CO₂ Mineral Sequestration Studies

Introduction, Issues and Plans

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Mineral Sequestration Program

Research effort seeks to refine and validate a promising CO_2 sequestration technology option, mineral sequestration also known as mineral carbonation

Goals:

- Understand the fundamental mechanisms involved in mineral carbonation
- Generate data to support process development
- Operate continuous, integrated small-scale process unit to support design



Current Partnerships

In order to effectively develop Mineral Sequestration, a multi-laboratory Working Group was formed in the Summer of 1998, participants include:

- Albany Research Center
- Arizona State University
- Los Alamos National Laboratory
- National Energy Technology Laboratory
- Science Applications International Corp.



What is Mineral Carbonation

- Reaction of CO2 with Mg or Ca containing minerals to form carbonates
- Lowest energy state of carbon is a carbonate and not CO2
- Occurs naturally in nature as weathering of rock
- Candidate Materials:
 - Magnesium Silicates
 - Calcium Silicates
 - Industrial residues





Advantages of Mineral Carbonation

Vast capacity - deposits of ultramafic rocks exceeding even the most optimistic estimate of coal reserves

Readily accessible near major high density power generation centers

No legacy issues - Long term stability unarguable naturally occurring and benign products





Carbonation Reaction Paths

Generalized reaction:

• (Mg, Ca)_xSi_yO_{x+2y+z}H_{2z} + $xCO_2 \rightarrow x(Mg,Ca)CO_3 + ySiO_2 + zH_2O$

Serpentine:

- $Mg_3Si_2O_5(OH)_4 + 3CO_2 \rightarrow 3MgCO_3 + 2SiO_2 + 2H_2O$
 - (MgO) = 38-45 wt pct (actual)
 - (Iron oxides) = 5-8 wt pct
 - (Water) = 13wt pct
- Exothermic reaction: + 64 kJ/mole
- One ton to dispose of 1/2 ton of CO2

Olivine (Primary mineral forsterite):

- $Mg_2SiO_4 + 2CO_2 \rightarrow 2MgCO_3 + SiO_2$
 - (MgO) = 45-50 wt pct (actual)
 - (Iron oxides) = 6-10 wt pct
- Exothermic reaction: + 95 kJ/mole
 - One ton to dispose of 2/3 ton of CO2



Structural model of Serpentine (Lizardite)



Mineral Sequestration Concept



Courtesy of Albany Research Center



Issues Related to Mining and Milling Evaluated

• Serpentine mines common

- road base & asphalt
- additional capacity would be required
- Scale of mining operations
 consistent with requirements
 - 1000 tpd avg. (450 MWe, 35%, 24hr)
- Mining costs of \$3 \$5/ton
- Olivine used for refractories and foundry sand
 - global resources not well characterized









Reaction Rate Increased by 10 Fold

Improvement of reaction rate is achieved by

 Pre-treat serpentine to remove chemically-bonded water and create open structure (600-650 C)

- Add sodium bicarbonate and NaCl solution as additives
- Sodium bicarbonate increases HCO_{3}^{-} concentration
- NaCl may help release Mg ions from silicate
- -78% conversion can be achieved in 30 minutes at 185 bar, & 155 °C





Critical Issues

- <u>Pretreatment Issues</u> which includes mining of minerals and preparation of solid, gaseous or liquid feedstocks
- <u>Carbonation Reaction</u> which includes mechanisms and reactor designs
- <u>Post-Treatment Issues</u> which includes separation of carbonation products, and disposal of process effluents
- Engineering Design, Assessment and Integration Activities which includes process integration, cost estimation, etc.



Critical Issues







Pretreatment Issues

- Sample Collection and Distribution
- Evaluate Effectiveness of Ore Impurities and Ore Pretreatment
- Evaluate the Effectiveness of Thermal and Chemical Mineral Pretreatment Processes
- Examination of two-step processes and the use of Alternate Feedstocks



Carbonation Reaction

- Construction of Additional Laboratory-Scale Reactors
- Temperature, Pressure & Solution Chemistry Effects
- Fundamental Support (e.g., modeling and data analysis)
- Construction & Operation of Continuous Bench-Scale Reactors

Vertical two-phase bubble column Rx 10lb/hr rock Continuous processing unit 5 lb/hr rock



Post-Treatment Issues

Characterization & Disposal of Affluent Recovery of Byproducts Testing of Separation



Engineering Design, Assessment and Integration Activities

- Develop Carbonation Reactor Designs, Heat Exchanger Concepts and Balance of Plant Requirements
- Perform Cost Estimates, Sensitivity Studies and Life Cycle Analyses (LCA)
- Pilot Plant, Demonstration Plant and Preliminary Sequestration Plant Design and Cost Estimation Activities
 - Construction & Operation of Integrated 500 lb/hr Carbonation Unit (1/2 MW)
 - Preliminary Design of 10MWe System



Design and assessment activities are necessary to continually evaluate process development requirements and guide R&D.

TimeLine





Current Activities FY 2001

- Gaining the mechanistic understanding required to identify a cost-effective carbonation route.
- Exploring promising two-step processes (i.e., separated dissolution and carbonation steps)
- Delineating operational parameters necessary to design a bench scale continuous reactor flexible
- Initiating an engineering assessment to establish an economic baseline and future research priorities.
- Pre- and post-treatment issues related to particle size effects, separation, crushing and grinding, byproduct recovery, waste disposal, and thermal or chemical mineral treatments.



Near Term Activities FY 2002

- Continue fundamentally oriented and applied laboratory carbonation studies
- Identify the most promising carbonation feedstock and route.
- Construction and operation of a continuous bench scale reactors, ARC and NETL
- Produce engineering data utilizing the 5 lb/hr bench scale carbonation reactor to evaluate potential operating characteristics
- Initiate by-product characterization and recovery
- Initiate studies on disposal of effluents



Future Program Activities

- 2003 Initiate small pilot-scale testing to produce realistic engineering design data.
- 2005 Complete technical and economic assessment and construct next-generation integrated pilot plant at relevant scale





Future Program Activities

- 2006- Design of a Demonstration scale unit will be completed
- 2007- Construction of the Demonstration scale carbonation system is completed and operation is begun



