

Appendix B

- **Table 1. Pressure Corrections to Indicated Volume of Prover (supplied by inspector; unique to individual prover)**
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Table 1

**Pressure Corrections to
Indicated Volume of Prover**

**(Replace this page with a copy of the pressure
correction table that was prepared for
your prover when it was calibrated.)**

Table 2. Temperature Corrections to Indicated Volume of a 100-Gallon LPG Prover

Temperature of Liquid in Prover °F	100-Gallon Correction Per °F Difference between Meter Temperature and Prover Temperature							
	Propane Specific Gravity 60/60 °F 0.500*		Propane Specific Gravity 60/60 °F 0.505*		Propane Specific Gravity 60/60 °F 0.510*		Butane Specific Gravity 60/60 °F 0.580*	
	cu in/°F	gal/°F	cu in/°F	gal/°F	cu in/°F	gal/°F	cu in/°F	gal/°F
-20 to -10	34.6	0.150	33.9	0.147	33.0	0.143	23.7**	0.103**
Over -10 to 0	35.0	0.152	34.1	0.148	33.4	0.145	24.0**	0.104**
Over 0 to 10	35.7	0.155	34.6	0.150	34.0	0.147	24.4**	0.106**
Over 10 to 20	36.4	0.158	35.7	0.154	34.7	0.150	24.4**	0.106**
Over 20 to 30	37.3	0.161	36.6	0.159	35.3	0.153	24.4**	0.106**
Over 30 to 40	37.9	0.164	37.0	0.160	35.7	0.155	24.5	0.106
Over 40 to 50	38.5	0.167	37.7	0.163	36.4	0.158	24.6	0.106
Over 50 to 70	39.3	0.170	39.3	0.170	37.0	0.160	25.4	0.110
Over 70 to 80	40.0	0.173	39.3	0.170	37.7	0.163	25.4	0.110
Over 80 to 90	41.1	0.178	39.7	0.172	38.8	0.168	25.4	0.110
Over 90 to 100	41.9	0.181	40.6	0.176	39.3	0.170	26.1	0.113
Over 100 to 110	42.6	0.184	41.3	0.179	39.8	0.172	26.2	0.113
Over 110 to 120	43.3	0.187	42.0	0.182	40.5	0.175	26.5	0.115

- Approximate specific gravities for some commercial LPG products
- ** Butane boils at 31.1 °F. Prover pressure will be less than one atmosphere below boiling point.

Note: The appropriate correction factor should be multiplied by the number of degrees difference between the meter and prover temperatures. If the temperature at the meter is *higher* than the temperature of the prover, the correction should be *added* to the prover gauge reading to compensate for the contraction of the liquid that has taken place after it was measured by the meter. If the temperature at the meter is *lower* than the temperature of the prover, the correction should be *subtracted* from the prover gauge reading to compensate for the expansion of the liquid that has taken place after it was measured by the meter.

**Table 2-A Temperature Corrections to Indicated Volume
of 100-Gallon Anhydrous Ammonia Liquid Meter Prover**

Temperature of Liquid in prover	100-gallon correction per °F difference between meter temperature and prover temperature	
	°F	cubic inches/°F
-20 to -10	28.0	0.121
Over -10 to 0	28.3	0.122
Over 0 to 10	28.5	0.124
Over 10 to 20	28.8	0.125
Over 20 to 30	29.0	0.126
Over 30 to 40	29.4	0.127
Over 40 to 50	29.8	0.129
Over 50 to 70	30.0	0.130
Over 70 to 80	30.4	0.132
Over 80 to 90	30.9	0.134
Over 90 to 100	31.3	0.135
Over 100 to 110	31.7	0.137
Over 110 to 120	32.2	0.139

Notes:

- The appropriate correction factor should be multiplied by the number of degrees difference between the meter and the prover temperatures.
- If the temperature at the meter is **higher** than the temperature of the prover, the correction should be **added** to the prover gauge reading to compensate for the contraction of the liquid that has taken place after the liquid was measured by the meter.
- If the temperature at the meter is **lower** than the temperature of the prover, the correction should be **subtracted** from the prover gauge reading to compensate for the expansion of the liquid that has taken place after the liquid was measured by the meter.

**Table 3: Volume Corrections for Thermal Expansion or Contraction
of a 100-gallon Low Carbon Steel LPG Prover**

Prover Temperature	Prover Correction	
	cubic inches	gallons
°F		
-20	-34	-0.15
-15	-32	-0.14
-10	-30	-0.13
-5	-28	-0.12
0	-26	-0.11
5	-24	-0.10
10	-21	-0.09
15	-19	-0.08
20	-17	-0.07
25	-15	-0.07
30	-13	-0.06
35	-11	-0.05
40	-9	-0.04
45	-6	-0.03
50	-4	-0.02
55	-2	-0.01
60	0	0
65	2	0.01
70	4	0.02
75	6	0.03
80	9	0.04
85	11	0.05
90	13	0.06
95	15	0.07
100	17	0.07
105	19	0.08
110	21	0.09
115	24	0.10
120	26	0.11

It should be noted that the deviations given with respect to temperature are applicable only to low carbon steel provers. For stainless steel provers the applicable coefficient of cubical expansion for the stainless steel composition used for the prover should be used to calculate the deviations.

Table 4. Volume Reduction to 60 °F for Liquefied Petroleum Gas

-50 to 50 °F.											
Observed Temperature, °F	Specific Gravity 60/60 °F.					Observed Temperature, °F.	Specific Gravity 60/60 °F.				
	0.500		0.505		0.510		0.500		0.505		0.510
	Factor for Reducing Volume to 60 °F.						Factor for Reducing Volume to 60 °F.				
-50	1.160	4	1.156	3	1.153	0	1.092	3	1.089	1	1.088
-49	1.159	4	1.155	3	1.152	1	1.090	2	1.088	2	1.086
-48	1.157	3	1.154	4	1.150	2	1.089	2	1.187	2	1.085
-47	1.156	4	1.152	3	1.149	3	1.088	2	1.086	2	1.084
-46	1.154	3	1.151	4	1.147	4	1.086	2	1.084	2	1.082
-45	1.153	3	1.150	4	1.146	5	1.085	2	1.083	2	1.081
-44	1.152	3	1.149	4	1.145	6	1.084	2	1.082	2	1.080
-43	1.151	3	1.148	4	1.144	7	1.082	2	1.080	2	1.078
-42	1.149	3	1.146	4	1.142	8	1.081	2	1.079	2	1.077
-41	1.148	3	1.145	4	1.141	9	1.079	1	1.078	2	1.076
-40	1.147	3	1.144	4	1.140	10	1.078	2	1.076	2	1.074
-39	1.146	3	1.143	4	1.139	11	1.077	2	1.075	2	1.073
-38	1.144	3	1.141	3	1.138	12	1.075	2	1.073	2	1.071
-37	1.143	3	1.140	4	1.136	13	1.074	2	1.072	2	1.070
-36	1.141	3	1.138	3	1.135	14	1.072	1	1.071	2	1.069
-35	1.140	3	1.137	3	1.134	15	1.071	2	1.070	2	1.068
-34	1.139	3	1.136	3	1.133	16	1.070	2	1.068	2	1.066
-33	1.138	3	1.135	3	1.132	17	1.069	2	1.067	2	1.065
-32	1.136	3	1.133	3	1.130	18	1.067	1	1.066	2	1.064
-31	1.135	3	1.132	3	1.129	19	1.066	2	1.064	2	1.062
-30	1.134	3	1.131	3	1.128	20	1.064	1	1.063	2	1.061
-29	1.133	2	1.130	3	1.127	21	1.063	2	1.061	1	1.060
-28	1.131	3	1.128	3	1.125	22	1.061	1	1.060	2	1.058
-27	1.130	3	1.127	1	1.124	23	1.060	2	1.058	1	1.057
-26	1.128	3	1.125	3	1.122	24	1.058	1	1.057	2	1.055
-25	1.127	3	1.124	3	1.121	25	1.057	2	1.055	1	1.054
-24	1.126	3	1.123	3	1.120	26	1.055	1	1.054	2	1.052
-23	1.124	3	1.121	3	1.118	27	1.054	2	1.052	1	1.051
-22	1.123	3	1.120	3	1.117	28	1.052	1	1.051	2	1.049
-21	1.121	3	1.118	3	1.115	29	1.051	2	1.049	1	1.048
-20	1.120	3	1.117	3	1.114	30	1.049	1	1.048	2	1.046
-19	1.118	2	1.116	3	1.113	31	1.047	1	1.046	1	1.045
-18	1.117	3	1.114	3	1.111	32	1.046	1	1.045	2	1.043
-17	1.115	2	1.113	3	1.110	33	1.044	1	1.043	1	1.042
-16	1.114	3	1.111	3	1.108	34	1.043	2	1.041	1	1.040
-15	1.112	2	1.110	3	1.107	35	1.041	1	1.040	1	1.039
-14	1.111	2	1.109	3	1.106	36	1.039	1	1.038	1	1.037
-13	1.109	2	1.107	3	1.104	37	1.038	1	1.037	1	1.036
-12	1.108	2	1.106	3	1.103	38	1.036	1	1.035	1	1.034
-11	1.106	2	1.104	3	1.101	39	1.035	1	1.034	1	1.033
-10	1.105	2	1.103	3	1.100	40	1.033	1	1.032	1	1.031
-9	1.104	2	1.102	3	1.099	41	1.031	0	1.031	1	1.030
-8	1.102	2	1.100	2	1.098	42	1.030	1	1.029	1	1.028
-7	1.101	2	1.099	3	1.096	43	1.028	1	1.027	0	1.027
-6	1.099	2	1.097	2	1.095	44	1.027	1	1.026	1	1.025
-5	1.098	2	1.096	2	1.094	45	1.025	1	1.024	0	1.024
-4	1.097	2	1.095	2	1.093	46	1.023	0	1.023	1	1.022
-3	1.096	3	1.093	1	1.092	47	1.022	1	1.021	0	1.021
-2	1.094	2	1.092	2	1.090	48	1.020	0	1.020	1	1.019
-1	1.093	3	1.090	1	1.089	49	1.019	1	1.018	0	1.018
0	1.092	3	1.089	1	1.088	50	1.017	0	1.017	1	1.016

Data reprinted from Table 24, Volume Reduction to 60 °F, "Petroleum Measurement Tables," API Standard: 2540 (ASTM Designation 9:1250) 1952, American Edition with the permission of the American Petroleum Institute.

Table 4. Volume Reduction to 60 °F for Liquefied Petroleum Gas

Observed Temperature, °F.	Specific Gravity 60/60 °F.					Observed Temperature, °F.	Specific Gravity 60/60 °F.				
	0.500		0.505		0.510		0.500		0.505		0.510
	Factor for Reducing Volume to 60 °F.						Factor for Reducing Volume to 60 °F.				
50	1.017	0	1.017	1	1.016	95	0.937	1	0.938	2	0.940
51	1.015	0	1.015	1	1.014	96	0.935	2	0.937	2	0.939
52	1.014	1	1.013	1	1.012	97	0.933	2	0.935	2	0.937
53	1.012	0	1.012	1	1.011	98	0.931	2	0.933	2	0.935
54	1.010	0	1.010	1	1.009	99	0.929	2	0.931	2	0.933
55	1.009	1	1.008	0	1.008	100	0.927	2	0.929	3	0.932
56	1.007	0	1.007	1	1.006	101	0.925	2	0.927	3	0.930
57	1.005	0	1.005	0	1.005	102	0.923	2	0.925	3	0.928
58	1.003	0	1.003	0	1.003	103	0.921	3	0.924	3	0.927
59	1.002	0	1.002	0	1.002	104	0.919	3	0.922	3	0.925
60	1.000	0	1.000	0	1.000	105	0.917	3	0.920	3	0.923
61	0.998	0	0.998	0	0.998	106	0.915	3	0.918	3	0.921
62	0.997	0	0.997	0	0.997	107	0.913	3	0.916	3	0.919
63	0.995	0	0.995	0	0.995	108	0.911	3	0.914	3	0.917
64	0.993	0	0.993	1	0.994	109	0.909	3	0.912	3	0.915
65	0.991	1	0.992	0	0.992	110	0.907	3	0.910	3	0.913
66	0.990	0	0.990	0	0.990	111	0.905	3	0.908	3	0.911
67	0.988	0	0.988	1	0.989	112	0.903	3	0.906	3	0.909
68	0.986	0	0.986	1	0.987	113	0.901	3	0.904	4	0.908
69	0.985	0	0.985	0	0.985	114	0.899	3	0.902	4	0.906
70	0.983	0	0.983	1	0.984	115	0.897	3	0.900	4	0.904
71	0.981	1	0.982	0	0.982	116	0.895	3	0.898	4	0.902
72	0.979	1	0.980	1	0.981	117	0.893	3	0.896	4	0.900
73	0.978	0	0.978	1	0.979	118	0.891	3	0.894	4	0.898
74	0.976	0	0.976	1	0.977	119	0.889	3	0.892	4	0.896
75	0.974	1	0.975	1	0.976	120	0.887	3	0.890	4	0.894
76	0.972	1	0.973	1	0.974	121	0.885	3	0.888	4	0.892
77	0.970	1	0.971	1	0.972	122	0.883	3	0.886	4	0.890
78	0.969	0	0.969	1	0.970	123	0.880	4	0.884	4	0.888
79	0.967	1	0.968	1	0.969	124	0.878	4	0.882	4	0.886
80	0.965	1	0.966	1	0.967	125	0.876	4	0.880	4	0.884
81	0.963	1	0.964	1	0.965	126	0.874	4	0.878	4	0.882
82	0.961	1	0.962	1	0.963	127	0.872	4	0.876	4	0.880
83	0.959	1	0.960	2	0.962	128	0.869	4	0.873	4	0.877
84	0.957	1	0.958	2	0.960	129	0.867	4	0.871	4	0.875
85	0.956	1	0.957	1	0.958	130	0.865	4	0.869	4	0.873
86	0.954	1	0.955	1	0.956	131	0.863	4	0.867	4	0.871
87	0.952	1	0.953	2	0.955	132	0.861	4	0.865	4	0.869
88	0.950	1	0.951	2	0.953	133	0.858	4	0.862	5	0.867
89	0.948	2	0.950	1	0.951	134	0.856	4	0.860	5	0.865
90	0.946	2	0.948	1	0.949	135	0.854	4	0.858	5	0.863
91	0.944	2	0.946	1	0.947	136	0.852	4	0.856	5	0.861
92	0.942	2	0.944	2	0.946	137	0.849	5	0.854	5	0.859
93	0.940	2	0.942	2	0.944	138	0.847	5	0.852	4	0.856
94	0.938	2	0.940	2	0.942	139	0.844	6	0.850	4	0.854
95	0.937	1	0.938	1	0.940	140	0.842	6	0.848	4	0.852

Table 4. Volume Reduction to 60 °F for Liquefied Petroleum Gas

-50 to 0 °F.

Observed Tempera- ture °F.	Specific Gravity 60/60 °F.													
	0.570		0.575		0.580		0.585		0.590		0.595		0.600	
	Factor for Reducing Volume to 60 °F.													
-50	1.116	2	1.114	3	1.111	2	1.109	3	1.106	2	1.104	2	1.102	
-49	1.115	2	1.113	3	1.110	2	1.108	3	1.105	2	1.103	2	1.101	
-48	1.114	2	1.112	3	1.109	2	1.107	3	1.104	2	1.102	2	1.100	
-47	1.113	2	1.111	3	1.108	3	1.105	2	1.103	2	1.101	2	1.099	
-46	1.112	2	1.110	3	1.107	3	1.104	2	1.102	2	1.100	2	1.098	
-45	1.111	2	1.109	3	1.106	3	1.103	2	1.101	2	1.099	2	1.097	
-44	1.110	2	1.108	3	1.105	3	1.102	2	1.100	2	1.098	2	1.096	
-43	1.109	2	1.107	3	1.104	3	1.101	2	1.099	2	1.097	2	1.095	
-42	1.108	2	1.106	3	1.103	2	1.101	2	1.099	2	1.097	2	1.095	
-41	1.107	2	1.105	3	1.102	2	1.100	2	1.098	2	1.096	2	1.094	
-40	1.106	2	1.104	3	1.101	2	1.099	2	1.097	2	1.095	2	1.093	
-39	1.105	2	1.103	3	1.100	2	1.098	2	1.096	2	1.094	2	1.092	
-38	1.104	2	1.102	3	1.099	2	1.097	2	1.095	2	1.093	2	1.091	
-37	1.103	2	1.101	3	1.098	2	1.096	2	1.094	2	1.092	2	1.090	
-36	1.102	2	1.100	3	1.097	2	1.095	2	1.093	2	1.091	2	1.089	
-35	1.101	2	1.099	3	1.096	2	1.094	2	1.092	2	1.090	2	1.088	
-34	1.100	2	1.098	3	1.095	2	1.093	2	1.091	2	1.089	2	1.087	
-33	1.099	2	1.097	3	1.094	2	1.092	2	1.090	2	1.088	2	1.086	
-32	1.098	2	1.096	2	1.094	2	1.092	2	1.090	2	1.088	2	1.086	
-31	1.097	2	1.095	2	1.093	2	1.091	2	1.089	2	1.087	2	1.085	
-30	1.096	2	1.094	2	1.092	2	1.090	2	1.088	2	1.086	2	1.084	
-29	1.095	2	1.093	2	1.091	2	1.089	2	1.087	2	1.085	2	1.083	
-28	1.094	2	1.092	2	1.090	2	1.088	2	1.086	2	1.084	2	1.082	
-27	1.093	2	1.091	2	1.089	2	1.087	2	1.085	1	1.084	2	1.082	
-26	1.092	2	1.090	2	1.088	2	1.086	2	1.084	1	1.083	2	1.081	
-25	1.091	2	1.089	2	1.087	2	1.085	2	1.083	1	1.082	2	1.080	
-24	1.090	2	1.088	2	1.086	2	1.084	2	1.082	1	1.081	2	1.079	
-23	1.089	2	1.087	2	1.085	2	1.083	2	1.081	1	1.080	2	1.078	
-22	1.088	2	1.086	2	1.084	2	1.082	1	1.081	2	1.079	1	1.078	
-21	1.087	2	1.085	2	1.083	2	1.081	1	1.080	2	1.078	1	1.077	
-20	1.086	2	1.084	2	1.082	2	1.080	1	1.079	2	1.077	1	1.076	
-19	1.085	2	1.083	2	1.081	2	1.079	1	1.078	2	1.076	1	1.075	
-18	1.084	2	1.082	2	1.080	2	1.078	1	1.077	2	1.075	1	1.074	
-17	1.082	1	1.081	2	1.079	2	1.077	1	1.076	1	1.075	2	1.073	
-16	1.081	1	1.080	2	1.078	2	1.076	1	1.075	1	1.074	2	1.072	
-15	1.080	1	1.079	2	1.077	2	1.075	1	1.074	1	1.073	2	1.071	
-14	1.079	1	1.078	2	1.076	2	1.074	1	1.073	1	1.072	2	1.070	
-13	1.078	1	1.077	2	1.075	2	1.073	1	1.072	1	1.071	2	1.069	
-12	1.077	1	1.076	2	1.074	1	1.073	2	1.071	1	1.070	2	1.068	
-11	1.076	1	1.075	2	1.073	1	1.072	2	1.070	1	1.069	2	1.067	
-10	1.075	1	1.074	2	1.072	1	1.071	2	1.069	1	1.068	2	1.066	
-9	1.074	1	1.073	2	1.071	1	1.070	2	1.068	1	1.067	2	1.065	
-8	1.073	1	1.072	2	1.070	1	1.069	2	1.067	1	1.066	2	1.064	
-7	1.072	1	1.071	2	1.069	1	1.068	1	1.067	2	1.065	2	1.063	
-6	1.071	1	1.070	2	1.068	1	1.067	1	1.066	2	1.064	2	1.062	
-5	1.070	1	1.069	2	1.067	1	1.066	1	1.065	2	1.063	2	1.061	
-4	1.069	1	1.068	2	1.066	1	1.065	1	1.064	2	1.062	2	1.060	
-3	1.068	1	1.067	2	1.065	1	1.064	1	1.063	2	1.061	2	1.059	
-2	1.068	2	1.066	1	1.065	1	1.064	1	1.063	2	1.061	2	1.059	
-1	1.067	2	1.065	1	1.064	1	1.063	1	1.062	2	1.060	2	1.058	
0	1.066	2	1.064	1	1.063	1	1.062	1	1.061	2	1.059	2	1.057	

Table 4. Volume Reduction to 60 °F for Liquefied Petroleum Gas

0 to 50 °F.

Observed Temperature °F.	Specific Gravity 60/60 °F.													
	0.570		0.575		0.580		0.585		0.590		0.595		0.600	
	Factor for Reducing Volume to 60 °F.													
0	1.066	2	1.064	1	1.063	1	1.062	1	1.061	2	1.059	2	1.057	
1	1.065	2	1.063	1	1.062	1	1.061	1	1.060	2	1.058	2	1.056	
2	1.064	2	1.062	1	1.061	1	1.060	1	1.059	2	1.057	2	1.055	
3	1.063	2	1.061	1	1.060	1	1.059	1	1.058	2	1.056	2	1.054	
4	1.062	2	1.060	1	1.059	1	1.058	1	1.057	2	1.055	1	1.054	
5	1.061	2	1.059	1	1.058	1	1.057	2	1.055	1	1.054	1	1.053	
6	1.059	1	1.058	1	1.057	2	1.055	1	1.054	1	1.053	1	1.052	
7	1.058	1	1.057	1	1.056	2	1.054	1	1.053	1	1.052	1	1.051	
8	1.057	1	1.056	1	1.055	2	1.053	1	1.052	1	1.051	1	1.050	
9	1.056	1	1.055	1	1.054	2	1.052	1	1.051	1	1.050	1	1.049	
10	1.055	1	1.054	1	1.053	2	1.051	1	1.050	1	1.049	1	1.048	
11	1.054	1	1.053	1	1.052	2	1.050	1	1.049	1	1.048	1	1.047	
12	1.053	1	1.052	1	1.051	2	1.049	1	1.048	1	1.047	1	1.046	
13	1.052	1	1.051	1	1.050	2	1.048	1	1.047	1	1.046	1	1.045	
14	1.051	1	1.050	1	1.049	2	1.047	1	1.046	1	1.045	1	1.044	
15	1.050	2	1.048	1	1.047	1	1.046	1	1.045	1	1.044	1	1.043	
16	1.048	1	1.047	1	1.046	1	1.045	1	1.044	1	1.043	1	1.042	
17	1.047	1	1.046	1	1.045	1	1.044	1	1.043	1	1.042	1	1.041	
18	1.046	1	1.045	1	1.044	1	1.043	1	1.042	1	1.041	1	1.040	
19	1.045	1	1.044	1	1.043	1	1.042	1	1.041	1	1.040	1	1.039	
20	1.044	1	1.043	1	1.042	1	1.041	1	1.040	1	1.039	1	1.038	
21	1.043	1	1.042	1	1.041	1	1.040	1	1.039	1	1.038	1	1.037	
22	1.042	1	1.041	1	1.040	1	1.039	1	1.038	1	1.037	0	1.037	
23	1.041	1	1.040	1	1.039	1	1.038	1	1.037	1	1.036	0	1.036	
24	1.040	1	1.039	1	1.038	1	1.037	1	1.036	1	1.035	0	1.035	
25	1.039	1	1.038	1	1.037	1	1.036	1	1.035	0	1.035	1	1.034	
26	1.037	0	1.037	1	1.036	1	1.035	1	1.034	0	1.034	0	1.033	
27	1.036	0	1.036	1	1.035	1	1.034	1	1.033	0	1.033	1	1.032	
28	1.035	0	1.035	1	1.034	1	1.033	1	1.032	0	1.032	1	1.031	
29	1.034	0	1.034	1	1.033	1	1.032	1	1.031	0	1.031	1	1.030	
30	1.033	0	1.033	1	1.032	1	1.031	1	1.030	0	1.030	1	1.029	
31	1.032	1	1.031	0	1.031	1	1.030	1	1.029	0	1.029	0	1.028	
32	1.031	1	1.030	0	1.030	1	1.029	1	1.028	0	1.028	1	1.027	
33	1.030	1	1.029	0	1.029	1	1.028	1	1.027	0	1.027	1	1.026	
34	1.029	1	1.028	0	1.028	1	1.027	1	1.026	0	1.026	1	1.025	
35	1.028	1	1.027	0	1.027	1	1.026	1	1.025	0	1.025	1	1.024	
36	1.027	1	1.026	1	1.025	0	1.025	1	1.024	0	1.024	1	1.023	
37	1.026	1	1.025	1	1.024	0	1.024	1	1.023	0	1.023	1	1.022	
38	1.025	1	1.024	1	1.023	0	1.023	1	1.022	0	1.022	1	1.021	
39	1.024	1	1.023	1	1.022	0	1.022	1	1.021	0	1.021	1	1.020	
40	1.023	1	1.022	1	1.021	0	1.021	1	1.020	0	1.020	1	1.019	
41	1.022	1	1.021	1	1.020	0	1.020	1	1.019	0	1.019	1	1.018	
42	1.021	1	1.020	1	1.019	0	1.019	1	1.018	0	1.018	1	1.017	
43	1.019	0	1.019	1	1.018	0	1.018	1	1.017	0	1.017	1	1.016	
44	1.018	0	1.018	1	1.017	0	1.017	1	1.016	0	1.016	1	1.015	
45	1.017	0	1.017	1	1.016	0	1.016	1	1.015	0	1.015	0	1.015	
46	1.016	1	1.015	0	1.015	0	1.015	1	1.014	0	1.014	0	1.014	
47	1.015	1	1.014	0	1.014	0	1.014	1	1.013	0	1.013	0	1.013	
48	1.013	0	1.013	0	1.013	0	1.013	1	1.012	0	1.012	0	1.012	
49	1.012	0	1.012	0	1.012	0	1.012	1	1.011	0	1.011	0	1.011	
50	1.011	0	1.011	0	1.011	0	1.011	1	1.010	0	1.010	0	1.010	

Table 4. Volume Reduction to 60 °F for Liquefied Petroleum Gas

50 – 100 °F

Observed Tempera- ture °F.	Specific Gravity 60/60 °F.													
	0.570		0.575		0.580		0.585		0.590		0.595		0.600	
	Factor for Reducing Volume to 60 °F.													
50	1.011	0	1.011	0	1.011	0	1.011	1	1.010	0	1.010	0	1.010	
51	1.010	0	1.010	0	1.010	0	1.010	1	1.009	0	1.009	0	1.009	
52	1.009	0	1.009	0	1.009	0	1.009	1	1.008	0	1.008	0	1.008	
53	1.008	0	1.008	0	1.008	1	1.007	0	1.007	0	1.007	02	1.007	
54	1.007	0	1.007	0	1.007	1	1.006	0	1.006	0	1.006	0	1.006	
55	1.006	0	1.006	0	1.006	1	1.005	0	1.005	0	1.005	0	1.005	
56	1.005	1	1.004	0	1.004	0	1.004	0	1.004	0	1.004	0	1.004	
57	1.003	0	1.003	0	1.003	0	1.003	0	1.003	0	1.003	0	1.003	
58	1.002	0	1.002	0	1.002	0	1.002	0	1.002	0	1.002	0	1.002	
59	1.001	0	1.001	0	1.001	0	1.001	0	1.001	0	1.001	0	1.001	
60	1.000	0	1.000	0	1.000	0	1.000	0	1.000	0	1.000	0	1.000	
61	0.999	0	0.999	0	0.999	0	0.999	0	0.999	0	0.999	0	0.999	
62	0.998	0	0.998	0	0.998	0	0.998	0	0.998	0	0.998	0	0.998	
63	0.997	0	0.997	0	0.997	0	0.997	0	0.997	0	0.997	0	0.997	
64	0.995	0	0.995	1	0.996	0	0.996	0	0.996	0	0.996	0	0.996	
65	0.994	0	0.994	0	0.994	1	0.995	0	0.995	0	0.995	0	0.995	
66	0.993	0	0.993	0	0.993	0	0.993	0	0.993	1	0.994	0	0.994	
67	0.992	0	0.992	0	0.992	0	0.992	0	0.992	1	0.993	0	0.993	
68	0.990	1	0.991	0	0.991	0	0.991	0	0.991	1	0.992	0	0.992	
69	0.989	1	0.990	0	0.990	0	0.990	0	0.990	1	0.991	0	0.991	
70	0.988	0	0.988	1	0.989	0	0.989	0	0.989	1	0.990	0	0.990	
71	0.987	0	0.987	1	0.988	0	0.988	0	0.988	1	0.989	0	0.989	
72	0.986	0	0.986	1	0.987	0	0.987	0	0.987	1	0.988	0	0.988	
73	0.985	0	0.985	1	0.986	0	0.986	0	0.986	1	0.987	0	0.987	
74	0.984	0	0.984	1	0.985	0	0.985	0	0.985	1	0.986	0	0.986	
75	0.983	0	0.983	0	0.983	1	0.984	0	0.984	1	0.985	0	0.985	
76	0.981	1	0.982	0	0.982	1	0.983	0	0.983	1	0.984	0	0.984	
77	0.980	1	0.981	0	0.981	0	0.981	1	0.982	1	0.983	0	0.983	
78	0.979	0	0.979	1	0.980	0	0.980	1	0.981	1	0.982	0	0.982	
79	0.978	0	0.978	1	0.979	0	0.979	1	0.980	1	0.981	0	0.981	
80	0.977	0	0.977	1	0.978	0	0.978	1	0.979	1	0.980	1	0.981	
81	0.975	1	0.976	1	0.977	0	0.977	1	0.978	1	0.979	1	0.980	
82	0.974	1	0.975	1	0.976	0	0.976	1	0.977	1	0.978	1	0.979	
83	0.973	0	0.974	1	0.975	0	0.975	1	0.976	1	0.977	1	0.978	
84	0.972	0	0.973	1	0.974	0	0.974	1	0.975	1	0.976	1	0.977	
85	0.971	0	0.971	1	0.972	1	0.973	1	0.974	1	0.975	1	0.976	
86	0.969	1	0.970	1	0.971	1	0.972	1	0.973	1	0.974	1	0.975	
87	0.968	1	0.969	1	0.970	1	0.971	1	0.972	1	0.973	1	0.974	
88	0.967	1	0.968	1	0.969	1	0.970	1	0.971	1	0.972	1	0.973	
89	0.966	1	0.967	1	0.968	1	0.969	1	0.970	1	0.971	1	0.972	
90	0.964	2	0.966	1	0.967	0	0.967	1	0.968	2	0.970	1	0.971	
91	0.963	1	0.964	1	0.965	1	0.966	1	0.967	2	0.969	1	0.970	
92	0.962	1	0.963	1	0.964	1	0.965	1	0.966	2	0.968	1	0.969	
93	0.961	1	0.962	1	0.963	1	0.964	1	0.965	2	0.967	1	0.968	
94	0.959	2	0.961	1	0.962	1	0.963	1	0.964	2	0.966	1	0.967	
95	0.958	1	0.959	2	0.961	1	0.962	1	0.963	2	0.965	1	0.966	
96	0.957	1	0.958	1	0.959	1	0.960	2	0.962	2	0.964	1	0.965	
97	0.956	1	0.957	1	0.958	1	0.959	2	0.961	2	0.963	1	0.964	
98	0.954	2	0.956	1	0.957	1	0.958	2	0.960	2	0.962	1	0.963	
99	0.953	2	0.955	1	0.956	1	0.957	2	0.959	2	0.961	1	0.962	
100	0.952	1	0.953	1	0.954	2	0.956	2	0.958	1	0.859	2	0.961	

Table 4. Volume Reduction to 60 °F for Liquefied Petroleum Gas

100 – 140 °F.

Observed Tempera- ture °F.	Specific Gravity 60/60 °F.													
	0.570		0.575		0.580		0.585		0.590		0.595		0.600	
	Factor for Reducing Volume to 60 °F.													
100	0.952	1	0.953	1	0.954	2	0.956	2	0.958	1	0.959	2	0.961	
101	0.951	1	0.952	1	0.953	2	0.955	2	0.957	1	0.958	2	0.960	
102	0.950	1	0.951	1	0.952	2	0.954	2	0.956	1	0.957	2	0.959	
103	0.948	1	0.949	2	0.951	1	0.952	2	0.954	2	0.056	2	0.958	
104	0.947	1	0.948	2	0.950	1	0.951	2	0.953	2	0.955	2	0.957	
105	0.946	1	0.947	2	0.949	1	0.950	2	0.952	2	0.954	2	0.956	
106	0.945	1	0.946	2	0.948	1	0.949	2	0.951	2	0.953	2	0.955	
107	0.943	2	0.945	2	0.947	1	0.948	2	0.950	2	0.952	2	0.954	
108	0.942	1	0.943	2	0.945	2	0.947	2	0.949	2	0.951	2	0.953	
109	0.940	2	0.942	2	0.944	2	0.946	2	0.948	2	0.950	2	0.952	
110	0.939	2	0.941	2	0.943	2	0.945	2	0.947	2	0.949	2	0.951	
111	0.938	2	0.940	2	0.942	2	0.944	2	0.946	2	0.948	2	0.950	
112	0.937	2	0.939	2	0.941	2	0.943	2	0.945	2	0.947	2	0.949	
113	0.935	2	0.937	2	0.939	2	0.941	2	0.943	3	0.946	2	0.948	
114	0.934	2	0.936	2	0.938	2	0.940	2	0.942	3	0.945	2	0.947	
115	0.933	2	0.935	2	0.937	2	0.939	2	0.941	3	0.944	2	0.946	
116	0.932	2	0.934	2	0.936	2	0.938	2	0.940	3	0.943	2	0.945	
117	0.931	2	0.933	2	0.935	2	0.937	2	0.939	3	0.942	2	0.944	
118	0.929	2	0.931	2	0.933	2	0.935	3	0.938	2	0.940	3	0.943	
119	0.928	2	0.930	2	0.932	2	0.934	3	0.937	2	0.939	3	0.942	
120	0.927	2	0.929	2	0.931	2	0.933	3	0.936	2	0.938	3	0.941	
121	0.926	2	0.928	2	0.930	2	0.932	3	0.935	2	0.937	3	0.940	
122	0.924	3	0.927	2	0.929	2	0.931	3	0.934	2	0.936	3	0.939	
123	0.923	2	0.925	2	0.927	2	0.929	3	0.932	3	0.935	3	0.938	
124	0.921	3	0.924	2	0.926	2	0.928	3	0.931	3	0.934	3	0.937	
125	0.920	3	0.923	2	0.925	2	0.927	3	0.930	3	0.933	3	0.936	
126	0.919	3	0.922	2	0.924	2	0.926	3	0.929	3	0.932	3	0.935	
127	0.917	3	0.920	2	0.922	3	0.925	3	0.928	3	0.931	3	0.934	
128	0.916	3	0.919	2	0.921	2	0.923	3	0.926	4	0.930	3	0.933	
129	0.914	3	0.917	2	0.919	3	0.922	3	0.925	4	0.929	3	0.932	
130	0.913	3	0.916	2	0.918	3	0.921	3	0.924	4	0.928	3	0.931	
131	0.912	3	0.915	2	0.917	3	0.920	3	0.923	4	0.927	3	0.930	
132	0.911	2	0.913	3	0.916	2	0.918	4	0.922	4	0.926	3	0.929	
133	0.909	3	0.912	2	0.914	3	0.917	3	0.920	5	0.925	3	0.928	
134	0.908	2	0.910	3	0.913	2	0.915	4	0.919	5	0.924	3	0.927	
135	0.907	2	0.909	3	0.912	2	0.914	4	0.918	5	0.923	3	0.926	
136	0.906	2	0.908	3	0.911	2	0.913	4	0.917	5	0.922	3	0.925	
137	0.904	3	0.907	2	0.909	3	0.912	4	0.916	5	0.921	3	0.924	
138	0.903	2	0.905	3	0.908	2	0.910	4	0.914	5	0.919	4	0.923	
139	0.901	3	0.904	2	0.906	3	0.909	4	0.913	5	0.918	4	0.922	
140	0.900	3	0.903	2	0.905	3	0.908	4	0.912	5	0.917	4	0.921	

Table 4A. Properties of Saturated Liquid Ammonia at Various Temperatures

Temperature ° F	Vapor Pressure (psig) ¹	Liquid Density		Volume Correction to 60 °F ²
		Pounds per Cubic Foot ¹	Pounds per U.S. Gallon ²	
-28	0.0	42.57	5.961	1.1057
-25	1.3	42.44	5.673	1.1023
-20	3.6	42.22	5.644	1.0966
-15	6.2	42.00	5.615	1.0909
-10	9.0	41.78	5.585	1.0852
-5	12.2	41.56	5.556	1.0795
0	15.7	41.34	5.526	1.0738
5	19.6	41.11	5.496	1.0678
10	23.8	40.89	5.466	1.0621
15	28.4	40.66	5.435	1.0561
20	33.5	40.43	5.405	1.0501
25	39.0	40.20	5.374	1.0442
30	45.0	39.96	5.342	1.0379
35	51.6	39.72	5.310	1.0317
40	58.6	39.49	5.279	1.0257
45	66.3	39.24	5.246	1.0192
50	74.5	39.00	5.214	1.0130
55	83.4	38.75	5.180	1.0065
60	92.9	38.50	5.147	1.0000
65	103.1	38.25	5.113	0.9935
70	114.1	38.00	5.080	0.9870
75	125.8	37.74	5.045	0.9803
80	138.3	37.48	5.010	0.9735
85	151.7	37.21	4.974	0.9665
90	165.9	36.95	4.939	0.9597
95	181.1	36.67	4.902	0.9525
100	197.2	36.40	4.866	0.9455
105	214.2	36.12	4.829	0.9382
110	232.3	35.84	4.791	0.9309
115	251.5	35.55	4.752	0.9234
120	271.7	35.26	4.714	0.9158
125	293.1	34.96	4.673	0.9081
130	315.6	34.66	4.633	0.9003
135	339.4	34.35	4.592	0.8922
140	364.4	34.04	4.550	0.8842

¹ Data from Nat'l Bureau of Stds Circular No. 142; ² Values calculated from liquid density in lb/cubic foot.

List of Suggested Fittings for an LPG Prover For Connecting to Non-Standard Supply Tanks

1. 1-3/4" Female Acme x 1-1/4" H.D. Male Evertite
2. 1-3/4" Female Acme x 2" H.D. Male Evertite
3. 1-1/4" Female Acme x 1-3/4" Male Acme
4. 1-3/4" Male Acme x 3/4" H.D. Female Evertite
5. 1-3/4" Male Acme x 1" H.D. Female Evertite
6. 1-3/4" Male Acme x 2-1/4" Female Acme
7. 1-3/4" Male Acme x 1-1/2" Female Evertite
8. 1-3/4" Male Acme x 2" H.D. Female Evertite
9. 1-3/4" Female Acme x 1-1/4" Male Acme
10. 3" Female Acme x 1-1/4" Male Acme