

# SECA 2003 Core Technology Program Review Meeting

## Model Tool Development & Application at NETL

- a) NETL/Fluent Fuel Cell Model
- b) Effects of Dynamic Loads on SOFCs

*R.S. Gemmen*  
*September 30, 2003*  
*Albany, NY*



Participants: Rogers, Prinkey, Shahnam, Johnson, Pineault, Gemmen  
Sponsor: SECA Program



# CFD Tools--Technical Issues

- **Success in the commercialization of SEC technology will depend on:**
  - reducing manufacturing costs
    - Improve power density ( $\sim 0.5 \text{ W/cm}^2$ )
  - producing a usable technology...
    - success in durability (>40,000 hours)
    - success in energy conversion efficiency
      - Manage flow distribution
      - Manage current distribution
      - Manage thermal stress distribution
- **One-Dim codes fine for performance prediction, but not “distribution design/management”.**



# R&D Objective

**Develop modeling tools that can provide developers with detailed information on cell performance**

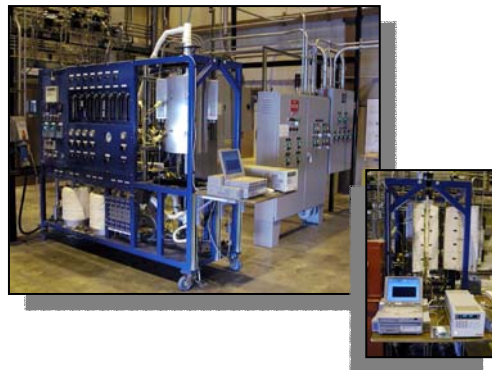
**to enable**

**design solutions for optimal performance and lifetimes**



# Approach

- **Develop and validate detailed fuel cell model**
  - Use commercial CFD code as underlying platform
    - FLUENT code is parallel, unstructured mesh, with well-validated models for fluid flow, heat transfer, species transport
    - Industry-accepted code already in use by SECA developers
    - Output compatible with ANSYS
  - Validate the code using experimental data
    - Single cell and cell stack data



## Approach (cont.)

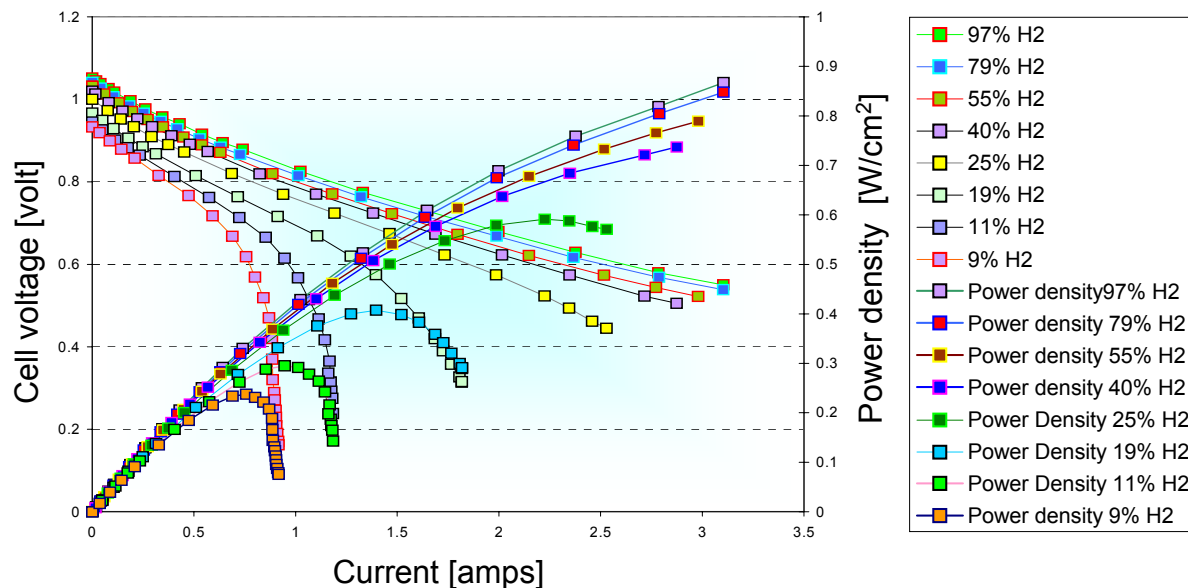
- **FLUENT handles all aspects of the hydrodynamics, species transport and heat transfer in the flow channels and the porous electrodes (anode and cathode).**
- **A User Defined Function (UDF) is used to model**
  - electrochemical reactions
  - potential field in the electrically conducting zones
- **The model is parallelized and shows identical scaling to normal Parallel FLUENT. The fuel cell model is only a small computation**
- **Includes treatment for CO/H<sub>2</sub> electrochemistry**
- **The model has been tested for stack configurations**



# Results

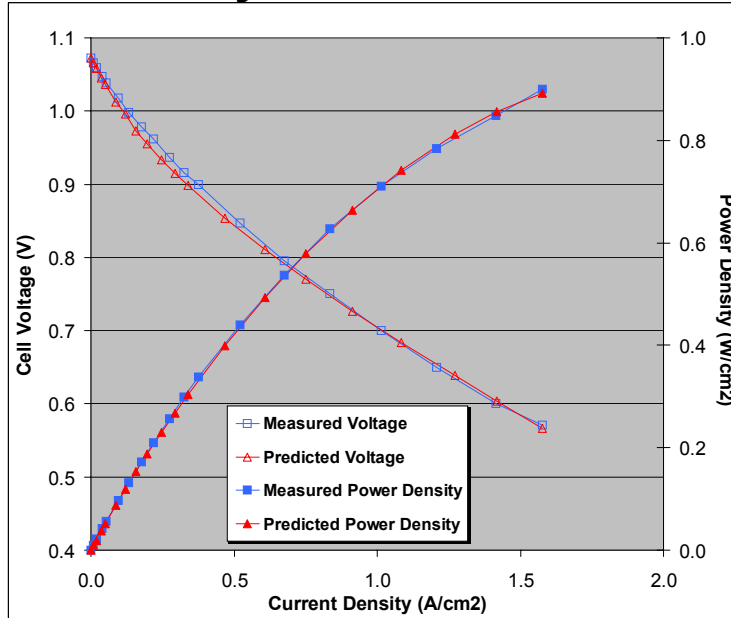
- **Electrochemical UDF code has been developed to provide electrochemical analysis suitable to**
  - analyze a wide range of fuel cell concepts
  - evaluate sensitivity to manufacturing tolerances and failure modes (e.g., effect of regional loss of connection b/t electrode and interconnects)
- **Tool now being validated using ‘standardized’ cells in collaboration with UoU.**

**NETL Data:  
Standard Cell (UoU),  
800C, varying fuel  
composition (H2,  
N2, H2O)**

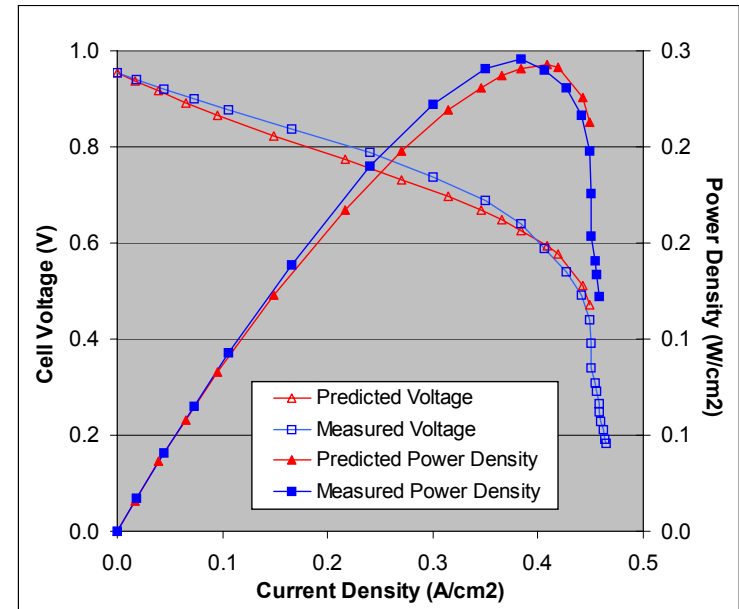


# Productivity and Results

- **Preliminary Validation of model**



- **Standard Cell: 800C, 97% H<sub>2</sub>, 3% H<sub>2</sub>O**
- **Best fit with data:**
  - Electrolyte resistivity = **1.9 ohm-m**
  - Cathode Exchange Current Density = **1000 A/m<sup>2</sup>**
- **Data for varying electrolyte thickness will provide more accurate values**

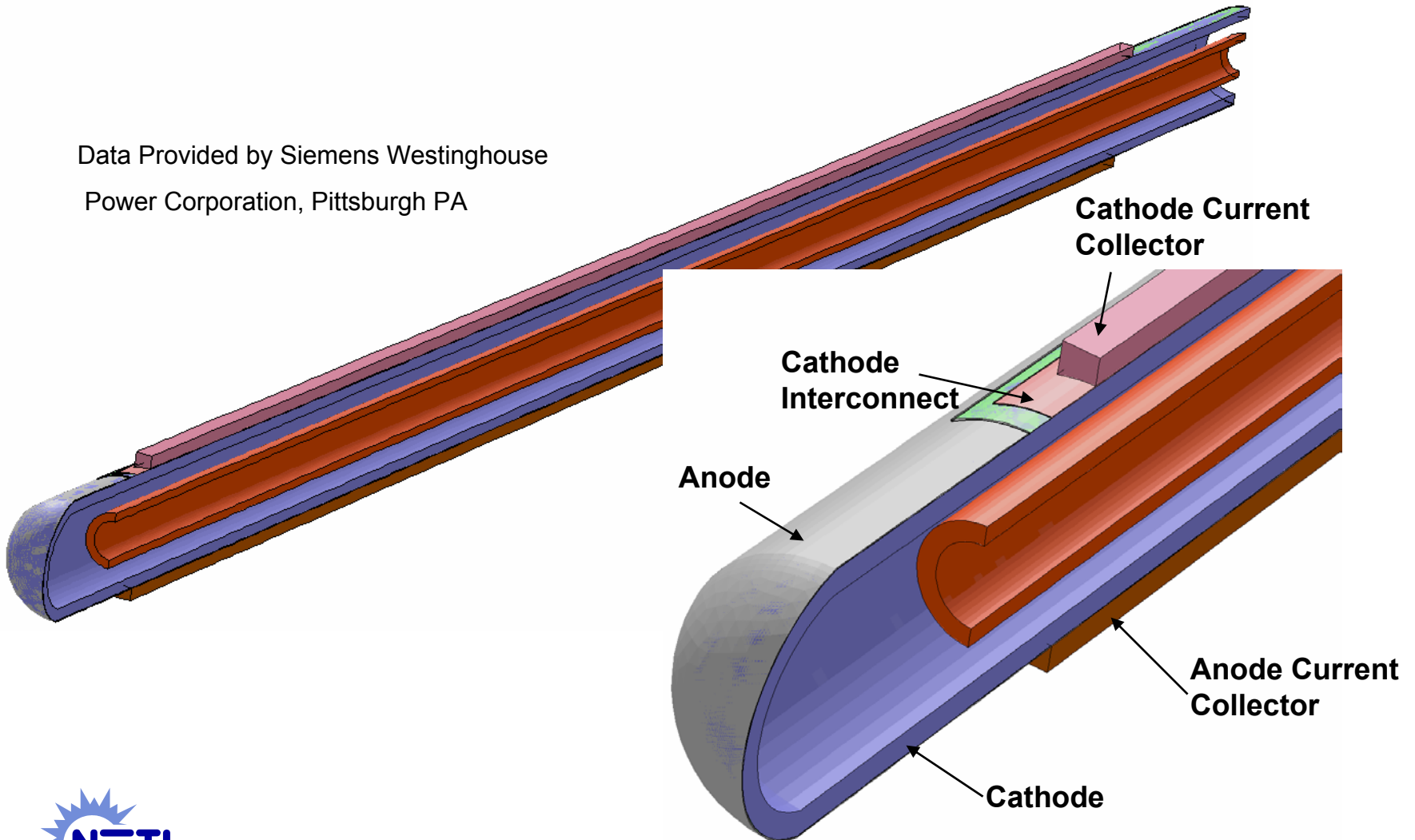


- **Standard Cell: 800C, 9% H<sub>2</sub>, 3% H<sub>2</sub>O, Balance N<sub>2</sub>**
- **Best fit based on qualitative agreement with data:**
  - Tortuosity in both regions = **3.3**



# Results (cont.)

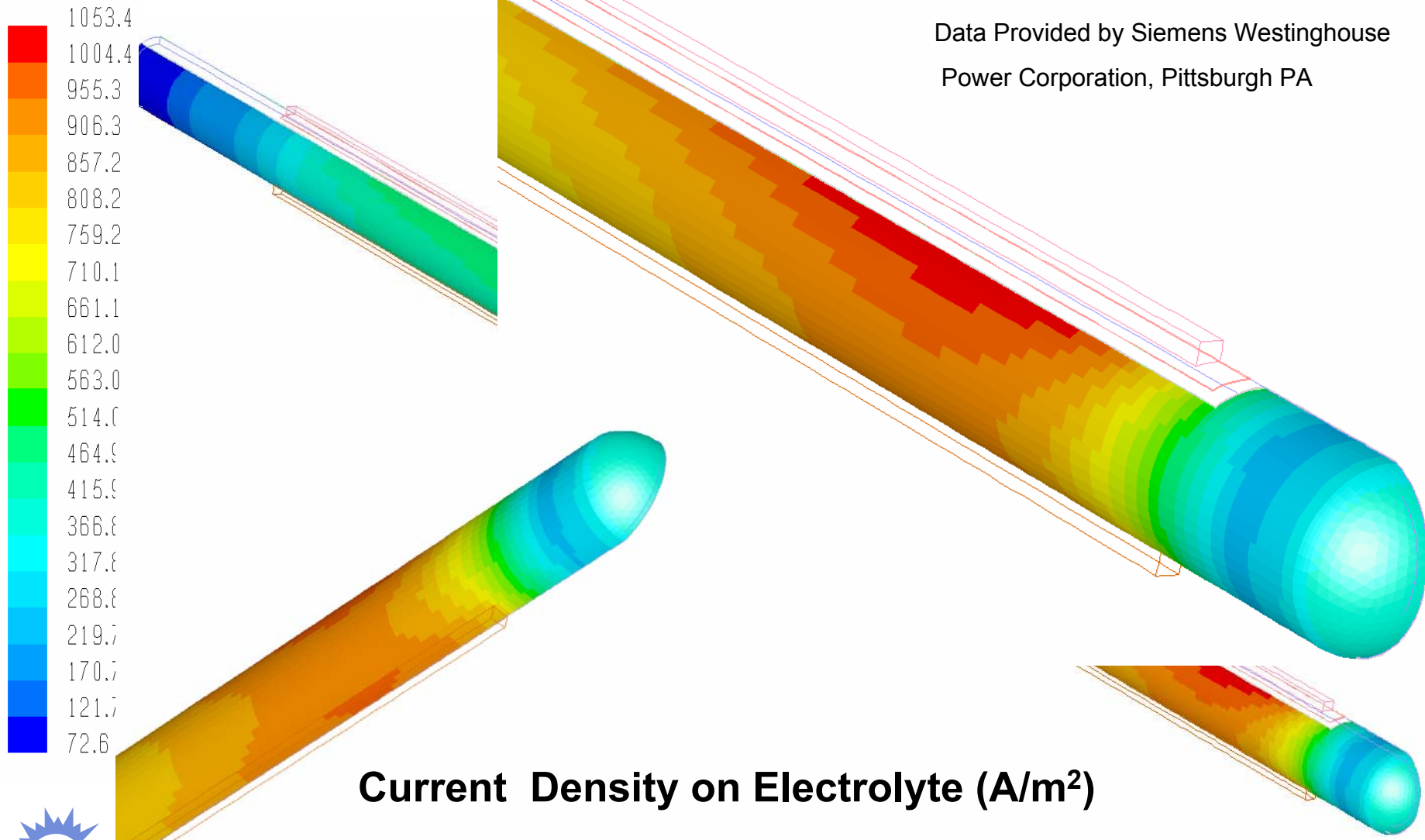
Data Provided by Siemens Westinghouse  
Power Corporation, Pittsburgh PA





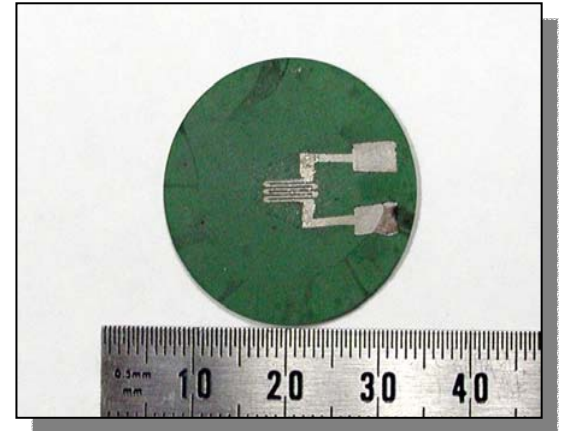
# Results (cont.)

Data Provided by Siemens Westinghouse  
Power Corporation, Pittsburgh PA



## Other Related Results (cont.)

- **Sensors for Fuel Cell Diagnostics**
  - High-temperature thin film sensors to measure temperature, strain and heat flux
  - Sensors can be applied to fuel cell anodes and cathodes, embedded on electrolyte, or applied to stack hardware such as seals and interconnects
  - Measure fuel cell strain
  - Measurements can be used for stress and temperature model validation



URI strain gage applied to SOFC anode

# Applicability to SOFC Commercialization

- **Providing basic engineering tools suitable for detailed cell and stack analysis.**
- **Capability enables fuel cell designers to better predict and manage flow, current and temperature distributions.**

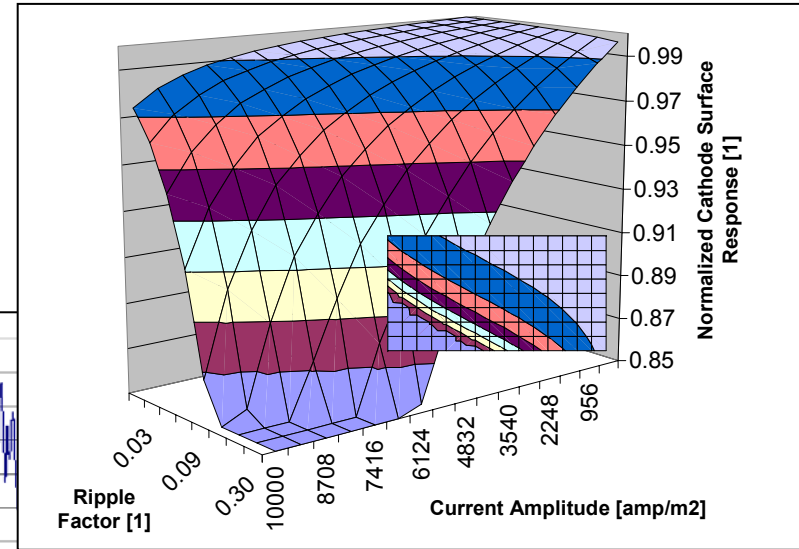
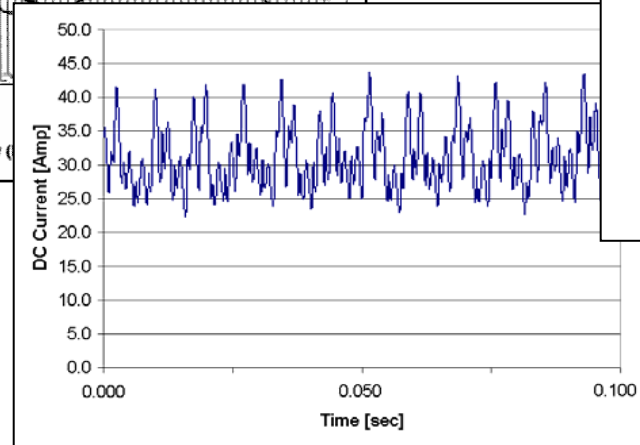
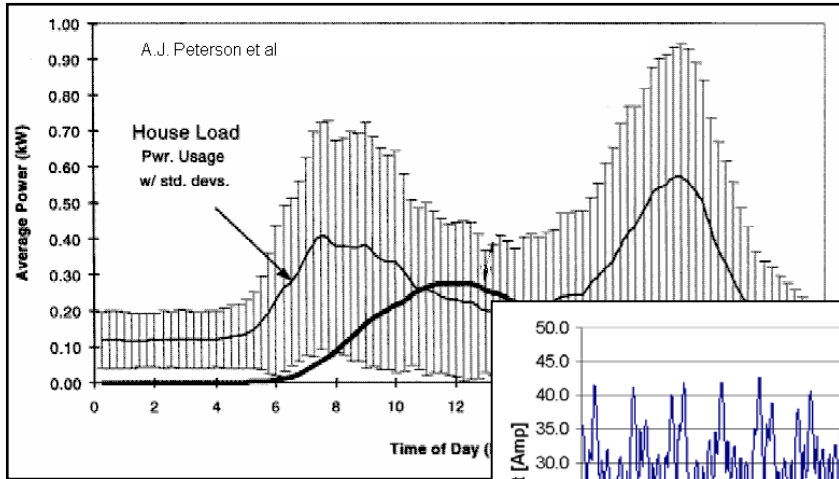


# FY04 Work Plans

- **Continued Validation (Q1-Q4/FY04)**
  - NETL data (button and full-size cells)
  - SW data
  - UTRC data
- **Transient Application of SOFC Model (Q1/FY04)**
- **Release to SECA Vertical Teams (Q2/FY04)**
- **Internal Reforming Model (Q2/FY04)**
- **Link NETL SOFC Model with ANSYS (Q3/FY04)**
  - validation
  - application



# Dynamic Analysis



# Technical Issues

- **Success in the commercialization of SECA technology will depend on:**
  - reducing manufacturing costs
  - producing a usable technology...
    - success in durability (>40,000 hours)
    - success in energy conversion efficiency
    - success in managing dynamics
      - less than XX minute startup (pick a number!)
      - safe and failure-free shutdown
      - load transients
      - ...



# Technical Issues (cont.)

## Power Conditioning Induced Load Dynamics



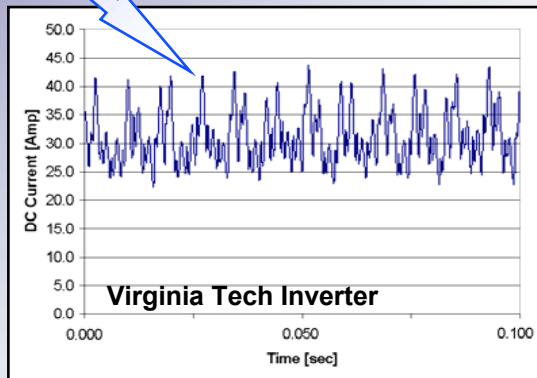
Virkar (2001)



Inverter  
AC Power



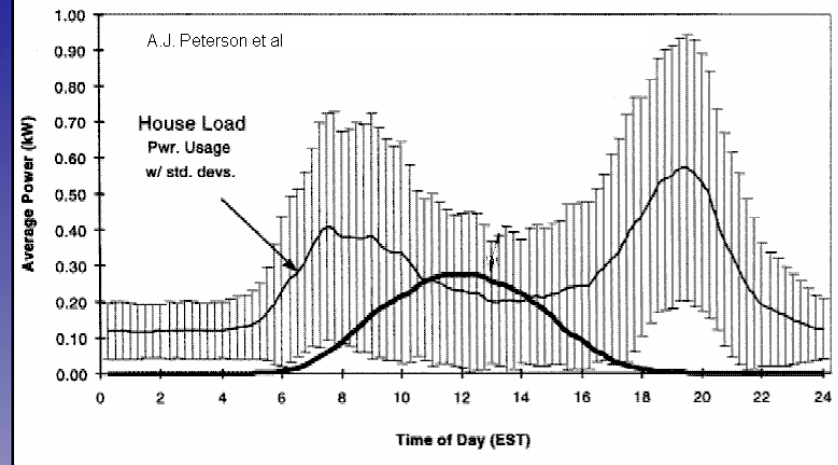
Lesster (2000)  
filtering for low ripple  
is costly.



### Research questions:

- how do dynamic loadings compare to steady?
- at what amplitude/cut-off frequency will such oscillatory loadings have negligible impact?

## Application Induced Load Dynamics



- Commonly use fast energy storage device (batteries)
- Minimize system cost (e.g., batteries) by allowing fuel cell load dynamics



# Background (cont.)

- A literature search on *fuel cell dynamics* yields little helpful information.
- Dynamic concerns at the cell level have not yet been addressed.
- Riso Nat. Lab studied impacts of steady loading on degradation. Jorgensen et al. (2000) indicate current loading causes degradation in cell materials.
- Degradation mechanisms (steady or non-steady loaded) not clear, Badwal (2001).
- Most prior transient studies focused on cell thermal behavior under heat-up, or employed simple lumped models for system studies (no detailed and coupled electrochemistry).





# Technical Investigations

- **Transient loads**
  - Application load driven
  - Inverter driven
- **Experimental**
  - Button cells
  - 10cmx10cm cells
- **Modeling**
- **Understanding to be acquired**
  - Details of cell operation
    - $Y(x,y,t)$
    - $T(x,y,t)$
    - $\sigma(x,y,t)$
  - Deviation in behavior from steady-state loads



# Technical Challenges for Investigating Effects of Dynamic Loads

- **Need improved understanding on resultant transient behavior in and around PEN to improve durability.**
- **Detailed electrochemical codes not ready for transient studies.**
- **Detailed transient studies can be time consuming.**
- **SOFC test conditions are challenging.**
- **Long duration tests often required to assess degradation.**
- **Reliable experimental results/conclusions require repeatability in specimen fabrication and test setup.**
- **Identifying correct degradation mechanisms is not easy even for steady-state loads.**



# R&D Objective

**Understand the impact of dynamic loads on the cell level reactant histories, thermal transients, component stress, and fuel cell degradation**

**to enable**

**design solutions for optimal startup and lifetimes**



# Technical Approach

- **Modeling**

- Goal: Identify impact of dynamic loads on species concentration and temperature changes to help quantify deviation from SS loads
- Apply existing (NETL developed) one-dimensional models
  - Investigate spatial transient behavior over a cell (cell performance model)
  - Investigate electrode response due to ripple (electrode transport model)
  - Guide experimental analysis by providing estimates for experimental load conditions



# Technical Approach (cont.)

- **Experimental**

- Work with external partners to acquire ‘standardized’ button cells (repeatable fabrication, well characterized). UoU-button.
- Use existing SOFCEL facility to run both steady-state (baseline) and dynamic (20-30% ripple) loadings.
- Apply AC impedance and galvanostatic/potentiostatic techniques to identify performance changes.
- Consult with materials experts to help with materials measurements and identifying material degradation mechanisms (PNNL, ORNL):
  - SEM - identify material structural changes
  - XRD - material phase changes
  - XPS – material phase changes



# Technical Approach (cont.)

- Results published in conference and journal articles.



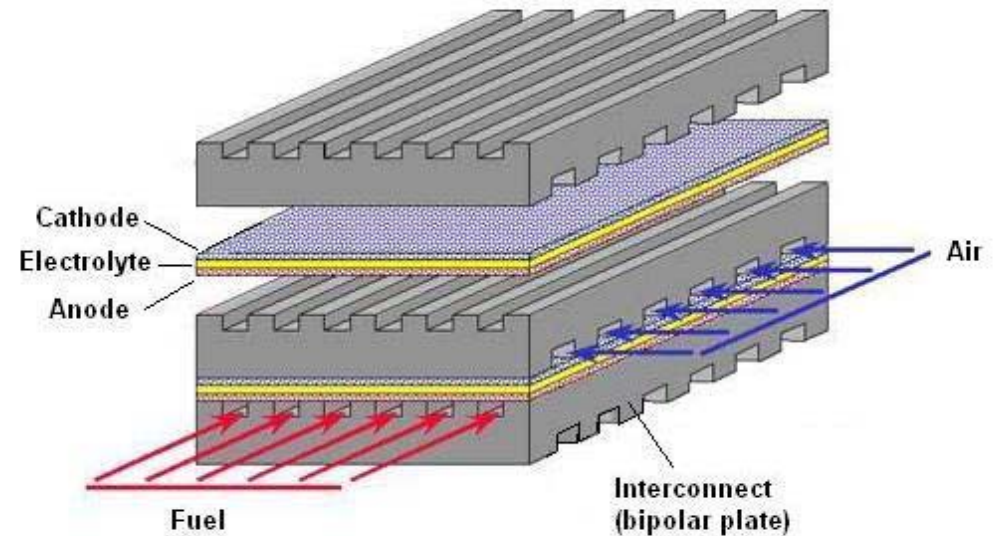
# Results

- **Applied existing Electrode Model and Cell Models to help begin understanding transient issues for SOFC technology.**
- **Journal article (Gemmen (2003))**
- **Conference presentation (Gemmen et al. (2003))**



# 10cm x 10cm Cell Dynamic Model

- **Based on 1-D code**
  - Liese, Gemmen et al. (1999)
- **Fully coupled electrochemistry and flow (V, T, species,  $i''$ )**
- **Cross Flow Geometry**
  - Anode supported
  - 8 x 8 channels
- **Active Area: 10cm x 10cm**
- **Nominal Steady Load Conditions**
  - Cell voltage=0.77 volt
  - Current density=0.74A/cm<sup>2</sup>
  - Power=0.57W/cm<sup>2</sup>
  - Temperature=860°C
  - FU=0.81
  - AU=0.11



- **Cases studied**
  - 0) Load change (incr./decr.)
  - 1) Idle (no load) to Steady State Load
  - 2) Introduce Ripple following Steady State Condition at 1
  - 3) Unload event





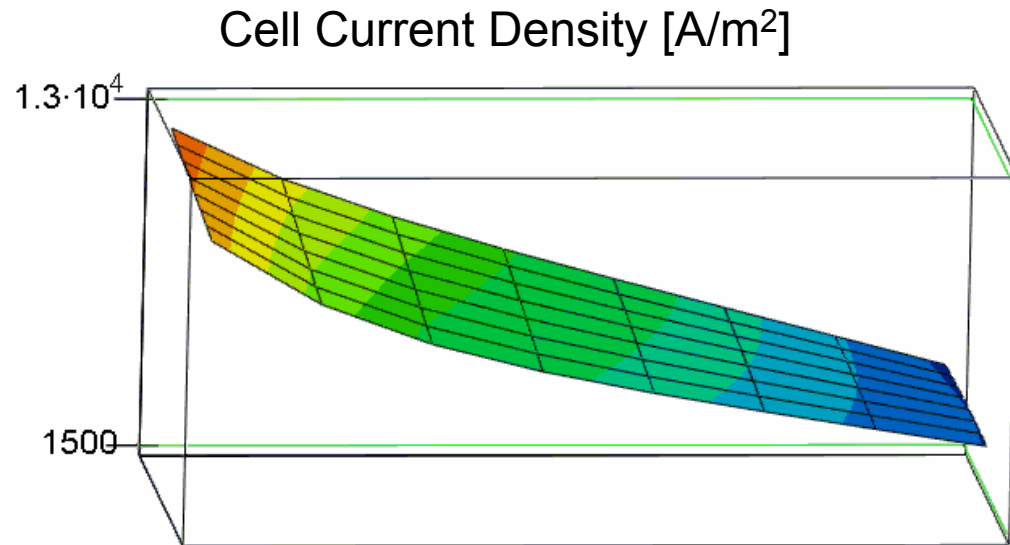
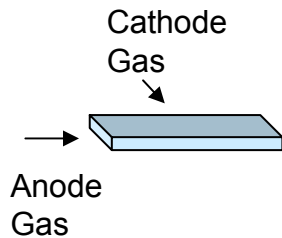
## Case 2: Ripple Case

- **Following Steady State Load...Impose Ripple**
  - Voltage controlled (0.77+/-0.015)



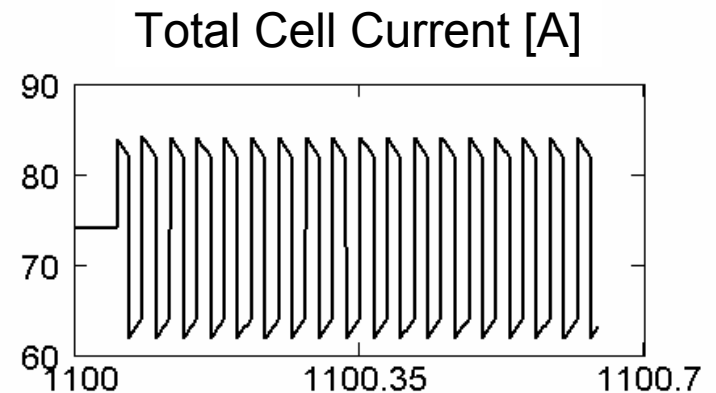
# Case 2: Cell Current Density

(10cm x 10cm; 30Hz Ripple; voltage driven; 8x8 nodes)



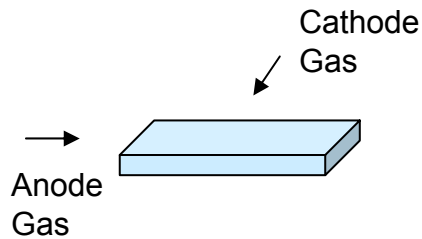
- **Current density response due to ripple is nearly uniform over cell, with minor asymmetric secondary response.**

CurrDenFRAME  
TimeFRAME = 900.1

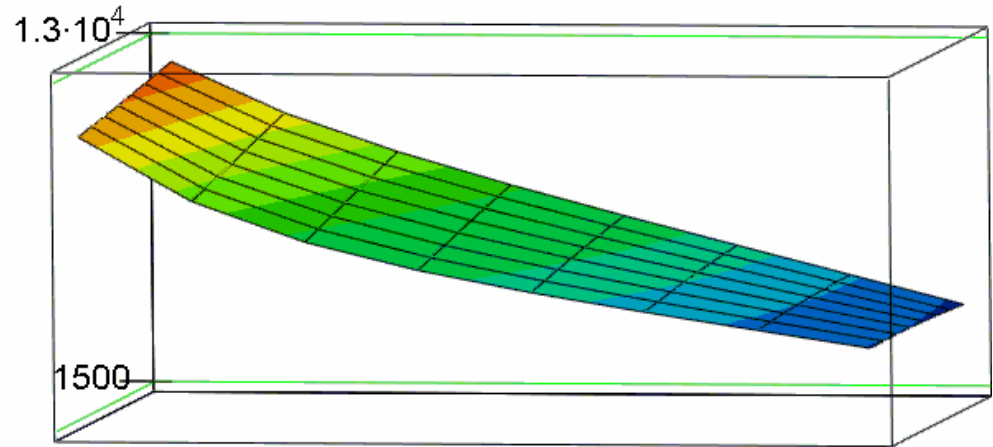


# Case 2: Cell Current Density

(10cm x 10cm; 120Hz Ripple; voltage driven; 8x8 nodes)



Cell Current Density [A/m<sup>2</sup>]

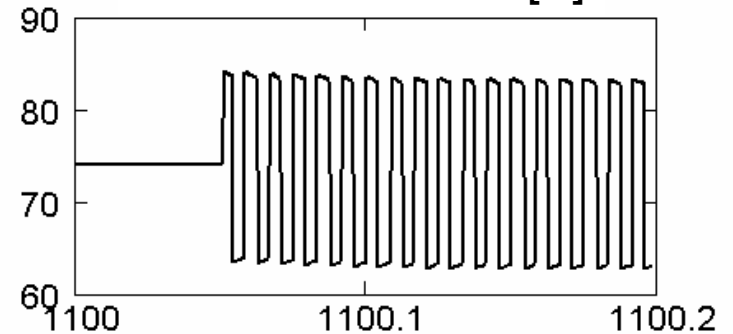


- 120Hz case similar to 30Hz case, with slightly weakened secondary.

urrDenFRAME

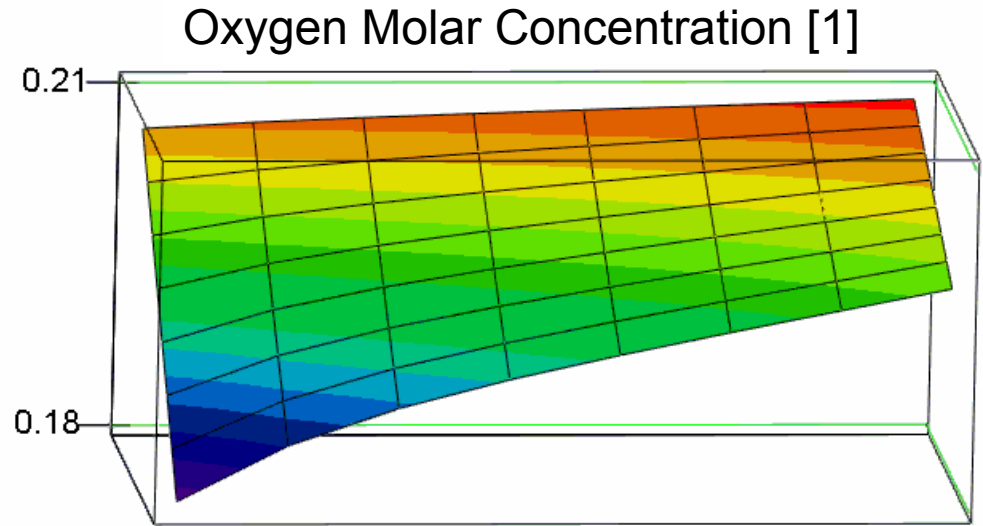
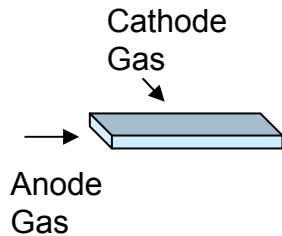
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Total Cell Current [A]



# Case 2: Oxygen Interfacial Concentration

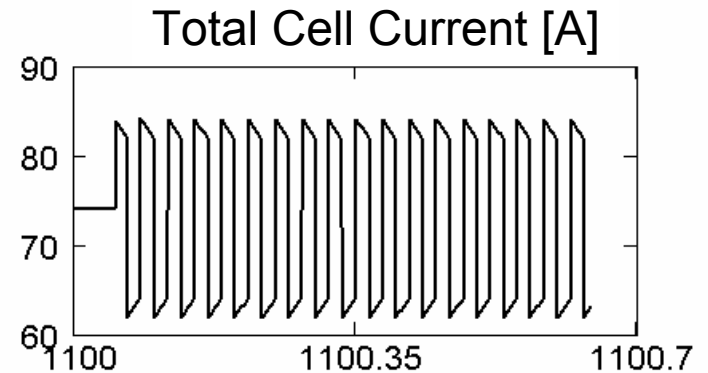
(10cm x 10cm; 30Hz Ripple; voltage driven; 8x8 nodes)



- O<sub>2</sub> response due to 30Hz ripple is like a wave, with largest oscillation at the exit.

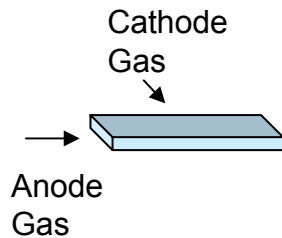
∩2InterfacialConcFRA

TimeFRAME = 900.1

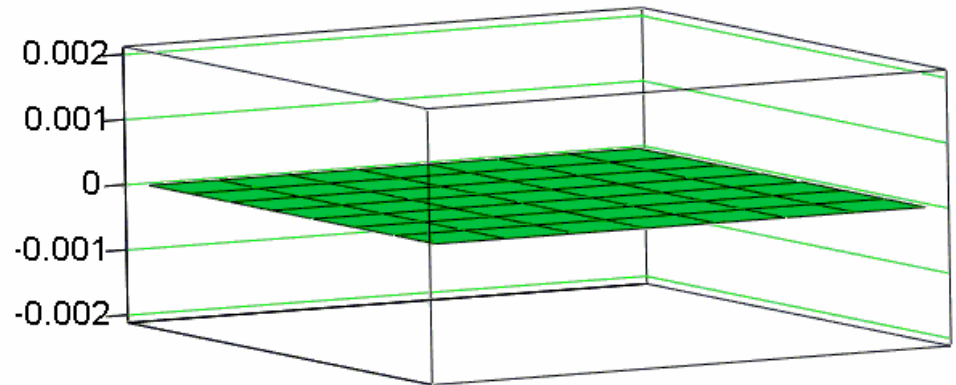


# Case 2: Oxygen Deviation from Steady State

(10cm x 10cm; 30Hz Ripple; voltage driven; 8x8 nodes)



Oxygen Molar Concentration [1]

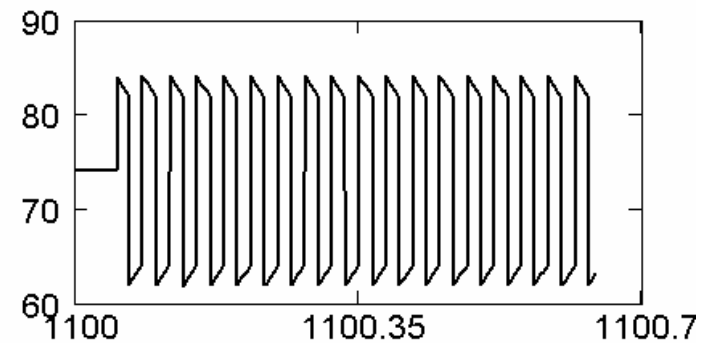


- **Ave. O<sub>2</sub> concentration toward exit nodes appears increased compared to SS condition. Needs to be investigated further.**

DeltaO2FRAME

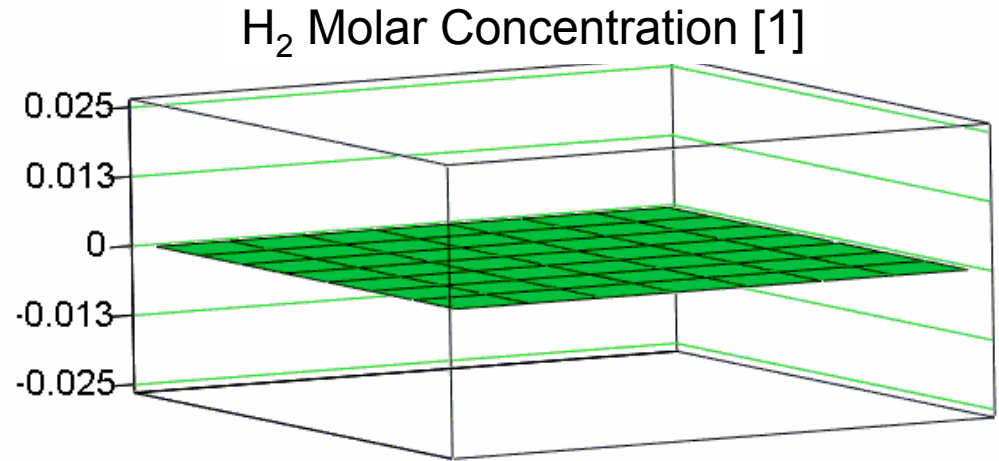
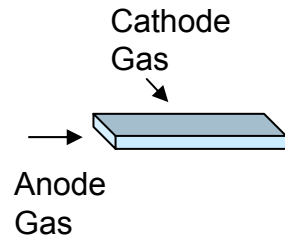
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Total Cell Current [A]



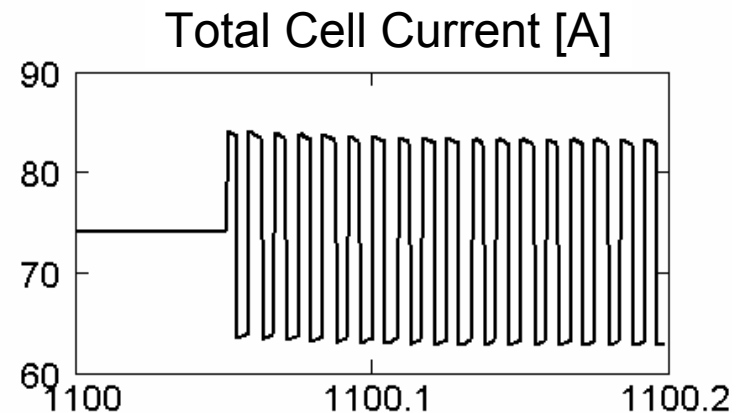
# Case 2: Hydrogen Deviation from Steady State

(10cm x 10cm; 30Hz Ripple; voltage driven; 8x8 nodes)



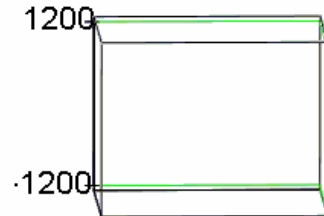
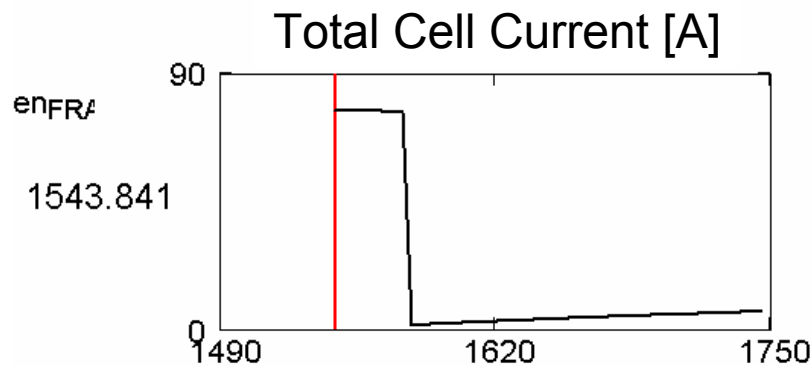
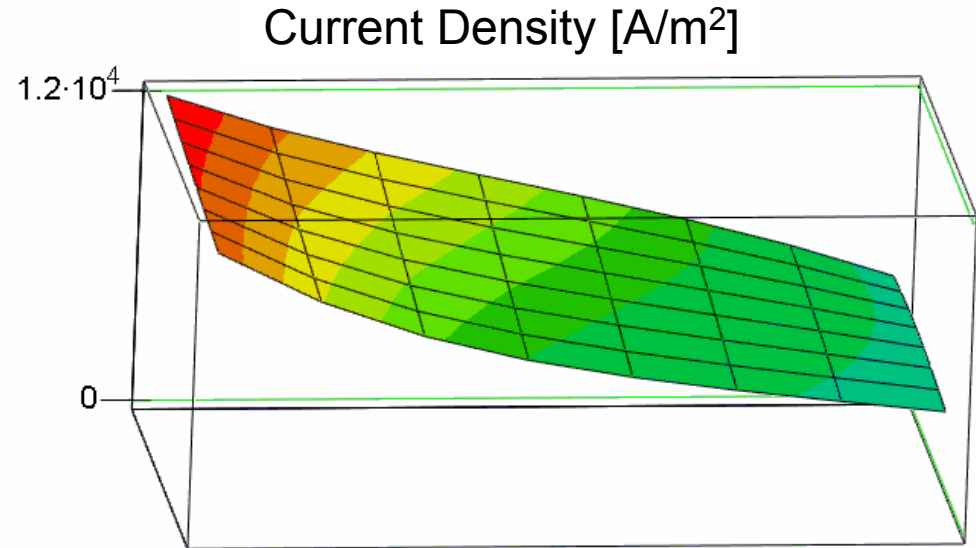
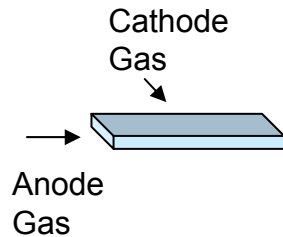
- **Ave. H<sub>2</sub> concentration toward air inlet side appears increased compared to SS condition. H<sub>2</sub> concentration toward air exit side appears decreased compared to SS condition.**

DeltaH2<sub>FRAME</sub>  
T<sub>FRAME</sub> = 1080.100



# Case 3: Unload

(10cm x 10cm; 8x8 nodes)



- Upon unload, current density over portions of the surface reverse (electrolysis) as cell attempts to reach new thermal and specie equilibrium.

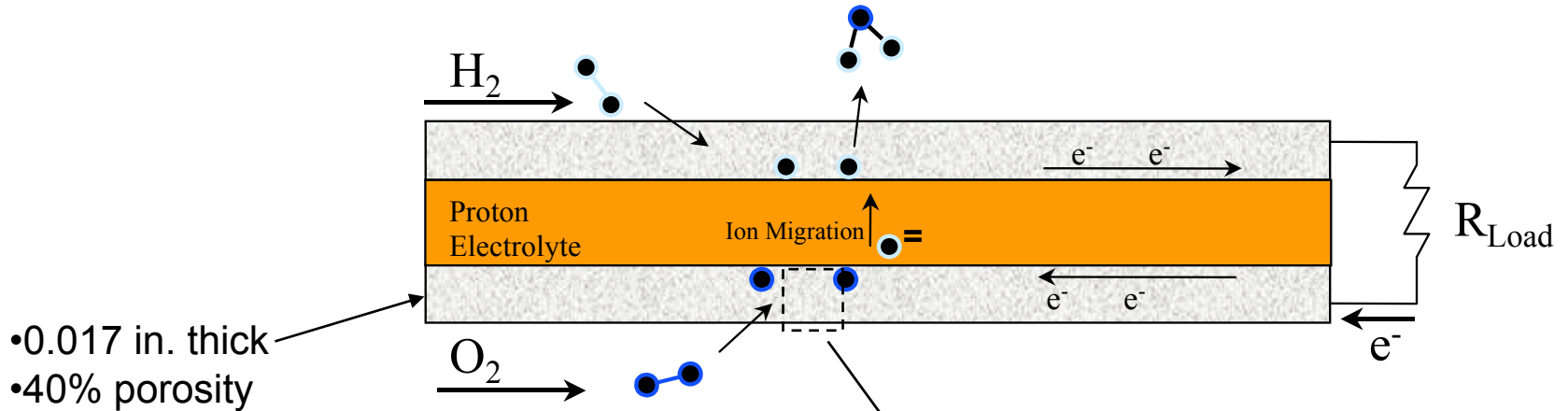
# Conclusions (Full Cell Transient Studies)

- For frequencies above 120Hz, response of fuel cell is mostly uniform over cell surface.
- For frequencies below 120Hz, oxygen response begins to become 'wave-like', while hydrogen response is mostly uniform over cell surface.
- Current density response is mostly uniform for all cases studied (little frequency dependency).
- Ripple induces a slightly modified time-average response to hydrogen (more H<sub>2</sub> conc. at air inlet side, less at exit side).
- Certain dynamic conditions (unloading) can cause current reversal over portions of the cell.





# 1-Dim. Electrode Model Results



•0.017 in. thick  
•40% porosity

$$\frac{dP_j}{dt} = \frac{RT_s}{V_s} \left( n_i Y_{j\_i} - n_o Y_{j\_o} - \frac{I(t)N}{Z_j F} \right)$$

$$\varepsilon \frac{dY_j}{dt} + u \nabla Y_j = D' \nabla^2 Y_j$$

$$D' = D \frac{\varepsilon}{\tau} \quad u = N / \rho \varepsilon^{2/3}$$

$D$ =Knudsen+Molecular Diffusion  
 $N$ =Molar Flux  
 $\rho$ =Molar density

# Ripple Model

- **Assume steady DC current component and a square wave ripple component imposed at the electrode/membrane interface:**

$$I(t) = A \cdot S [1 + x \cdot \text{sq}(\omega \cdot t)]$$

where,

A = current amplitude factor [amp/m<sup>2</sup>]

S = active area [m<sup>2</sup>]

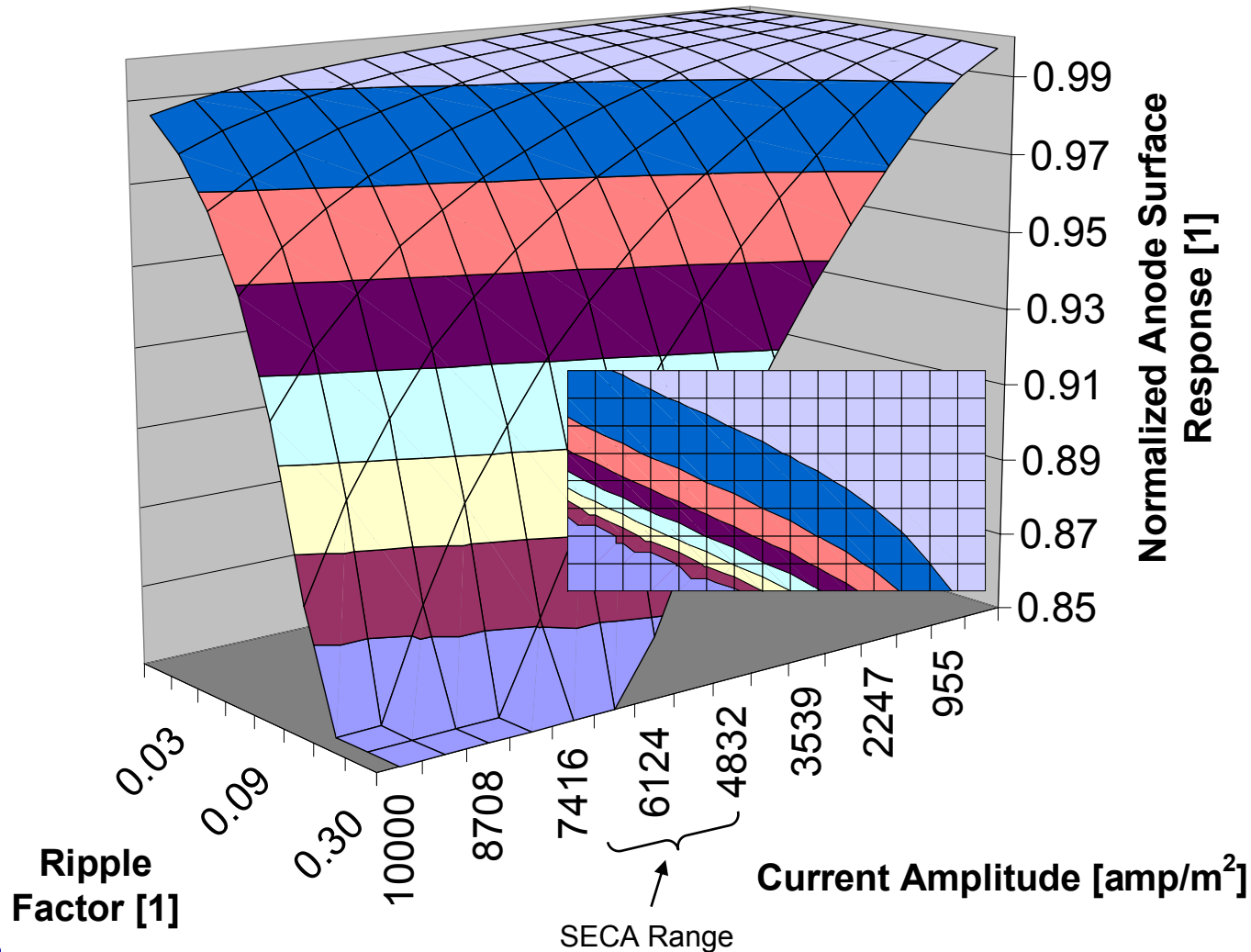
x = ripple factor [1]

sq( $\omega \cdot t$ ) = square wave of unity amplitude and frequency  $\omega$ .



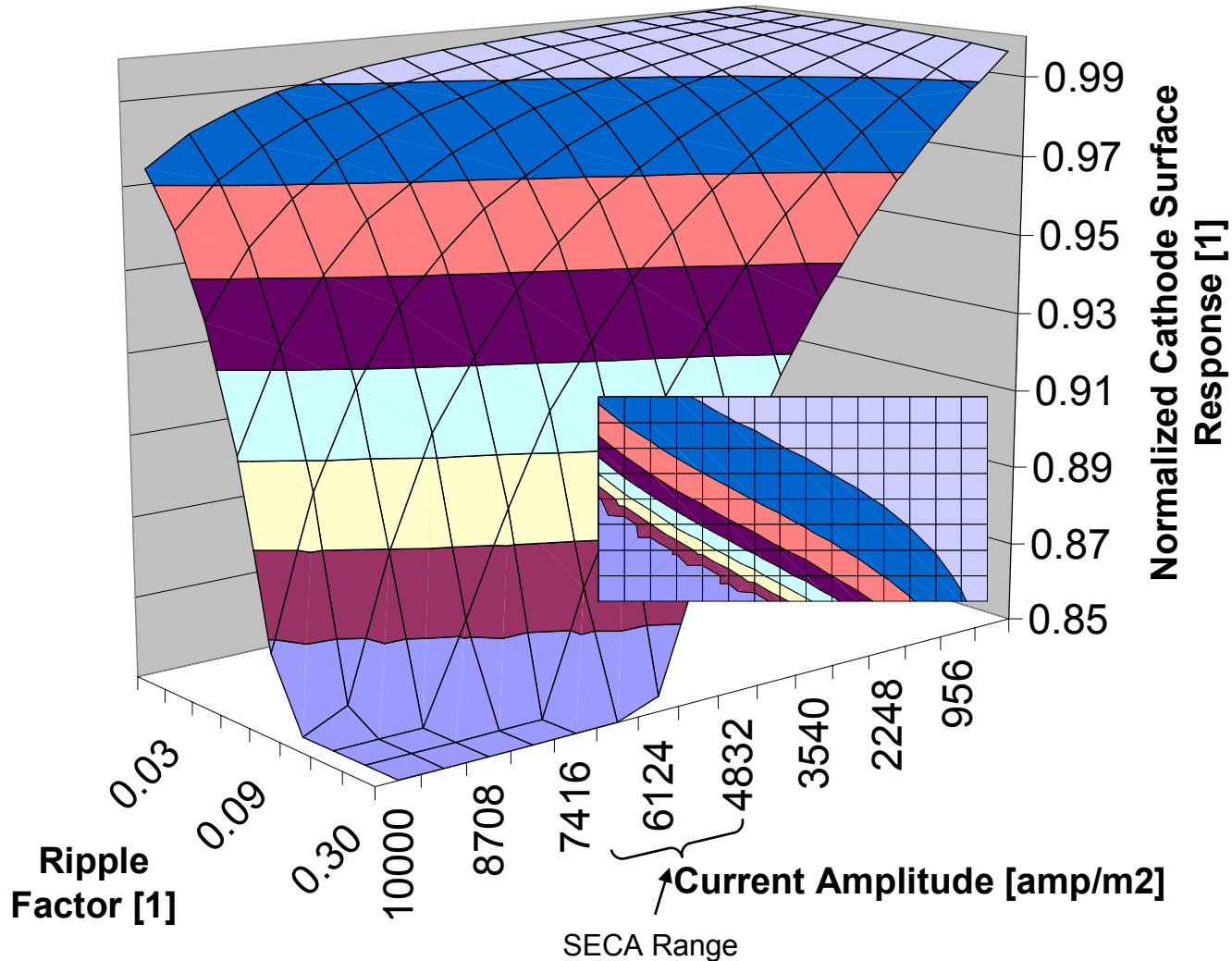
# Impact of Inverter Dynamic Load

Anode Electrode Model H2 Response (120 Hz fixed 0.8 utilization)

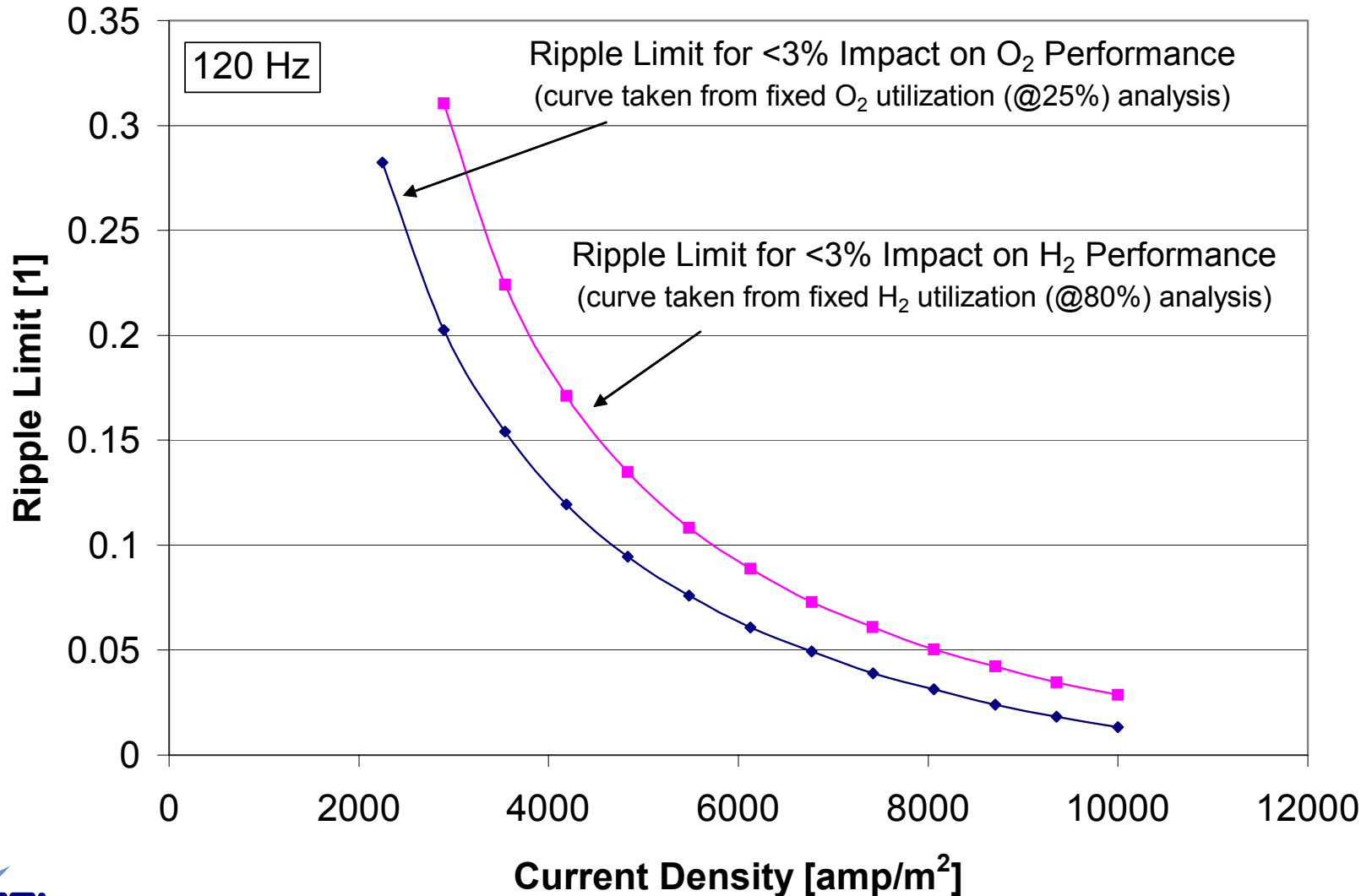


# Impact of Inverter Dynamic Load

## Cathode Electrode Model O<sub>2</sub> Response (120 Hz fixed 0.25 utilization)



# Ripple Limits – Anode & Cathode



# Conclusion (Electrode Study)

- Unmitigated, inverter loads can significantly modify the conditions within and around the fuel cell electrodes as compared to *equivalent* steady loads.
- Both anode and cathode supported electrodes should be carefully examined...cathode supported electrodes are impacted more severely, however.
- To ensure minor impact to the fuel cell conditions, inverter ripple factors should be controlled to less than 6%-9%.
- Ripple frequencies above 400 Hz have minor effects.



## Results (cont.)

- **Built & configured hardware needed to experimentally assess ripple and other dynamic issues for SOFC's.**
- **1<sup>st</sup> experimental ripple study now underway.**



# Applicability to SOFC Commercialization

- **Providing basic understanding (engineering knowledge base) for how dynamic loads deviate from steady loads.**
- **Gained following understanding:**
  - Inverter loads can significantly modify the conditions within and around the fuel cell electrodes as compared to *equivalent* steady loads.
  - To ensure minor impact to the fuel cell conditions, inverter ripple factors should be controlled to less than 6%-9%.
  - Ripple frequencies above 400 Hz have minor effects.
  - For frequencies above 120Hz, response of fuel cell is mostly uniform over cell surface.
  - For frequencies below 120Hz, oxygen response begins to become 'wave-like', while hydrogen response remains mostly uniform over cell surface.
  - Current density response is mostly uniform for all cases studied (little frequency dependency).
  - Ripple induces a slightly modified time-average response to hydrogen (more H<sub>2</sub> conc. at air inlet side, less at exit side).





# FY04 Project Tasks

- **Task 1 – Obtain experimental data on cell degradation**
  - Obtain baseline steady load degradation rate using standard cells
  - Impose ripple (20-30% at simulated high utilization) to determine change in degradation rate
  - Acquire resistance data—impedance spectroscopy; potentiometric/galvanic interrupt studies
  - Run duplicate cases: 2+ at steady load and 2+ unsteady load
- **Task 2 – Evaluate material properties**
  - Evaluate material properties of both unsteady and steady cells to identify different or accelerated degradation behavior
    - SEM, XPS, EDS, XRD
- **Task 3 – Model experimental conditions**
  - Apply models to experimental cases
  - Provide detailed understanding of performance at the cell level
- **Task 4 – Journal publications and presentations**

