

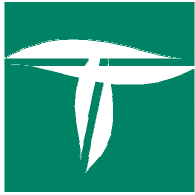
Marianne Mintz  
Stephen Folga  
John Molburg  
Jerry Gillette

10<sup>th</sup> Annual NEMS/AEO Conference  
March 12, 2002

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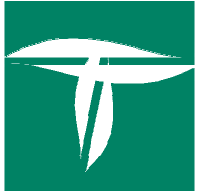


***This work was sponsored by the Department of Energy's Office of Advanced Automotive Technologies. The authors acknowledge the support of Bob Kirk, Ed Wall, Pete Devlin and Steve Chalk.***



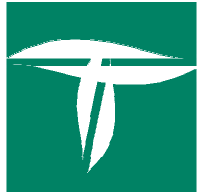
## ***Boundaries of This Presentation***

- **Long term (2030)**
- **Light-duty vehicles**
- **Capital costs of fuel production and distribution infrastructure (excluding exploration)**
- **Technically feasible propulsion systems with potential for substantial improvement over conventional ICE fuel efficiency (hybrids and fuel cells)**
- **Natural-gas-based motor fuels (methanol, LNG, Fischer-Tropsch diesel (FTD) and hydrogen)**

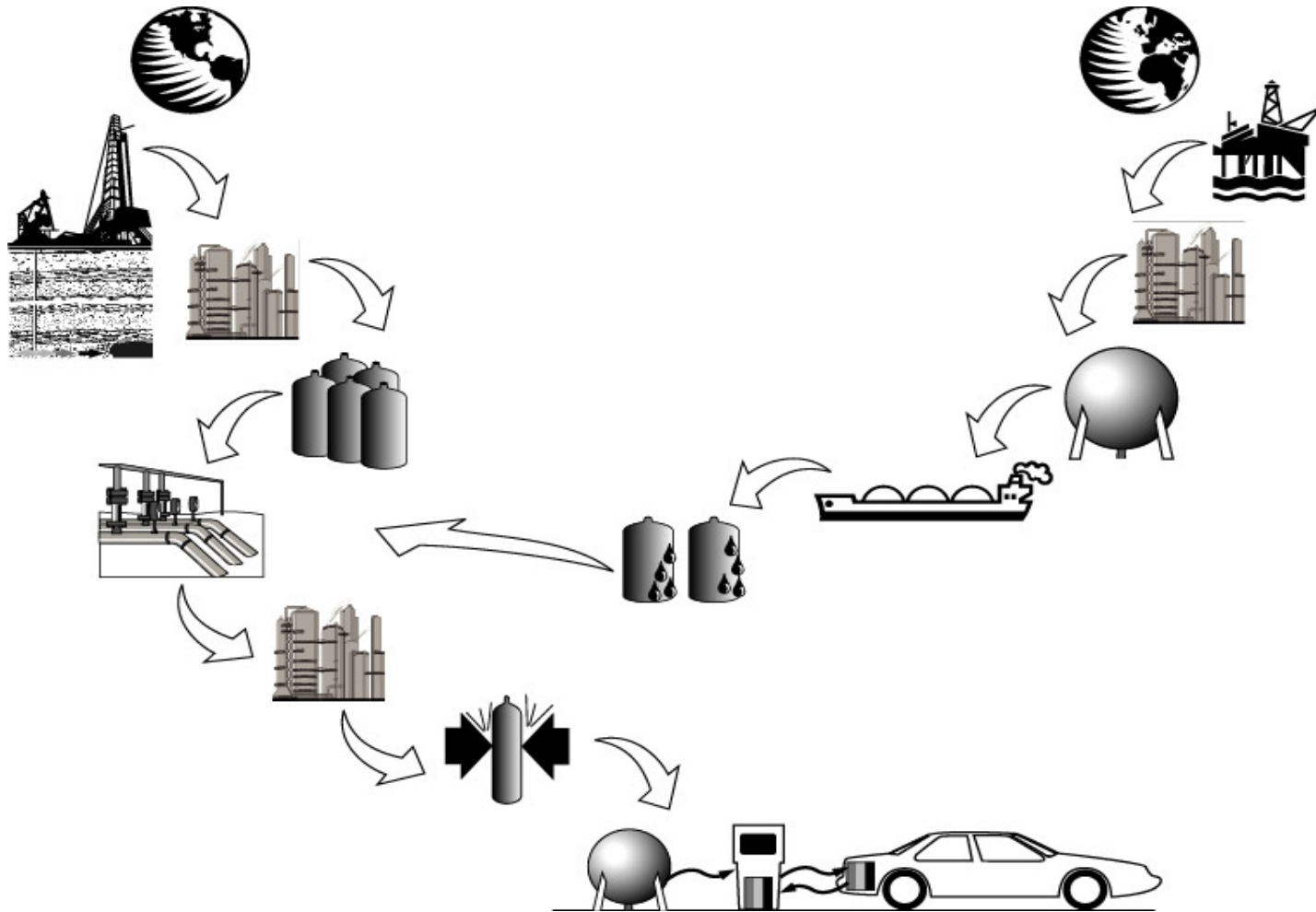


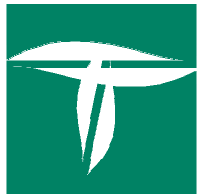
# ***Cost Modeling Was Conducted Via a Five-Step Process***

- **Define paths**
  - North American (NA) or non-North American (NNA) natural gas
  - NG production, compression, storage and transport; conversion to alternative fuel, transport and dispensing
- **Determine “tank-in” fuel requirement**
  - Market penetration
  - Vehicle and pathway efficiencies
- **Size pathway components**
- **Estimate component costs**
- **Calculate pathway costs (NICC model)**

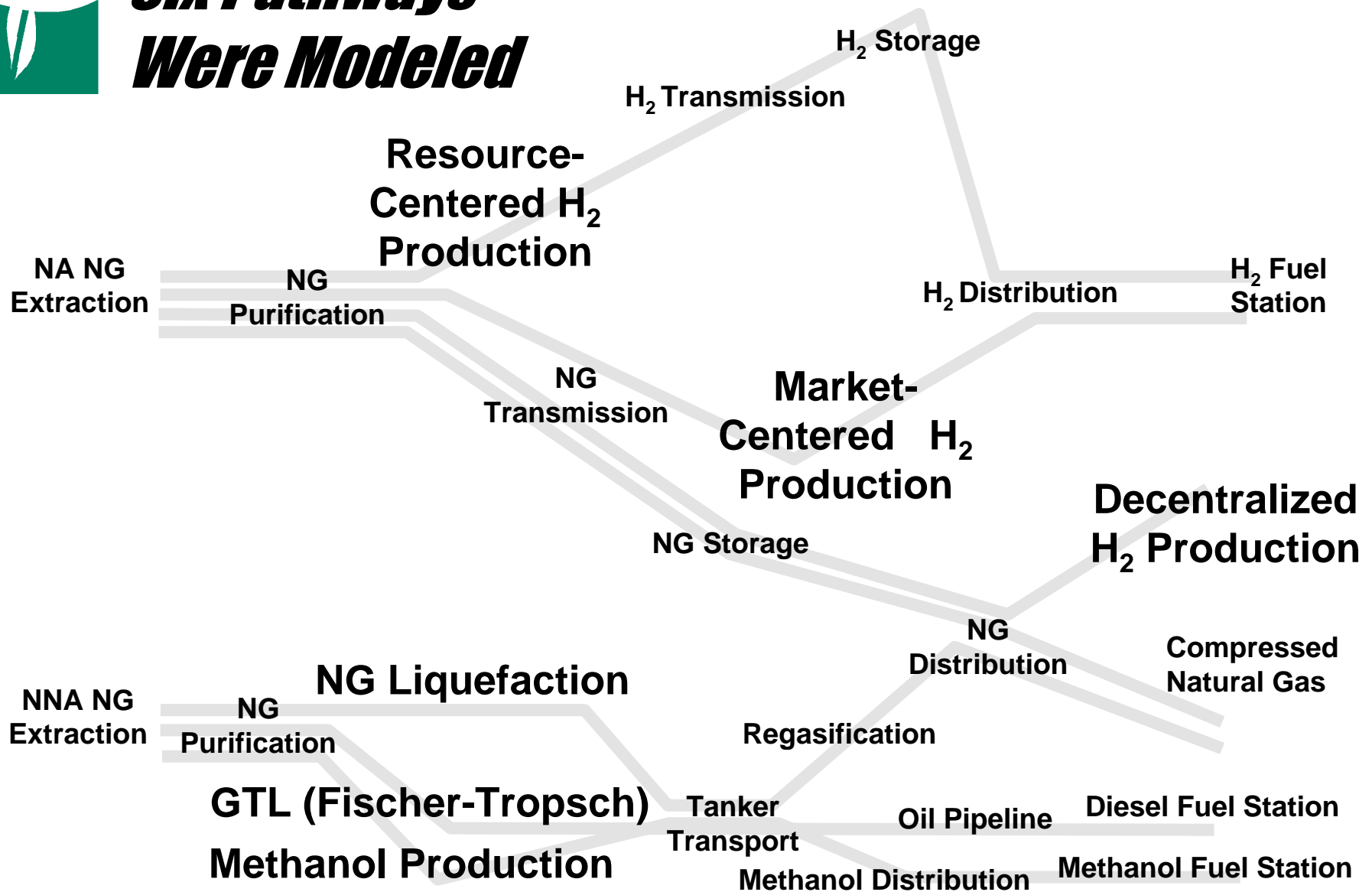


# ***Natural Gas-Based Fuels Could Take Several Paths from “Well” to “Tank”***

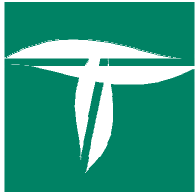




# *Six Pathways Were Modeled*

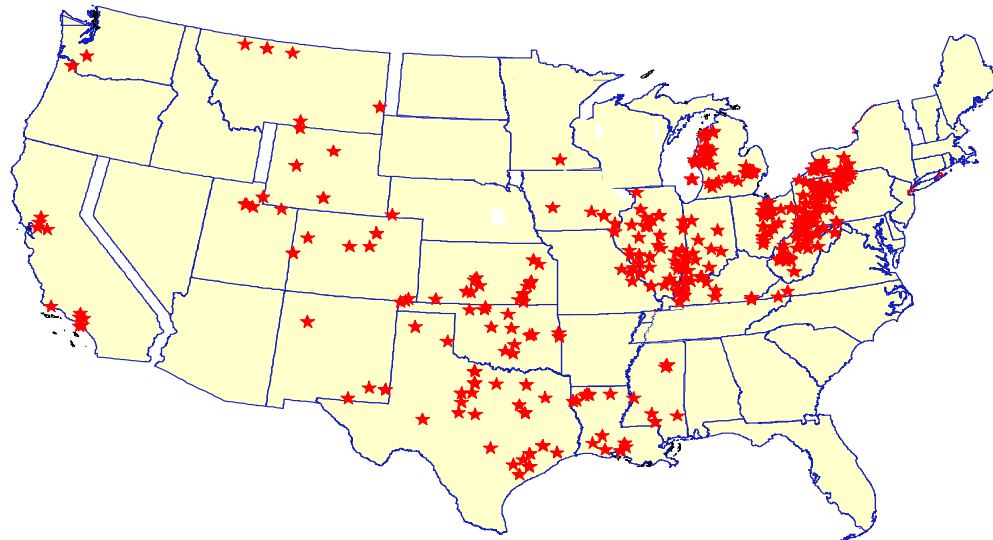


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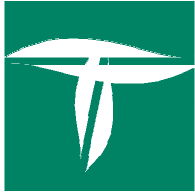


# ***All Pathways Include Underground Storage***

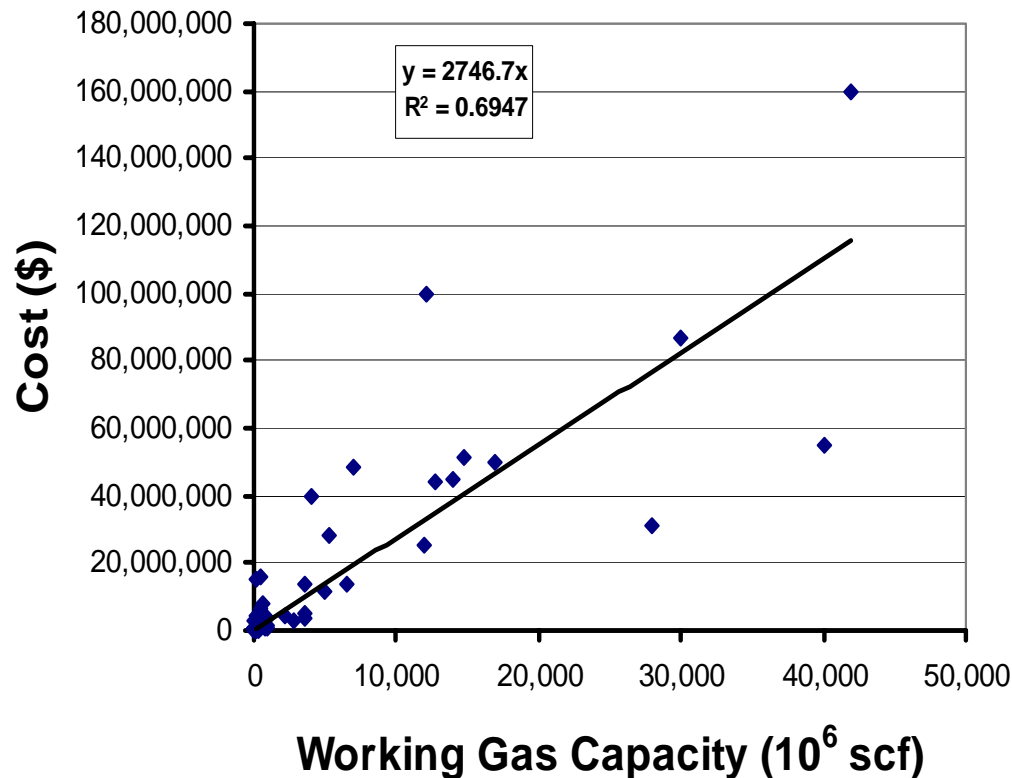
**At the end of 1998 there were 410 underground natural gas storage sites in the U.S.**



*With 76 Bcf per day of Withdrawal  
Capability and 3,933 Bcf of Working  
Gas Capacity*

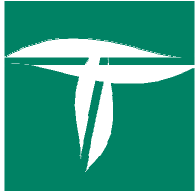


# ***The Cost of Underground Storage of Natural Gas Is a Function of Working Gas Capacity***

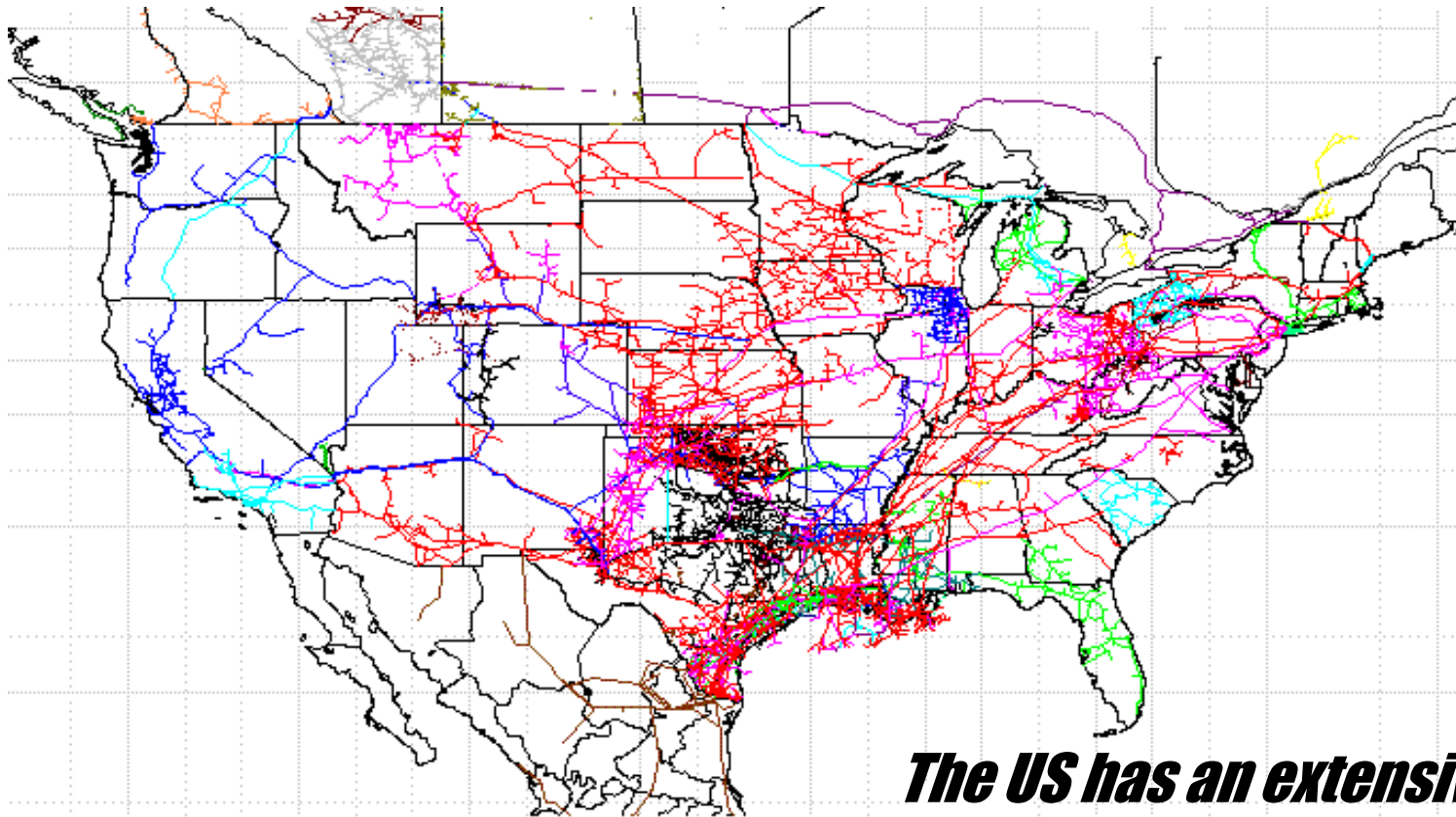


- **Linear relationship for underground storage (projects with 2001-04 completion, 1999\$)**
- **Working gas capacity per field:  $5 \times 10^9$  scf**
- **Unit O&M cost: \$0.224 per  $10^3$  scf delivered (Young Storage Field, CO)**





# ***All Pathways Require Additions to the Existing Natural Gas Transmission Infrastructure***



***The US has an extensive  
in-place NG transmission  
infrastructure .....***

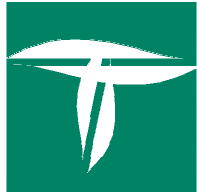
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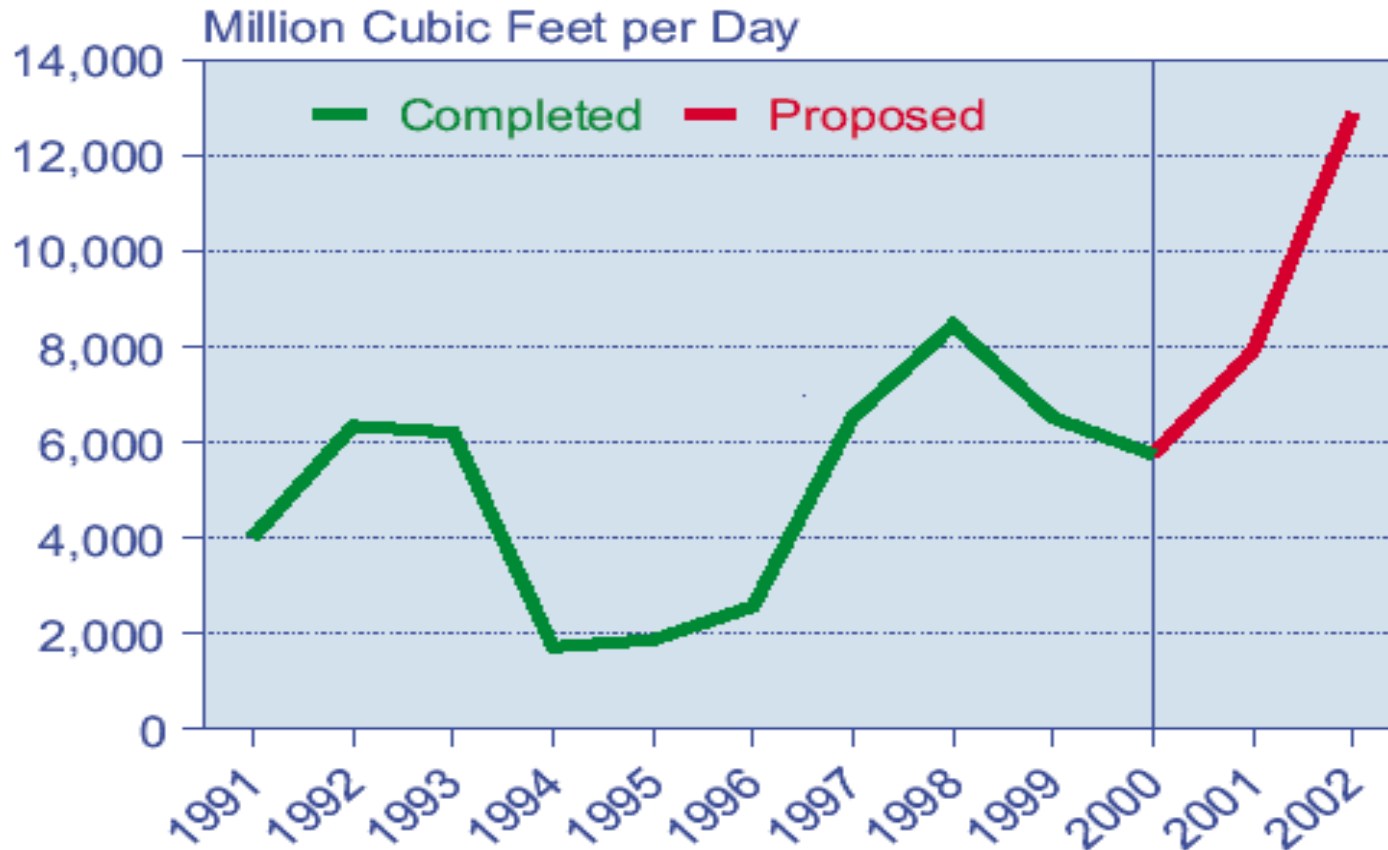


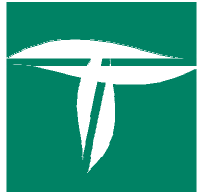
## ***And a Track Record of Continually Expanding Transmission Capacity***

- **New pipelines**
- **Additional compression**
- **Looping**
- **All of the above**

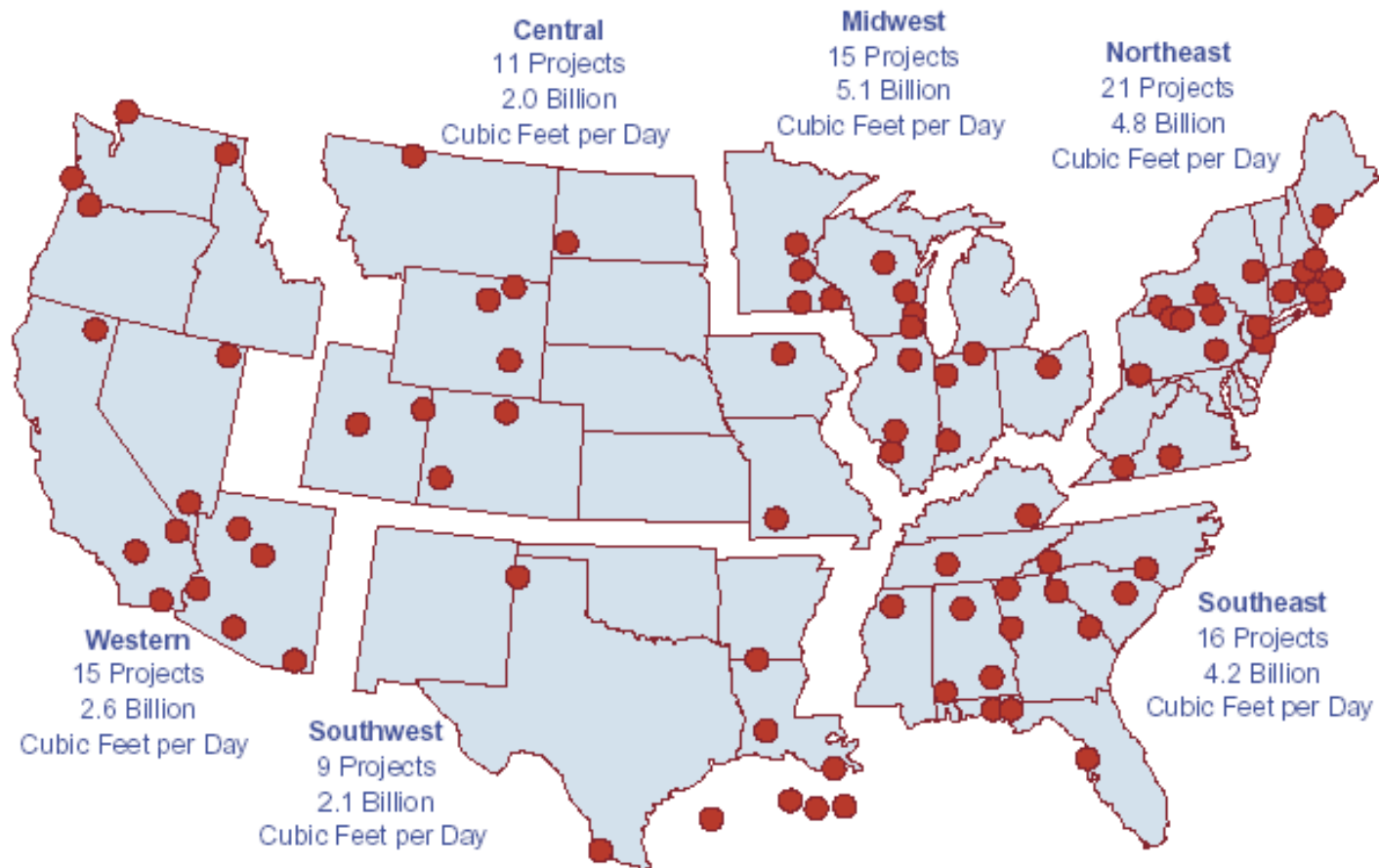


# ***1991-2000 Annual Capacity Additions Averaged > 4 x 10<sup>9</sup> scfd; Proposed Additions Are Higher***

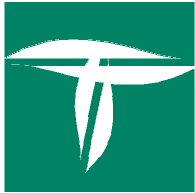




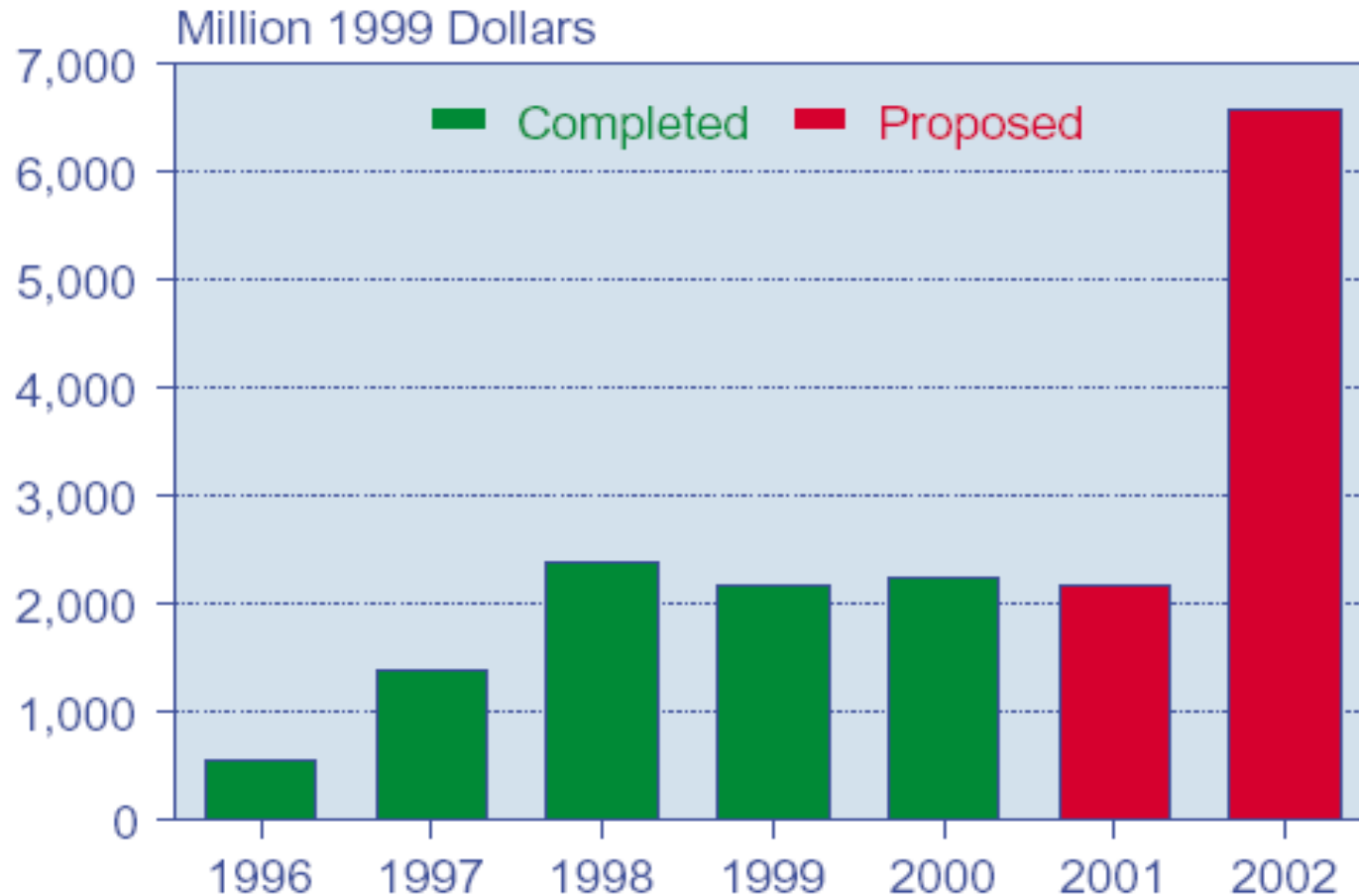
# ***Yearly Capacity Additions Could Rise to $10 \times 10^9$ scfd in 2001-2002***



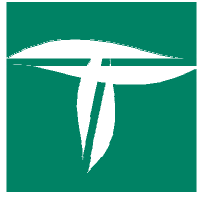
Source: Energy Information Administration, EIAGIS-NG Geographic Information System, Natural Gas Proposed Pipeline Construction Database (as of March 2001).



## ***According to EIA, Over \$6 Billion Will Be Spent on Pipeline Expansion in 2002***

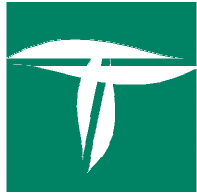


Source: Energy Information Administration, EAGIS-NG Geographic Information System, Natural Gas Proposed Pipeline Construction Database (as of March 2001).



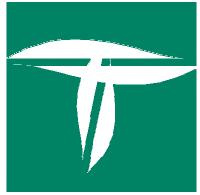
## ***Expansion Reflects Shifts in the Structure of the Industry and Its Resource Base***

- **Increased production in deep-water Gulf of Mexico and in western and offshore eastern Canada**
- **Reduced production in mature provinces**
- **Shippers seeking greater access to alternate sources of supply**
- **Producers seeking greater access to non-traditional markets (market integration)**
- **Increased use for power generation with resulting shifts in seasonal demand patterns**

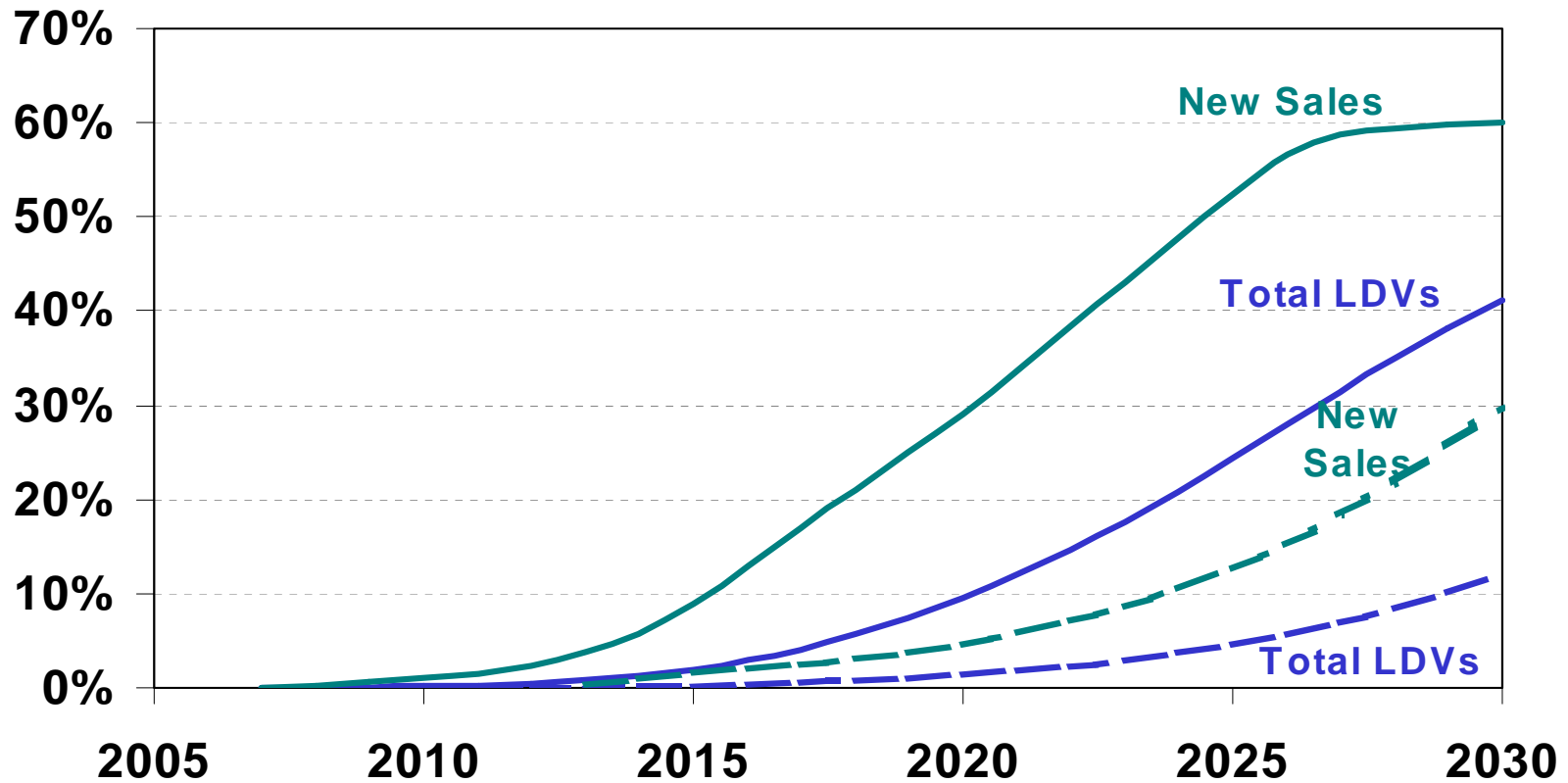


## ***But Given the Scale of Motor Fuel Demand, Is It Reasonable to Expect Additional Expansion?***

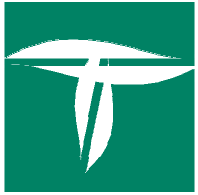
<b>NG System Component</b>	<b>Capacity Additions</b>	<b>Unit Cost (10<sup>6</sup>)</b>	<b>Capital Cost (10<sup>9</sup>)</b>
<b>Pipelines</b> <ul style="list-style-type: none"><li>•Transmission</li><li>•Distribution</li></ul>	<b>6000 mi</b> <b>630,000 mi</b>	<b>\$1.5/mi</b> <b>\$0.1-0.2/mi</b>	<b>\$9</b> <b>\$85</b>
<b>Underground Storage</b>	<b>185</b>	<b>\$13.7</b>	<b>\$2.5</b>
<b>Compressor Stations</b>	<b>38</b>	<b>\$12</b>	<b>\$0.5</b>
<b>NG Throughput</b>	<b>6 x 10<sup>12</sup> scf</b>	<b>NA</b>	<b>NA</b>



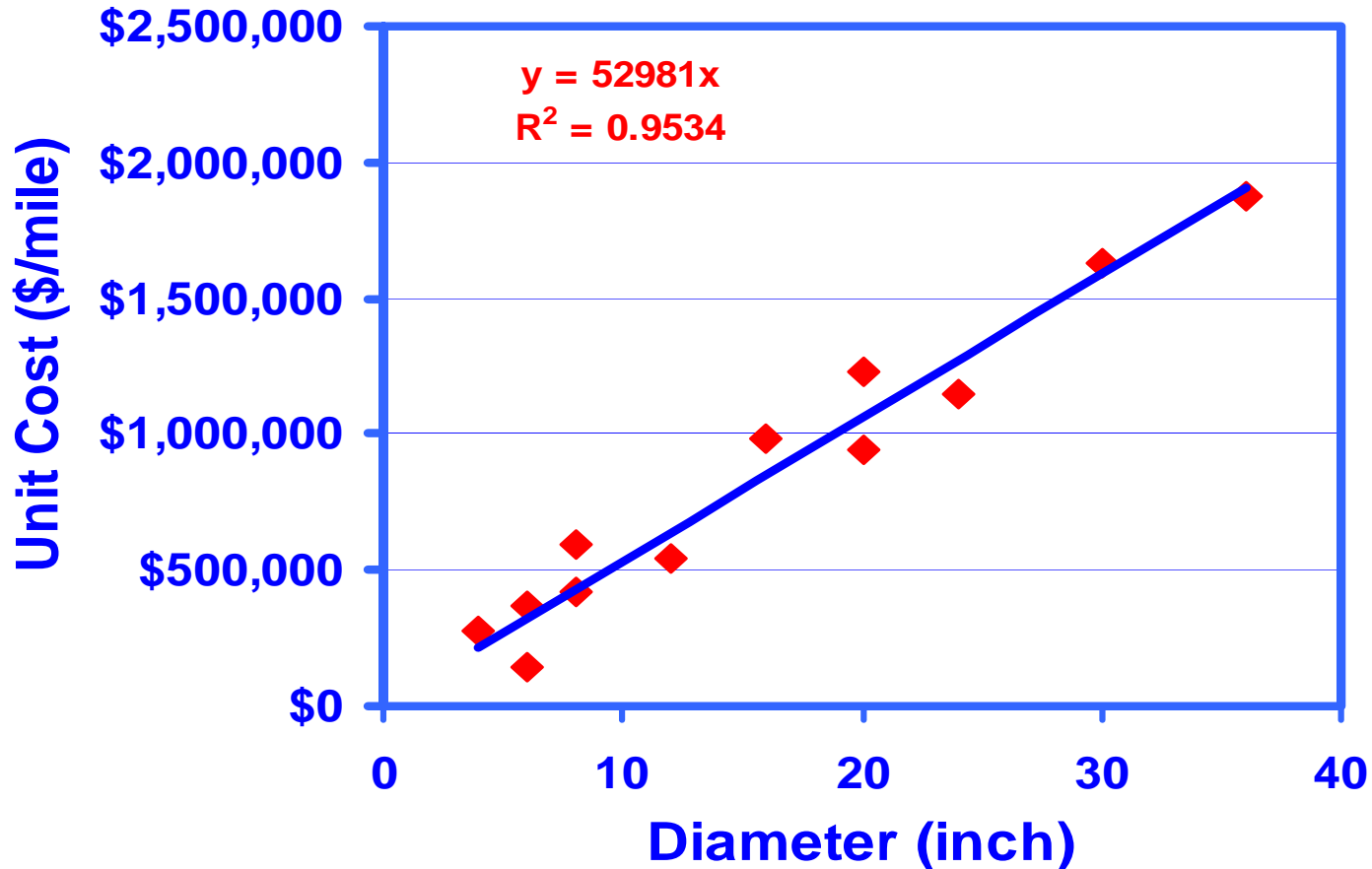
# ***Two Market Penetration Cases Were Modeled***

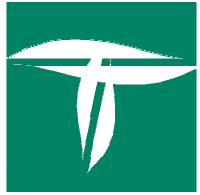




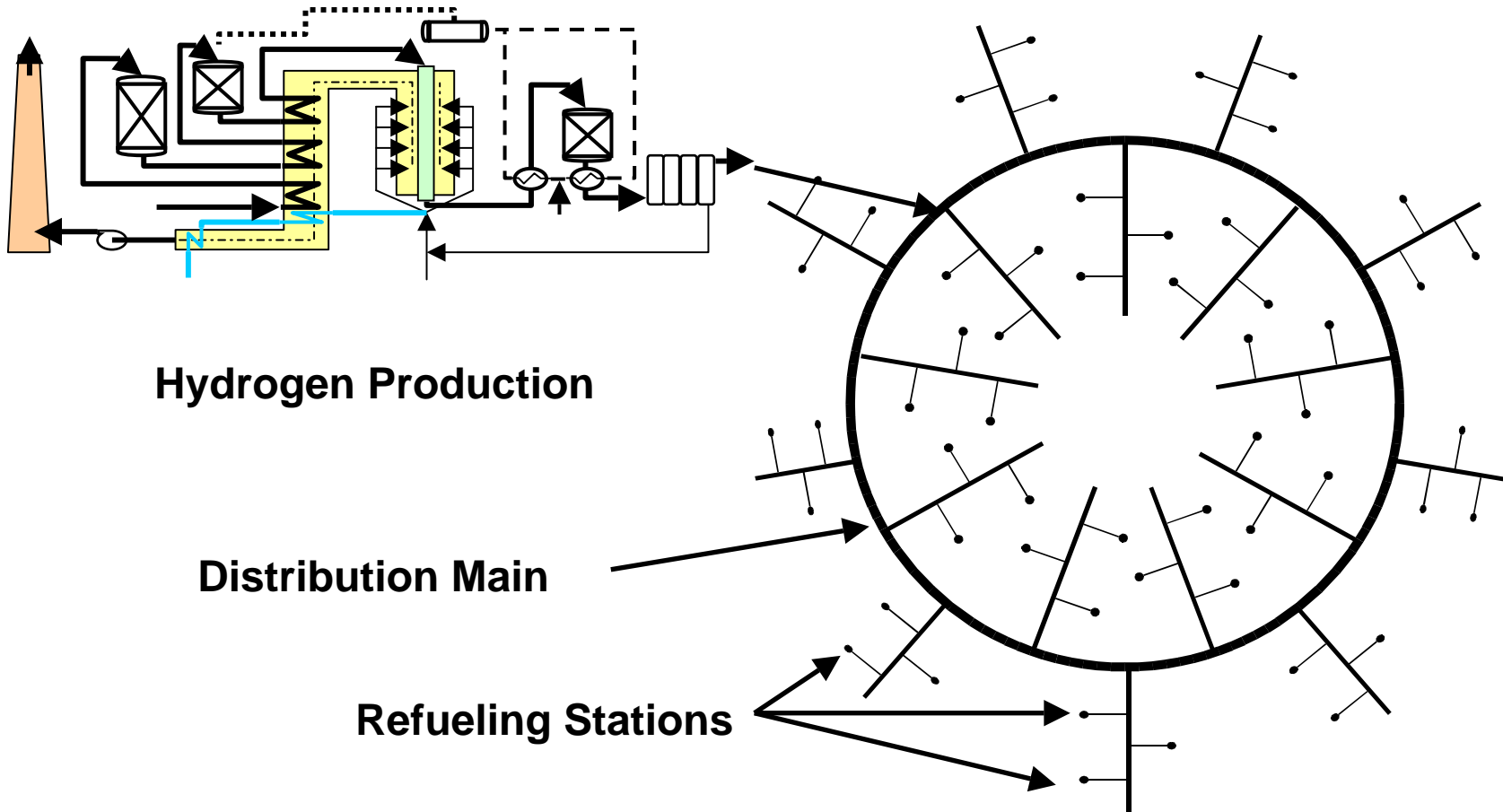


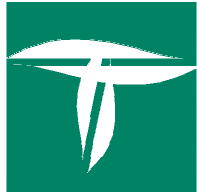
# ***Unit Cost of Natural Gas Transmission Pipelines Is a Function of Diameter***



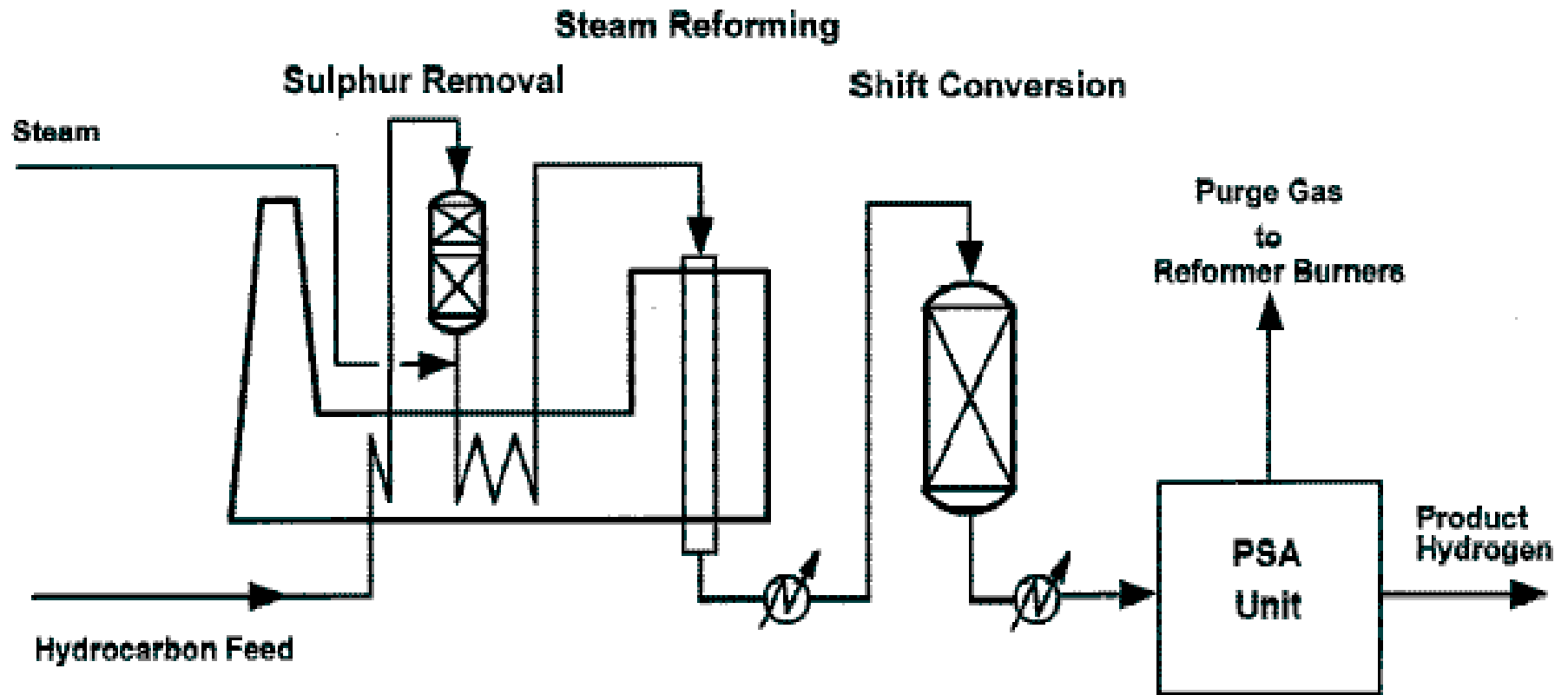


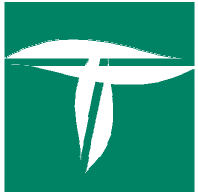
# ***Conceptual Representation of Hydrogen Pipeline Loop Supporting Local H<sub>2</sub> Delivery***



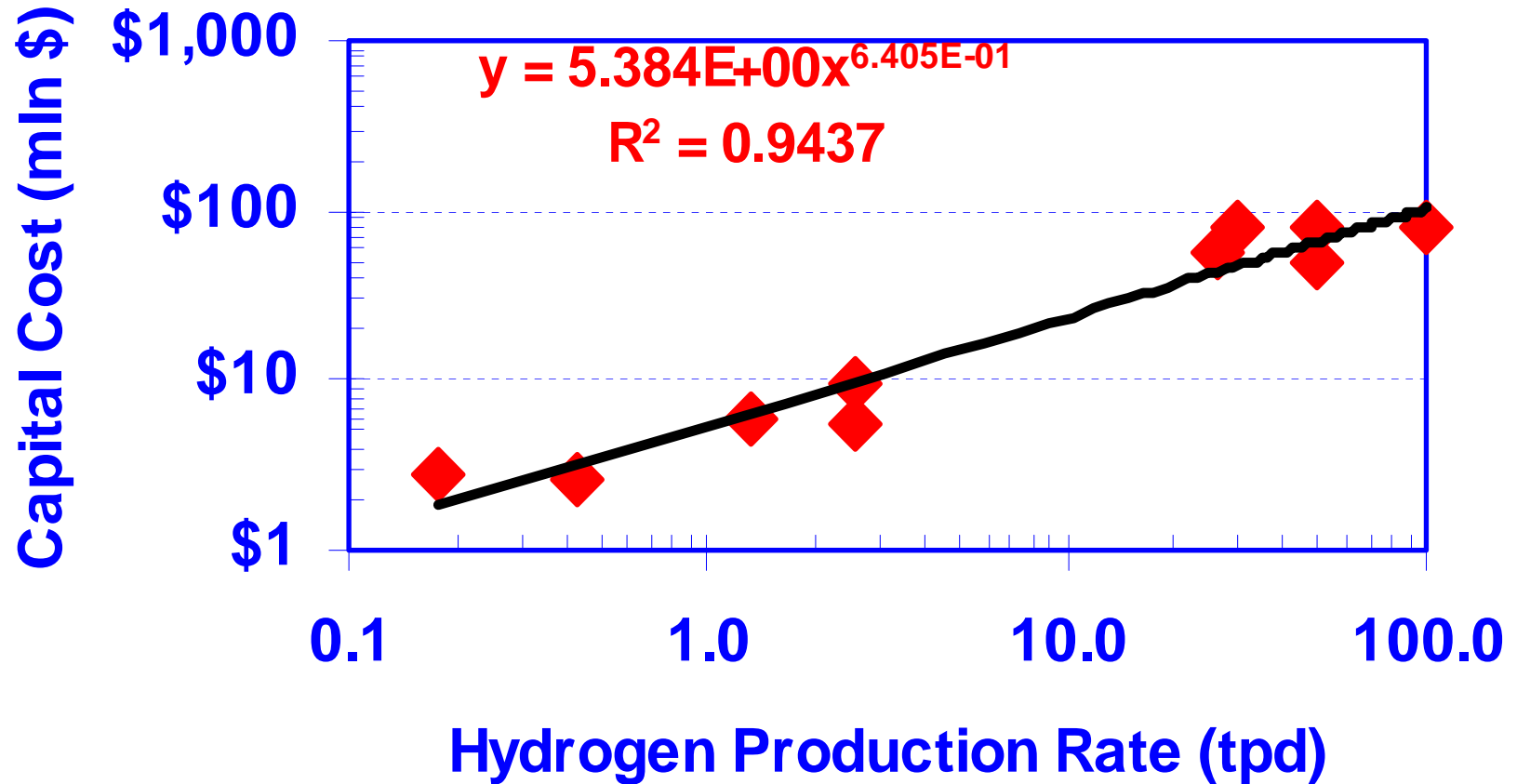


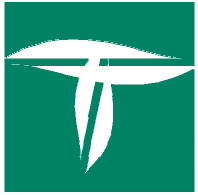
# ***Steam Reforming Inputs Are Water and Hydrocarbon Feedstock; Outputs Are Hydrogen and Purge Gases***



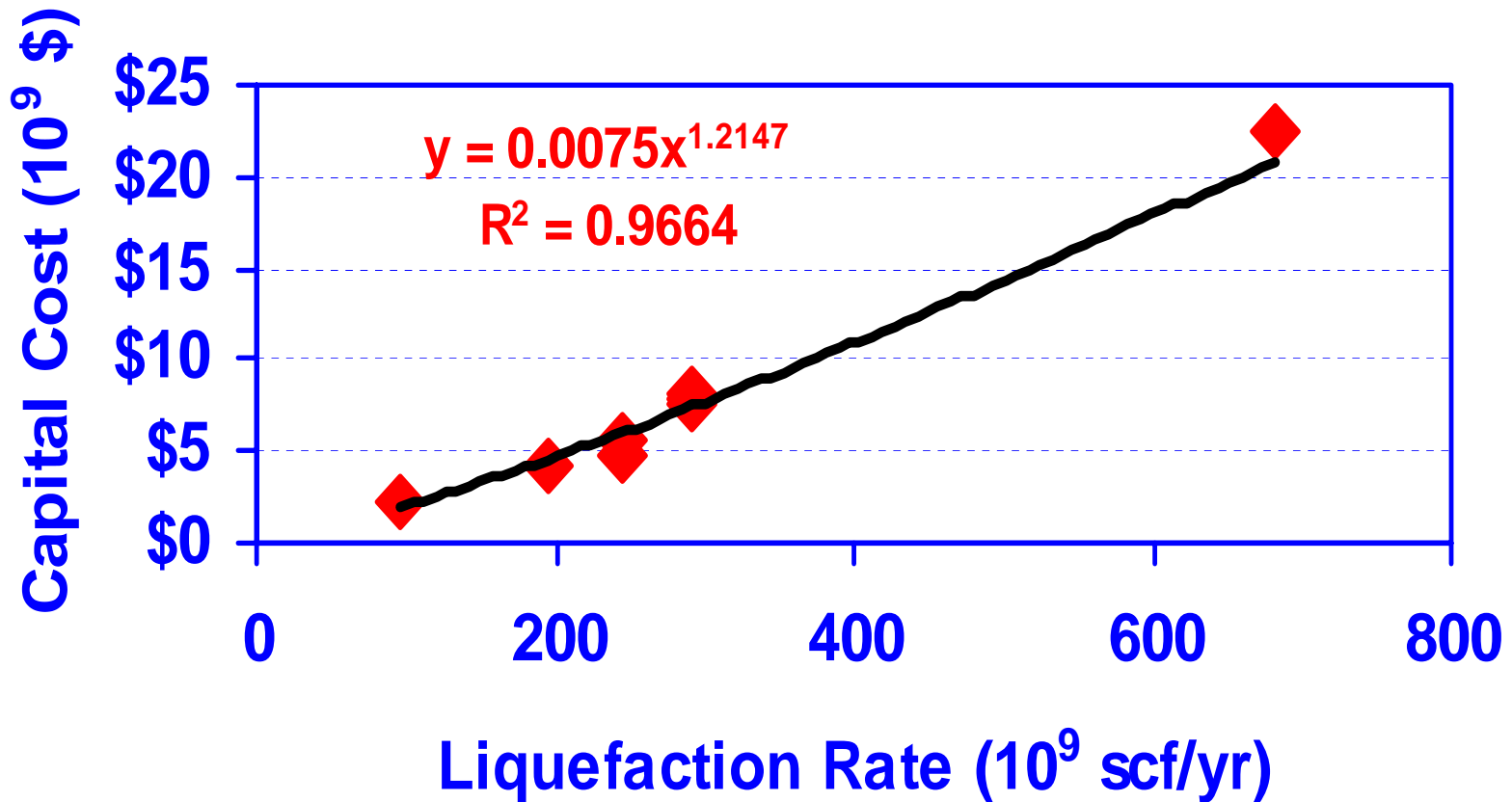


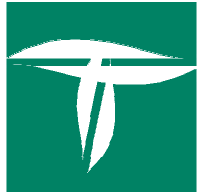
# ***Current SMR Plants Have Large Economies of Scale***





# ***Capital Cost of LNG Liquefaction Is a Function of Liquefaction Rate***

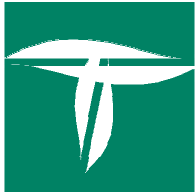




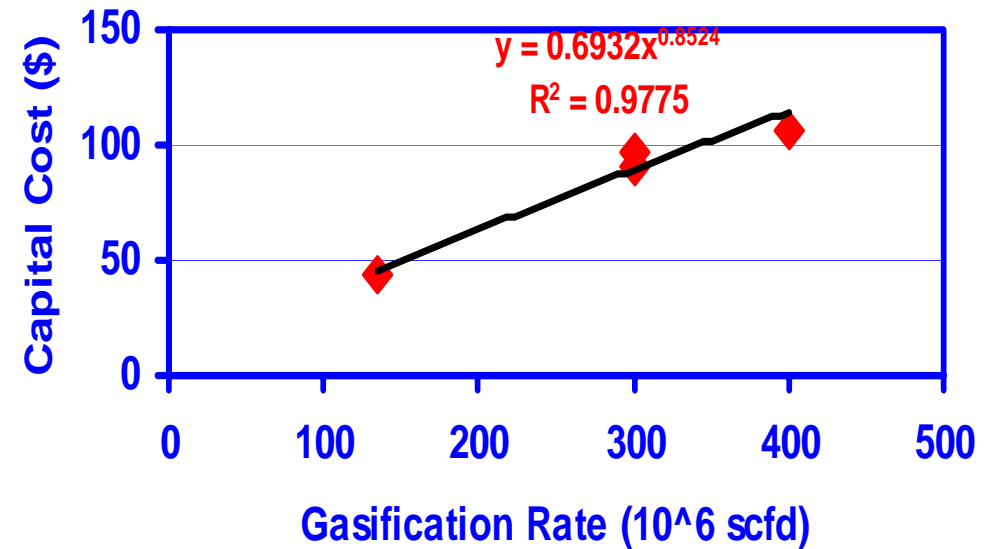
## ***Once Liquefied, Non-North American Natural Gas Is Shipped to LNG Terminals***

- **Capacity of 138,000 m<sup>3</sup> with four independent spherical tanks**
- **Effective lifespan 30-40 years**

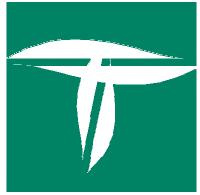




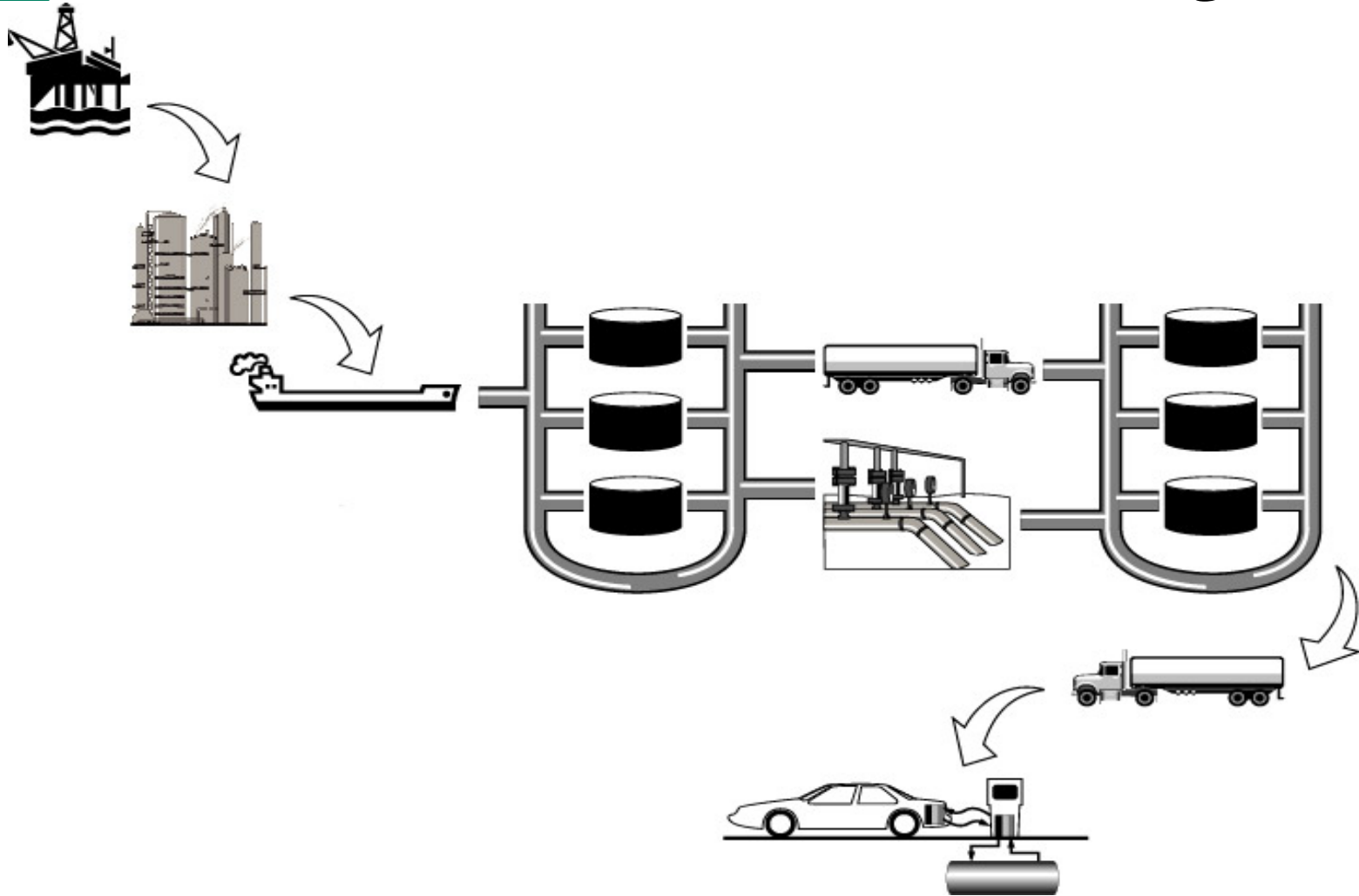
## *Characteristics of LNG Terminals*



- **Capital Cost: \$127,000,000**
- **Annual Capacity Factor: 90%**
- **Capacity: 450 x 10<sup>6</sup> scfd**
- **Unit O&M Cost: \$0.30/10<sup>6</sup> Btu**



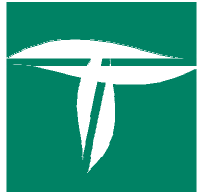
# ***Methanol and FTD Move by Truck or Pipeline from Ports to Terminals and Refueling Stations***



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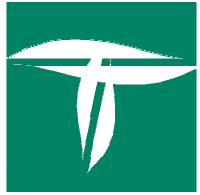
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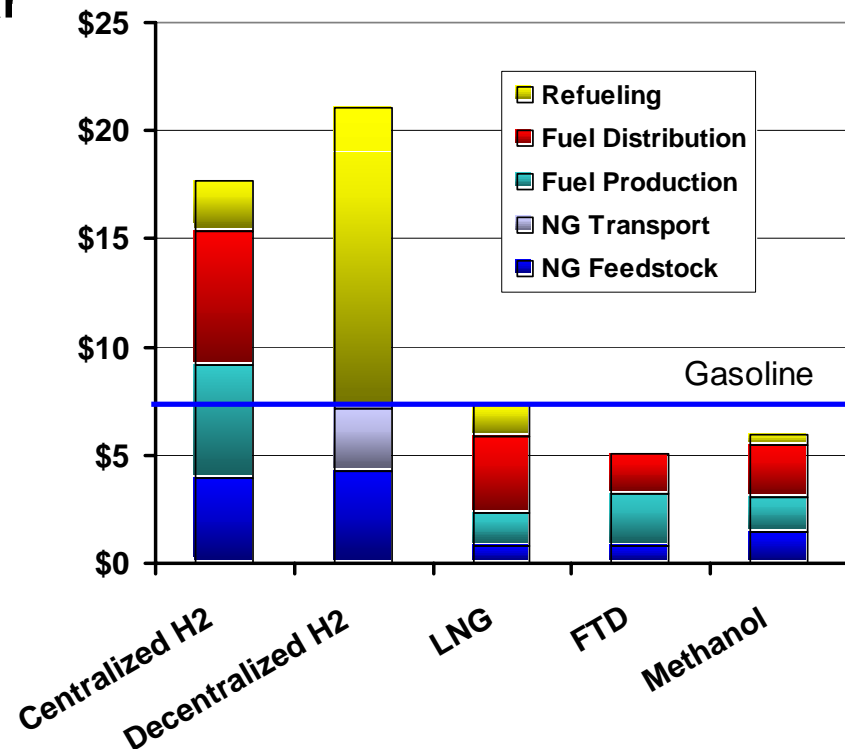
# ***“Tank-In” Fuel Requirement Is a Function of MPGE and Market Penetration***

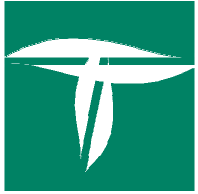
<b>Pathway</b>	<b>Engine Technology</b>	<b>MPGE</b>	<b>High Penetration</b>
<b>Hydrogen</b>	<b>FCV (on-board H<sub>2</sub>)</b>	<b>55</b>	<b>4.8 x 10<sup>9</sup> GJ (4.5 Q)</b>
<b>LNG</b>	<b>ICE</b>	<b>27.5</b>	<b>9.5 x 10<sup>9</sup> GJ (9.0 Q)</b>
<b>Methanol</b>	<b>FCV (on-board reforming)</b>	<b>41.2</b>	<b>6.4 x 10<sup>9</sup> GJ (6.1 Q)</b>
<b>FTD</b>	<b>Hybrid</b>	<b>38.5</b>	<b>6.8 x 10<sup>9</sup> GJ (6.4 Q)</b>



# ***Excluding Profit and Taxes, Unit Cost of NG-Based Fuels Varies from \$5 to \$21/GJ***

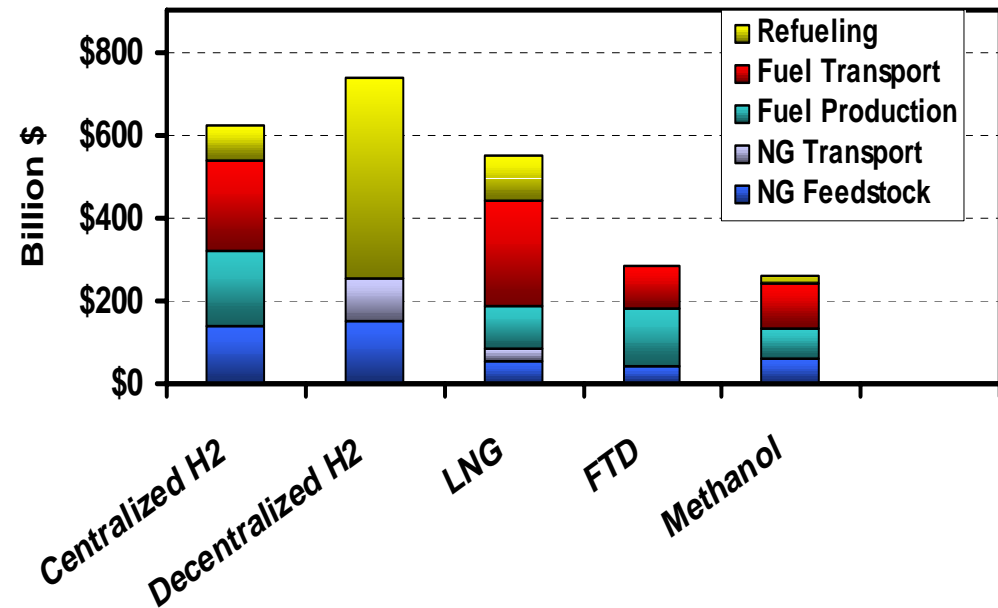
- For all pathways, hydrogen is far more costly than LNG, FTD or methanol (\$2.00 vs.\$0.60-0.80/GGE)
- FTD is the lowest cost alternative, largely because it requires the least infrastructure
- Low-cost, non-North American feedstock makes LNG, FTD and methanol less costly
- Reformers and pipelines further increase hydrogen cost

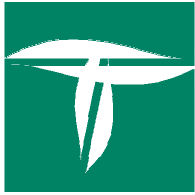




## ***Total Infrastructure Costs Are Highest for Hydrogen; Lowest for FTD and Methanol***

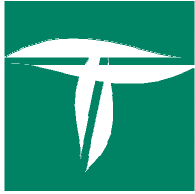
- Relatively lower mpge, LNG delivery volumes and infrastructure cost.
- Higher relative efficiency of hydrogen-fueled vehicle reduces ratio of total cost relative to unit cost to about double
- For all three hydrogen pathways, total cost is \$600-\$700 billion; FTD and methanol are about half.





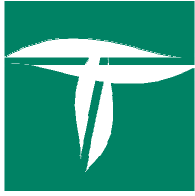
## ***Some Conclusions:***

- **With current technologies, on a well-to-tank basis, the unit cost of hydrogen is likely to be 2-3 times that of gasoline.**
- **To offset this, the mpge of hydrogen-fueled vehicles must be more than double gasoline.**
- **With current technologies, the hydrogen delivery infrastructure to serve 40% of the light duty fleet is likely to cost over \$600 billion.**
- **With low-cost feedstock and use of in-place infrastructure, FTD is competitive with gasoline.**

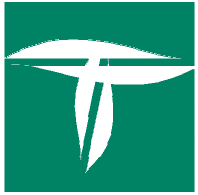


## ***Conclusions (cont'd)***

- **With current technologies, scale economies are large for centralized hydrogen production; small for decentralized**
- **H<sub>2</sub> transport and production are the largest components of all paths examined, hence appropriate focus for cost reduction.**



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## ***Next Steps: Several Additional Technologies and Fuel Options Should Be Examined***

- **Additional LNG alternatives, including station reforming and hybrid vehicles.**
- **Mixed cases, incorporating more than one pathway and targeted to market niches that exploit relative advantages.**
- **Additional hydrogen production options, including high-temperature thermochemical water splitting, methane pyrolysis and coal gasification**
- **Transition issues**