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ANNUAL REPORT

NO. 2

DEVELOPMENT OF
IMPROVED BLOWOUT PREVENTION PROCEDURES
TO BE USED IN DEEP WATER DRILLING OPERATIONS

Submitted To

THE UNITED STATES GEOLOGICAL SURVEY

Department of the Interior

Reston, Virginia



PETROLEUM ENGINEERING DEPARTMENT

Louisiana State University

Baton Rouge, Louisiana 70803

February 15, 1981

ANNUAL SUMMARY REPORT

August, 1979 - July, 1980

Development of Improved Blowout Prevention
Procedures for Deep Water Drilling Operations

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The United States Geological Survey

The Department of Interior

Reston, Virginia

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February 15, 1981

RESEARCH OBJECTIVES

The primary objective of this research program is the development of improved blowout prevention procedures to be used in deep water floating drilling operations. The overall research plan was divided into eight tasks which will take approximately four years for completion at a total cost to the USGS of \$822,962. These tasks are as follows:

1. Design of a research well facility for accurately modeling blowout control operations on a floating drilling vessel in deep water.
2. Construction of research well facility.
3. Documentation of blowout control equipment configuration and procedures currently used on deep water floating drilling vessels.
4. Experimental study of shut-in procedures for blowout control on deep water floating drilling vessels.
5. Experimental study of procedures for handling upward gas migration during the shut-in period.
6. Experimental study of pump start-up procedures.
7. Experimental study of pump out procedures with emphasis on problems occurring when a gas kick reaches the seafloor.
8. Development of a mathematical model of well behavior during the control of gas kicks on floating drilling vessels.

It should be pointed out that this research project is being jointly sponsored by industry, and the total cost of the project is approximately two million dollars. At the end of this reporting period, the second year on this project has been completed with USGS funding to date totaling \$197,096.00 for Tasks 1, 3, and 5 and a portion of Task 4.

This report is intended to be a concise and credible discussion of our technical progress, findings, and accomplishments by task.

Task 1 - Research Well Facility Design

Significant modifications in blowout prevention equipment and procedures are required for floating drilling vessels used in deep water drilling operations. The current trend of the oil industry to much greater water depths (shown in Figure 1) emphasizes the importance of working towards improvements in blowout control equipment and procedures for these vessels. Future plans by the National Science Foundation call for scientific ocean drilling in up to 13,000 ft of water during the next decade. The NSF Ocean Margin Drilling Program will be a joint venture between government and industry.

As part of the USGS-sponsored research at LSU, a new research well facility has been designed to allow improved blowout prevention procedures to be experimentally investigated under simulated threatened blowout conditions in an actual well. Construction of the new facility is being accomplished under the dual support of industry and the USGS. Task 1, the design of the new research well facility, has been completed. The location of the new well facility is the site of the Goldking LSU No. 1 well on the southwestern edge of the LSU Campus, as shown in Figure 2. A scale model of the facility has been constructed and is shown in Figure 3.

Details of the completed design are given in Appendix A. The heart of the new facility will be an actual well for modeling well control operations in deep water. Shown in Appendix A as Figure A-1 is the well design which will be used. A water depth of approximately 3000 ft will

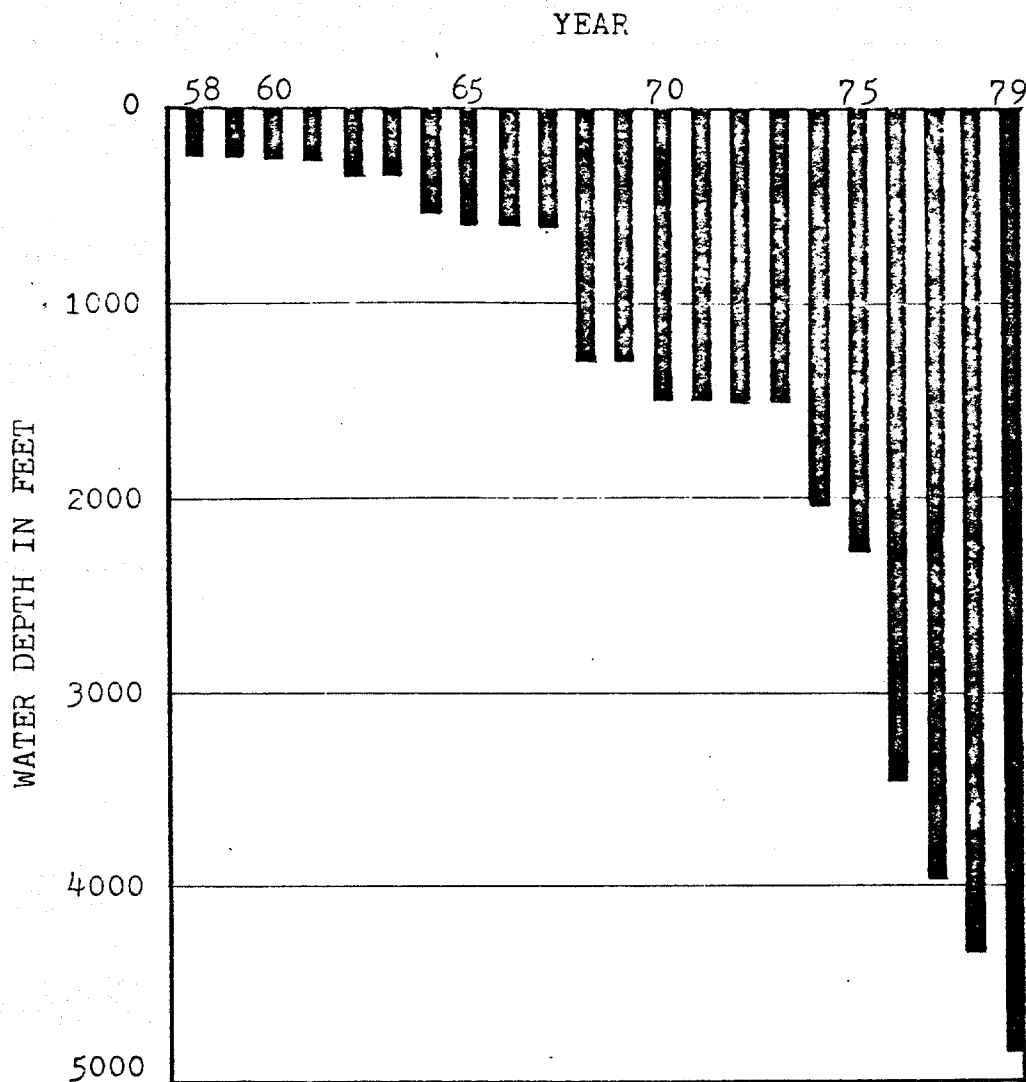


Figure 1 - History of Water Depth Record for Floating Drilling Vessels

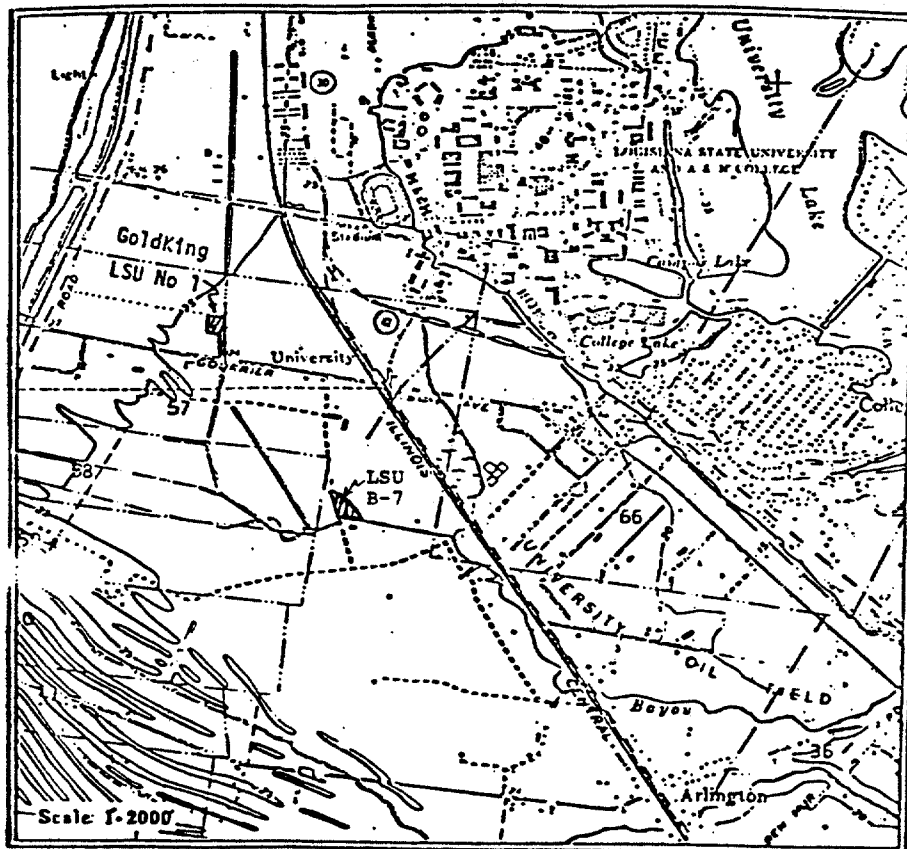


Figure 2 - Location of Research Well Facility

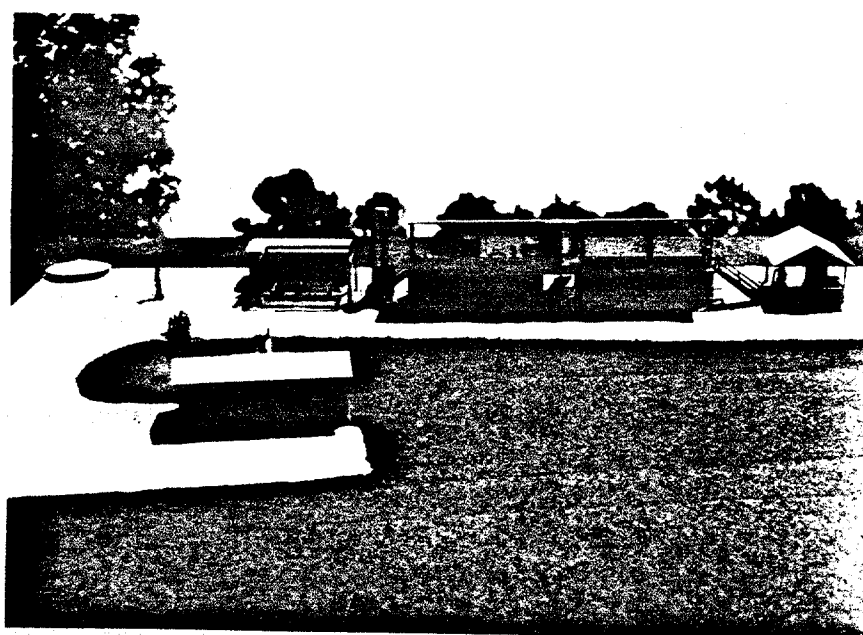


Figure 3 - Scale Model of New Research
Well Facility

be simulated using a Baker packet and triple parallel flow tube placed in the well at this depth. A total well depth of 6000 ft has been chosen. The lengths and sizes of the well tubulars were selected after extensive computer simulations of both actual and model well behaviors under various assumed kick conditions. The new well facility should allow a range of pressure behaviors under simulated well control conditions which are very similar to the behavior of an offshore well being drilled by a floating drilling vessel.

A detailed schematic of the surface and subsurface piping of the new facility is shown in Figure A-2. This arrangement will allow the realistic duplication of pressure control operations using the most modern well control equipment available. The piping will also allow several flow options not normally available on a drilling rig in order to allow the collection of experimental data needed to define more precisely the operating characteristics of several of the drilling chokes used. The piping arrangement will also allow several innovative pressure control procedures to be tested.

The most complex portion of the surface pressure control piping used on drilling rigs is the choke manifold, which contains the high pressure, remote operated, adjustable chokes. The Choke Manifold design is documented in Figures A-3 and A-4. The manifold being used will be one of the largest in the world and will allow several flow options not usually available in current practice.

Considerable surface pit volume will be required to simulate the pressure control operations and conduct the experimental research program. The plans for two 300 bbl mud tanks are shown in Figure A-5. The surface layout plan showing the physical arrangement of the mud

tanks, choke manifold, and associated pumps, mud gas separators, and degassers are shown in Figure A-6. A site plan showing the placement of the access road, shell mats, and concrete equipment foundations is shown in Figure A-7. The site electrical plans are shown in Figure A-8. Plans for the control house foundations and metal shell are shown in Figure A-9.

Task 3 - Documentation of Current Practice

There exist considerable differences among the various well operators as to the best equipment configuration and pressure control procedures which should be used on floating drilling vessels in deep water. As a first step in the development of improved blowout prevention procedures, a study documenting the existing equipment and procedures currently in use has been initiated. This study is being documented by Mr. Bob Surcouf in an M.S. Thesis entitled, "An Examination of Blowout Prevention Equipment and Procedures Used on Floating Drilling Vessels." The topical outline he has constructed is as follows:

1. Introduction
2. Description of Available Well Control Equipment
 - (a) Subsea Blowout Preventer Stacks
 - (b) Blowout Preventer Control Systems
 - (c) Marine Risers
 - (d) Diverter Systems
 - (e) Choke and Kill Manifolds
 - (f) Drilling Chokes
 - (g) API Recommended Equipment Configurations
 - (h) Government Regulations

3. Survey of Deep Water Drilling Vessels
 - (a) Deep Water Rig Availability
 - (b) Survey Sample
 - (c) Survey Results
 - (d) Typical Piping Diagrams
4. Current Well Control Procedures
 - (a) Government Regulations
 - (b) Approved Well Control Manuals for Subsea BOP Stacks
 - (c) Well Shut-in Procedures
 - (d) Pump Start-up Procedures
 - (e) Pump Out Procedures
5. Theoretical Limitations of Well Control Operations
 - (a) Computed Deep Water Fracture Gradients
 - (b) Computed Diverter System Capacities
 - (c) Computed Choke Pressure Requirements
6. Conclusions and Recommendations

In this study, equipment currently being manufactured was first cataloged. A survey of deep water rigs was then conducted to identify how the available equipment was being configured in actual practice. A number of drillships and semi-submersible rigs were visited in conjunction with this study. Next, all USGS approved subsea well control manuals were surveyed in order to catalog the various recommended procedures for use of the existing equipment. Finally, some limitations of existing equipment and procedures were explored through mathematical analysis and computer simulations. Documentation of the results of this study is still in progress.

Photographs taken during one of Mr. Surcouf's offshore visits are shown in Figures 4 and 5. Example well control piping diagrams for a typical diverter system used for drilling the shallow portion of a well and the blowout preventer system used for drilling the deeper portion of a well are shown in Figures 6 and 7.

For the past two years, the record water depth for floating drilling has been advanced by the Discoverer Seven Seas Drillship. In 1978 a well was drilled by this vessel off the African coast in 4342 ft of water, and in 1979 a well was drilled offshore Newfoundland in 4876 ft of water. Special emphasis was placed in this study on these two wells. Well data obtained from the well operators was obtained to allow computer simulations of pressure control operations for various assumed kick conditions. Shown in Figure 8 is a photograph of the Discoverer Seven Seas, and shown in Figure 9 are the results of computer simulations of pressure control operations computed for this vessel using well data from the 1979 record water depth well drilled off the African coast. The results of computer simulations of this type proved very valuable in designing the new research well facility.

Task 4 - Improved Shut-In Procedures

Task 4 is not scheduled for completion until after construction of the new research well facility. However, work which could be done using existing facilities has been initiated. This initial work includes the following subtasks:

- 4a. An experimental determination of frictional area coefficients for modern drilling chokes used in pressure control operations.
- 4b. An experimental determination of frictional area coefficients of a modern annular blowout preventer during closure.

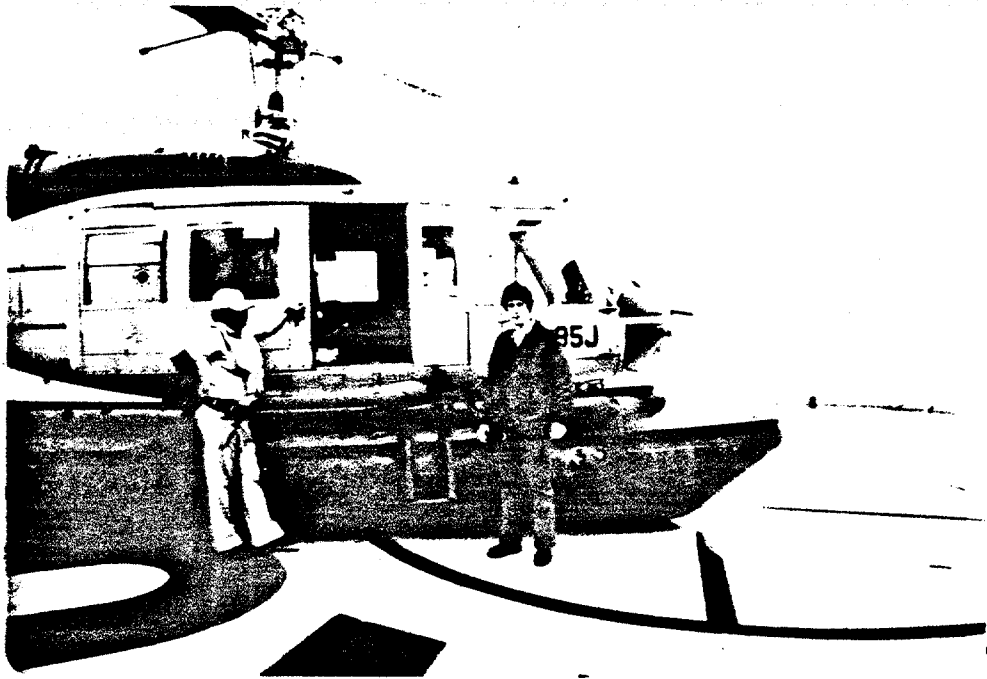


Figure 4

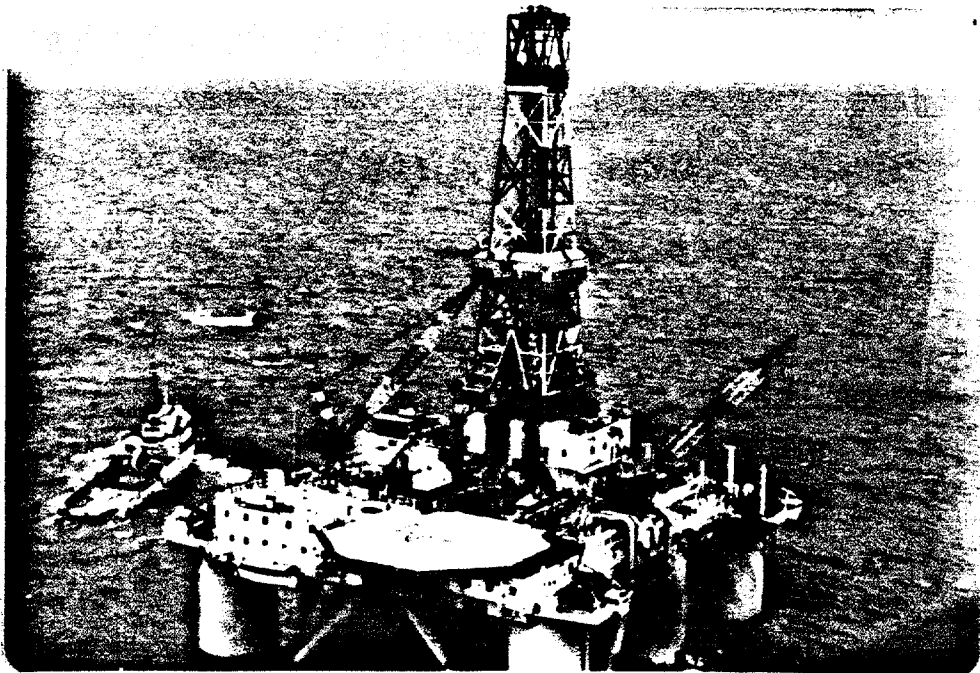


Figure 5

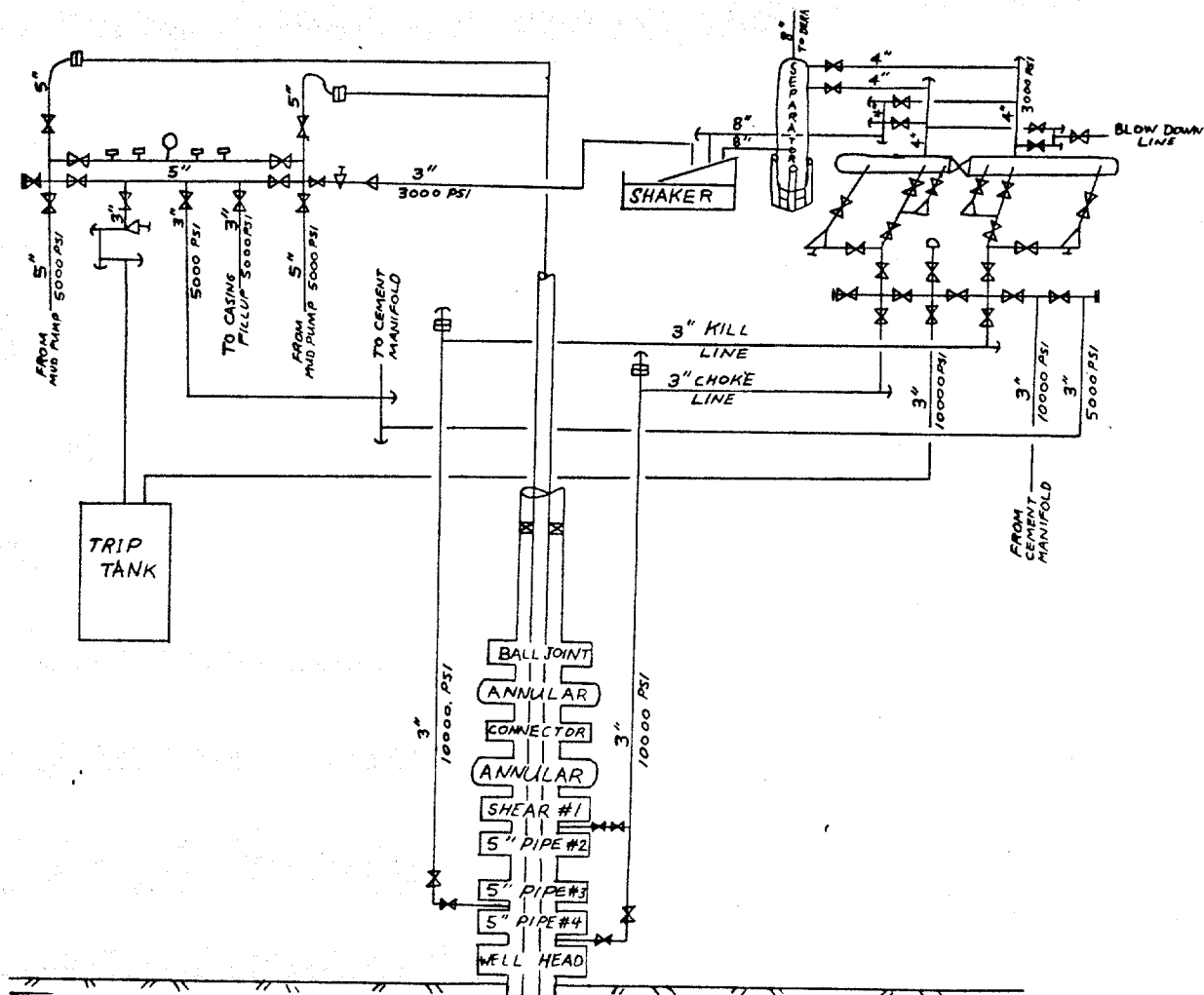


Figure 7 - Typical Well Control System

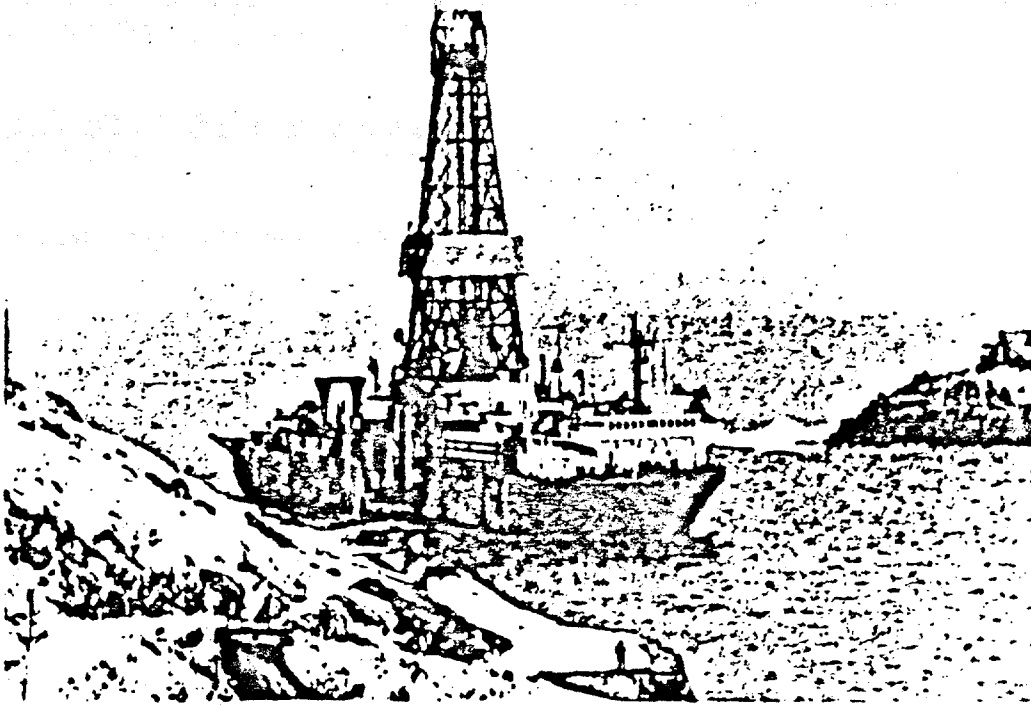


Figure 8 - Discoverer Seven Seas Drillship

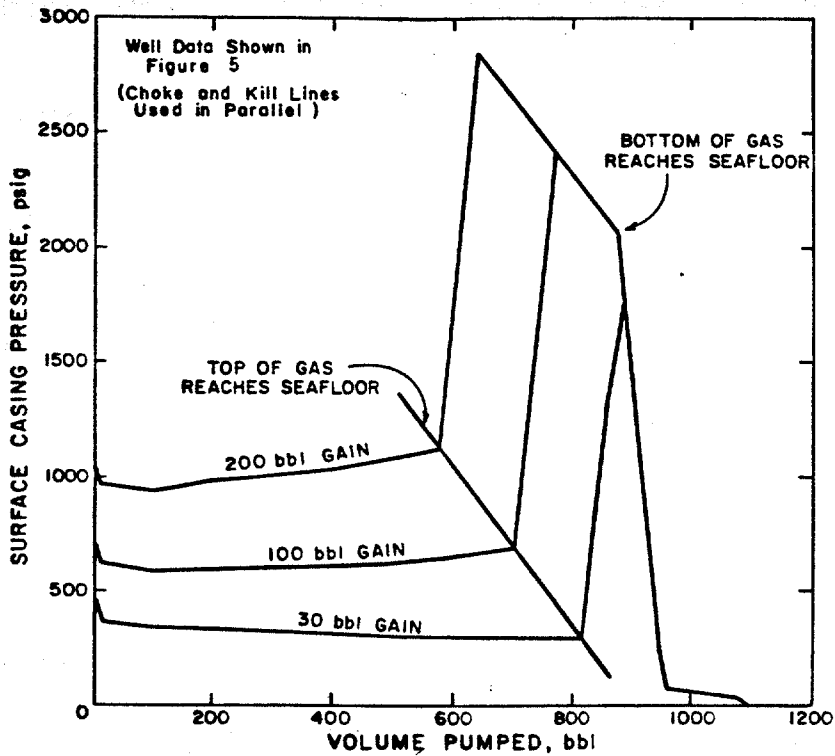


Figure 9 - Pressure Control Simulation Results for
Well Drilled by Discoverer Seven Seas

Subtask 4a is being accomplished by Mr. Kerry Redmann and Subtask 4b is being accomplished by Mr. Scott Doyle. These two individuals are performing these tasks as part of their M.S. thesis research.

One goal of this research is the development of much improved algorithms for predicting the response of a well to actions taken by the rig crew during pressure control operations. It is hoped that the frictional area coefficient data collected on each of the commercially available drilling chokes will lead to greatly improved algorithms for computing the changes in well pressures and flow rates with time associated with incremental changes in choke position by the choke operator. The incorporation of more realistic choke response algorithms in pressure control simulation programs is needed to allow a more valid comparison of alternative well control procedures. Similarly, it is hoped that the frictional area coefficient data collected on an annular blowout preventer will lead to more accurate algorithms for predicting initial pressure surges during well closure and ultimately to improved shut-in procedures.

A schematic of the experimental flow loop used for Subtask 4a is shown in Figure 10. Drilling fluid having the desired rheological characteristics is first mixed in the available pits. By opening a bypass valve (6) and closing the normal drill pipe valve (7), drilling fluid could be circulated from one pit directly through any of the available chokes (1), (2), (3), or (4) and returned to a second pit. Flow rates were computed both from the recorded stroke rate of the positive displacement triplex pump and from the observed change in pit level. For some of the runs, a magnetic flow meter had been installed in return line (10), providing a third check on the measured flow rates.

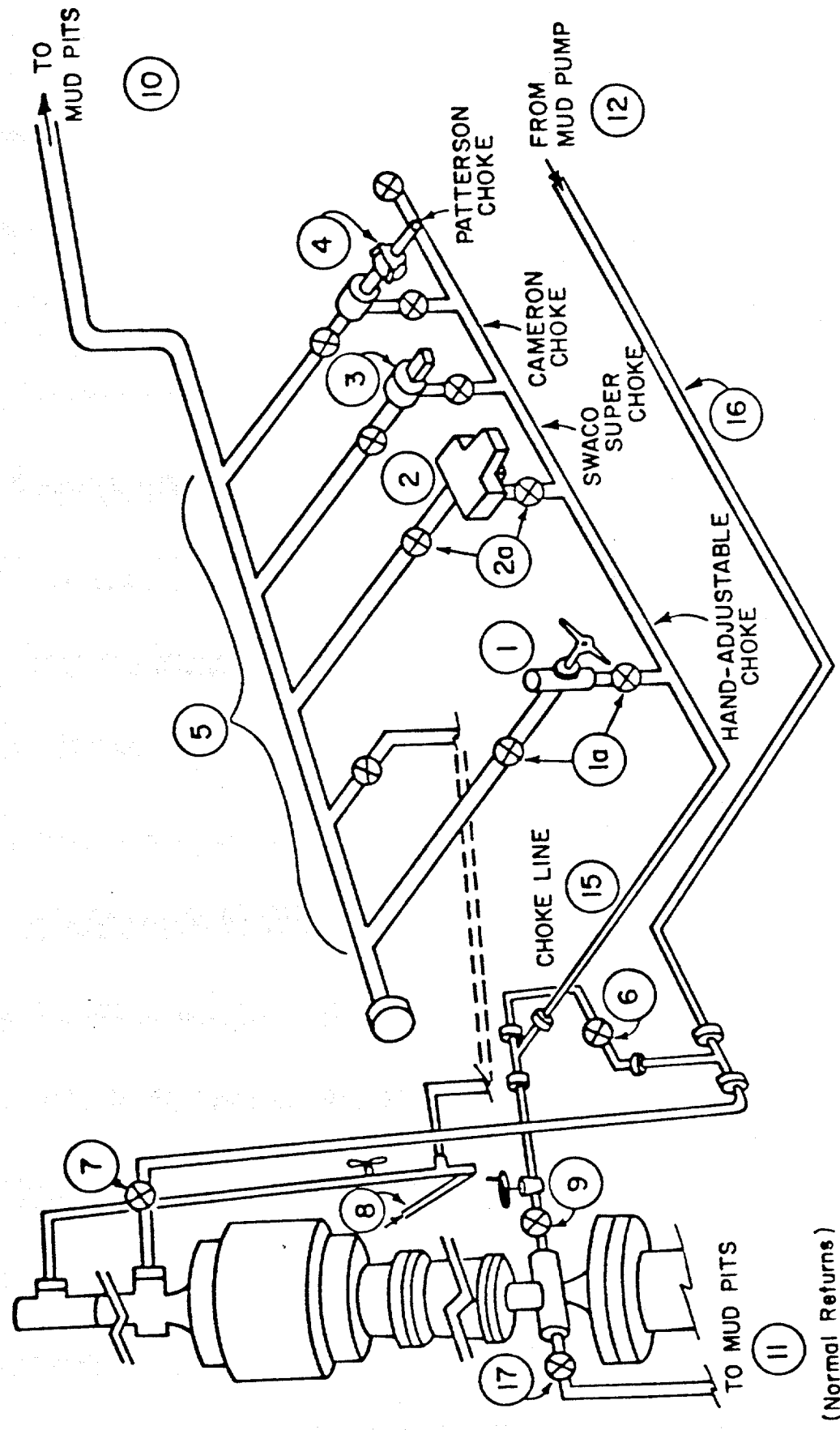


Figure 10 - Surface Layout of LSU Training Well

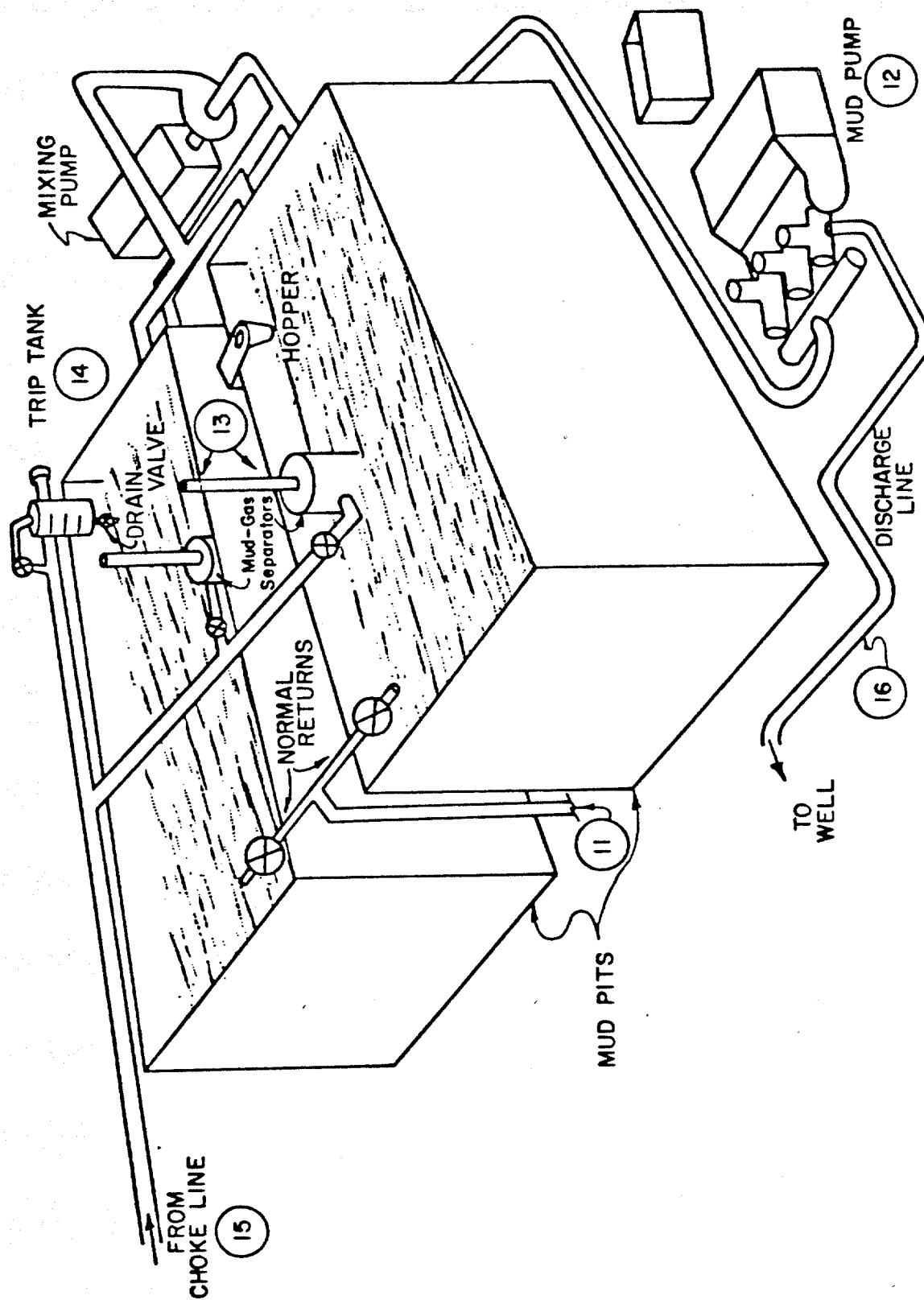


Figure 10 - Continued

Pressures upstream of the chokes were monitored using a recording pressure gauge, and pressures downstream of the choke were essentially atmospheric.

Example drilling choke data obtained on the cameron hand-adjustable drilling choke, cameron remote-adjustable drilling choke, swaco high-pressure drilling choke, and Patterson drilling choke are shown in Appendix B. Drilling fluid properties used in these tests are also given in this appendix. Documentaion of the results of Subtask 4a is now underway by Mr. Kerry Redmann in an M.S. thesis entitled, "Flow Characteristics of Adjustable Drilling Chokes Used in Well Control Operations."

A schematic of the experimental flow loop used for Subtask 4b is shown in Figure 11. Flow could be directed through the annular preventer in the same manner as previously described for the drilling choke flow loop used for Subtask 4a, and the same equipment was used to monitor the pressures and flow rates. The flow characteristics of the annular blowout preventer are being determined at various stages of blowout preventer closure. These data should greatly assist us in developing improved algorithms for determining inertial pressure surges during well closure. Example data obtained using this apparatus are shown in Appendix C.

Task 5 - Improved Procedures for Handling Gas Migration

After a well has been shut-in due to the flow of a gas kick into the wellbore, there may be a considerable lapse of time until conventional well control procedures can be implemented. This time lapse can be due to mechanical difficulties or to weighting up the mud to the

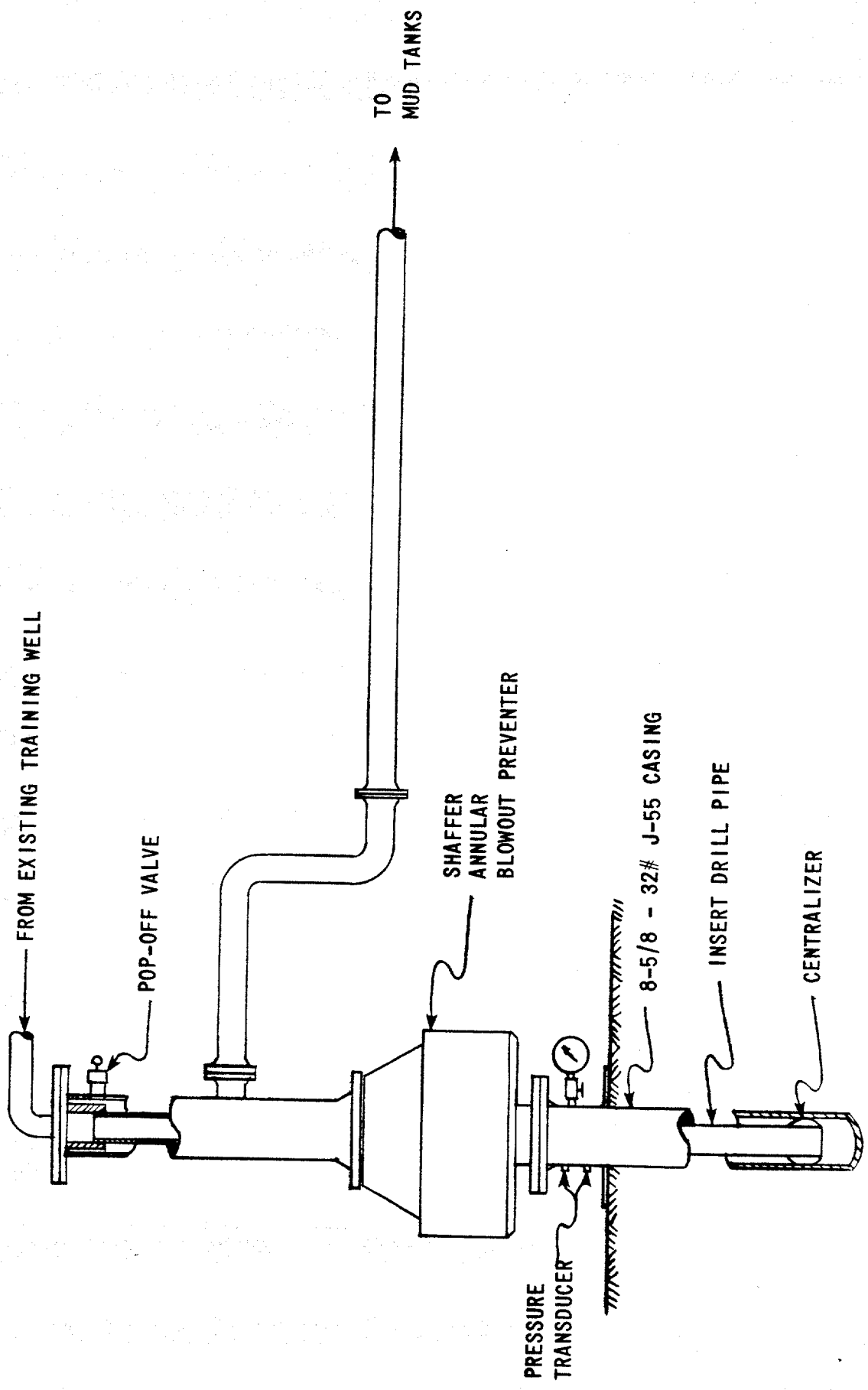


Figure 11 - Experimental Apparatus for Measuring Flow Characteristics of Annular Preventer During Shut-In

required kill value. During this time, upward migration of the gas occurs due to the large density difference between the mud and the gas. As this gas rises on the shut-in well, wellbore pressures continuously increase until 1) pressure is bled off at the surface, or 2) formation fracture and the resulting underground blowout occurs at the weakest zone in the open hole, usually at the casing seat.

The basic problem, as earlier stated, is that gas rising in the shut-in well can cause excessive wellbore pressures. Refer to the real gas equation of state,

$$PV = ZnRT \quad (1)$$

where

P = pressure, psia

V = volume, ft³

Z = gas compressibility factor

n = number of lb-moles of gas

R = 10.732 psia-ft³/lb-mole-°R

T = temperature, degrees Rankine

Since the well remains shut-in, the gas volume and number of moles remains constant, assuming an incompressible system. Since the value for Z does not change very much over relatively large pressure and temperature variations, and assuming constant temperature of the gas, the result is that the pressure of the gas remains essentially constant at the initial shut-in bottomhole pressure as it rises upward.

Figure 12 illustrates the detrimental aspects of maintaining the well shut-in during this period. At initial shut-in conditions, the gas (bottomhole) pressure is 5220 psig. The fracture gradient at the

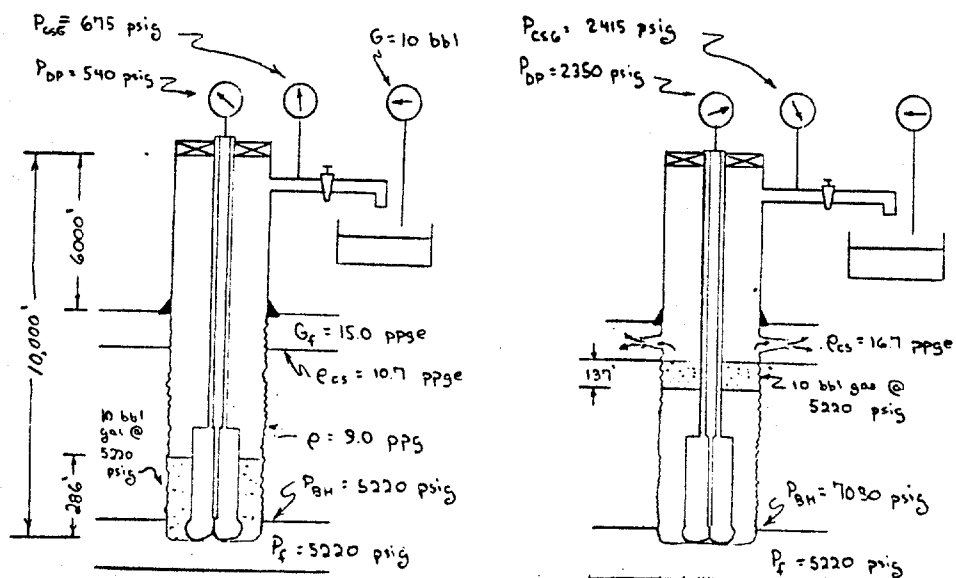


Figure 12 - Problem of Upward Gas Migration
in a Shut-In Well

casing shoe was established at 15 ppg, and at initial conditions it has not been exceeded, since the equivalent shut-in density at the shoe is 10.7 ppg. However, at a later time the gas has migrated to the casing shoe with a 16.7 ppg resulting equivalent density at the shoe. This is in excess of the formation strength, and fracturing of the formation and an underground blowout will occur. It can also be seen that the bottom-hole pressure has increased to over 7000 psig. This is for in excess of the pressure required to maintain well control. Also, the surface drillpipe and annular pressures have also increased, signifying that the gas is migrating upwards.

The usual procedure for handling upward gas migration prior to normal well control operations is to maintain a constant drillpipe pressure, slightly greater than the initial shut-in value. This procedure maintains the bottomhole pressure at a value slightly greater than the formation pore pressure, since a continuous column of mud lies between the surface and the formation.

To maintain a constant, drillpipe pressure mud is bled periodically through a surface choke to allow the migrating gas to expand and subsequently reduce its pressure.

However, situations can arise when a meaningful drillpipe pressure is not available. In one case, the bit could be plugged, preventing pressure communication between the drill string and formation. In another instance, the drill string could be off-bottom with the bit initially well above the intruding gas. The drillpipe would "see" the same fluid column - mud and gas - as the casing, resulting in the drillpipe and casing pressure reading the same. In the extreme case,

the pipe could be out of the hole entirely.

In all the above cases, a meaningful drillpipe pressure would not be available. It is for these instances that a volumetric method was proposed by several authors. The method utilizes casing pressure-pit level changes, theoretical in nature, and had been largely untested in the field. For these reasons work was conducted at LSU to test the theory and see if it had application to field practices.

The procedure suggested by the earlier authors is as follows:

- 1) Allow the casing pressure to rise to a value slightly above initial shut-in pressure to allow for a margin of safety.
- 2) Let the casing pressure rise by a selected pressure increment. Usually 50 psi is adequate.
- 3) Bleed at constant casing pressure the volume of mud which would generate a hydrostatic pressure equal to the selected pressure increment.
- 4) Once the mud has been bled at the surface, repeat steps 2 and 3 as necessary until gas is produced at the surface.

The procedure outlined above is known as the static procedure, since no circulation of mud occurs in any manner. A second procedure, called the dynamic method, utilizes the rig pumps and the kill line to pump across the top of the annulus. Mud is pumped through the kill line, across the annulus, and into the choke line to the metering pit. This procedure has the advantage that it is easier to hold casing pressure constant. Mud is now "kicked" from the well by the expansion of the gas. Once sufficient mud has been bled, pump pressure is increased as required.

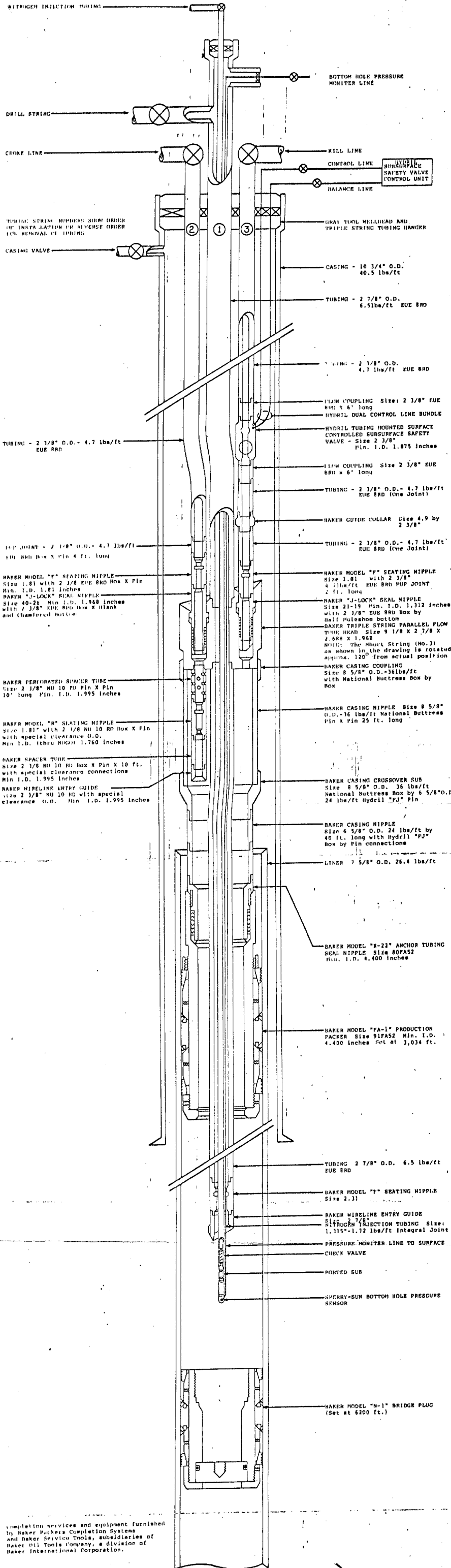
In order to evaluate experimentally the volumetric methods of well control, the 6000 ft LSU B-7 training well was utilized. Experimental runs were made for a wide variety of conditions. The results of these experiments are summarized in the May, 1980 M.S. thesis by Jeff Matheras entitled "Upward Auguration of Gas Kicks in a Shut-In Well." One copy of this thesis, enclosed with this annual report, was sent to Mr. John Gregory, the technical coordinator of this project.

As a result of the experimental work done in this study, the following conclusions were made:

1. The assumption that the gas kick remains as a continuous slug during upward gas migration was found to be invalid.
2. The trailing edge of a gas bubble was found to rise much slower than predicted due to gas fragmentation.
3. In spite of a portion of the gas reaching the surface prematurely, the modified volumetric procedure for handling upward gas migration was found to be a valid and practical technique.
4. Contrary to previously accepted practices, the venting of gas that reaches the surface prematurely was found not to cause any significant problems in maintaining well control, as long as a portion of the gas is still rising in the well.

Appendix A
Detailed Design for New Well Facility

Figure A-1 - Design of Research Well

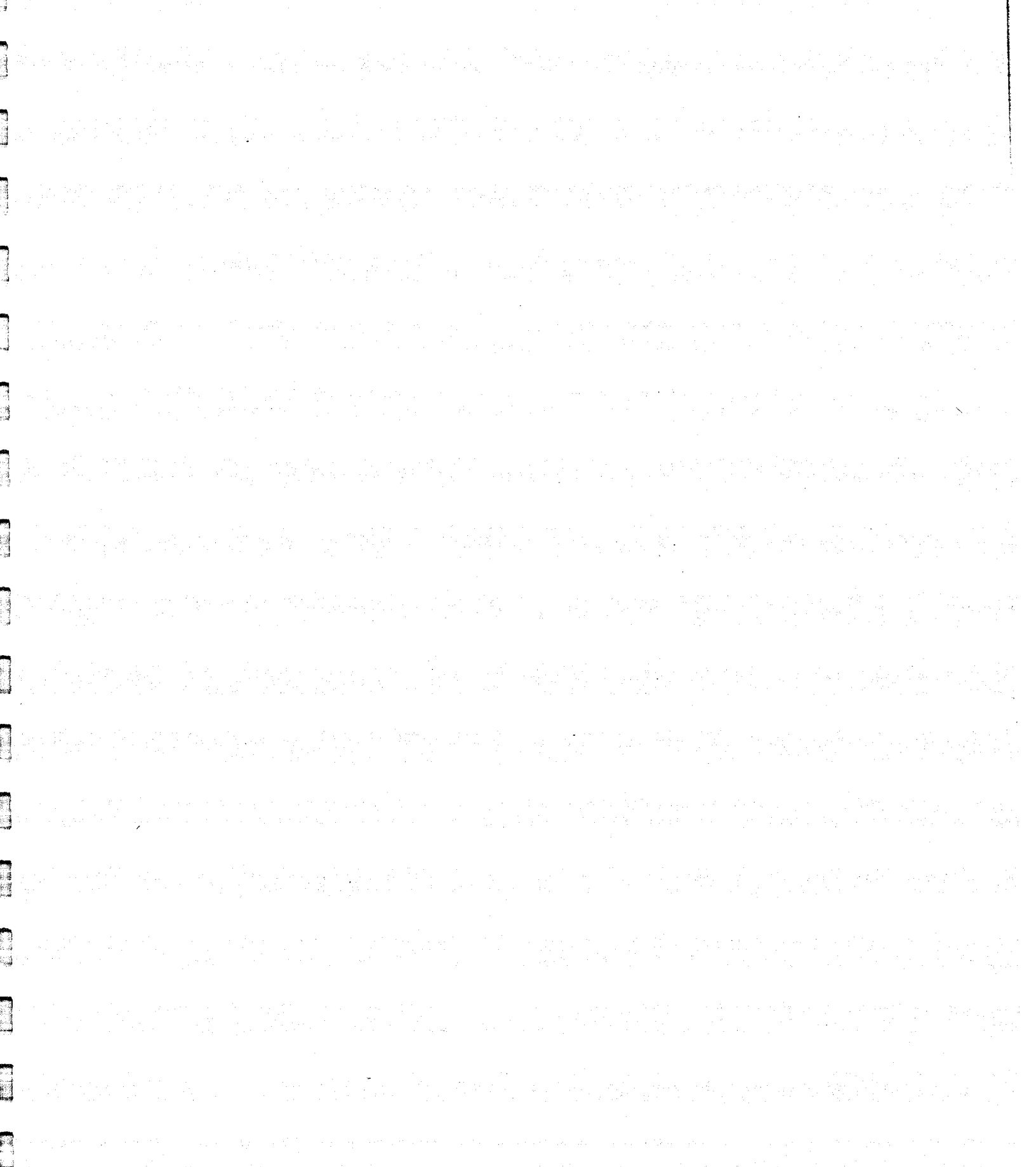


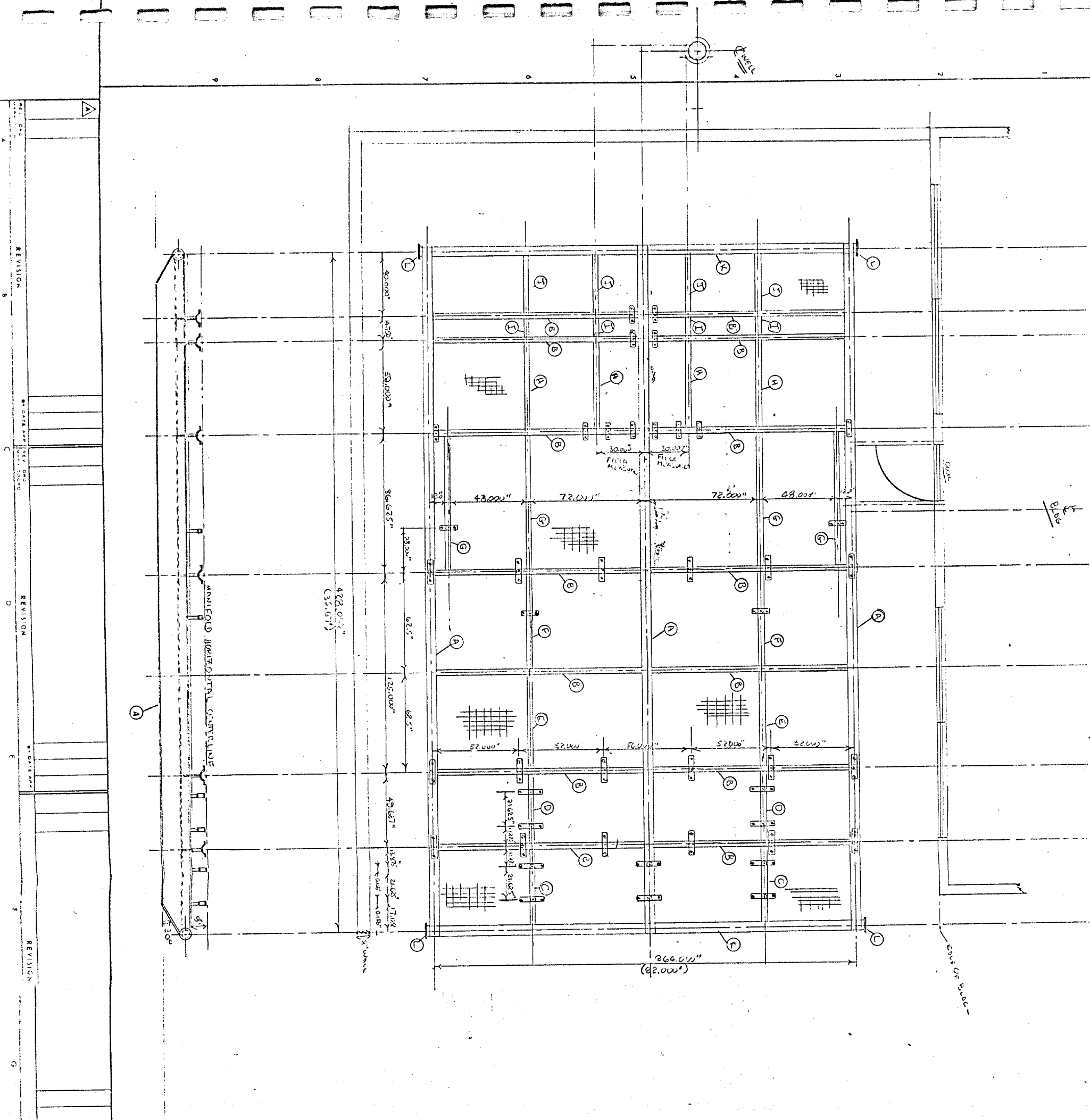
Completion services and equipment furnished by Baker Packers Completion Systems and Baker Service Tools, subsidiaries of Baker Oil Tools Company, a division of Baker International Corporation.

Figure A-2 - Piping Diagram

Figure A-3 - Choke Manifold Design

Figure A-4 - Choke Manifold Skid Design

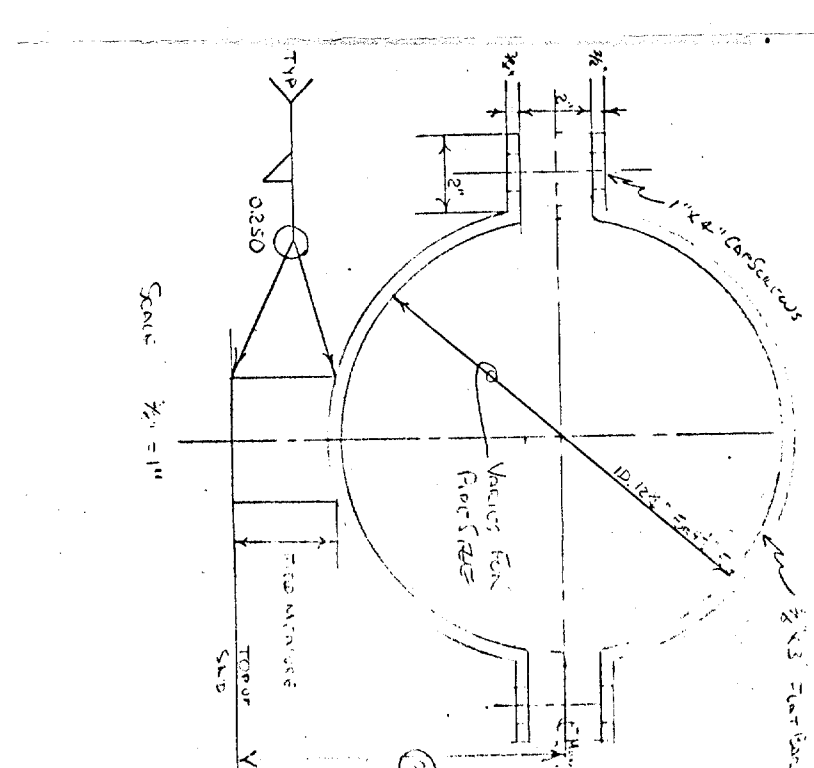




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DRAWN	JHG	(11/20/57)
CHECKED	JHG	(11/20/57)
APPROVED	JHG	(11/20/57)
NOTED		
W.C. REP.		

ORIGINAL B.M. NO. _____

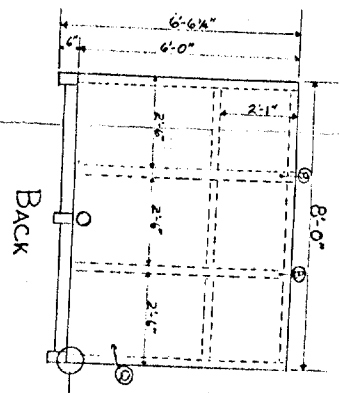
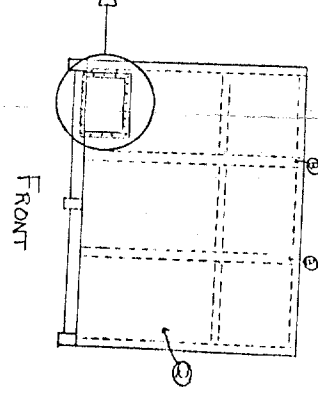
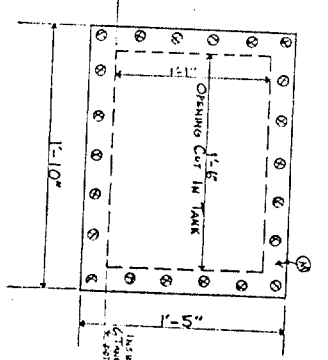
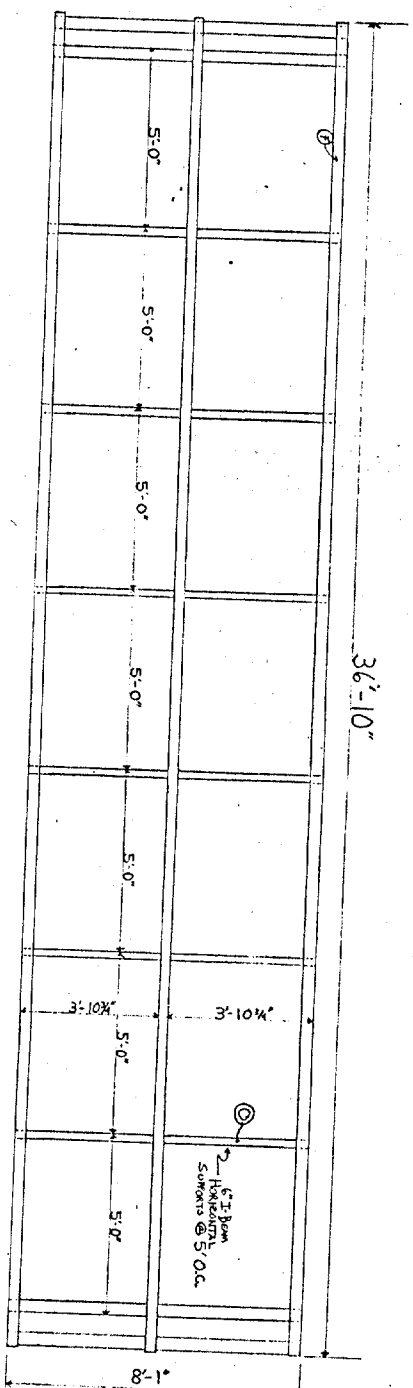
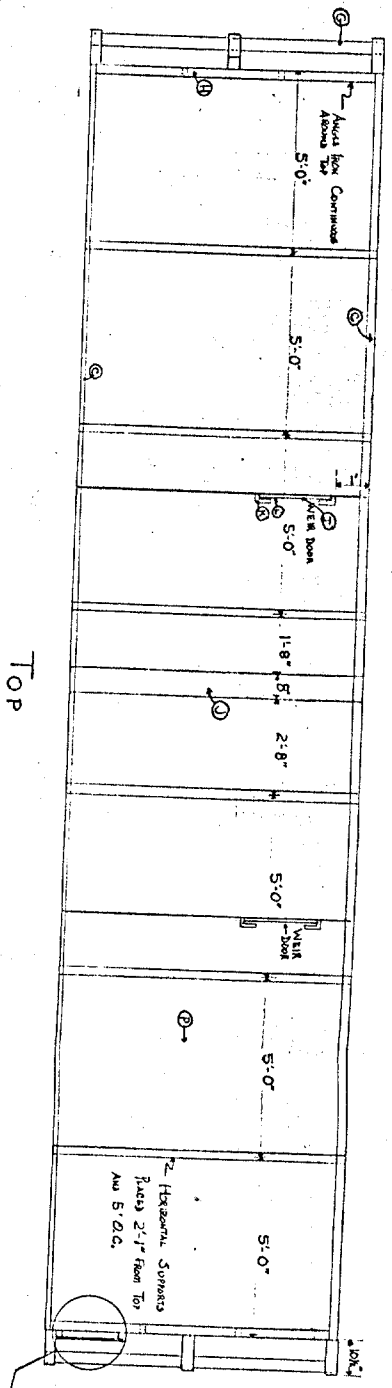
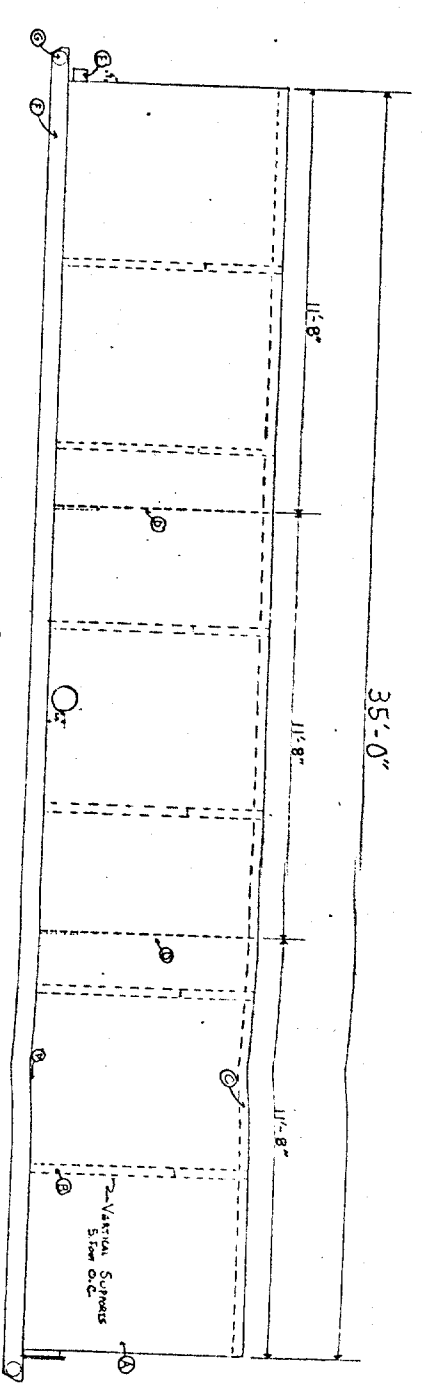
LSU SUBSTANTIAL RESEARCH BLDG
 MONIFOLD CELL
 JOB NUMBER _____
 SCALE _____



BILL OF MATERIALS

ITEM	QTY	DESCRIPTION
A	3	15" X 15" X 5/8" STEEL PLATE 431 LBS
B	14	6" X 3/4" X 17.75" I BEAM 132 LBS
C	2	6" X 3/4" X 17.75" I BEAM 53 LBS
D	2	6" X 3/4" X 17.75" I BEAM 53 LBS
E	2	6" X 3/4" X 17.75" I BEAM 53 LBS
F	2	6" X 3/4" X 17.75" I BEAM 53 LBS
G	4	6" X 3/4" X 17.75" I BEAM 53 LBS
H	4	6" X 3/4" X 17.75" I BEAM 53 LBS
I	4	6" X 3/4" X 17.75" I BEAM 53 LBS
J	4	6" X 3/4" X 17.75" I BEAM 53 LBS
K	2	6" X 3/4" X 17.75" I BEAM 53 LBS
L	4	6" X 3/4" X 17.75" I BEAM 53 LBS
M	732 FT	GENUINE SAND TO COVER TOP OF SAND

Figure A-5 - Mud Tank Design



ITEM	QTY	DESCRIPTION
A	2	1/2" x 35'-0" x 1/2" PLATE C.S.
B	2	2 1/2" x 2 1/2" x 1/2" ANGLE 5-11/16" LAMB
C	2	2 1/2" x 2 1/2" x 1/2" ANGLE 35'-0" LONG PLATE 35'-0" LONG
D	2	6'-0" x 7-11/16" x 1/2" PLATE C.S. WITH WELD
E	1	4" O.D. DRUM PIPE WITH INSIDE THREADED
F	3	1/2" x 3 1/2" x 1/2" BEAM 30'-10" LONG
G	2	4 1/2" x 3 1/2" x 1/2" BEAM 30'-10" LONG
H	2	2 1/2" x 2 1/2" x 1/2" ANGLE 7'-11" LONG PLATE 35'-0" LONG
I	2	1'-0" x 2'-0" x 1/2" WELD DRUM PLATE
J	1	8" x 8" PIPE 8'-0" LONG
K	8	GUIDES 1 1/2" x 1/2" x 1/2" LONG TUBES
L	2	GUIDES 1 1/2" x 1/2" x 1/2" LONG TUBES
M	2	1-1/2" x 1-1/2" x 1/2" PLATE C.S.
N	1	1/4" x 1'-0" x 1'-5" RUBBER SEAL
O	2	6" x 3 1/2" x 1/2" BEAM 8'-1" LONG
P	1	8'-0" x 35'-0" x 1/2" PLATE C.S.
Q	2	8'-0" x 6'-0" x 1/4" PLATE C.S.
R	22	BOLTS

NOTE: WELD DOGS ARE TO BE OMMitted FROM ABOVE.
ALL SKIDS TO BE WELDED.

NOTE: ALL WELD DOGS TO BE WELDED TO WELDED FRAMES

SKID ASSEMBLY

DESIGNED	CHECKED	APPROVED	NOTED	W.C. REF.
DRANN				

ORIGINAL B.W. NO. _____

FOR CONSTRUCTION FOR REFERENCE ONLY

LSU SUZSEA RESEARCH FACILITIES
MUD TANK 300 BBL CAPACITY

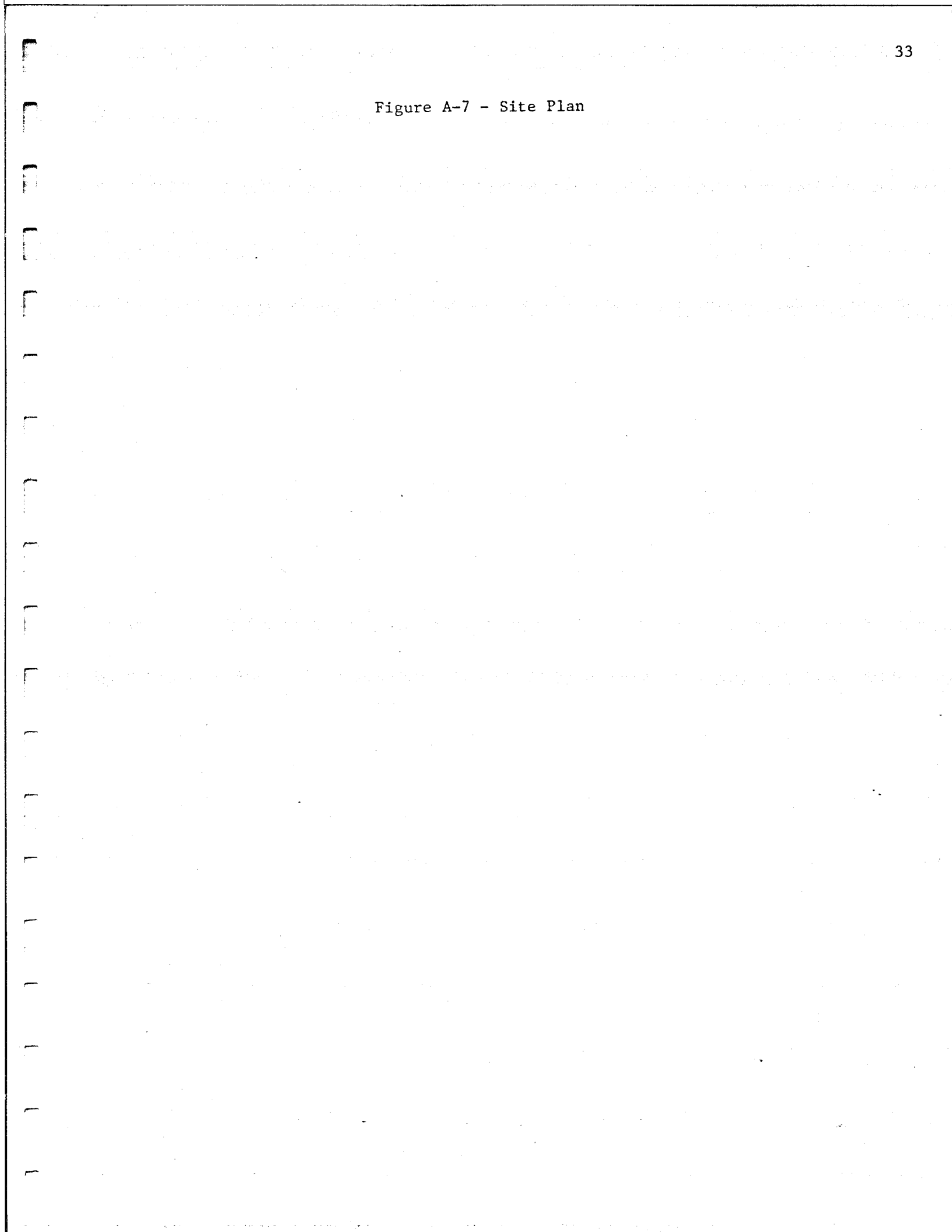
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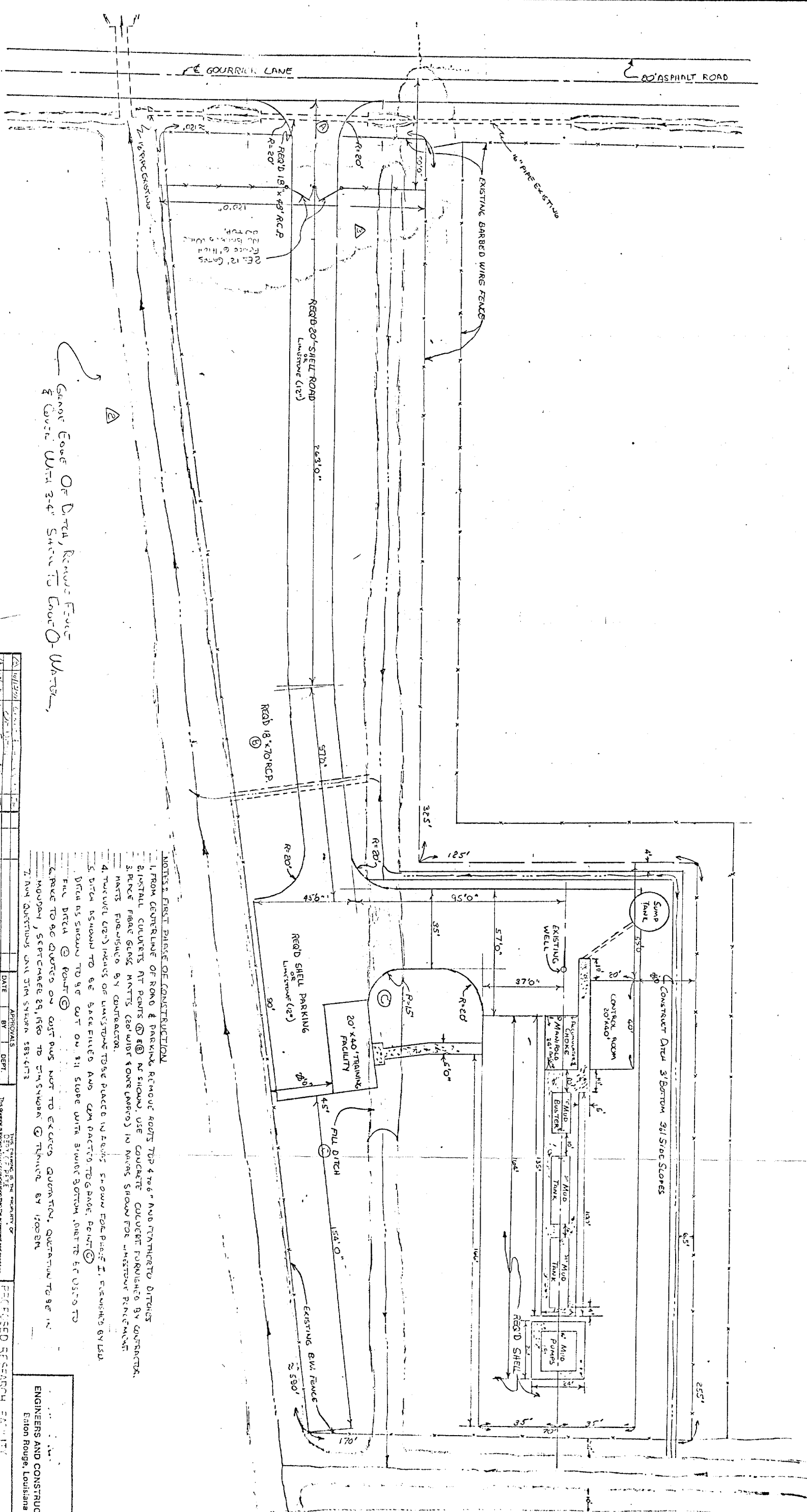
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REV.	DATE	BY	CHKD.	DESCRIPTION
A				
B				
C				
D				
E				
F				
G				
H				
I				

Figure A-6 - Surface Layout Plan

Figure A-7 - Site Plan





△ GENE EDGE OF DITCH, REMOVE FENCE & CURB WITH 3-4" SLOPE TO EDGE OF WATER.

NOTES: FIRST PHASE OF CONSTRUCTION

1. FROM CENTERLINE OF ROAD & PARKING REMOVE ROOTS TOP 4 TO 6" AND REPAIR TO DITCHES
2. INSTALL CULVERTS AT POINTS (A) & (B) AS SHOWN. USE CONCRETE. CULVERT FURNISHED BY CONTRACTOR.
3. PLACE FIBER GLASS MATS (20' WIDE COVER LAPPED) IN AREAS SHOWN FOR "WETTED PERMANENT MATS FURNISHED BY CONTRACTOR."
4. THE WEL (12") INDICES OF LIMESTONE TO BE PLACED IN AREAS SHOWN FOR FILL. FURNISHED BY LSU.
5. DITCH AS SHOWN TO BE BACK FILLED AND COMPACTED TO GRADE. POINT (C)
6. PRICE TO BE QUOTES ON COST PAWS NOT TO EXCEED QUANTUM. QUANTUM TO BE IN MONTHS, SEPTEMBER 29, 1980 TO MAY 31, 1981. (C) THROUGH BY 1200PM
7. ANY QUESTIONS CALL TIM SYMON 583-4173

DATE	BY	DEPT.	APPROVALS
10/12/79	Tim Symon	SAFETY	
10/14/79	Tim Symon	TECH	

RECEIVED RESEARCH FACILITY
 ENGINEERS AND CONSTRUCTORS
 Baton Rouge, Louisiana

2-3

Figure A-8 - Electrical Site Plans

Figure A-9 - Control House Design

Appendix B

Flow Coefficient Data on Commercial

Drilling Chokes

Table A-1 - Flow Data for Cameron Manually Adjustable Drilling Choke
(2 in diameter)

<u>Drilling Fluid Sample</u>	<u>Choke Position (fraction open)</u>	<u>Flow Rate (GPM)</u>	<u>Upstream Pressure (PSIG)</u>	<u>Valve Capacity Coefficient Cv</u>
1	0.500	280	20	63.80
		285	80	32.47
		305	180	23.17
		315	220	21.64
		320	285	19.32
	0.375	270	50	38.91
		285	100	29.04
		295	150	24.54
		307	220	21.09
		315	300	18.53
	0.313	275	105	27.35
		285	180	21.65
		290	250	18.69
		300	340	16.58
		310	440	15.06
2	0.281	270	100	27.51
		275	190	20.33
		285	280	17.36
		295	400	15.03
		307	630	12.46
	0.250	263	120	24.47
		275	320	15.67
		285	460	13.54
		295	620	12.07
		300	800	10.81
	0.219	260	180	19.75
		270	380	14.11
		280	570	11.95
		285	820	10.14
		290	1070	9.03

Table A-1 (Continued)

<u>Drilling Fluid Sample</u>	<u>Choke Position (fraction open)</u>	<u>Flow Rate (GPM)</u>	<u>Upstream Pressure (PSIG)</u>	<u>Valve Capacity Coefficient Cv</u>
3	0.188	255	265	15.96
		265	600	11.02
		270	820	9.61
		275	1120	8.37
		280	1400	7.63
	0.156	250	360	13.43
		255	690	9.89
		260	1180	7.71
		262	1520	6.85
		265	1870	6.24
	0.125	245	350	13.34
		250	850	8.74
		255	1250	7.35
		260	1900	6.08

Table A-2 - Flow Data for Patterson Remote Adjustable Drilling Choke

<u>Drilling Fluid Sample</u>	<u>Choke Position (fraction open)</u>	<u>Flow Rate (GPM)</u>	<u>Upstream Pressure (PSIG)</u>	<u>Valve Capacity Coefficient Cv</u>	
4	0.750	282	15	74.20	
		290	17	71.67	
		303	19	70.84	
		305	20	69.50	
	0.625	278	15	73.15	
		285	20	64.94	
		295	25	60.12	
		300	30	55.81	
	0.500	258	240	16.97	
		265	660	10.51	
		273	1230	7.93	
		280	1640	7.05	
5	0.333	252	260	15.93	
		256	610	10.56	
		267	1200	7.85	
		270	1880	6.35	
	0.250	245	630	9.95	
		248	1100	7.62	
		250	1340	6.96	
		252	1920	5.86	
	6	0.200	240	560	10.33
			243	890	8.30
			245	1340	6.82
			247	1790	5.95
0.167		240	650	9.59	
		242	1040	7.65	
		244	1480	6.46	
		246	1960	5.66	

Table A-3 - Flow Data for Swaco Super Remote Adjustable Drilling Choke

<u>Drilling Fluid Sample</u>	<u>Choke Position (fraction open)</u>	<u>Flow Rate (GPM)</u>	<u>Upstream Pressure (PSIG)</u>	<u>Valve Capacity Coefficient Cv</u>
7	0.750	280	20	63.62
		285	23	60.38
		300	42	47.04
		312	62	40.26
		320	70	38.86
		323	80	36.69
	0.625	277	27	54.17
		295	55	40.42
		308	70	37.40
		320	80	36.35
		328	100	33.33
		0.500	275	40
	295		80	33.52
	305		105	30.24
	315		120	29.22
	320		135	27.98
	0.333		265	40
		270	50	38.80
		273	70	33.15
		275	100	27.94
		277	130	24.69
		0.250	267	90
	271		170	21.12
	273		270	16.88
	275		370	14.53
	277		540	12.11
	0.200		265	360
270		870	9.30	
273		1200	8.01	
0.167	251	830	8.85	
	255	1120	7.74	
	260	1500	6.82	

Table A-3 (Continued)

<u>Drilling Fluid Sample</u>	<u>Choke Position (fraction open)</u>	<u>Flow Rate (GPM)</u>	<u>Upstream Pressure (PSIG)</u>	<u>Valve Capacity Coefficient Cv</u>
14	0.500	265	450	12.73
		269	950	8.89
		272	1460	7.25
	0.333	255	480	11.86
		260	1060	8.14
		264	1410	7.16
		267	1880	6.28
	0.250	252	520	11.26
		257	920	8.63
		261	1340	7.27
		264	1920	6.14
	0.200	250	320	14.24
		253	940	8.41
		257	1300	7.26
		260	1840	6.18
	0.167	246	340	13.60
		250	880	8.59
		254	1400	6.92
257		1820	6.14	

Table A-4 - Flow Data for Cameron High Pressure Remote Adjustable Drilling Choke

<u>Drilling Fluid Sample</u>	<u>Choke Position (fraction open)</u>	<u>Flow Rate (GPM)</u>	<u>Upstream Pressure (PSIG)</u>	<u>Valve Capacity Coefficient Cv</u>
8	0.500	163	20	37.03
		190	50	27.30
		237	100	24.08
		263	140	22.58
		273	160	21.93
9	0.375	160	40	25.70
		210	130	18.71
		220	170	17.14
		247	220	16.92
		265	280	16.09
10	0.250	96	120	8.90
		121	250	7.78
		149	380	7.77
		173	580	7.30
		192	750	7.12
11	0.125	13	390	0.699
		19	700	0.730
		20	1020	0.636
		39	1380	1.067
		40	1850	0.945
12	0.188	67	290	4.000
		73	700	2.804
13	0.188	86	1070	2.671
		105	1320	2.936
		111	1670	2.760

Drilling Fluid Sample	Density ppg	Plastic Viscosity cp	Yield Point lb/100 ft ²	Temperature F	Gel Strength lb/100 ft ²		Fann Viscometer			Dial Readings		
					@ 10 sec	@ 10 min	600 rpm	300 rpm	200 rpm	100 rpm	6 rpm	3 rpm
1	8.65	20.0	9.5	60	4.0	14.0	49.5	29.5	22.5	13.5	-	-
2	8.65	14.0	14.5	85	2.5	12.0	42.5	28.5	21.0	12.5	-	-
3	8.65	12.5	15.0	108	2.5	11.0	40.0	27.5	20.5	11.0	-	-
4	8.65	10.5	4.0	73	3.0	3.5	25.0	14.5	11.0	6.5	1.0	0.5
5	8.65	11.5	5.0	83	3.5	4.0	28.0	16.5	12.7	7.5	1.5	1.0
6	8.65	12.0	4.5	76	3.0	4.0	28.5	16.5	12.0	7.0	1.5	1.0
7	8.60	20.0	10.0	72	2.0	7.0	50.0	30.0	23.0	15.0	-	-
8	8.60	11.5	10.5	98	2.0	15.0	33.5	22.0	17.0	11.5	-	-
9	8.60	11.0	10.5	104	2.0	15.0	32.5	21.5	17.0	11.5	-	-
10	8.60	12.5	10.5	86	2.0	15.0	35.5	23.0	17.5	11.5	-	-
11	8.60	11.0	11.5	98	2.0	15.0	33.5	22.5	17.0	11.0	-	-
12	8.60	13.0	10.0	85	3.0	16.0	36.0	23.0	17.5	12.5	-	-
13	8.60	13.0	10.0	88	3.0	15.0	36.0	23.0	17.5	12.5	-	-
14	8.65	21.0	16.0	58	11.0	30.0	58.0	37.0	28.5	19.0	8.0	6.5

Table A-5 - Properties of Drilling Fluids Used in Determining Flow Characteristics of Drilling Chokes

Appendix C

Flow Coefficient Data on NL-Shaffer

Annular Blowout Preventer

Drilling Fluid Sample	Temp. (°F)	Density (lb/gal)	Plastic Viscosity (cp)	Yield Point (lb/100 ft ²)	Gel Strength @ 1 min @ 10 min	Fann Dial Readings					
						600 rpm	300 rpm	200 rpm	100 rpm	6 rpm	3 rpm
1	70	8.33	1.0	0.0	0.0	2.0	1.0	.67	0.33	-	-
2	80	8.6	6.5	2.0	1.0	2.0	15.0	8.5	6.0	4.0	1.0
	86	8.6	7.0	1.0	1.0	3.0	15.0	8.0	6.0	4.0	1.0
	106	8.6	7.0	3.0	1.0	3.0	17.0	10.0	8.0	5.0	1.0
3	93	8.6	20.0	22.0	29.0	44.0	62.0	42.0	35.0	27.0	12.0
4	89	8.6	11.0	6.0	5.0	13.0	28.0	17.0	14.0	9.0	2.0
	104	8.6	11.0	11.0	11.0	19.0	33.0	22.0	18.0	14.5	2.5
5	101	8.7	17.0	16.0	8.0	High	50.0	33.0	25.0	16.5	5.0
											3.5

Table C-1 - Drilling Fluid Properties Used in Determining Flow Characteristics of Annular Blowout Preventer

Table C-2 - Flow Characteristics of 6 in.
Annular Blowout Preventer

Drill Pipe O.D. (in.)	Drilling Fluid Sample	Piston Position (in.)	Frac. (open)	Flow Rate (gpm)	Hydraulic Pressure (psig)	Well Pressure (psig)	Value Coefficient Cv
2.375	1	0	1.000	162.6	0	0	-
		1.552	0.483	168.0	0	20	37.6
		1.968	0.613	168.0	0	30	30.7
		2.3715	0.7386	168.0	0	30	30.7
		2.7854	0.8675	130.9	0	580	5.4
		2.8840	0.8982	84.0	0	1400	2.2
		3.211	0.0	0.0	-	-	0
2.375	1	0.000	1.000	168.0	0	0	-
				122.0	0	0	-
				63.0	0	0	-
		2.4458	0.7496	176.0	0	0	-
				116.0	0	0	-
				59.0	0	0	-
		2.6507	0.8124	177.0	0	60	22.9
				119.0	0	20	26.6
				48.0	0	3	27.7
				180.0	0	40	28.46
				113.5	0	20	25.4
				48.5	0	3	28.0
		2.8546	0.8748	157.5	0	320	8.8
				107.5	0	190	7.8
				46.0	0	40	7.3
				150.5	0	420	7.3
				120.0	0	320	6.7
				47.5	0	140	4.0
		3.0585	0.9373	101	250	1280	2.8
				54.5	250	820	1.9
				20.5	250	560	0.87
- Automatic Closure -							
2.375	2	0.0	1.000	171.5	0	0	-

Table C-2 (Continued)

<u>Drill Pipe O.D. (in.)</u>	<u>Drilling Fluid Sample</u>	<u>Piston Position (in.)</u>	<u>Frac. (open)</u>	<u>Flow Rate (gpm)</u>	<u>Hydraulic Pressure (psig)</u>	<u>Well Pressure (psig)</u>	<u>Value Coefficient Cv</u>
		1.6450	0.5000	171.5	0	0	-
		2.4675	0.7500	171.5	220	30	31.3
		2.6733	0.8125	168	300	140	14.2
				158.5	300	280	9.4
				130.5	300	60	16.9
				84.0	300	20	18.8
		2.8788	0.8750	120	440	780	4.3
				117	440	860	4.0
				90	440	700	3.4
				77	440	580	3.2
				46.5	440	440	2.2
2.375	3	0	1.000	118.5	0	0	-
		2.4675	0.7500	168.0	220	20	37.6
		2.6733	0.8126	157.5	300	240	10.2
				114.5	300	160	9.1
				76.0	300	70	9.1
		3.0844	0.9375	- Automatic Closure -			
3.500	4	0.0	1.000	168	-	100	16.8
				118.5	-	40	18.7
				53	-	20	11.9
				42	-	10	13.3
		1.511	0.5182	168	-	100	16.8
				109.5	-	60	14.1
				41.0	-	40	6.4

Table C-2 (Continued)

<u>Drill Pipe O.D. (in.)</u>	<u>Drilling Fluid Sample</u>	<u>Piston Position (in.)</u>	<u>Frac. (open)</u>	<u>Flow Rate (gpm)</u>	<u>Hydraulic Pressure (psig)</u>	<u>Well Pressure (psig)</u>	<u>Value Coefficient Cv</u>
		2.201	0.7549	168	-	120	15.3
				91	-	60	11.7
				41	-	40	6.5
		2.558	0.8774	86	-	1380	2.3
				65.5	-	1100	2.0
				42.5	-	880	1.4
3.500	5	0.0	1.000	174.0	-	100	17.4
				111.0	-	60	14.3
				41.0	-	20	9.2
				165.0	-	100	16.5
				106.5	-	60	13.7
				43.5	-	20	9.7
		2.187	0.7500	168	-	90	17.7
				99.5	-	60	12.8
				43.5	-	40	6.9
		2.551	0.8750	95.5	-	1180	2.8
				66.0	-	900	2.2
				33.5	-	760	1.2
		2.733	0.9375	- Automatic Closure -			
4.500	1	0.0	1.0	48	0	3.4	26.0
		1.757	0.6174	50	100	3.8	25.6
				100	100	5.2	43.8
				143	100	7.6	51.9
				185	100	11.0	55.8
		1.933	0.700	19	100	13.5	5.17
				46	100	47	6.7
				101	100	150	8.3
				141	100	180	10.5

Table C-2 (Continued)

<u>Drill Pipe O.D. (in.)</u>	<u>Drilling Fluid Sample</u>	<u>Piston Position (in.)</u>	<u>Frac. (open)</u>	<u>Flow Rate (gpm)</u>	<u>Hydraulic Pressure (psig)</u>	<u>Well Pressure (psig)</u>	<u>Value Coefficient Cv</u>
		2.134	0.7500	26	200	250	1.6
				44	200	280	2.6
				94	200	325	5.2
				143	200	350	7.6
<hr/>							
		2.277	0.8000	8	200	425	0.39
				45	195	500	2.01
				87	140	550	3.71
				141	200	560	5.96
<hr/>							
		2.423	0.851	6	1150	750	0.22
				13	1150	975	0.42
				51	1200	1175	1.5
				76	1200	1300	2.1
				87	1200	1800	2.1
<hr/>							
		2.561	0.8999	- Automatic Closure -			
<hr/>							