

Current State of Literature on CO₂ Clathrate Hydrates

Transport Related Issues

CO₂ Transport Mechanisms in the literature:

Transport model and analysis

Hydrate in suspension models

Model (3)



Analysis



Perforated plate models

Model (2)



Analysis



CO₂ Permeable Plate models

Model (2)

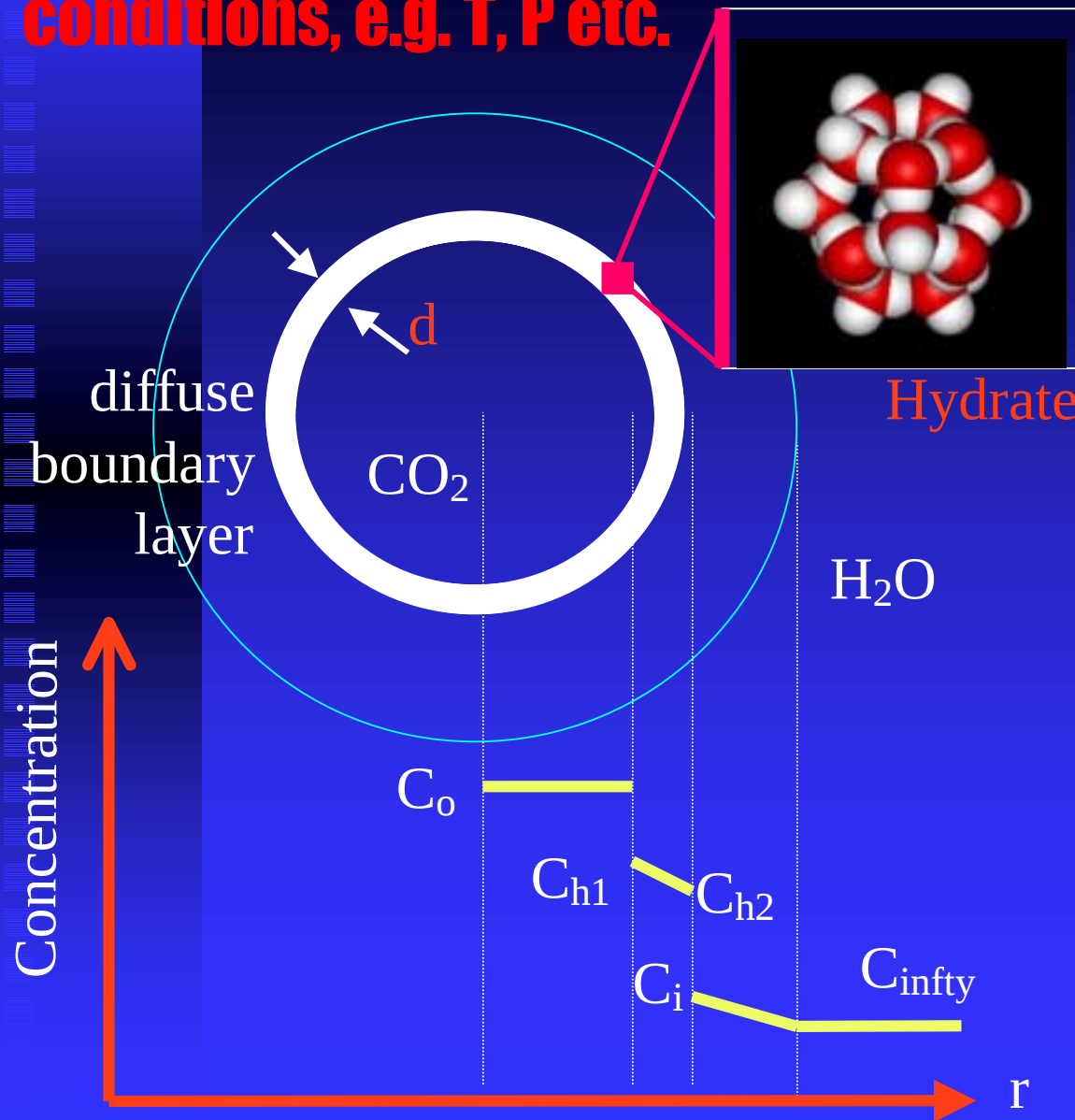


Analysis



-  Wrong or no physical basis
-  Not proven correct
-  Correct and/or consistent

Objective: To develop a quantitative and predictive model for the dispersion of CO₂ in the ocean, under varying conditions, e.g. T, P etc.



C_0 : Conc. of pure liq CO₂

C_{h1} : Conc. of CO₂ at full occupancy

C_{h2} : Conc. of CO₂ in hydrate at interface that is in equilibrium with water saturated with CO₂.

C_i : Conc. of CO₂ in liq. water adjoining hydrate

C_{infty} : Conc of CO₂ in water

k_L : mass transfer coeff. in the water rich phase

$D_{hydrate}$: D CO₂ in hydrate

$$\begin{aligned} \text{CO}_2 \text{ Flux} &= k_L (C_i - C_{infty}) \\ &= (D_{hydrate} / d) (C_{h1} - C_{h2}) \end{aligned}$$

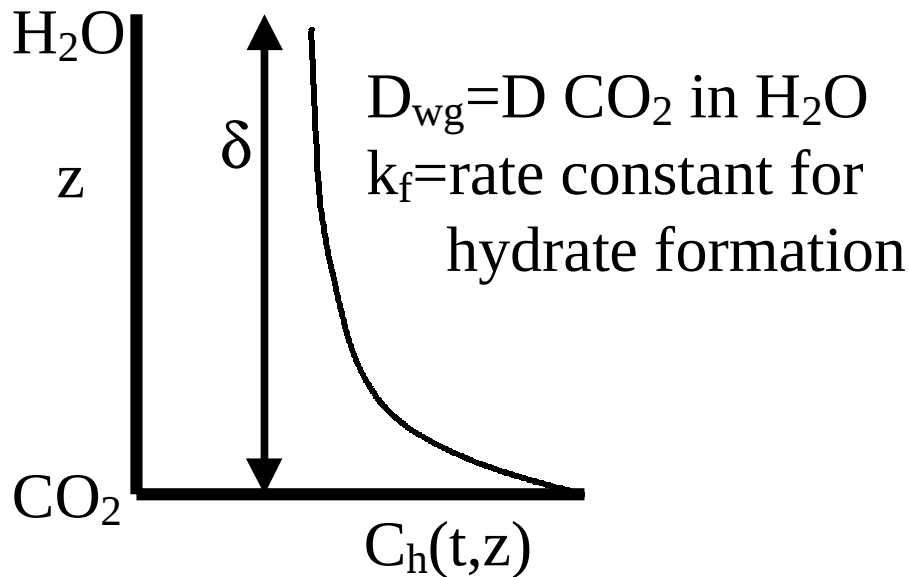
Steady State Analysis:

?

- C_i , C_{infty} determined by solubility data 
- C_{h1} , C_{h2} determined by hydrate occupancy and hydrate stability data. 
- k_L -mass transfer coeff.
 - correlations of the form $Sh = Sh(Re, Sc)$ 
 - expt data for dR/Dt for CO_2 without hydrate film. 
- D_{hydrate} – conceptual models 
- δ From mass balance (not independent of D_{hydrate})

Hydrate in Suspension Models

[Shindo 1995, Lund 1994, Teng 1995]



δ =film thickness

ρ =mass density of H_2O

M =mol. wt. of H_2O

n_h =hydration number

C_g =conc. of CO_2

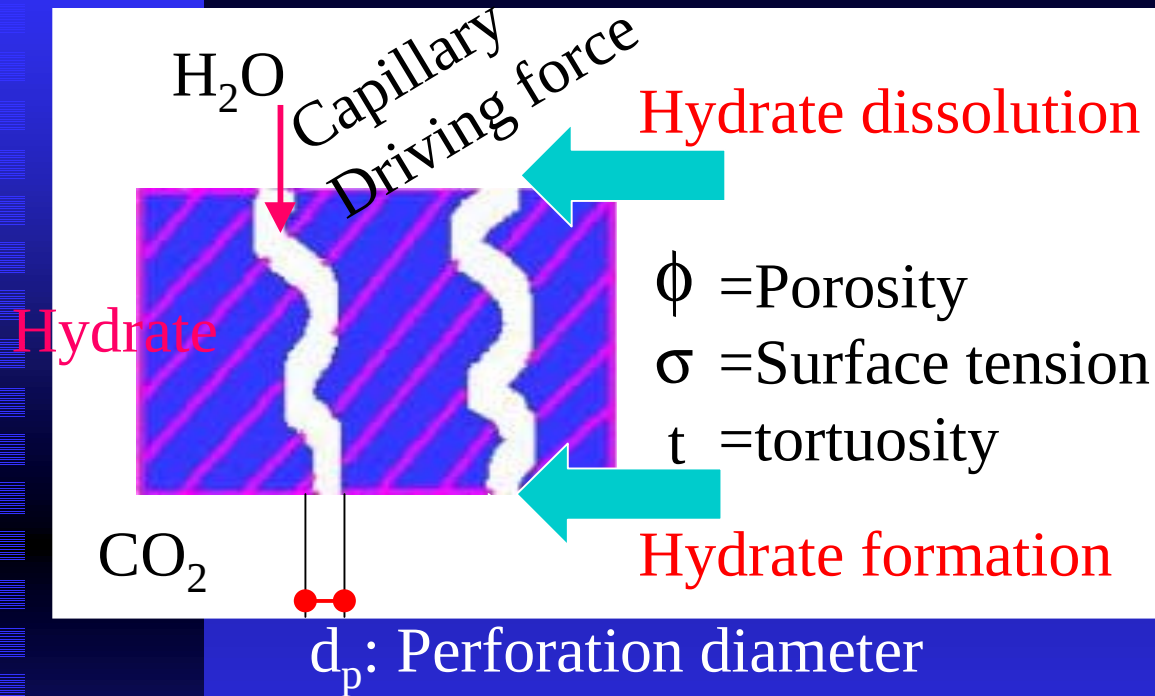
C_h =conc. of hydrate

$$\text{Molar flux of } CO_2 = \left. \frac{dC_g}{dz} \right|_{z=\delta} = f(D_{wg}, k_f)$$
$$\delta = (D_{wg}/k_f)^{1/2}$$

Flux and δ can be compared to experiment. This model has been parameterized by the reaction rate constant k_f , that has to be determined independently. The tensile strength measurements by Aya et al. invalidate the physical basis of the model.

Perforated Plate Models

[Hirai 1996, Mori 1998, Mori 2000]



δ =film thickness
 ν =viscosity of H_2O
 θ =contact angle
 at CO_2/H_2O interface
 ρ =mass density of H_2O
 M =mol. wt. of H_2O
 n_h =hydration number
 k_L =mass transfer coeff.

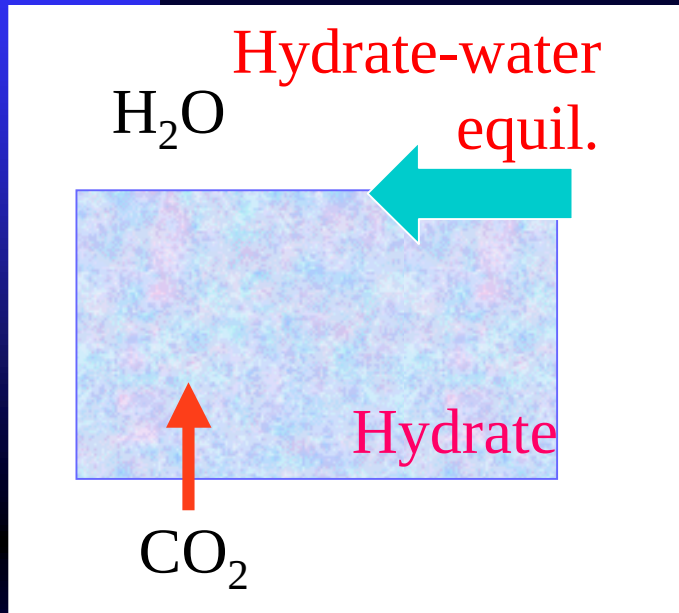
$$\text{Molar flux of } CO_2 = \phi d_p \sigma \cos \theta / 8 M \delta \tau^2 \nu n_h$$

$$= k_L \rho (C_i - C_{infty}) / M$$

Flux and δ can be compared to experiment. This model has the ability to predict the flux. As far as the prediction for δ goes, there is one equation and four unknowns, with no sound physical basis.

Solid Plate Models

[Teng 1996, Warzinski 1996]



δ =film thickness

ρ =mass density of H₂O

M =mol. wt. of H₂O

k_L =mass transfer coeff.

$D_{\text{hydrate}}=D$ CO₂ in hydrate

Molar flux of CO₂

$$= (D_{\text{hydrate}}/d) (C_{h1}-C_{h2})$$

$$= k_L \rho (C_i - C_{\infty}) / M$$

Flux and δ can be compared to experiment. This model has the ability to predict the flux. As far as the prediction for δ goes, independent measurement/prediction of D_{hydrate} is required.

Teng et al.: $D_{\text{hydrate}}=10^{-12}$ m²/s,
they predict δ in the range 10^{-5} - 10^{-6} m.

because this is typical of
diffusion of CO₂ in zeolites.

*Their prediction of δ was accurate because of fortuitous cancellation of errors

Warzinski et al.: $D_{\text{hydrate}}=10^{-15}$ m²/s,
they predict δ in the range 10^{-4} m.

because this is typical of diffusion
of molecules in polymers.

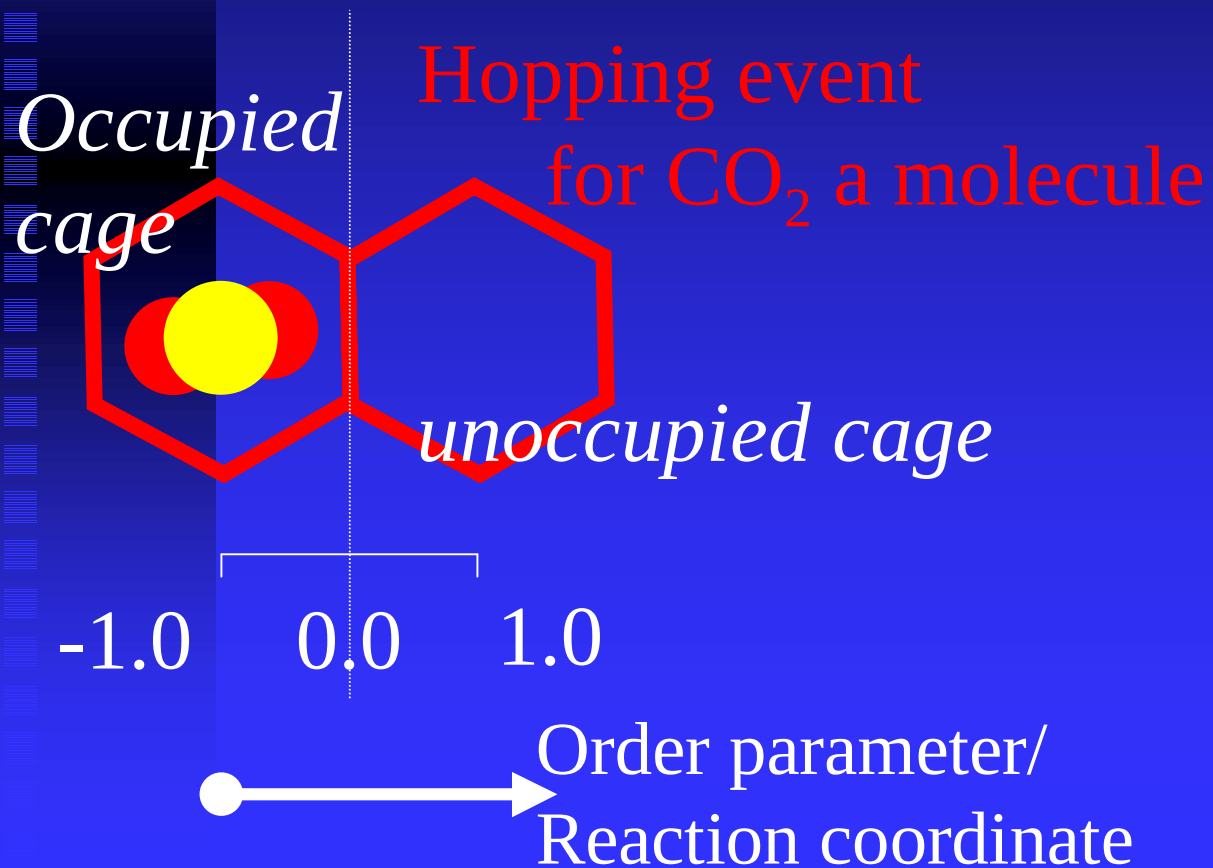
There is a need for the accurate prediction of the diffusivity of CO₂ through the hydrate phase

Diffusion in Clathrates

- Diffusion of CO₂ molecules in a defect free single crystalline clathrate is almost zero.
- Hopping of CO₂ molecule between adjacent cages is observed when H₂O vacancy is present. Time scale for a hopping event is of the order of 0.1ns.

Diffusion in Clathrates

Estimation of free energy barrier heights for hopping events using Monte Carlo methods



Cage occupancy at equilibrium conditions

Large cage	0.95*
Small cage	0.7*

* Experimental values

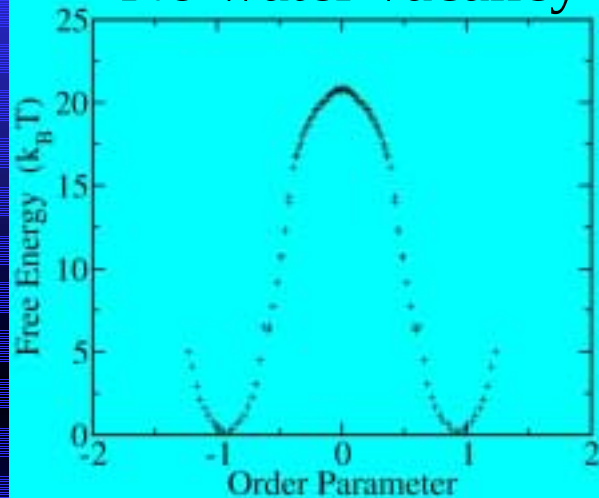
Free energy of creation
of a water vacancy

0.49 eV * at 200K

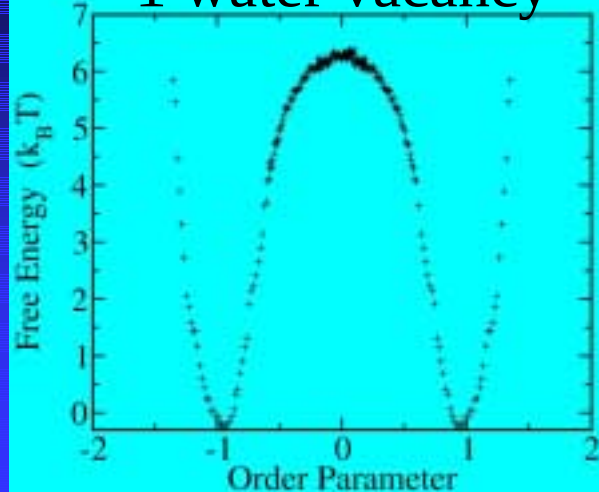
*using thermodynamic
integration

Free Energy barrier for hopping

No water vacancy



1 water vacancy



	Free energy Barrier / $k_B T$	Hopping rate / s^{-1}
Large-large no vacancy	21	$3.7e+3$
Large-Large(hex): 1 H ₂ O vacancy*	7.5	$2.5e+9$
Large-Large(Pent): 1 H ₂ O vacancy*	6.5	$8.5e+9$
Small-Large: 1 H ₂ O vacancy*	4.5	$6.6e+10$
Large-Small: 1 H ₂ O vacancy*	12	$3.0e+7$

*concentration of water vacancies in clathrate is $O(10^{-4})$, based on free energy of defect formation.

Based on the barrier hopping mechanism D_{CO_2} is $O(10^{-13} m^2/s)$

Diffusivity

$$D_H = (1/6) \frac{d \langle r(0) r(t) \rangle}{dt}$$

$$D_H = 0.166 * (d_{\text{cage}} - \text{cage})^2 * (\text{hopping rate}) * \\ * (\text{connectivity of large cages}) * (1 - \text{occ. of large cages}) \\ * (\# \text{ water molecules in pentagonal plane}) \\ * (\text{conc. of water defects})$$

$$D_H = 0.166 * (36 * 10^{-20}) * (8.5 * 10^{-9}) * (10) * (1 - 0.9) * (4) * (0.5 * 10^{-4})$$

$$D_H = 1.5 * 10^{-13} \text{ m}^2/\text{s}$$

CO₂ flux-

comparison with experiment:

Flow conditions	CO ₂ flux, d Simulation	CO ₂ flux,d Experiment
Re=0 Sh=2	7.0e-6 mol/m ² s 10 μm	5.0e-4 mol/m ² s 32 μm
Re=250 (u=2.5cm/s) Sh=75	5.0e-3 mol/m ² s 0.3 μm	4.0e-3 mol/m ² s 0.43 μm

For a CO₂ droplet (1 cm in diameter) submerged in a pure water phase that is stationary at 275 K and 18 Mpa.

Conclusion:

We have a self-consistent model for the prediction of the dissolution rate of CO₂. that works in the T, P, X_{CO₂} range of interest and under flow conditions $Re < 1000$

The results predicted by the model are consistent with the experimental results in the literature with regard to CO₂ flux and morphology of CO₂ hydrate films