

## Low Cost Options for Moderate Levels of Mercury Control 2007 Update on TOXECON II™



DOE/NETL Mercury Control Technology Conference December 11, 2007 Tom Campbell, ADA-ES, Inc.

DOE/NETL Project Manager: Andrew O'Palko DOE Cooperative Agreement DE-FC26-05NT42307



## **Test Participants**

- DOE/ NETL Andrew O'Palko
- EPRI Ramsay Chang
- Entergy Independence Station
- ADA-ES
- DOE Phase II Participants
- Modeling
  - REI
  - NELS
  - ADA-ES



## **TOXECON II™ Evaluation Co-funders**

Alliant Atco Power DTE **Entergy\*** Oglethorpe Power Southern Company Xcel Energy ADA-ES Arch Coal EPCOR EPRI NORIT Americas Calgon Carbon

\* Host Sites







## **TOXECON II™ Full-Scale Evaluation**

- Entergy's Independence Steam Electric Station
  - 880 MW
  - PRB Coal from North Antelope
  - Test on 1/8 of Unit 2
- Cold Side ESP
   540 SCA
- Project goal
   50-70% Hg removal



Ash sold for concrete

 PAC/ash routed to
 separate silo during tests



## **General TOXECON II Layout**





#### **ISES ESP General Arrangement**



## **ESP** Layout



NELS Model 1/2 of 4 ESP boxes on Unit 2 (3<sup>rd</sup> field not installed)



#### **TOXECON II™ Design Challenge: Grid Size**





#### **Silo and Booster Blower**







# **Injection Grid**





## **2006 Test Results – Summary**

- Achieved project goal of 50 to 70% Hg removal
- TOXECON II<sup>™</sup> Hg removal limited to < 80% at full load with up to 8 lb/MMacf DARCO<sup>®</sup> Hg-LH
- TOXECON II<sup>™</sup> Hg removal varied significantly with load (lower removal at high load)
- Hg removal > 80% with pre-ESP injection of DARCO<sup>®</sup> Hg-LH at 1 to 2 lb/MMacf

Suspected that poor distribution contributed to conflicting results from injection upstream of ESP versus TOXECON II<sup>TM</sup> grid



# 2007 Testing

- Goals for Testing
  - Improve mercury removal efficiency
  - Inject continuously to evaluate grid operability
  - Minimize sorbent use
    - Manage costs
    - Minimize potential of increased particulate emissions
  - Assess impact of injection on particulate emissions (through EPRI funding)
- Baseline/Parametric/30 day test with Lance Design 2 January – February 2007
- Five-Day Continuous Injection Test with Lance Design 3 May 2007





#### **Original Lance Design – High Load**



## **Phase II - New Distribution Design**

- Installed new penetrations to allow on-line lance insertion and maintenance
- Redesigned lances for better top to bottom carbon distribution
- Redesigned nozzles for better plume development and to better direct carbon into gas flow
- Redesigned carrier air distribution for better penetration into gas passages



## Design 2 – High Load





### **ISES TOXECON II™ Results Summary**





#### Hopper, E Field, and Spring 2007 Lance Locations



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## **Hopper Ash Comparison**



★ = Carbon migrating towards control side



#### **Test Results – Balance of Plant**

#### Opacity

- Some opacity spikes measured during last field rapping while operating at reduced ESP power
- Testing with full ESP power and varying the rapping sequence limited the particulate and opacity spikes for all sorbents tested
- Minimal other plant impacts

- Potential fouling with ash handling valves



### **PAC Injection and ESP Power**





### **Results of February 2007 PM Tests**





# Fall 2007 Testing

- EPRI/Entergy Supported
- Test 1/2 of B ESP or 1/8 of Unit
  - Install 24 more lances
  - Modify manifold arrangement and carrier line sizes
- Conduct PM measurements on Control and Test sides
- Goals
  - Obtain 90% mercury removal at high load and low load conditions
  - Assess impact of PAC injection on PM emissions



# Fall 2007 Testing



Testing 1/8 of unit - 1/2 of B ESP



## **Preliminary Economics for Independence**

Mercury Removal Rate	85%*
Brominated PAC Injection rate for above removal	5 lb/MMacf (960 lbs/hr)
Native Mercury Removal	10 – 15%
Stack Flow	3.2M acfm
Average Coal Mercury Concentration	5.5 lb/ TBtu
Mercury Removed	643 lb/ yr
20 Year Levelized Cost	\$ 7.8M **
20 Year Levelized \$/lb Mercury Removed	\$ 12.0K **

\* Includes baseline removal.

\*\* Includes loss of ash sales and disposal fees.

Capital Cost Estimate: \$5.15/kW O&M Cost Estimate: 1.03 mills/KW-hr



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