

Sonic Enhanced Ash Agglomeration and Sulfur Capture

**Quarterly Report
July - September 1995**

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Work Performed Under Contract No.: DE-AC21-89MC26288

For
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PREFACE

This 25th Quarterly Technical Progress Report presents the results of work accomplished during the period July 1, 1995 through September 24, 1995 (July, August, and September) under Contract No. DE-AC21-88MC26288 entitled "Sonic Enhanced Ash Agglomeration and Sulfur Capture."

During this reporting period, design, design analysis and procurement proceeded as scheduled. An independent analysis of the structure was completed and the concrete pad was found to be inadequate. It will be re-designed.

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SECTION 1.0

INTRODUCTION

1.1 PROJECT DESCRIPTION AND WORK STATUS

A major concern with the utilization of coal in directly fired gas turbines is the control of particulate emissions and reduction of sulfur dioxide, and alkali vapor from combustion of coal, upstream of the gas turbine. Much research and development has been sponsored on methods for particulate emissions control and the direct injection of calcium-based sorbents to reduce SO₂ emission levels. The results of this research and development indicate that both acoustic agglomeration of particulates and direct injection of sorbents have the potential to become a significant emissions control strategy.

The Sonic Enhanced Ash Agglomeration and Sulfur Capture program focuses upon the application of an MTCI proprietary invention (Patent No. 5,197,399) for simultaneously enhancing sulfur capture and particulate agglomeration of the combustor effluent. This application can be adapted as either a "hot flue gas cleanup" subsystem for the current concepts for combustor islands or as an alternative primary pulse combustor island in which slagging, sulfur capture, particulate agglomeration and control, and alkali gettering as well as NO_x control processes become an integral part of the pulse combustion process.

The goal of the program is to support the DOE mission in developing coal-fired combustion gas turbines. In particular, the MTCI proprietary process for bimodal ash agglomeration and simultaneous sulfur capture will be evaluated and developed. The technology embodiment of the invention provides for the use of standard grind, moderately beneficiated coal and WEM for firing the gas turbine with efficient sulfur capture and particulate emission control upstream of the turbine. The process also accommodates injection of alkali gettering material if necessary. This is aimed at utilization of relatively inexpensive coal fuels, thus realizing the primary benefit being sought by direct firing of coal in such gas turbine systems. The proposed technology provides for practical, reliable,

and capital (and O&M) cost-effective means of protection for the gas turbine from impurities in the coal combustor effluent.

1.2 PROGRAM OBJECTIVES

The major objective of the Phase I test program is to confirm the feasibility of the MTCI bimodal particle size approach to enhance particulate control by acoustic ash agglomeration. An ancillary objective of the Phase I effort is to demonstrate and confirm the feasibility of an acoustic field to enhance sulfur capture by increasing sorbent reactivity. Phase I tests are designed to cover the frequency range between 50 and 1400 Hz, establish monomodal baseline performance as a benchmark from which to measure the degree of enhancement expected from the bimodal approach, and, finally, to confirm the effectiveness of low-frequency fields over high-frequency fields for realistic particulate streams.

The program will demonstrate the effectiveness of a unique approach which uses a bimodal distribution composed of large sorbent particles and fine fly ash particles to enhance ash agglomeration and sulfur capture at conditions found in direct coal-fired turbines. Under the impact of high-intensity sound waves, sorbent reactivity and utilization, it is theorized, will increase while agglomerates of fly ash and sorbents are formed which are readily collected in commercial cyclones. The work will extend the concept from the demonstration of feasibility (Phase I), through proof-of-concept (Phase II) to the construction (Phase III) of a coal-fired pulsed combustor with in-furnace sorbent injection. For Phase I, Pennsylvania State University will conduct studies for enhanced sulfur capture in The Combustion Laboratory and agglomeration tests in the High Intensity Acoustic Laboratory.

1.3 SUMMARY STATUS FOR THE PERIOD

During this reporting period, design, design analysis and procurement proceeded as scheduled. An independent analysis of the structure was completed and the concrete pad was found to be inadequate. It will be re-designed.

SECTION 2.0

TECHNICAL DISCUSSION OF THE WORK ACCOMPLISHED DURING THE REPORTING PERIOD

2.1 TASK 2: ADDITIONAL TEST FACILITY MODIFICATIONS AND SHAKEDOWN TESTING

During this reporting period, design, procurement and fabrication was continued. Procurement is now 70 percent completed. Progress in design and fabrication of the PDU and components are shown in Table 1. Figure 1 shows the updated design of the pulse combustor-HGCU system. Figures 2 - 12 present further design development of the bimodal system components, and Figure 13 shows a draft of the supporting structure layout. Analysis of the design of the refractory lining of the pulse combustor, U-bend section, agglomeration chamber, and primary cyclone with refractory lining were also completed (Figures 14, 15, 16 and 17).

TABLE 1:
DESIGN AND FABRICATION PROGRESS CHART - BIMODAL PDU

Item No.	Description of Components	Design Accomplished, %	Fabrication Accomplished, %
1	Air Plenum	100	20
2	Coal Injector	100	100
3	Pilot Burner	100	90
4	Aeroválve	100	100
5	Water Jacket of Pulse Combustor	100	30
6	U-Bend Water Jacket	100	95
7	Agglomeration Chamber (60" dia.)	100	*
8	Slag-Handling Section	50	10
9	Ash Drain Section	50	10
10	Reburning Coal Injector	50	10
11	Primary Cyclone	100	10
12	Secondary Cyclone	30	10
14	Dipleg and Ash Recycle Section	30	10
15	Refractory and Insulation	75	0
16	Splitter of Coal and Air Mixture	0	0
17	Flue Gas Heat Exchanger	0	0
18	Steam Drum	0	0
19	Air Preheater in the Flare	0	0
20	Structure	50	0
21	Instrumentation and Control	20	0

* Top section is 75% complete, middle and bottom sections are 97% complete.

ITEM	QTY	DWG NO.	DESCRIPTION	UNIT WT.	TOT. WT.
1	1	ESM-911	DUAL INJECTOR	14.9	14.9
2	1	ESM-912	AIR FLOW ASSEMBLY	14.9	14.9
3	1	ESM-913	ARMATURE	0.29	0.29
4	1	ESM-914	FLUT BURNER ASSEMBLY	0.29	0.29
5	1	ESM-915	REFRACTORY PULSE COMPONENT	0.29	0.29
6	1	ESM-916	WATER JACKET ASSEMBLY	0.29	0.29
7	1	ESM-917	WALL/IN REFRACTORY	0.29	0.29
8	1	ESM-918	TEMPERATURE RECORDING PORT	0.29	0.29
9	1	ESM-919	TEMPERATURE RECORDING PORT	0.29	0.29
10	1	ESM-920	PRESSURE TOLERANT PORT	0.29	0.29
11					
12					
TOTAL WT.				2862	

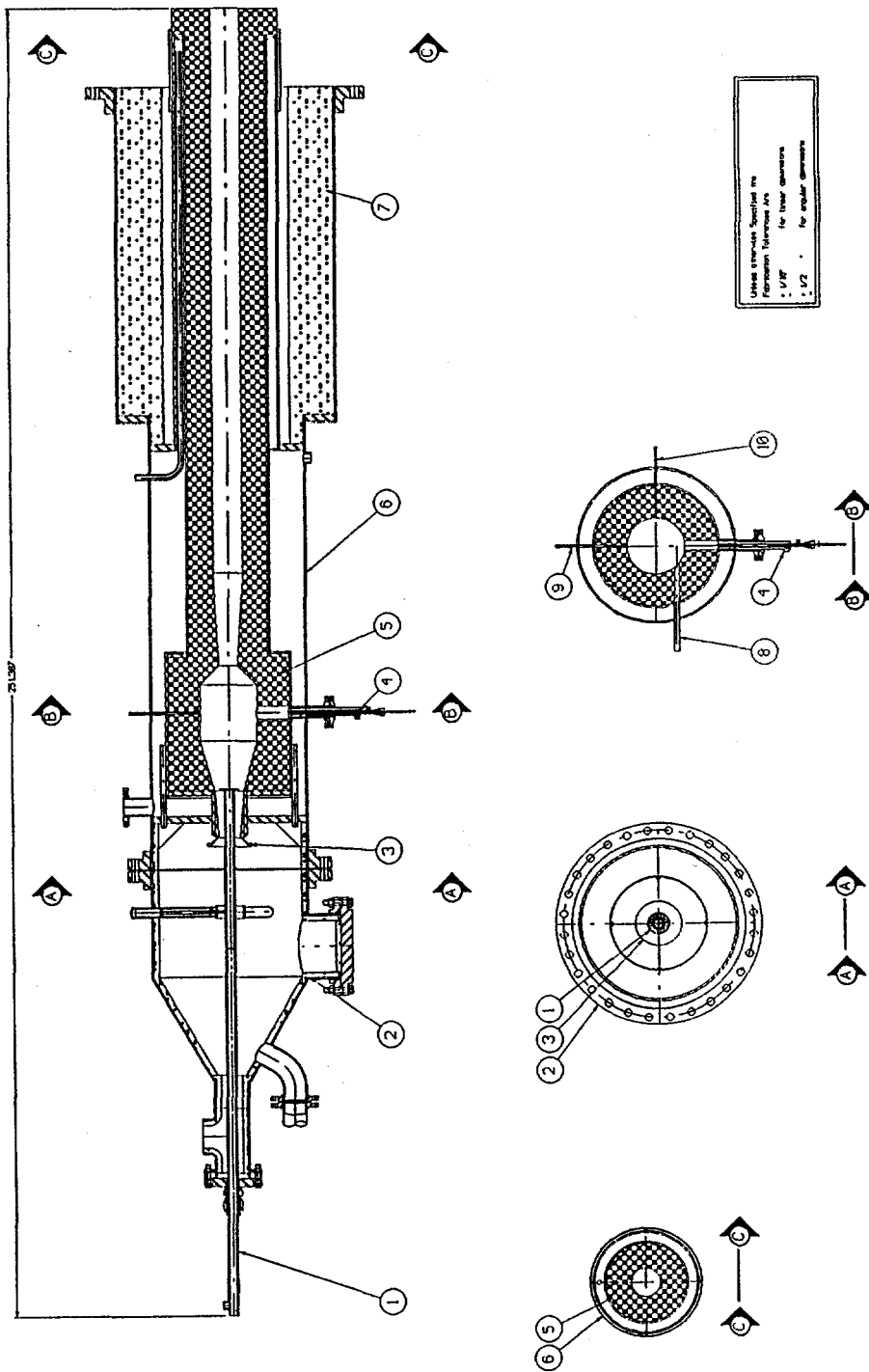


FIGURE 2: PULSE COMBUSTOR ASSEMBLY

ITEM	QTY	DWG NO.	DESCRIPTION	NET WT.	GR. WT.
1	1	ED-412	WALVE 2" SA	214	214
2	8	ED-412	SALT 3/4" CS L-1"	68	68
3	8	ED-412	WTS 3/4" CS	63	148
4	8	ED-412	WALVE 2 1/2" CS	81	81
5	1	ED-412	SLIP-ON FLANGE F. FR. LR. CS.	268	268
6	1	ED-412	SLIP-ON FLANGE F. FR. LR. CS.	268	268
7	1	ED-412	CORSET FOR F. FLANGE	188	188
8	1	ED-412	PIPE F. 3/4" CS L-1"	328	328
9	1	ED-412	TEE F. 3/4" CS	628	628
10	1	ED-412	PIPE F. 3/4" CS L-1"	328	328
11	1	ED-412	PIPE F. 3/4" CS L-1"	328	328
12	1	ED-412	PIPE F. 3/4" CS L-1"	328	328
13	1	ED-412	PIPE F. 3/4" CS L-1"	328	328
14	1	ED-412	PIPE F. 3/4" CS L-1"	328	328
15	1	ED-412	PIPE F. 3/4" CS L-1"	328	328
16	1	ED-412	PIPE F. 3/4" CS L-1"	328	328
17	1	ED-412	PIPE F. 3/4" CS L-1"	328	328
18	1	ED-412	PIPE F. 3/4" CS L-1"	328	328
19	1	ED-412	PIPE F. 3/4" CS L-1"	328	328
20	1	ED-412	PIPE F. 3/4" CS L-1"	328	328
21	1	ED-412	PIPE F. 3/4" CS L-1"	328	328
22	3	ED-412	PIPE F. 3/4" CS L-1"	108	108
23	3	ED-412	PIPE F. 3/4" CS L-1"	108	108
24	3	ED-412	PIPE F. 3/4" CS L-1"	108	108
25	3	ED-412	PIPE F. 3/4" CS L-1"	108	108
26	1	ED-411	CON. SECTION WHEEL	48	48
27	1	ED-411	PIPE F. 3/4" CS L-1"	328	328
28	1	ED-411	WOODEN F. INSE	288	288
29	1	ED-411	PIPE F. 3/4" CS L-1"	328	328
30	2	ED-411	SLIP-ON FLANGE F. CS. FR. LR.	124	124
31	2	ED-411	CORSET THROUGHT-UP	648	648
32	8	ED-411	SALT 3/4" CS L-1"	63	63
33	8	ED-411	WALVE 3/4" CS	63	63
34	8	ED-411	WALVE 3/4" CS	63	63
35	1	ED-411	PIPE F. 3/4" CS L-1"	63	63
				TOTAL WT.	3988

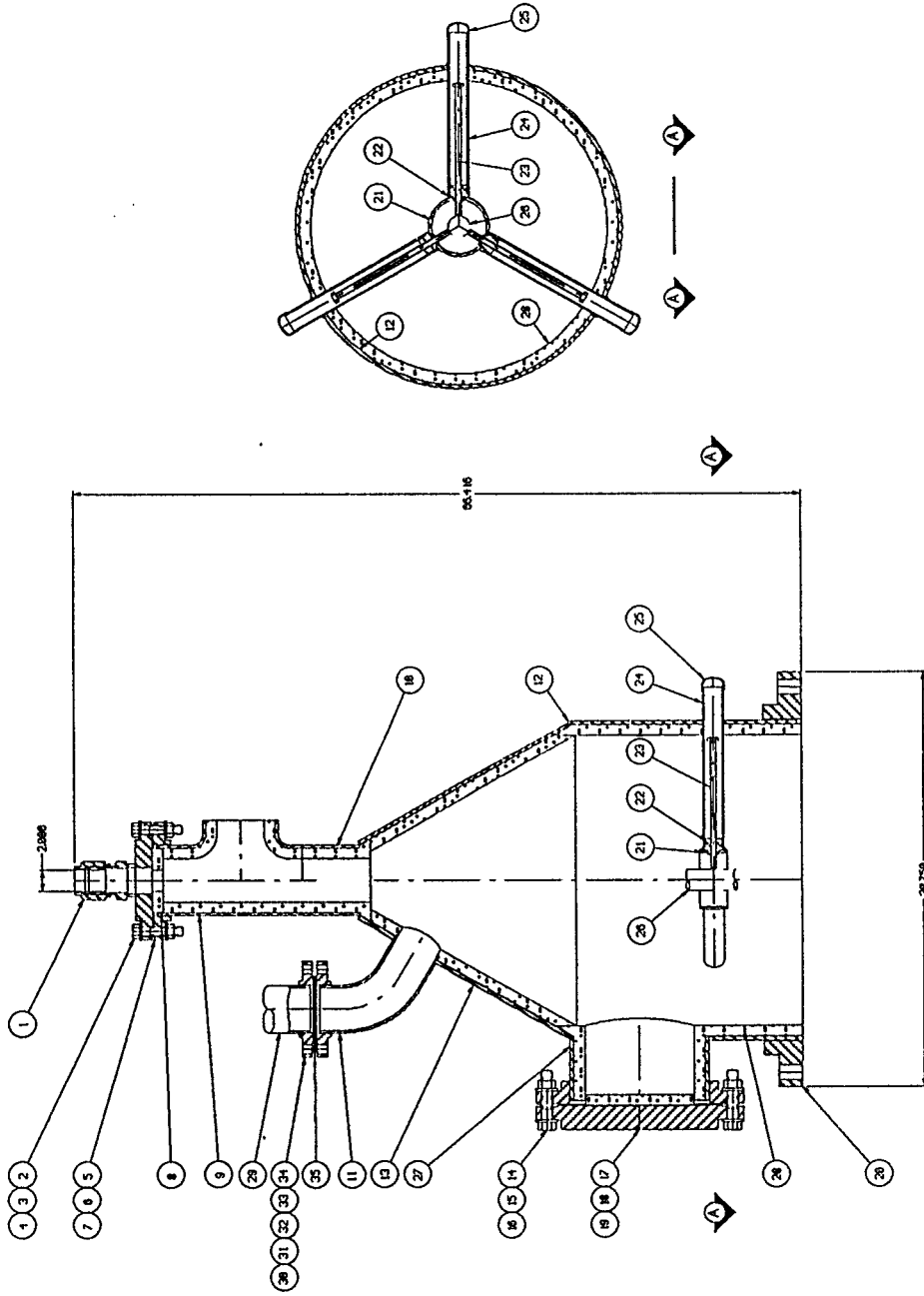
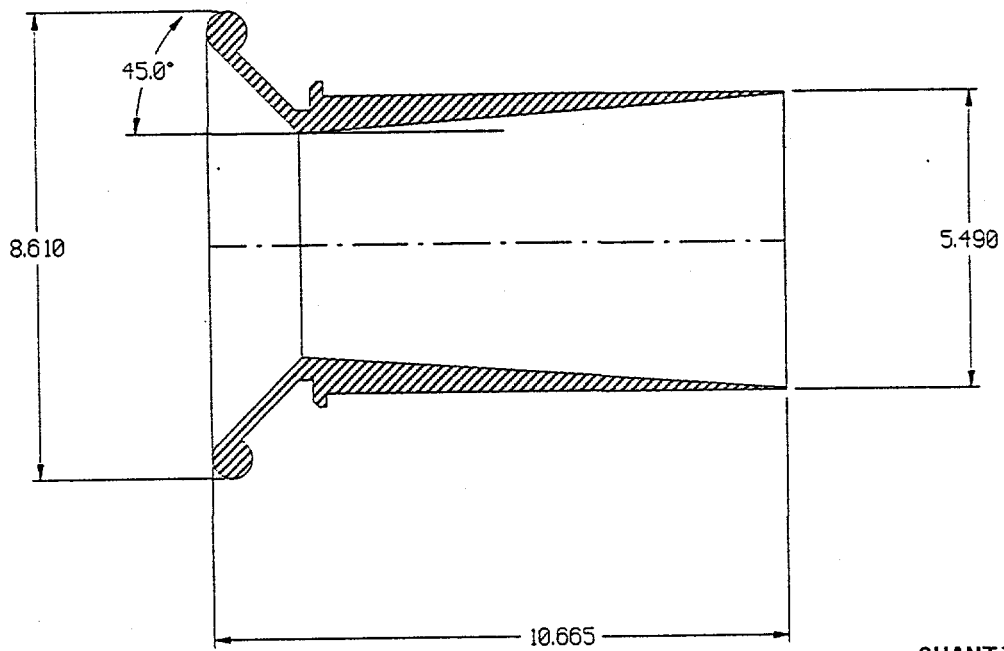


FIGURE 3: AIR PLENUM ASSEMBLY



QUANTITY: 1
 MATERIAL: S.S. 304

Unless otherwise specified the
 Fabrication Tolerances are
 - 1/32" for linear dimensions
 - 1/2° for angular dimensions

FIGURE 4: AEROVALVE

ITEM	QTY	DWG NO	DESCRIPTION	UNIT	MT	TOT. WT.
1	1	EXP-111	WELDED PLATE SECTION	LIN	1.98	14.98
2	1	EXP-111	2" TUBE 14' SECTION	LIN	14.98	114.98
3	1	EXP-111	THICKNESS 8.00" SECTION	INCH	8.00	64.00
4	1	EXP-111	THICKNESS 8.00" SECTION	INCH	8.00	64.00
5	1	EXP-111	1" HALF COUPLING SECTION	INCH	1.50	12.00
6	1	EXP-111	2" FLEXIBLE HOSE SECTION	FT	12.00	12.00
TOTAL				MT	34.44	344.96

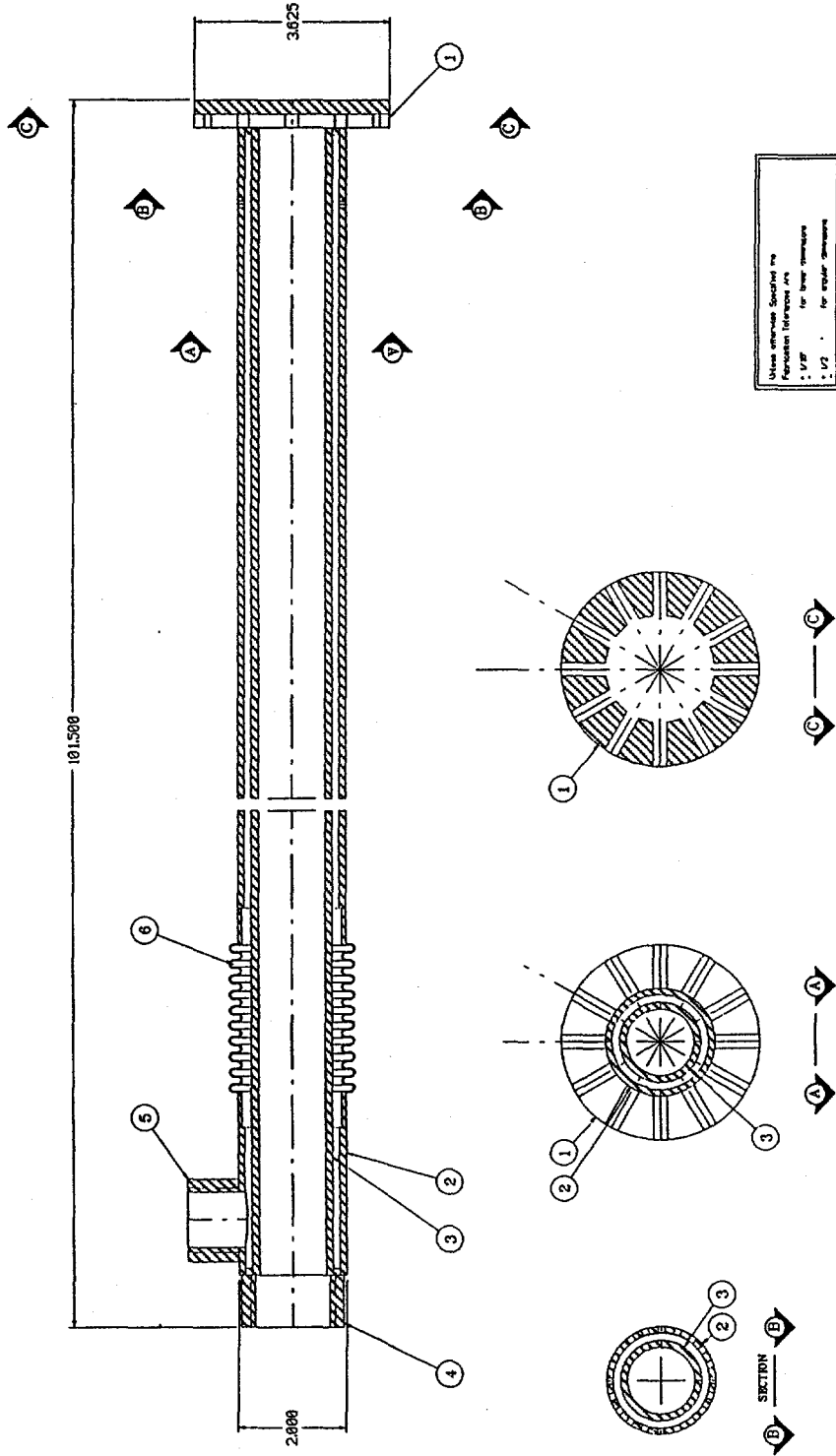
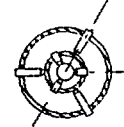
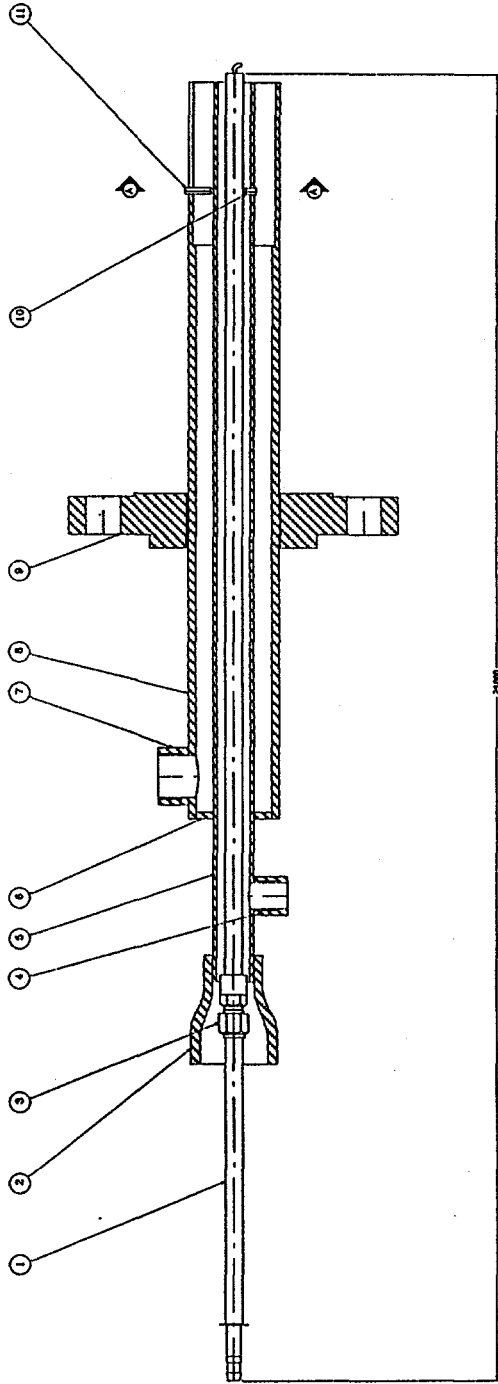


FIGURE 6: COAL INJECTOR

ITEM	QTY	DWG NO.	DESCRIPTION	UNIT WT.	TOT. WT.
1	1	DSR-414	SPARK PLUG 1-3/4"	6.9	6.9
2	1	DSR-414	REDUCER 1-1/2" SS304	6.9	6.9
3	1	DSR-414	WASHER 3/4" SS304	6.9	6.9
4	1	DSR-414	HALF COUPLER 1/2" SS304	6.9	6.9
5	1	DSR-414	TEE 3/4" SS304	6.9	6.9
6	1	DSR-414	4WG SS304 COUPLER 1/2"	6.9	6.9
7	1	DSR-414	HALF COUPLER 3/4" SS304	6.9	6.9
8	1	DSR-414	TEE 1/2" 304 SS304 L-1037	6.9	6.9
9	1	DSR-414	BLAD PLATE 2" US	6.9	6.9
10	3	DSR-414	SCREW 1/2" SS304	6.9	20.7
11	1	DSR-414	SCREW 1/2" SS304	6.9	6.9
TOTAL WT.				661	661



Unless otherwise specified the
 dimensions shown are
 1/16" for their diameters
 1/32" for regular dimensions

FIGURE 7: PILOT BURNER

ITEM	QTY	DWG NO.	DESCRIPTION	UNIT	TOT. VOLUME
1	2	DSM-428	4" BLANK CS. F. 4" THICKNESS 3/4"	1918	20228
2	2	DSM-428	4" BLANK CS. F. 4" THICKNESS 3/4"	918	8228
3	2	DSM-428	2" PIPE LENGTH 32"	28	48
4	2	DSM-421	180 CS. THICKNESS 1/8"	907	8074
5			10 3/4" V.F. ID. 1/2" V.F.		
6	1	DSM-428	1/2" STD. FLANGE ON LB.	2628	2628
7					
8	1	DSM-428	1/2" PIPE STD. CS. THICK. 3/4" L. 8.25"	1518	1418
9	1	DSM-428	1/2" PIPE STD. CS. THICK. 3/4" L. 8"	818	818
10	1	DSM-428	1/2" FLANGE STD. CS. ON LB.	278	278
11	1	DSM-428	1/2" PIPE STD. CS. LENGTH 11"	288	288
12	2	DSM-428	1 1/4" PIPE STD. CS. LENGTH 10 1/2"	23	44
13	2	DSM-428	3/4" PIPE STD. CS. LENGTH 8"	63	68
14	1	DSM-421	180 CS. THICKNESS 1/8"	2618	2618
15	1	DSM-428	10 3/4" V.F. ID. 1/2" V.F.		
16	8	DSM-421	180 CS. THICKNESS 1/8"	318	2818
17	1	DSM-428	10 3/4" V.F. ID. 1/2" V.F.	181	181
18	1	DSM-428	10 3/4" V.F. ID. 1/2" V.F.	181	181
19	1	DSM-428	10 3/4" V.F. ID. 1/2" V.F.	181	181
20	1	DSM-428	10 3/4" V.F. ID. 1/2" V.F.	181	181
21	1	DSM-428	10 3/4" V.F. ID. 1/2" V.F.	181	181
22	1	DSM-428	10 3/4" V.F. ID. 1/2" V.F.	181	181
23	1	DSM-428	10 3/4" V.F. ID. 1/2" V.F.	181	181
24	1	DSM-428	10 3/4" V.F. ID. 1/2" V.F.	181	181
25	1	DSM-428	10 3/4" V.F. ID. 1/2" V.F.	181	181
26	1	DSM-428	10 3/4" V.F. ID. 1/2" V.F.	181	181
27	1	DSM-428	10 3/4" V.F. ID. 1/2" V.F.	181	181
28	1	DSM-421	180 CS. THICKNESS 1/8"	181	181
29	1	DSM-421	180 CS. THICKNESS 1/8"	181	181
30	1	DSM-428	10 3/4" V.F. ID. 1/2" V.F.	181	181
31	1	DSM-428	10 3/4" V.F. ID. 1/2" V.F.	181	181
32	1	DSM-428	10 3/4" V.F. ID. 1/2" V.F.	181	181
33	1	DSM-421	180 CS. THICKNESS 1/8"	181	181
34	1	DSM-421	180 CS. THICKNESS 1/8"	181	181
35	1	DSM-421	180 CS. THICKNESS 1/8"	181	181
36	1	DSM-421	180 CS. THICKNESS 1/8"	181	181
				TOTAL VOLUME	180337

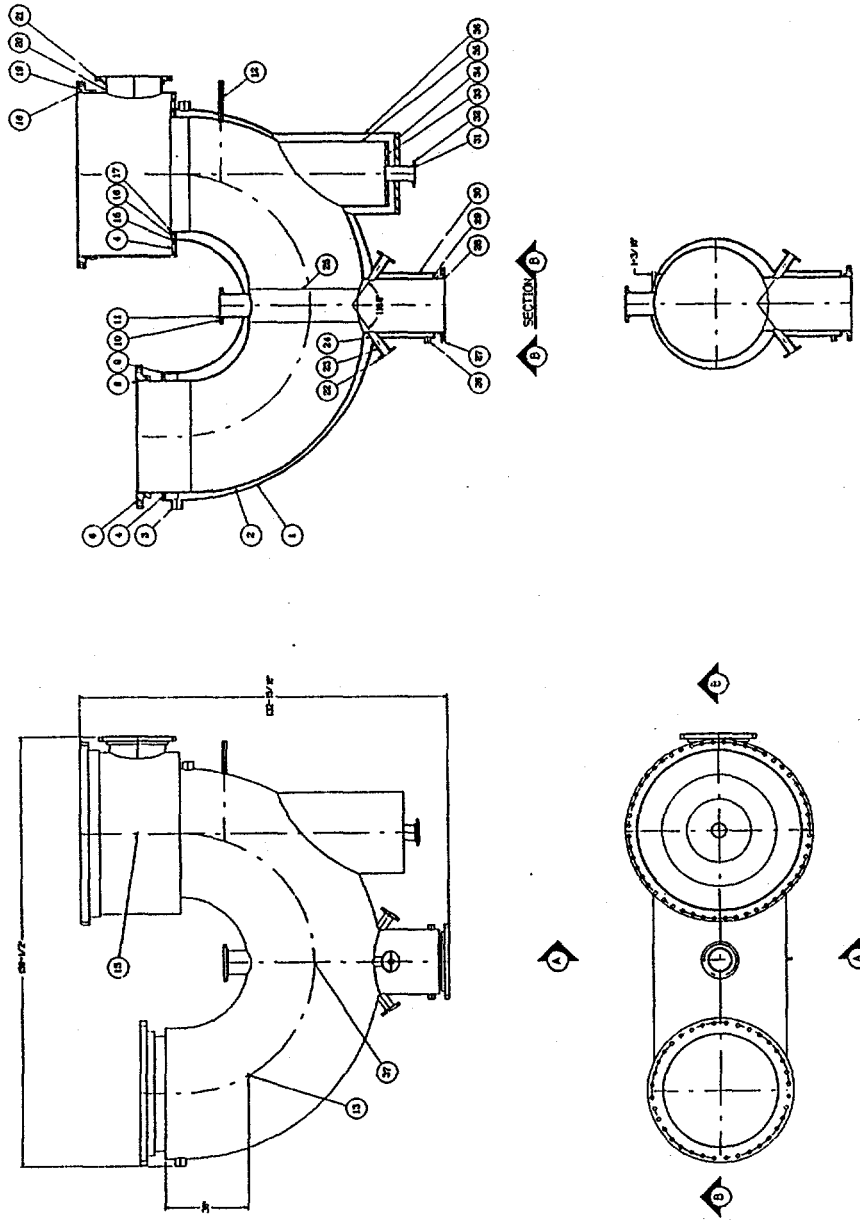


FIGURE 8: U-BEND SECTION ASSEMBLY (WITHOUT REFRACTORY)

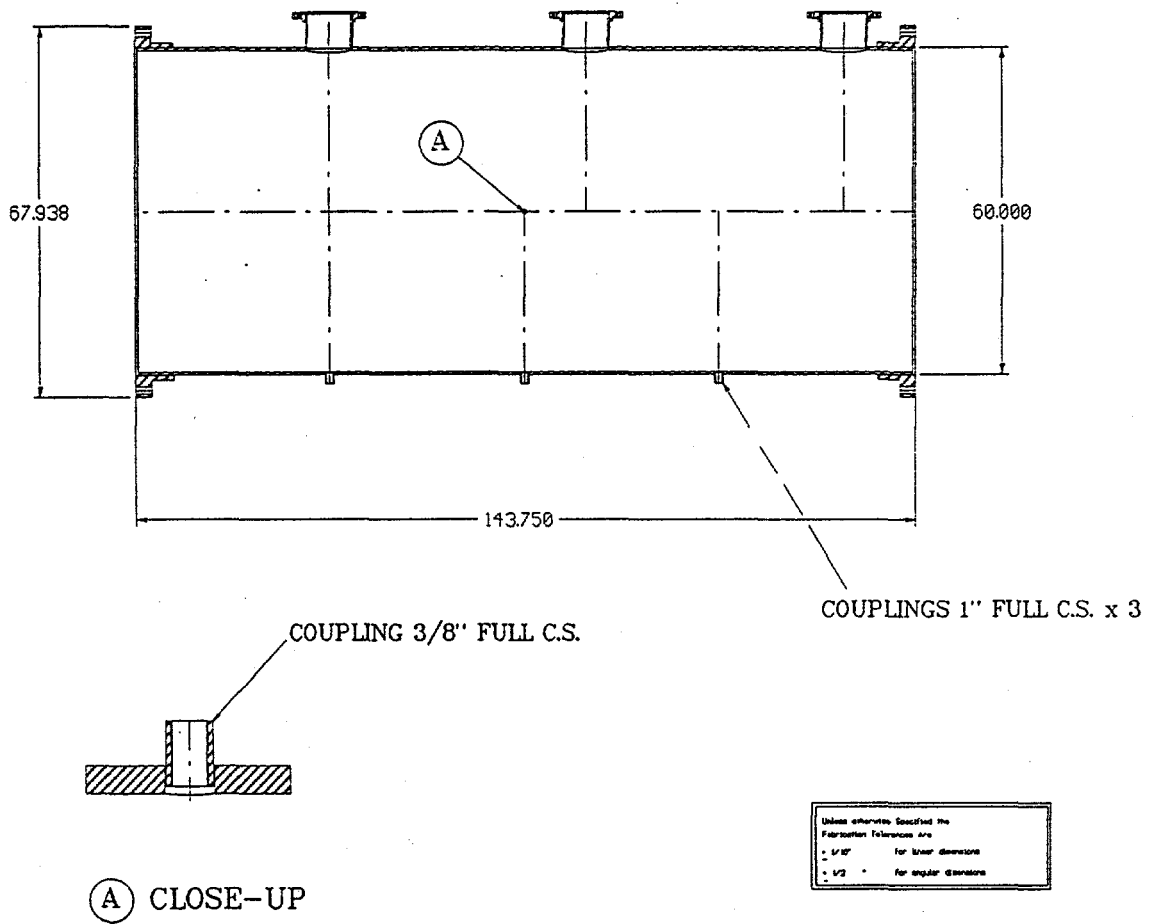
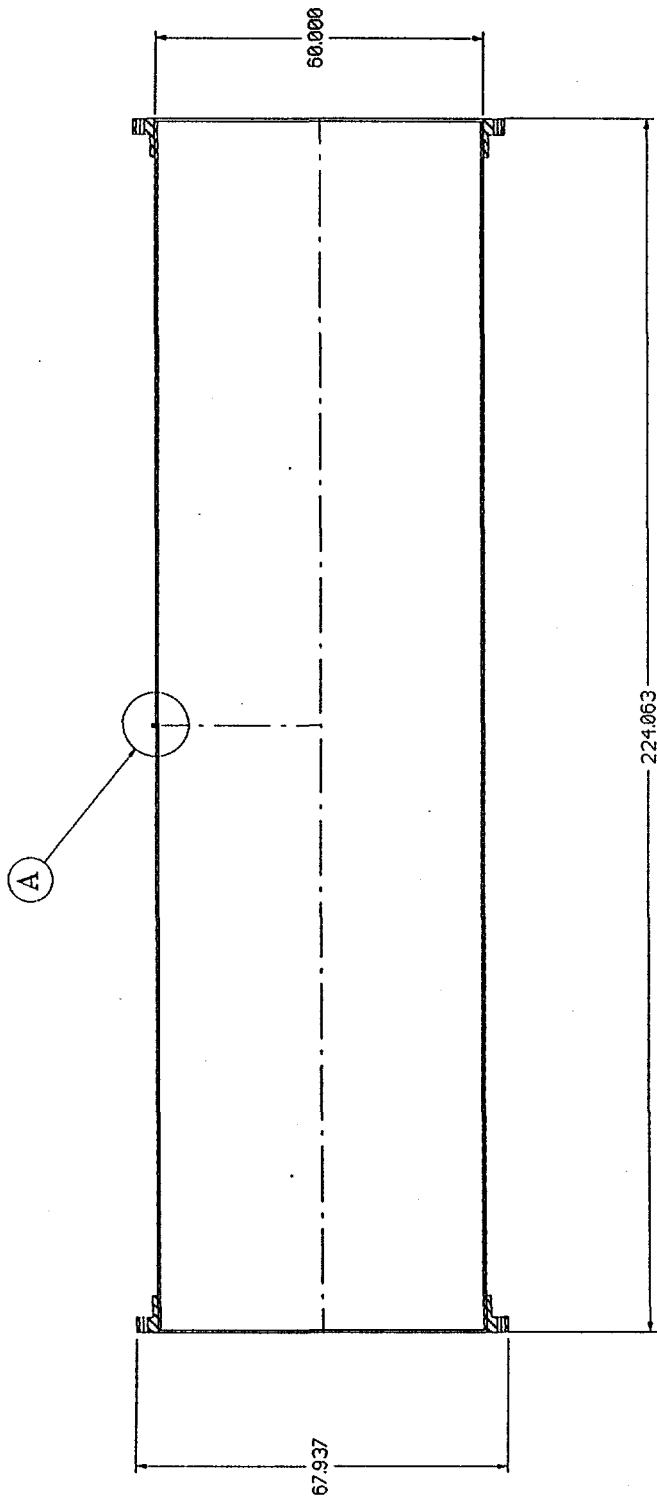


FIGURE 10: BOTTOM SECTION OF AGGLOMERATION CHAMBER



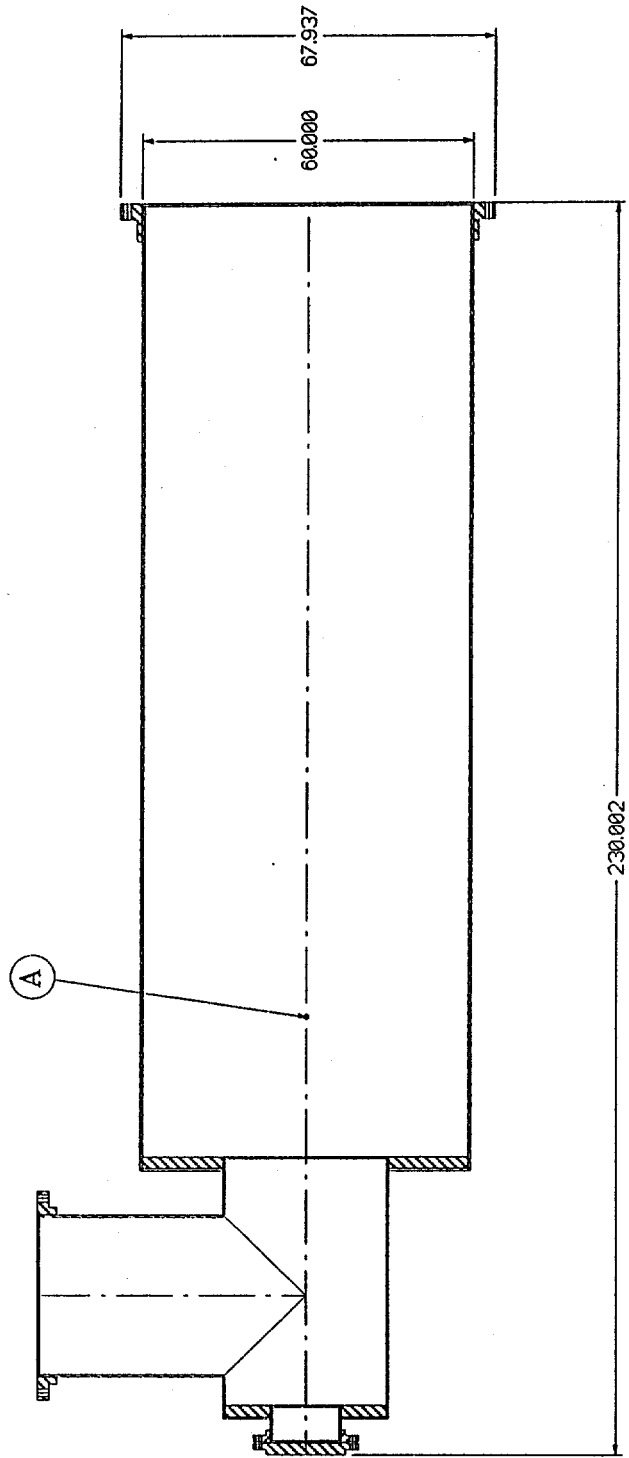
COUPLING 3/8" FULL C.S.



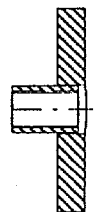
(A) CLOSE-UP

Unless otherwise specified the
 dimensions shall be in
 inches.
 : 1/8" for hole diameters
 : 1/16" for pin diameters

FIGURE 11: MIDDLE SECTION OF AGGLOMERATION CHAMBER

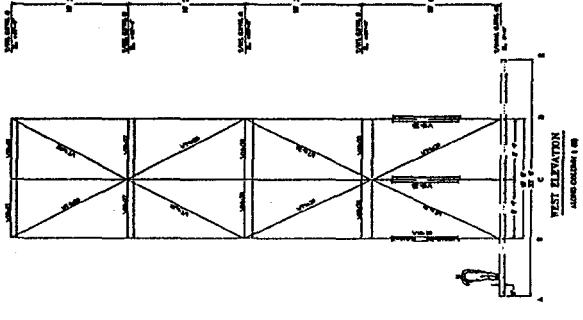
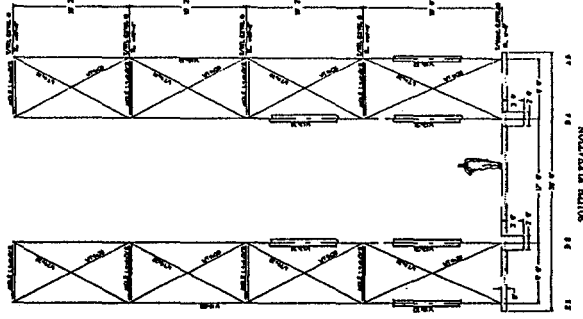
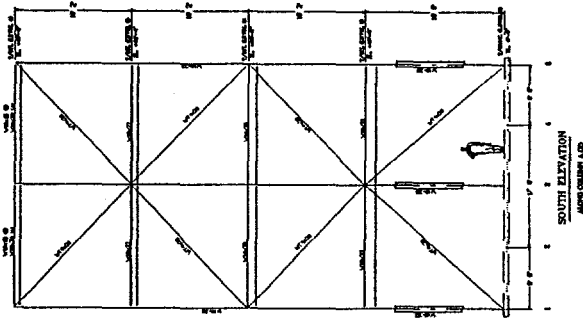
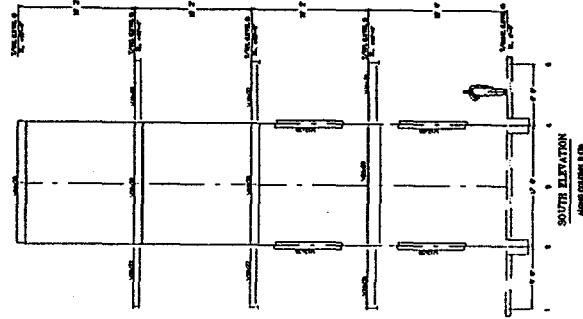
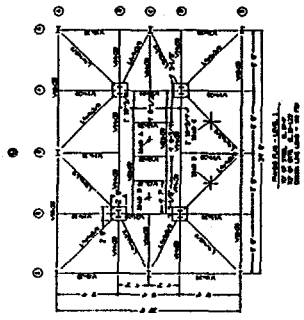
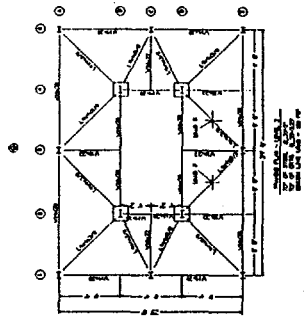
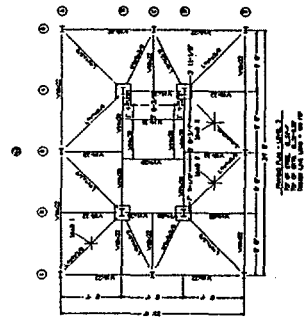
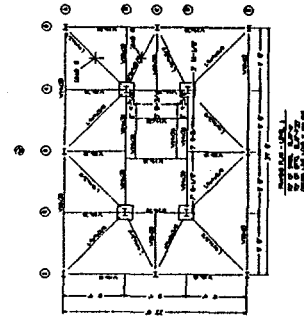


Unless otherwise specified the
 dimensions shall be in
 millimeters and fractions
 thereof shall be in
 decimal fractions of a millimeter



(A) CLOSE-UP

FIGURE 12: TOP SECTION OF AGGLOMERATION CHAMBER



COL.	A	B	C	D	E	F	G	H	I
SPAN	4.0	4.0	4.0	4.0	4.0	4.0	4.0	4.0	4.0
TOTAL									

FIGURE 13: STRUCTURE LAYOUT (DRAFT)

ITEM	QTY	QTY	DESCRIPTION	UNIT	QTY	TOT. WT.
1	1	1	WATER JACK ASSEMBLY	ASSEMBLY	4000	4000
2	1	1	LOW DENSITY REFRACTORY	REFRA.	2000	2000
3	1	1	HIGH DENSITY REFRACTORY	REFRA.	1000	1000
TOTAL QTY.					10000	

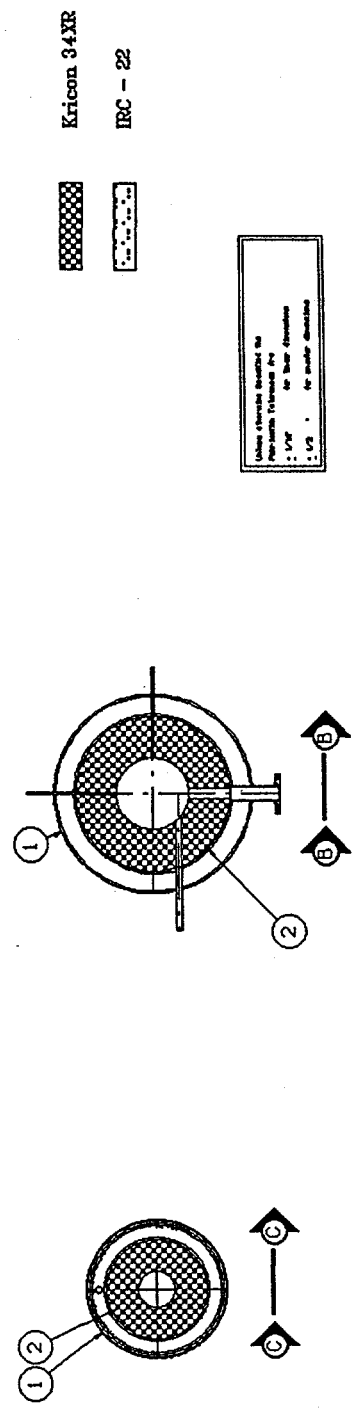
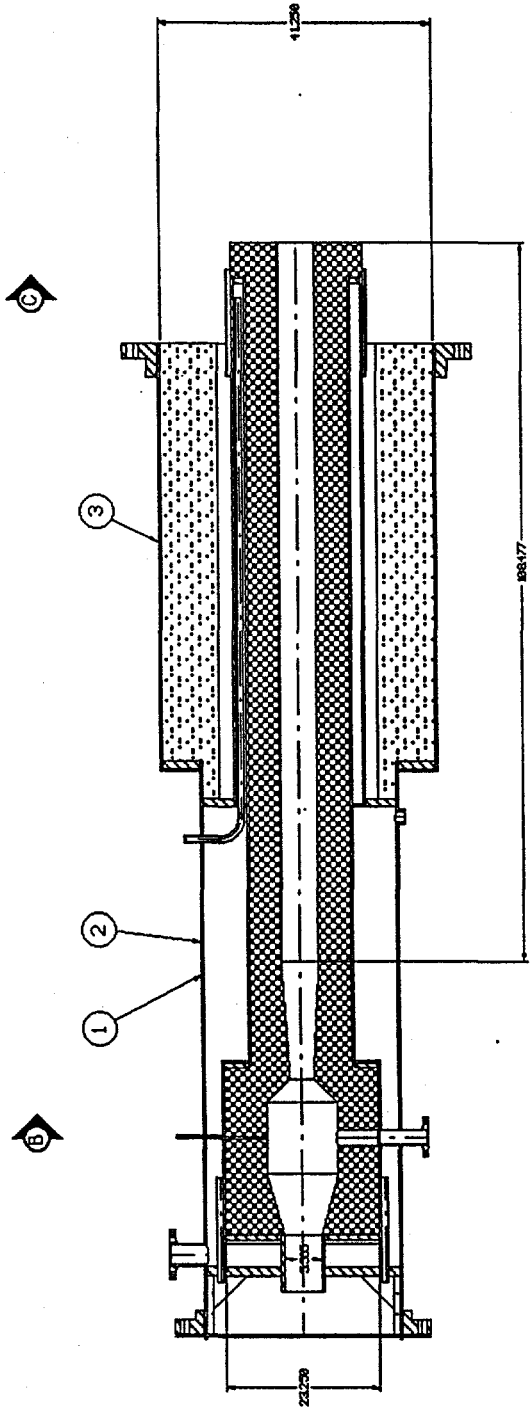


FIGURE 14: PULSE COMBUSTOR REFRACTORY

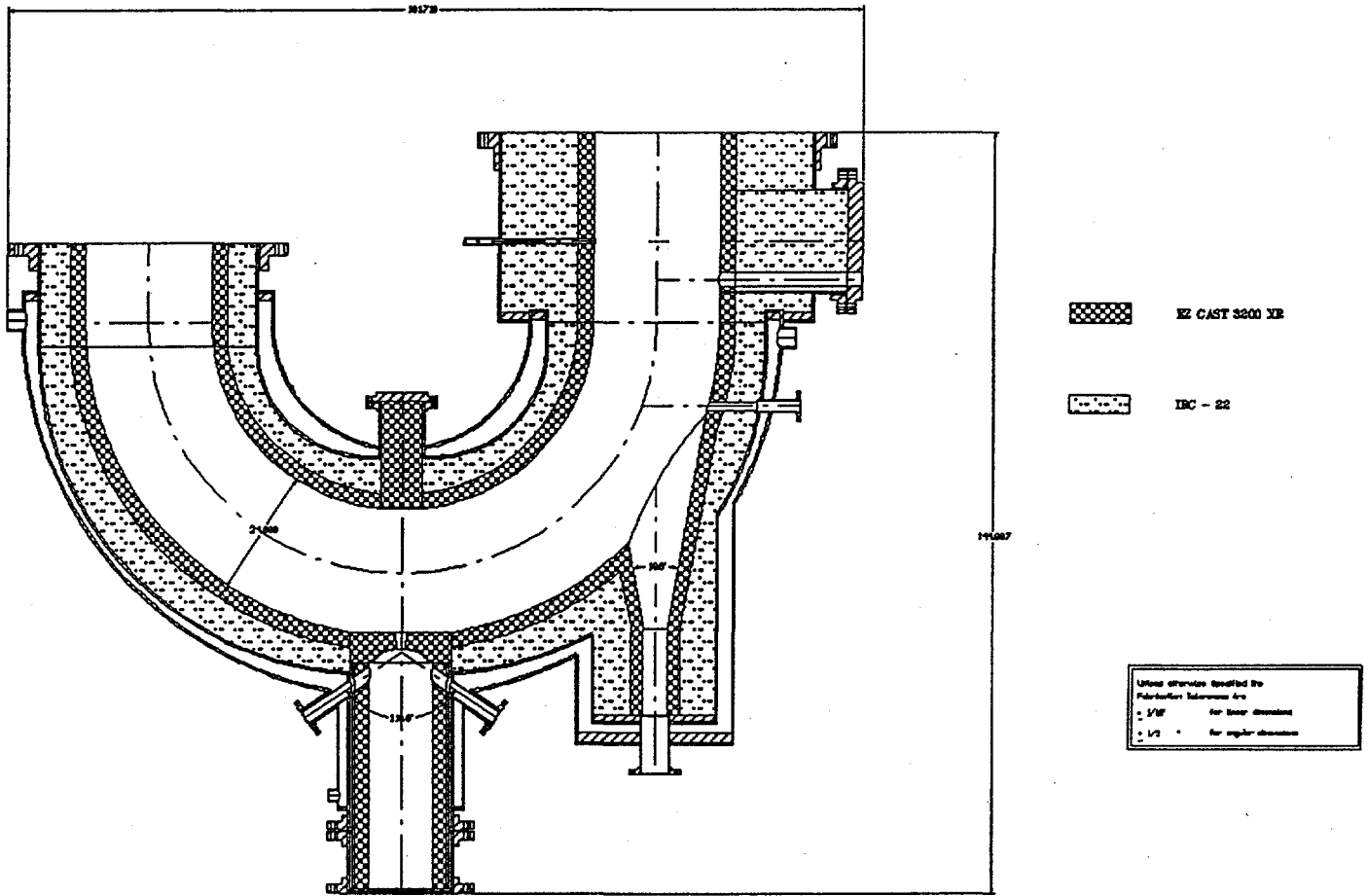
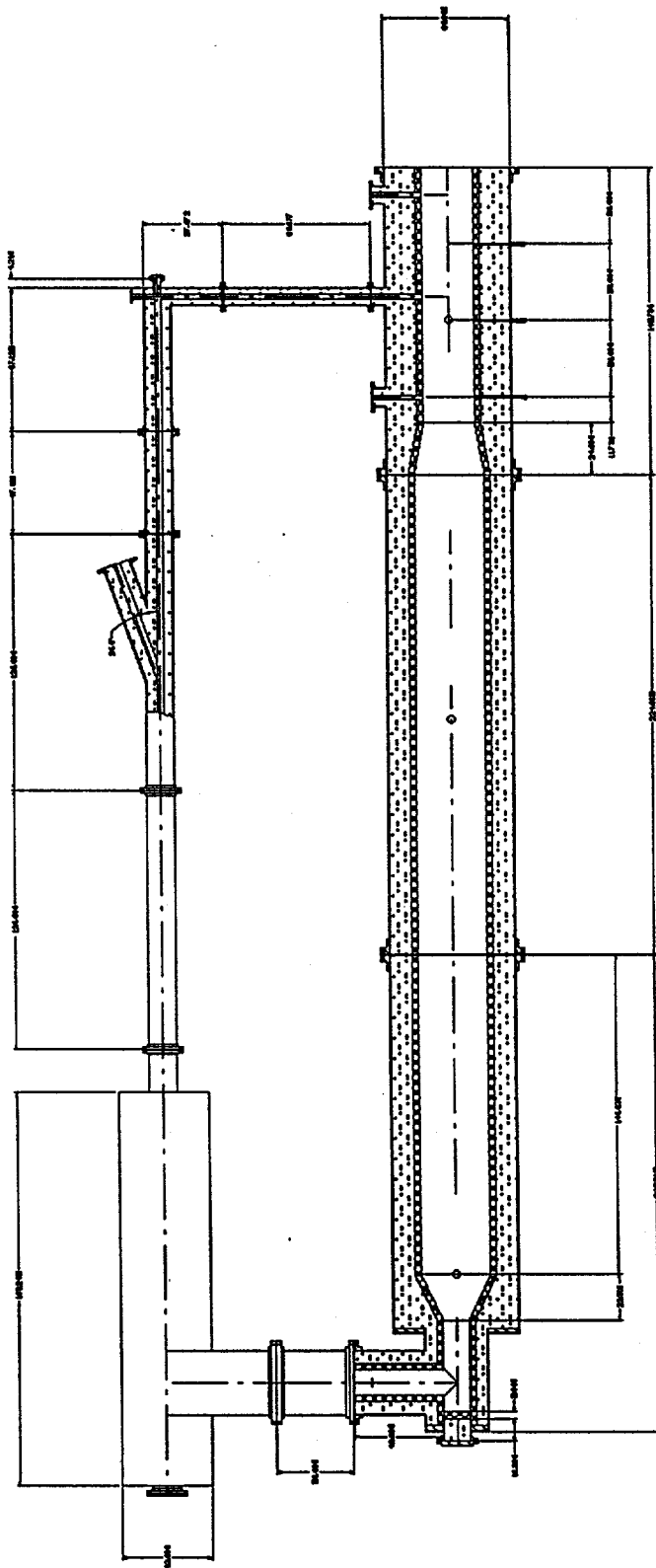


FIGURE 15: U-BEND SECTION REFRACTORY



KRICON 28XR

IRC 22

Unless otherwise specified, all
 materials shall conform to
 1. ASTM for their respective
 2. SPS for their respective
 3. SPS for their respective

FIGURE 16: AGGLOMERATION CHAMBER AND DIPLEG REFRACTORY

MTCI received quotes from three refractory subcontractors: Chiz Bros. Inc., Lynn Whitsett Corporation, and French Construction Services, Inc. Chiz Bros. Inc. was selected because they offered a warranty, have cooperative relationships with National Refractories & Minerals Company, and their cost bid was between each of the other respondents.

MTCI contracted for an independent design review of the preliminary structural design with Dr. Glenn Hazen of the Civil Engineering Department, Ohio University. Their review indicated some minor changes were required for the structure but that the concrete pad was totally inadequate. Changes to the pad are being made and will be re-submitted for analysis. The following is Dr. Hazen's analysis report:

Introduction

For this project we analyzed a four-story steel frame intended to support wind loads, mechanical piping, and a 100-psf live load. Also analyzed was a concrete pad intended to support the frame and all of its loads. All steel allowable loads were determined by allowable stress design as outlined in the AISC manual of steel construction, ninth edition. For the analysis of the frame, SAP90 structural analysis software was used. This software is based on the assumption of stresses only in the elastic range. The concrete pad was analyzed using procedures of the ACI building code for reinforced concrete (1992 revision).

Results

The preliminary design of this structure was logical and well carried out. However, there were problems with some of the members intended to carry significant loads. On each of the four levels, mid-span point loads ranging from 5 to 14 kips are placed on 4"x 4" x 3/8" angles. These members are too small to carry loads of this magnitude.

On the first level, W21 x 50 beams intended to carry the 96-kip load of a pipe were too small. On the top level, W10 x 15 beams also failed in flexure. Both beams were only marginally underdesigned.

The foundation on the other hand is extremely underdesigned. Many assumptions were made in the analysis of the slab but it seems obvious that it is far too weak to carry the loading.

Conclusions

The frame is well-designed and if the above discrepancies are corrected, the frame should be satisfactory for the intended purpose. The most significant problem is the direct loading of the angles. The loads either need to be moved to the joints of the connection or the member size significantly increased. The concrete slab, as stated above, is entirely too weak to carry the loads. No analysis was performed on the soil due to lack of information.

2.2 PENN STATE UNIVERSITY

WORK ON AGGLOMERATION OF SORBENT PARTICLES

Currently, work is being done on two different aspects. A small experiment is being conducted which seeks to verify the effects of an acoustic field on sulfation of large sized (~500 micron) sorbent particles. The sorbent particles will be suspended in an entrained flow reactor in an acoustic field and tests will compare sulfation results with and without sound. It is planned to verify the sorbent model predictions for long residence times (~60 seconds) and low temperatures (~800-900 C). The second part continues with the study on acoustic agglomeration.

There are many different ways in which transport of sorbent/coal particles in a combustor can be modeled. Since the physical impossibility of tracking every particle is manifest, a statistical approach will be adopted. A transport equation for the particle number density can be written for 2-D axisymmetric flows. Such a transport equation will account for convective as well as turbulent diffusive transport. Following the approach of Song,⁽¹⁾ and in the presence of an acoustic field, the transport equation can be suitably modified to account for acoustic agglomeration using an Acoustic Agglomeration Frequency Function, hereafter called AAFF. Although there is still a great deal of uncertainty about the precise mechanism that is responsible for acoustic agglomeration, the AAFF takes into account the agglomeration of individual particles and breakup of agglomerates in a statistical fashion. Hoffmann⁽²⁾ in his thesis describes the different mechanisms in a comprehensive review. Briefly, acoustic wave-particle interaction phenomena can occur due to linear (orthokinetic interaction, first order scattering interaction) or non-linear (radiation pressure force, mutual radiation pressure by scattered waves, or acoustic wake effects due to asymmetric flow fields around particles). Hoffmann, however, has pointed out that the acoustic wake effect is potentially a major contributor to the agglomeration phenomenon. Hoffmann derived an expression for the relative velocity of the two particles for a single orientation, i.e., the on-axis case, where the axis of the particles is in the same direction as the acoustic field. However, this is not enough, and we are trying to get an

approximate analytical expression for the relative convergent velocity for any arbitrary orientation. Further details will be forthcoming in the near future.

Song derived the AAFF for the orthokinetic and hydrodynamic contributions to the agglomeration frequency function. However, the hydrodynamic contribution consists of both the radiation pressure interaction and the acoustic wake interaction. Song disregarded any effects of the acoustic wake effect. Efforts are currently underway to obtain an agglomeration kernel based on the acoustic wake effect. To derive the AAFF based on the acoustic wake effect, the procedure outlined by Song will first be followed.

The procedure involves obtaining an expression for the relative convergent velocity between two particles due to the acoustic field for any arbitrary orientation. Once this expression is obtained using it in the expression for the acoustic agglomeration frequency function as shown by Song gives us the desired result.

It therefore appears possible to derive an AAFF which incorporates the effects of the phenomena mentioned above, whereby the transport equation for the particle number density has a source/sink term describing the interaction of particles of different/similar sizes with each other and the resulting breakup or agglomeration of that particle. While Song used a 1-dimensional transport equation, the current version will be 2- dimensional and axisymmetric.

References

- 1) Song, L., Modeling of Acoustic Agglomeration of Aerosol Particles, Ph.D Thesis, The Pennsylvania State University, 1990.
- 2) Hoffmann, T., Visualization of Particle Interaction and Agglomeration in an Acoustic Field, Ph.D Thesis, The Pennsylvania State University, 1993.

SECTION 3.0

PLANS FOR NEXT PERIOD

- Continue the design of the PDU.
- Continue the fabrication of the PDU.