO_x Control Efficiency = 86%
 - Emission Reduction = 1.8 TPD SO_x
 - Emission Rate = 11 Lbs/Mbarrels
 - CE = \$4,200 Per Ton SO_x Reduced *

* Cost-Effectiveness Does Not Include PM₁₀ Reduction Benefits and Annual Operating Costs

BARCT Top Down Analysis

FCCUs

- **Best Performance of Individual Control?**
- **Combination of Control?**
- **Cost-Effectiveness?**
- **Goal: ≤ 7 lbs/Mbarrels or ≤ 10 ppmv?**
- **Potential Emission Reduction = 2 TPD*?**

* Calculated from 2005 baseline assuming all 6 refineries will meet an average emission rate of 7 lbs/Mbarrels

Survey Responses

SRUs – Tail Gas Treatment

- **Tier I Level = 1.61 TPD (1988 – 1992)**
- **2005 Emissions = 0.96 TPD**
- Operating at 60% - 87% Design Capacity
- Two to Four Trains of SRUs (Claus)
- Tail Gas Treatment Units
 - SCOT, WELLMAN–LORD, FLEXSORB
- Thermal Oxidizers

Survey Responses

SRUs – Tail Gas Treatment

- SCOT: 96% - 99.5% Sulfur Recovery
 - 3 ppmv - 10 ppmv from Tail Gas Treatment System
 - 20 ppmv - 150 ppmv SO_x from Thermal Oxidizer
- **WELLMAN–LORD: 99.9% – 99.99%**
 - 59 ppmv – 77 ppmv SO_x from Thermal Oxidizer
- **FLEXSORB: 99.9%**
 - 16 ppmv – 20 ppmv SO_x from Thermal Oxidizer

BARCT Top Down Analysis

SRUs – Tail Gas Treatment

- Wet Gas Scrubbers: 99.99% and Below 1 ppmv SO_x at Other Refineries
- **Goal: 99.9% Sulfur Recovery (or 3ppmv Outlet from Tail Gas Treatment System, or 10 ppmv SO_x Outlet from Thermal Oxidizer)?**
- **Cost-Effective?**
- **Potential Emission Reduction = 0.3 TPD*?**

*Calculated from 2005 Baseline and 99.9% Sulfur Recovery Efficiency

Survey Responses

Boilers/Heaters

- **Tier I Allocation = 0.89 TPD (All Units)**
- **Tier II Allocation = 0.58 TPD (All Units)**
- **Current Emissions**
 - **3 TPD (All Units)**
 - Top 15 Emitters: Crude Heaters, Delayed Coking Unit Heaters, Steam Generation Boilers
 - **1 TPD for Top 15 Emitters**

Survey Responses

Boilers/Heaters

- Current System - Fuel Gas Treatment
 - Amine for H₂S Removal At All Refineries
 - Merox for Carbonyl Sulfides, Mercaptan At Some Refineries
 - Not All Fuel Gas Treated Prior to Combustion
 - Fuel Sulfur Content = 23 ppmv – 450 ppmv+
 - SO_x = 3 ppmv – 45 ppmv (Measured or Calculated from Fuel Sulfur Content)

Survey Responses

Boilers/Heaters

- Example - Performance at One Refinery
 - Amine and Merox Treatment
 - Fuel Sulfur Content: 47 ppmv Average
 - SOx: Avg 6.5 ppmv, Max 25 ppmv (3% O₂)

BARCT Top Down Analysis

Boilers/Heaters

- **Goal:**
 - **Upgrading Fuel Gas Treatment System?**
 - **Wet Scrubber for Top Emitters?**
 - **25 ppmv Total Sulfur Measured As H₂S**
 - **<5 ppmv Outlet SO_x Concentration?**
- **Cost-Effective?**
- **Potential Emission Reduction =
0.46 TPD* - 2.42 TPD****

* 50% Reduction for Top 15 Emitters

** 80% Reduction for All Units To Be At Tier II Allocations

Survey Responses

Sulfuric Acid Manufacturing

- **Tier I Level: 4.00 – 9.48 Lbs/Ton Acid**
- Current Emission Rates
 - **Facility 1: 0.22 – 0.36 Lbs/Ton Acid**
 - Facility 2: 1.58 – 1.84 Lbs/Ton Acid
- Current SO_x Concentrations
 - Facility 1: 26 ppmv
 - Facility 2: 145 ppmv

Survey Responses

Sulfuric Acid Manufacturing

- Current Control Technology
 - **Facility 1: Wet Regenerative Scrubber**
 - Facility 2: Double Absorption
- Consent Decree Limits
 - **Facility 3: 0.2 Lbs/Ton Acid**
 - Facility 2: 1.7 Lbs/Ton Acid

BARCT Top Down Analysis

Sulfuric Acid Manufacturing

- Can Double Absorption Meet 0.2 Lbs/Ton?
- Is Wet Scrubber Cost-Effective?
- **Goal: 0.2 – 0.3 Lbs/Ton?**
- **Potential Emission Reduction = 1 TPD*?**

* Calculated from 2005 baseline assuming Facility 2 will meet an emission rate of 0.3 lbs/ton acid

Survey Responses

Container Glass

- **Tier I Level: 2.1 – 3.2 Lbs/Ton Glass**
- Current Performance
 - Two Glass Furnaces Venting To Two Dry Scrubbers and Three ESPs
 - One Scrubber At 80% Control
 - SOx: 73 ppmv Average, 445 ppmv Maximum
 - **Emission Rate: 0.63 – 1.05 Lbs/Ton**

BARCT Top Down Analysis

Container Glass

- SJVAPCD Proposed Rule: 0.8 Lbs/Ton
- **Wet Scrubber (Tri-Mer): 0.1 Lbs/Ton, 99.9% Control Efficiency**
- **Goal: <0.6 Lbs/Ton?**
- **Is Wet Scrubber Cost-Effective?**
- **Potential Emission Reduction = 0.29 TPD*?**

* Based on 2005 Emissions Reduced From 0.6 Lbs/Ton To 0.1 Lbs/Ton

Survey Responses

Coke Calciner

- **Tier I Level: 2.47 Lbs/Ton**
- **Dry Scrubber** Design Parameters
 - 1,296 TPD Green Coke
 - Emission Rates: **0.21 Lbs/Ton** – 1.64 Lbs/Ton
 - 90% Control Efficiency
- Current Emission Rates
 - **0.56 Lbs/Ton (2005)**
 - 0.97 Lbs/Ton (2006)
 - 0.89 Lbs/Ton (2007)

Survey Responses

Coke Calciner

- Current SO_x Outlet Concentration
 - 27 ppmv (2005)
 - 52 ppmv (2006)
 - 43 ppmv (2007)
 - 82 ppmv - 84 ppmv (RATA)
- Current Control Efficiency: 98% - 99%

BARCT Top Down Analysis

Coke Calciner

- **Wet Scrubber/Wet ESP** Design Levels at BP Cherry Point Refiner
 - 1,301 TPD Green Coke
 - 96% Control Efficiency
 - **35 ppmv Limit (Tested: 10 ppmv – 12ppmv)**
 - **0.14 Lbs/Ton**

BARCT Top Down Analysis

Coke Calciner

- **Goal: 0.14 – 0.2 Lbs/Ton?**
- **Is Wet Scrubber Cost-Effective?**
- **Potential Emi Red = 0.23 – 0.26 TPD*?**

* Based on 2005 Emissions and 0.14 Lbs/Ton – 0.2 Lbs/Ton

Survey Responses

Cement Kilns & Coal-Fired Boiler

- **Tier I Allocations: 0.33 TPD (0.30 TPD for Coal-Fired Boiler Not In Operation)**
- **2005 Emissions: 0.27 TPD (2 Kilns)**
- **Current Performance**
 - Cement Kiln = 0.5 Lbs/Ton Clinker
 - Coal-Fired Boiler = 7 Lbs/Ton Coal
- **SO_x Concentration = 49 ppmv**

BARCT Top Down Analysis

Cement Kilns & Coal Fired Boiler

- **Goal: Wet Scrubber at 99% Control?**
- **Is Wet Scrubber Cost-Effective?**
- **Potential Emission Reductions?**

Survey Responses

Other Industry Suggestions

- Team Effort - WSPA & AQMD
- Consultants to Conduct Research

A&WMA Conference

- **May 14, 2008**
- U.S. EPA, CARB, SCAQMD
- INTERCAT & GRACE DAVISON
- BELCO, CANSOLV, DYNAWAVE, TRI-MER
- Hydrotreating?
- Fuel Gas Treating System?

Tentative Schedule

- Next Working Group Meeting
- Public Workshop & CEQA Scoping: May-June
- Public Hearing: October - December