#### **EERC** *Technology...* Putting Research into Practice

## Mercury Control Technology R&D Program Review

#### Large-Scale Mercury Control Technology Testing for Lignite-Fired Utilities – Oxidation Systems for Wet FGD

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NETL Project Manager – Andy O'Palko December 12, 2006

#### **Partnership Team**



# Goal

- Evaluate cost-effective approaches for capturing the Hg in lignite derived combustion flue gases using a cold-side electrostatic precipitator (ESP) and/or wet flue gas desulfurization (FGD) system using oxidation methods.
- ESP-wet FGD Hg removal efficiency of <u>>55%</u> on a consistent basis.



# Introduction

- Two host sites for field testing
  - Minnkota Power Cooperative Milton R. Young (MRY) Station Unit 2 near Center, North Dakota
  - TXU Monticello Steam Electric Station Unit 3 near Mt. Pleasant, Texas

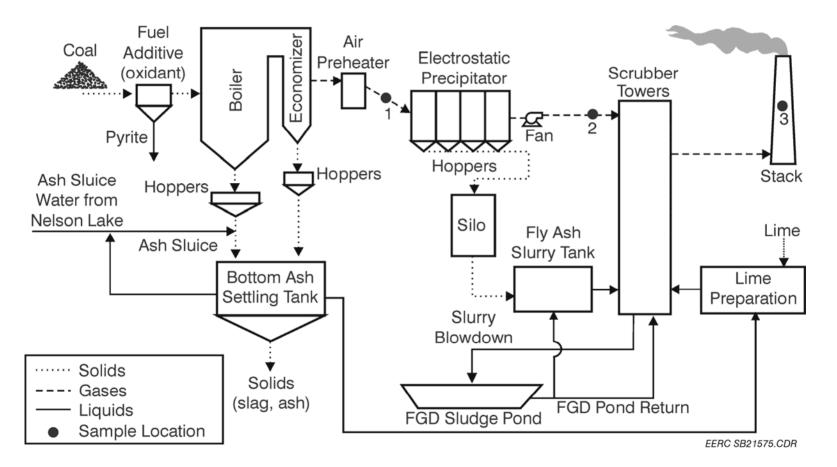


# MRY Unit 2

- B&W Carolina-type radiant boiler
  - Cyclone-fired, balanced-draft, pump-assisted circulation boiler
  - Began commercial operation in May 1977
  - Base-loaded at 450 MW gross
  - Lignite from Center Mine
- Pollution controls
  - Cold-side ESP (specific collection area of 375 ft<sup>2</sup>/kacfm)
  - Spray tower FGD (alkaline ash and lime)



### **Schematic of MRY Unit 2**





# Potential Mercury Control Technologies

- Hg<sup>0</sup> oxidizing agents
  - $-CaCl_2$
  - $-MgCl_2$
- Sorbent enhancement agent
  - SEA2
- PAC injection
  - NORIT Americas Inc. DARCO® Hg



# **Pumping and Metering Skid**



• 0.1–2.2 gal/min =  $\leq$ 500 ppm (as-fired coal basis)



## **Injection Lances**



 Injected into four coal feed pipes of the twelve Unit 2 cyclones



# **PAC Injection System**

- Apogee Portapac metering skid, blower, connecting lines, and injection lances
- PAC injected at 16 locations into the ductwork upstream of the ESP

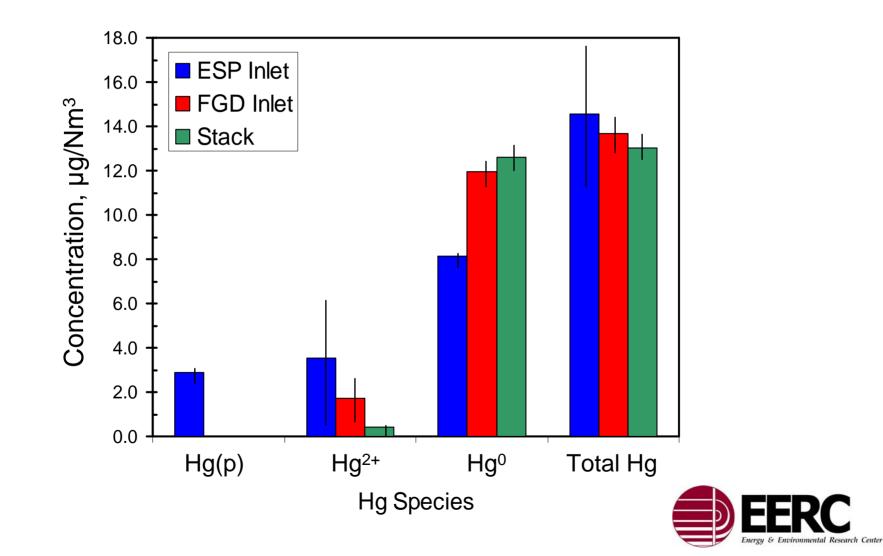


#### **Experimental**

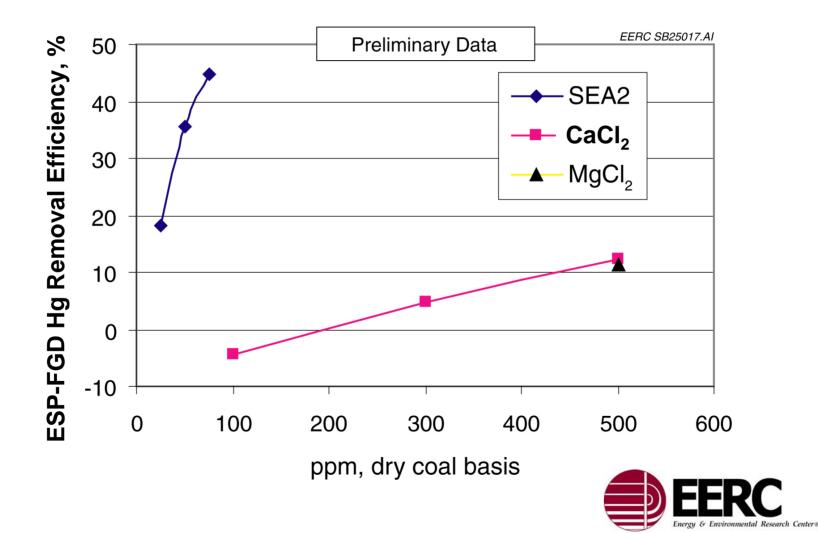
- Flue gas Hg measurements
  - ASTM International Method D6784-02 (Ontario Hydro [OH] method)
  - Continuous mercury monitoring (CMM)
    - Tekran Model 2537A atomic fluorescence-based Hg vapor analyzer combined with a PS Analytical S235C400 wet-chemistry conversion unit



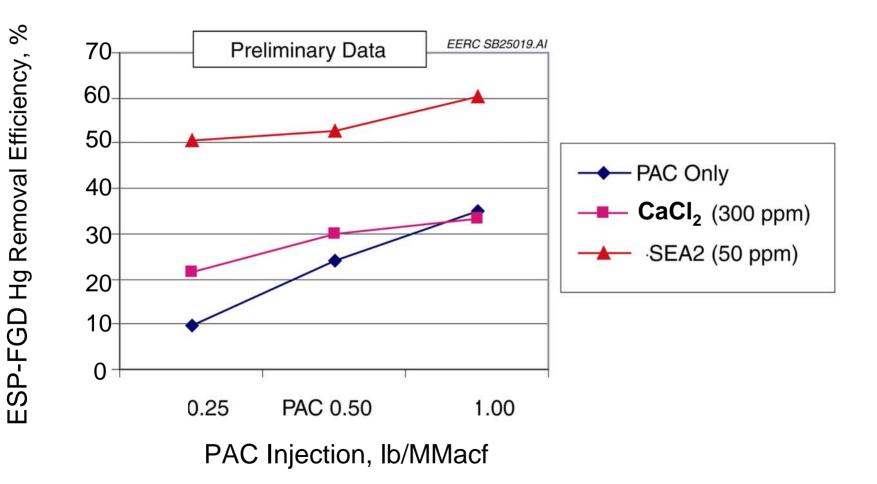
# Baseline MRY Unit 2 Hg Measurements (March 16–18, 2005)



# Chemical Addition Effects on Hg Capture

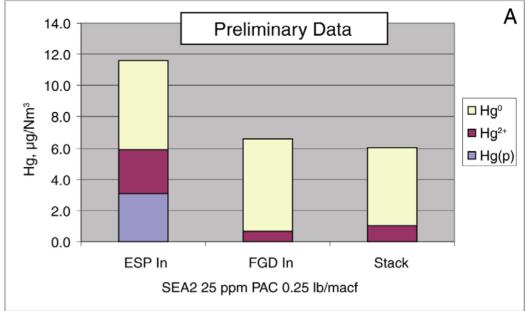


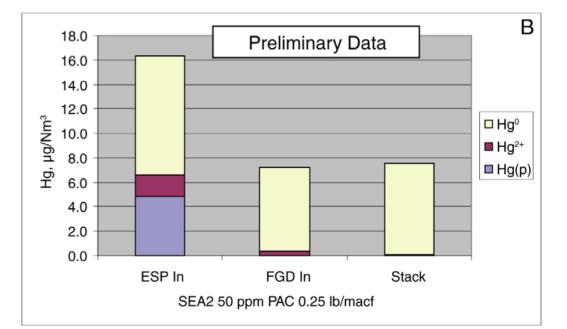
## Effects of PAC and Chemical Injections on Hg Capture



#### SEA2 and PAC Injection

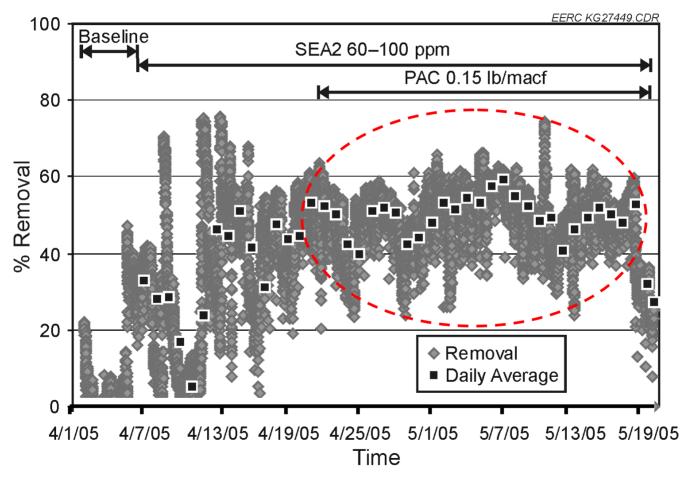
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# Long-Term Hg Control Test Results





## Conclusions

- Lignite combustion flue gas at MRY Unit 2 contained primarily Hg<sup>0</sup> (>70%).
- SEA2 was more effective in enhancing ESP– FGD Hg removal relative to CaCl<sub>2</sub> and MgCl<sub>2</sub>.
- ESP–FGD Hg removals of <a>>55%</a> were maintained by injecting 50 ppm SEA2 and 0.15 lb/MMacf.
- The Hg in baseline and SEA2- and PAC-containing fly ashes was insoluble.
- The Hg in SEA2- and PAC-containing fly ash was thermally more stable relative to baseline fly ash



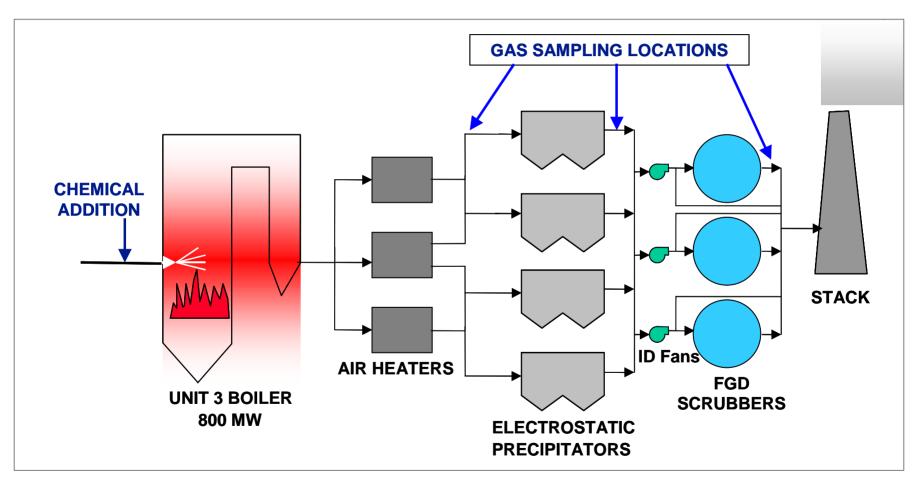
# **Monticello Unit 3**

- 793 MW
- Fires a blend of Texas lignite and PRB coals
- Equipped with cold-side ESP
- Equipped with wet FGD scrubber
  - Limestone forced oxidation
  - Spray tower





## **Monticello Unit 3**







## **Method of Salt Addition**

- Add liquid salt to the coal
  - Spray on belt upstream of pulverizer

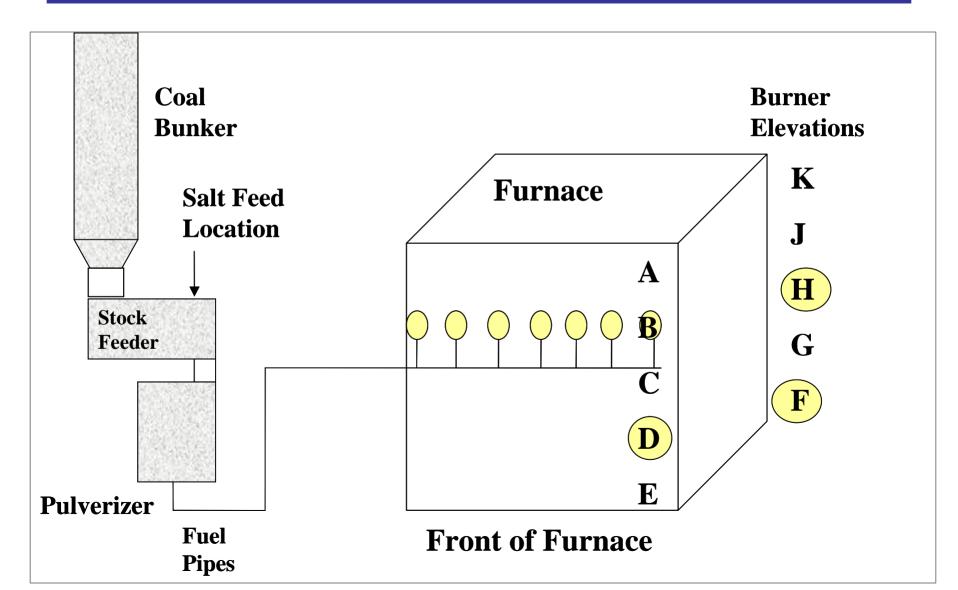








#### **Method of Salt Addition**



# **Baseline Hg Concentrations**

- Coal Hg concentrations

   PRB: 0.05 0.10 ppm, dry
   TxL: 0.15 0.35 ppm, dry
- ESP Inlet Hg
  - 10–30 µg/dNm<sup>3</sup>
  - 10%-40% oxidation
- Less than 20% Hg removal by fly ash
- FGD outlet Hg
   10–18 µg/dNm<sup>3</sup>
- Removal across ESP/FGD: 10%-40%



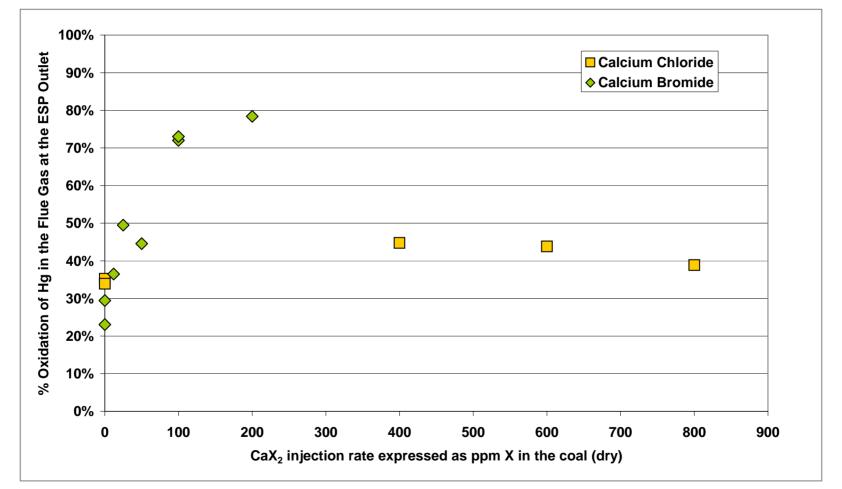


# **Parametric Test Plan**

- Compare performance of two salts
- Measure Hg oxidation vs. injection rate
- $-CaCl_2$ 
  - Cost is \$ 0.31/lb Cl
  - Tested at rates of 400, 600, 800 ppm CI in the coal
- CaBr<sub>2</sub>
  - Cost is \$ 1.76/ lb Br
  - Br more reactive with Hg
  - Tested at rates of 12, 50, 100, 200 ppm Br in the coal



# Parametric Test Results Hg Oxidation vs. Injection Rate







# Long-Term Test Plan

- Evaluate salt's ability to maintain high level of Hg oxidation
- Evaluate balance-of-plant impacts
- First 2-week test of CaBr<sub>2</sub> at 55 ppm Br in coal
- Second 2-week test of CaBr<sub>2</sub> at 113 ppm Br in the coal





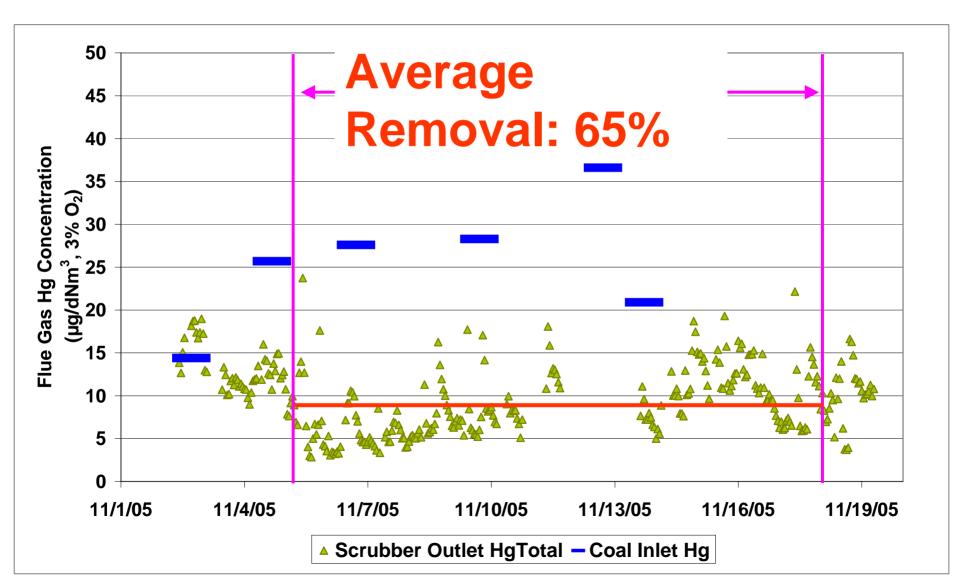
# % Hg Oxidation: 55 ppm Br in the Coal

- Compare average coal inlet Hg to average SCEM Hg<sup>0</sup> at FGD inlet
- 67% oxidation of mercury at 55 ppm Br in coal





# Coal Inlet vs. FGD Outlet: 55 ppm Br in the Coal



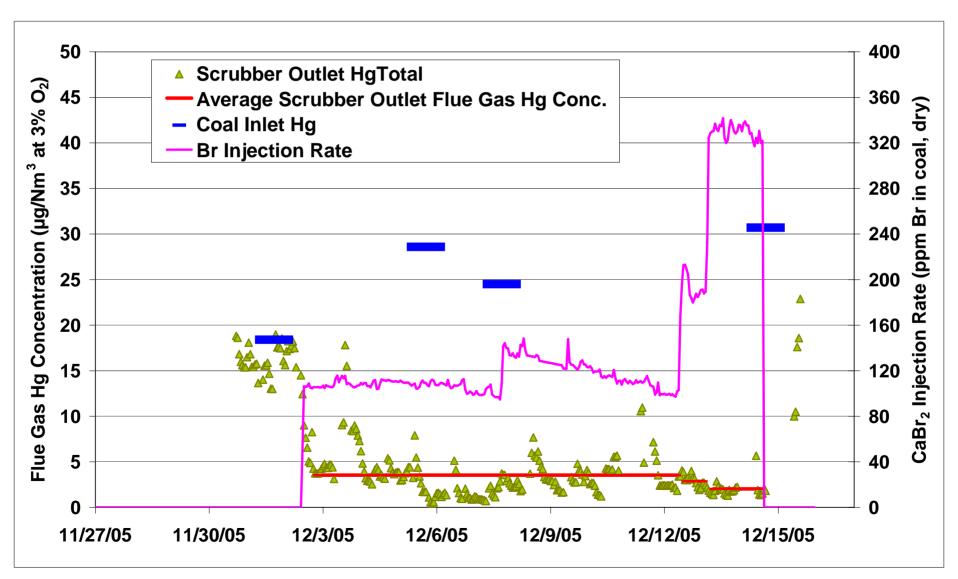
# % Hg Oxidation: Second Long-Term Test

- Compare average coal inlet Hg to average SCEM Hg<sup>0</sup> at FGD inlet
  - 113 ppm Br: 85%
  - 193 ppm Br: 91%
  - 330 ppm Br: 93%





# Coal Inlet vs. FGD Outlet: 113 ppm Br in the Coal



# Summary

- Oxidation of flue gas mercury was increased with CaCl<sub>2</sub> and CaBr<sub>2</sub> salts.
- Removal of Hg across wet scrubber correlated well with oxidation of Hg.
- Results of long-term test (FGD outlet vs. average coal Hg)
  - Baseline: 10%–40% removal
  - 55 ppm Br in coal: 65% removal
  - 113 ppm Br in coal: 86% removal
  - 330 ppm Br in coal: 92% removal





# **Further Testing Needed**

- Evaluate long-term operation
- Characterization of potential balance-of-plant impacts of chemical injection
  - Corrosion
  - Air heater plugging
  - FGD performance
  - FGD materials of construction
  - Effects on by-products





#### **Contact Information**

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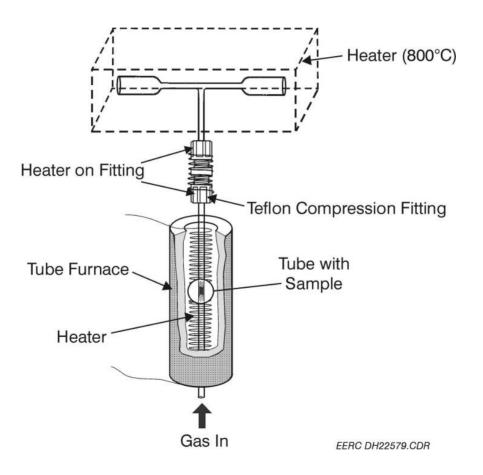


# Hg Leachability from Fly Ashes

 Hg concentrations in baseline and Hg control (SEA2 and PAC) fly ash leachates from SGLP and LTLP were <0.01 µg/L.</li>

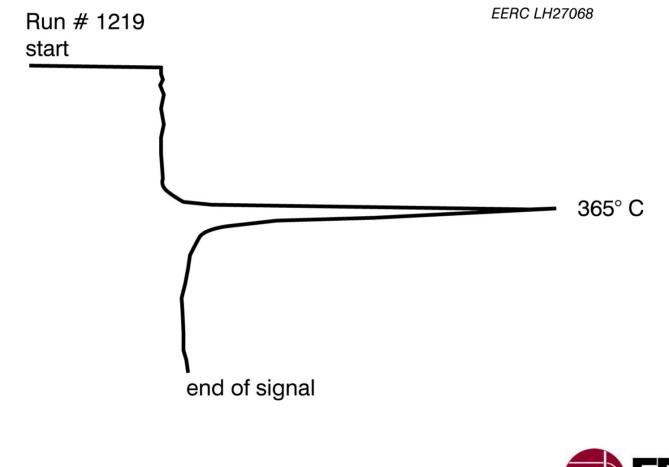


# **Hg Thermal Desorption Apparatus**





## Hg Thermal Desorption from Baseline Fly Ash





#### Hg Thermal Desorption from Fly Ash Sampled During SEA2 and PAC Injections

