SECA Fuel Cells for Larger Applications

Jan Thijssen

Arthur D Little

3rd Annual SECA Workshop, Washington, DC, March 21-22, 2002

- Background & Objectives
- Methodology
- Results:
 - System design
 - Performance
 - Cost
- Conclusions



Application of stack modules to larger capacity applications is key to SECA's strategy.

- Develop ~5 kW SOFC modules for mass-customization
- Small-capacity applications (1-5 stacks), including:
 - Residential / light commercial DG
 - Auxiliary power for vehicles
 - Remote power
- Larger capacity applications:
 - Large commercial / industrial DG (10-1000s stacks)
 - Sub-station level DG and central generation (synergy with Vision21 program)
- How to scale-up to hundreds of kW or MW?

SECA wanted to understand the issues involved in scaling up to 100-kW to 1-MW systems.

Objective: to assess whether and how SECA stack modules can be integrated into a 250 kWe plant.

- Develop thermodynamic design, system lay-out, performance estimate, and cost estimates
- SOFC stack:
 - Use 5 kW planar SOFC modules *
 - Combine into super-modules
 - Implications for electric interconnection of the units?
 - Implications for manifolding?
- Balance of plant:
 - Determine scale and integration
 - Impact of scale-up on system performance and cost?
- Simple-cycle operation

We developed a conceptual design for a 250-kW $_{\rm e}$ distributed generation system SOFC.

System Specifications	Assumptions	
 System output: 250-kW_e net @ 380V 3-phase AC Electrical system efficiency >50% (LHV) Availability >99% T_{Surface} < 45°C High production volume (10,000 units per year) 	 Stack 5 kW modules Cell voltage 0.7 V Anode-supported technology T_{stack} 650 - 800°C Power density 0.6 W/cm² 85% fuel utilization per pass in fuel cell 	 Balance of Plant Water supplied (no water recovery) Steam reformer Natural gas fuel, (20" H₂O gauge)

We used a multi-level modeling approach to develop direct manufacturing cost estimates for the system.



Scope of Cost Analysis

To estimate installed cost, value-chain mark-up and installation cost must be added.



The cost model contains both purchased components and manufactured components.

Purchased Components	Manufactured Components
 Air blowers Natural gas compressor Water pump Air and fuel filters Control and solenoid valves Controllers for rotating equipment, 	 Fuel cell stack Fuel cell stack hardware Fuel cell packaging Recuperators Zinc bed Steam reformer
 processors and hardware Piping, fittings & connectors Thermocouples/sensors Wiring for sensors & valving Insulation (high and low temperature) 	 Raw Materials Steel sheet Metal foil Chemicals Nickel oxides

Use of a SMR offers opportunities for tight thermal integration.



We developed a conceptual system design, to assess implications of manifolding and interconnection.



We limited integration to the reformer and air preheaters, to maintain reasonable access.



With cylindrical stacks, a simpler manifolding arrangement may be feasible...



... and a more compact overall design.



With careful thermal integration, a system efficiency of 51% can be achieved in simple-cycle configuration.

Anode Fuel Utilization	85%
Fuel Cell, Cell Voltage	0.7 V
Fuel Cell Efficiency	47.1%
Cathode Inlet Air Temperature	650°C
Cathode Excess Air (for Cooling)	7.7 times
Blower Pressure	1.17 bar
Exhaust temperature	177 °C
Parasitic Loads	19 kW
Required Fuel Cell gross power rating	269 kW
Resultant Overall Efficiency	51%

Extensive energy recovery from hot exhaust gas is critical to achieving high system efficiency.



Cost Estimate

The direct manufacturing cost of the 250 kW system is estimated to be around \$150,000.



Installed cost ~ \$1000 / kW, CoE 5 - 9 ¢/kWh. **Arthur D Little**

15

Integration of SECA modules into cost-effective highperformance larger-scale systems appears feasible.

- Integration of over fifty stacks appears feasible:
 - Several manageable configurations identified
 - Manifolding and interconnection losses acceptable
 - Cost savings in balance of plant
- High-efficiency simple-cycle plant appears feasible, and result in attractive cost
 - Lower-efficiency, lower-cost systems may be more flexible in operation and preferable in some situations
 - Combined-cycle configurations may ultimately lead to even higher efficiency
- Cost and performance would be attractive
 - In the 250 kW system, benefits of economy of scale are largely offset by lower production volumes compare to 5 kW systems



Further improvements could be made, but additional challenges must be overcome.

- Achieving projected cost and performance requires:
 - Raising power density under realistic conditions
 - Proving long life and high reliability (steady state and cycling)
 - Subsystem and component design and development
 - Achieving high manufacturing volumes (cost at intermediate production volumes may be critical to ultimate success)
- Ultimately, further system improvements could be made, mainly by improving stack performance:
 - Lower temperature operation
 - More internal reforming / direct oxidation
 - Increased stack temperature gradient
 - Larger stack tiles

SOFC GROVE™ Initial Results Temperature in 6 x 6 cm² cell





SOFC GROVE™ Initial Results Current Density in 6 x 6 cm² cell