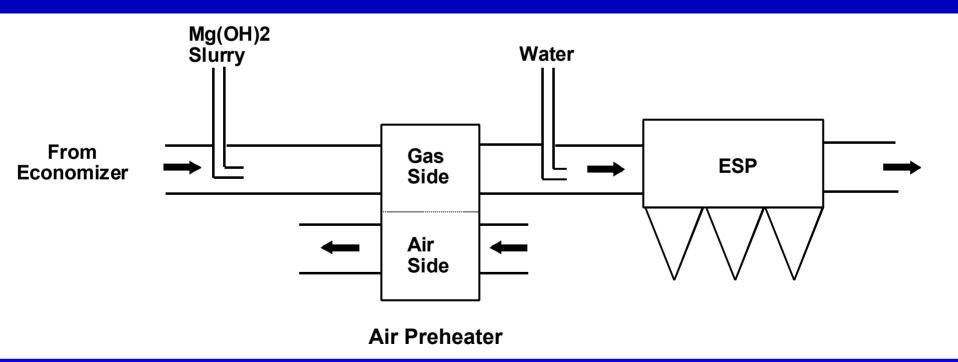
R. A. Winschel, M. L. Fenger

Research & Development 4000 Brownsville Road South Park, PA 15129

Concept

- Absorb Hg on particulate by cooling flue gas to 220-240 °F with air preheater or water spray
- Collect particulate with ESP to remove Hg
- Protect against acid corrosion by introducing Mg(OH)₂ into flue gas upstream of preheater

Concept



Prior Development Work CONSOL pilot-scale combustor ▶ 90% Hg removal from Illinois coal, depending on gas temperature and ash carbon content CONSOL bench-scale work ► FGD by-product Mg(OH)₂ slurry is an active sorbent for SO₃ at economizer outlet temperatures

POTENTIAL BENEFITS OF TECHNOLOGY

- 80-90% Hg removal expected
- Projected cost order of magnitude lower (\$/lb Hg) than carbon injection
- Suitable for retrofit or new plants
- Potential applicability to full range of coal types
- Effective SO₃ reduction
 - Visible plume mitigation, TRI reduction
 - SCR/SNCR benefits
 - Secondary fine particulate reduction
 - Potential to improve heat rate by 2%
 - 2% reduction in NO_x, SO₂, CO, particulate and CO₂
 - ~ \$600,000/y fuel cost savings for 600 MW plant

HOST PLANT SITE

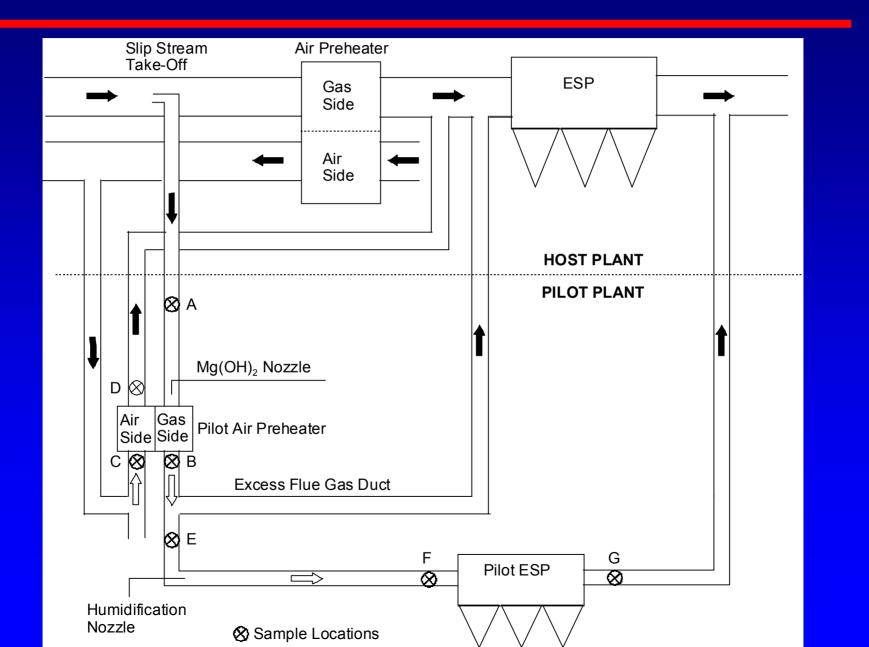
Allegheny Energy Mitchell Station

- Courtney, PA
- 288 MW Unit 3
- In service 1963
- Thiosorbic Lime wet FGD, ESP, no SCR
- Fired with eastern bituminous coal
 - ► 3.5% S and 0.1% CI typical

ALLEGHENY MITCHELL STATION



PILOT PLANT PROCESS SCHEMATIC

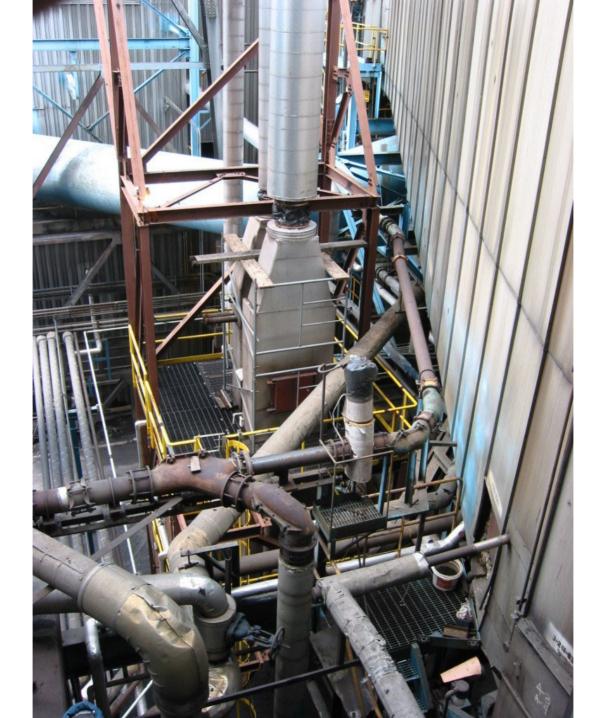












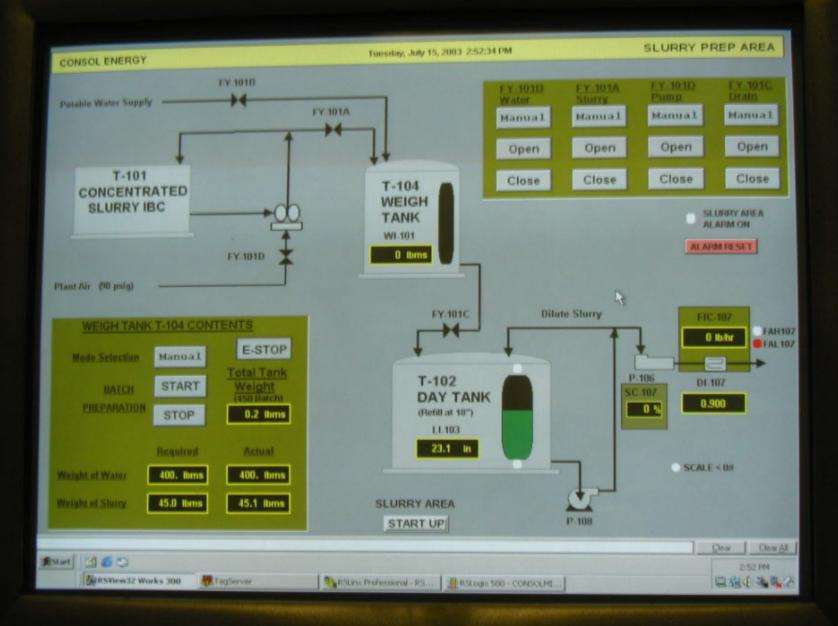




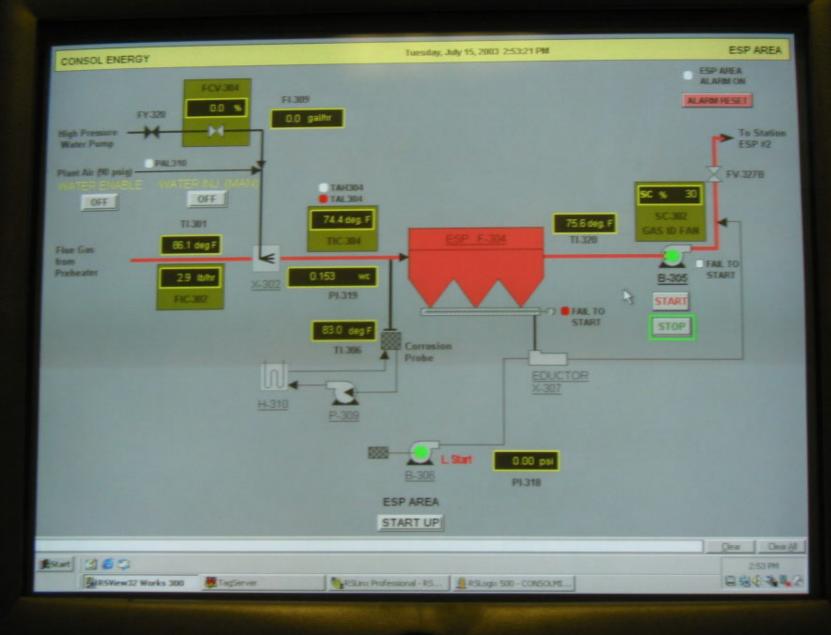








Dest







EXPERIMENTAL PLAN

- Flue gas flowrate: 16,500 lb/h (1.7 MW)
- Mg/SO₃ molar ratio: 2/1 5/1
- Gas temperature at ESP inlet: 225 315 °F
- Water spray cooling: on/off
- Gas sampling for Hg, particulate, SO₂, SO₃
- Speciate Hg at inlet/outlet of air preheater and ESP
- Evaluate air preheater and ESP performance and corrosion
- Evaluate stability of captured Hg

PILOT PLANT PROGRAM GOALS

- Demonstrate 80-90% Hg removal
- Evaluate Hg removal by species
- Determine optimum operating conditions for costeffective Hg control
- Determine sorbent rate for cost-effective SO₃ control
- Determine impact of reduced cold-end temperature and SO₃ control on air heater and ESP performance and corrosion
- Demonstrate long-term operability
- Determine stability (leachability, volatility) of captured Hg
- Disseminate information

STATUS OF PROJECT AS OF JULY 31, 2003

- Design and construction completed
- Pilot plant start-up 8/03
- Project completion 3/05

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