

NOVEL TECHNIQUES FOR MERCURY CONTROL

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**U.S. Department of Energy
National Energy Technology Laboratory**

**Mercury Control Technology
R&D Program Review Meeting
August 12-13, 2003**



LAB-SCALE RESEARCH OBJECTIVES

- **Develop cost-effective novel sorbents.**
- **Elucidate mercury-sorbent interactions.**
- **Explore innovative techniques for mercury removal, for example, photochemical oxidation.**
- **Develop high temperature mercury sorbents for gasification applications.**



A Technique to Control Mercury From Flue Gas: The Thief Process

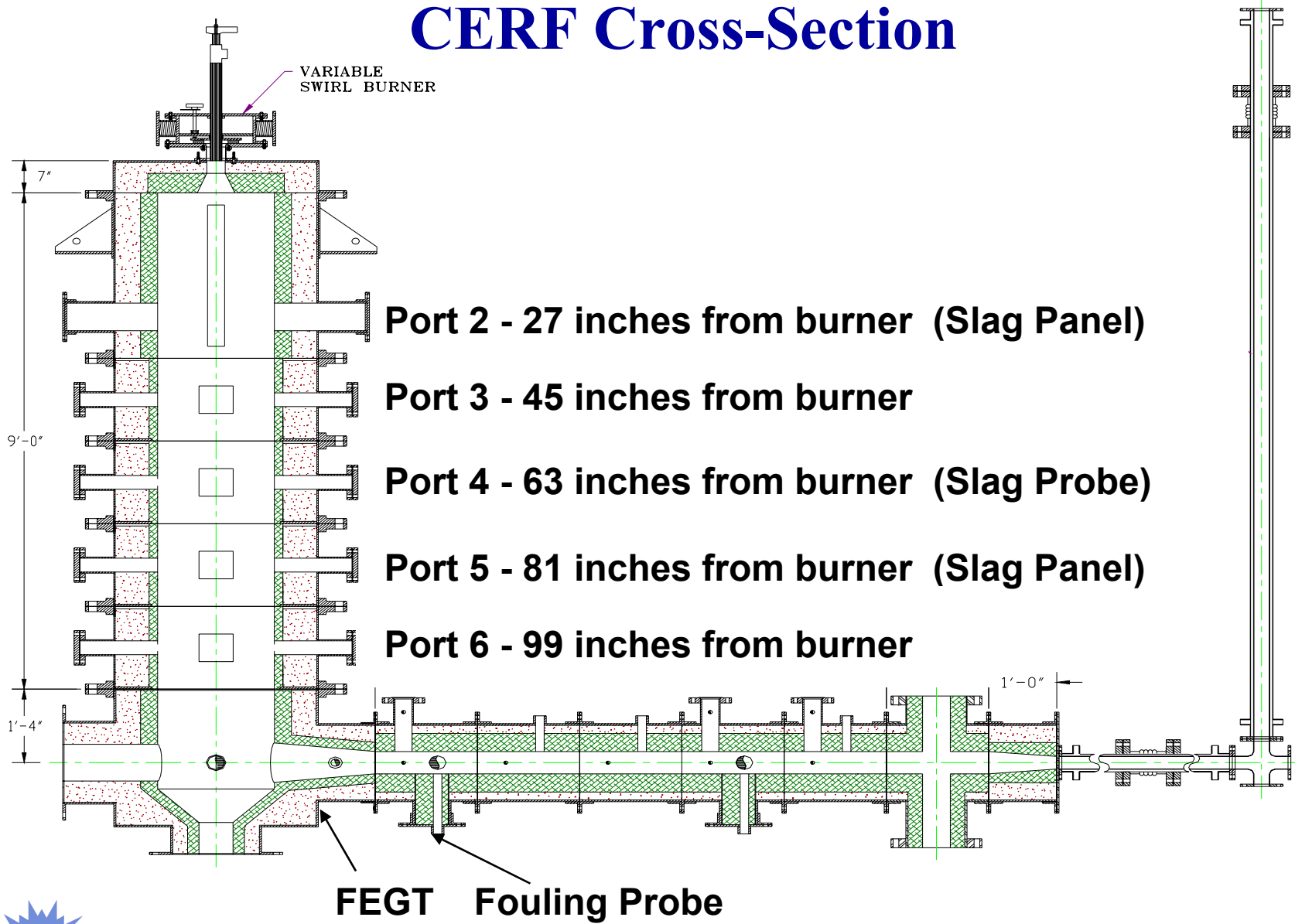
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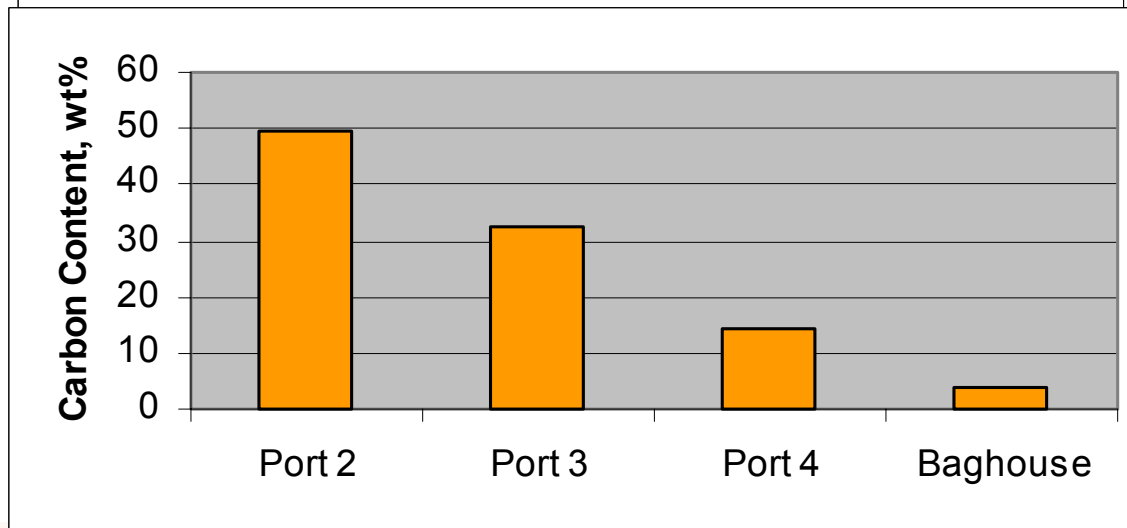
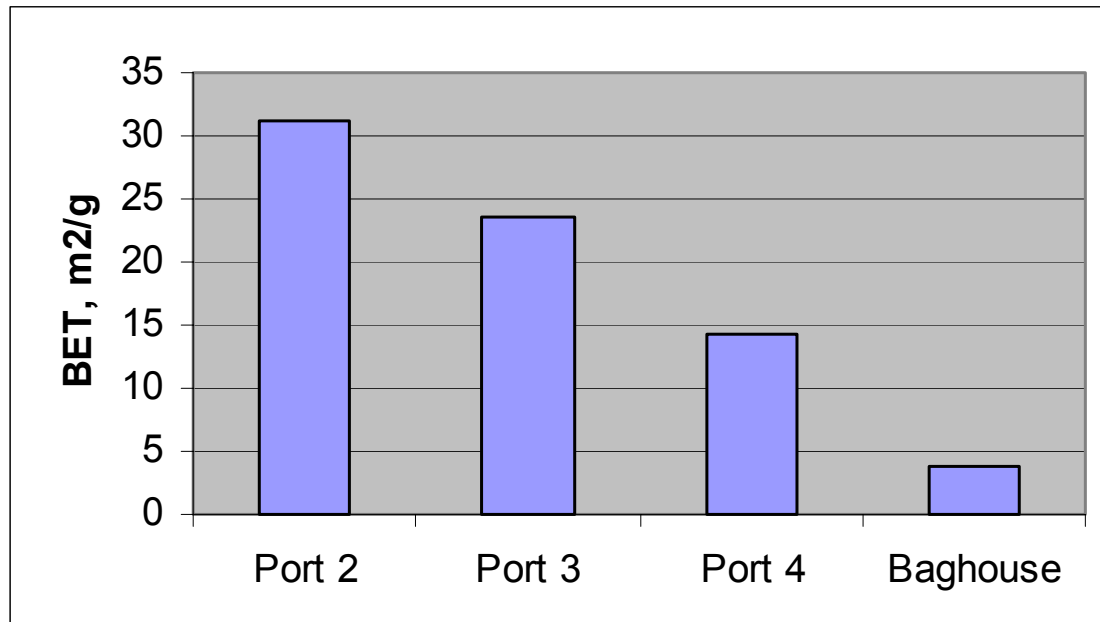
CERF Cross-Section



Sorbent Characterization

- **Physical**
 - Surface area (BET) and pore volume
 - Bulk chemical analysis
 - Particle size
 - Raman microanalysis
- **Chemical**
 - Mercury capacity

Evergreen Bituminous Coal

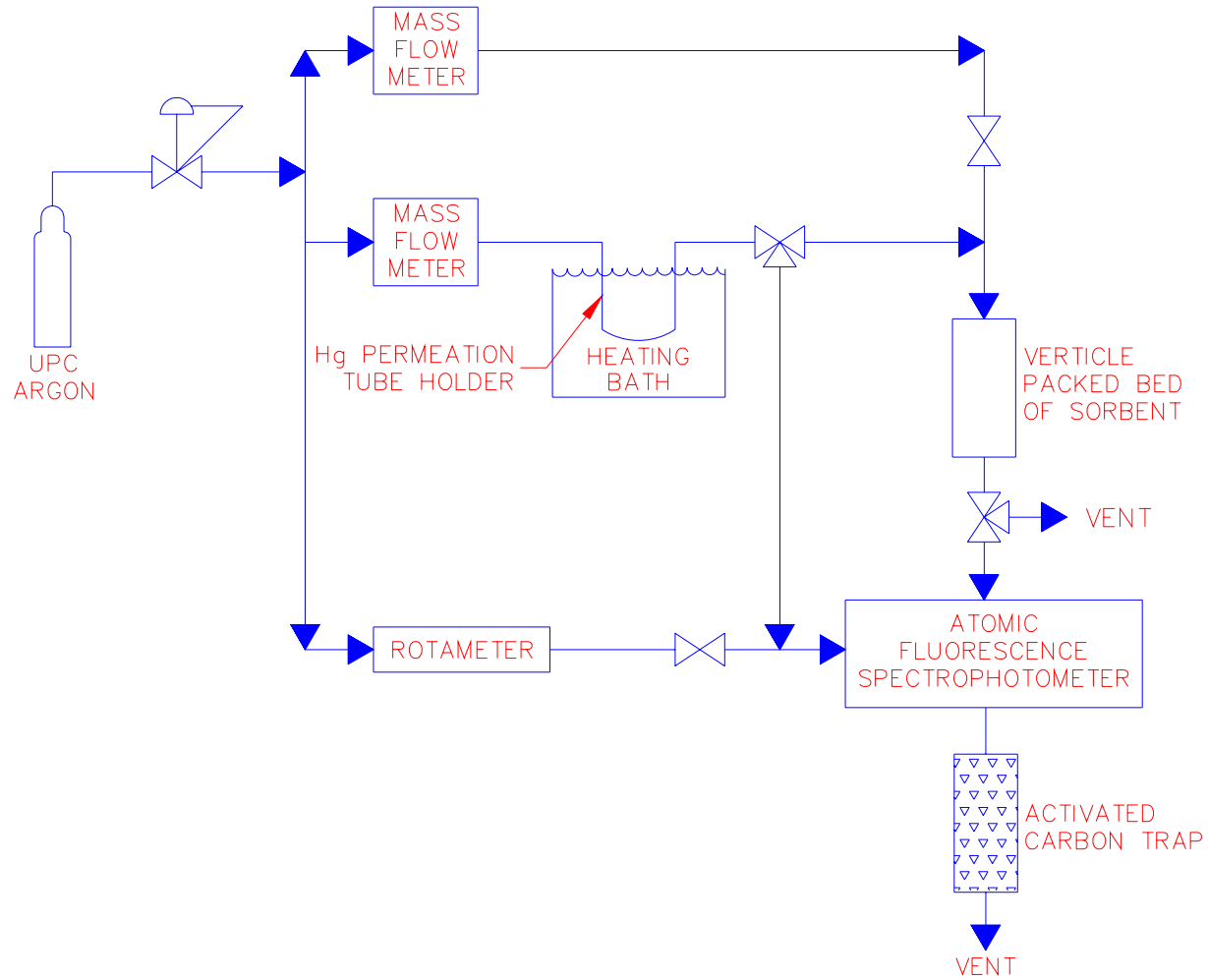


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LAB-SCALE SORBENT SCREENING UNIT

Figure 1. Schematic of Sorbent Screening Unit



Parametric Scan In Packed-Bed Reactor

Sorbents/Promoters: Carbons/Sulfur

Temperatures: 140, 280, 350°F

Gases: Simulated Flue Gases

Elemental Mercury Concentration: 270 ppb

Mass of Sorbent: 10 mg

Time: 350 minutes

Mercury Measurement: CVAAS

Coals: Evergreen and Pittsburgh #8



Results: Commercial Carbons

<u>Sorbent</u>	<u>Capacity (mg/g)</u>	<u>Temp (°F)</u>
FluePac AC	0.89	280
Darco AC	1.60	280
Insul AC	1.96	280
Insul AC	0.19	400
S-AC-1	1.55	280
S-AC-2	1.39	280

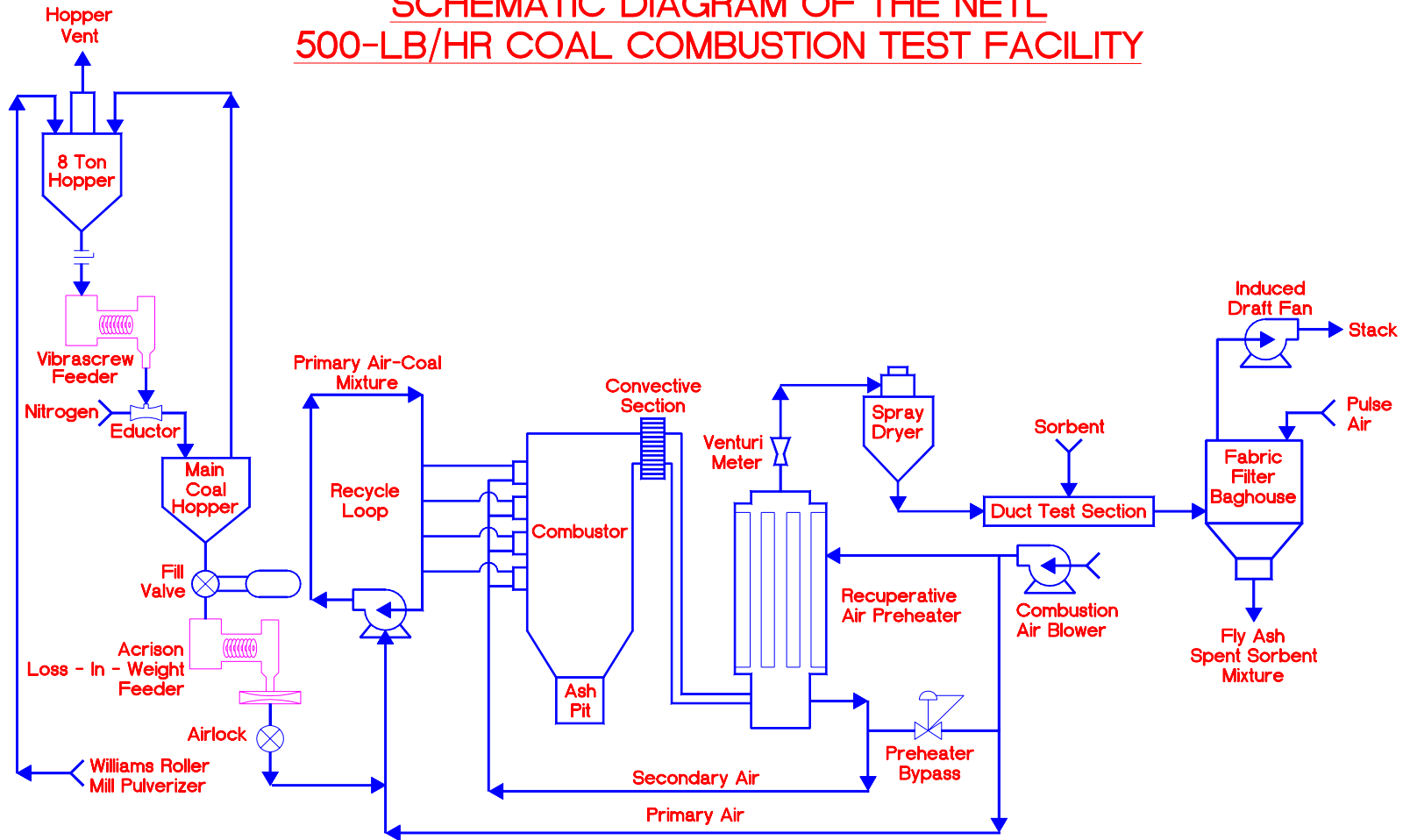
- Unpromoted carbons display good capacity
- Adsorption favored by low temperature
- Sulfur promotion does not increase capacity

Results: Thief Sorbents

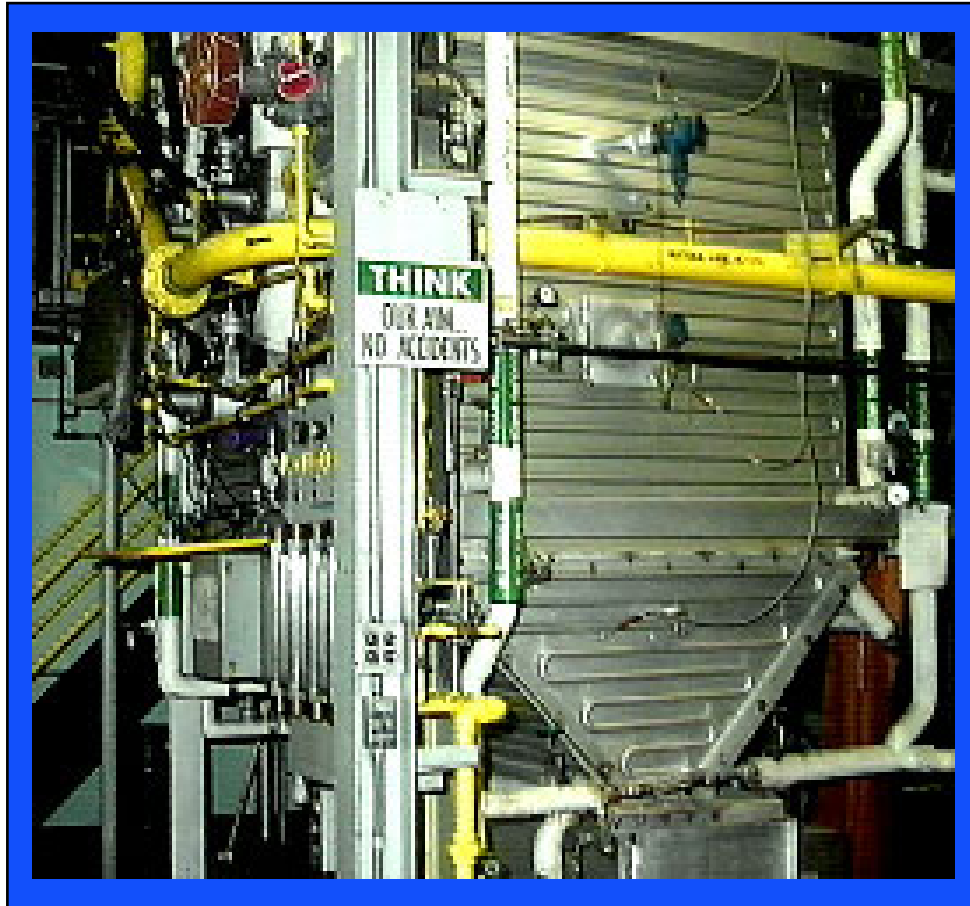
<u>Sorbent</u>	<u>Capacity (mg/g)</u>	<u>Temp (°F)</u>
Evergreen-Port 2	2.03	280
Pittsburgh #8-Port 2	1.38	280

- Partially combusted coal, produced in-situ and removed from furnace by lance (“thief”)
- Similar capacity to activated carbon
- Cheaper than activated carbons

SCHEMATIC DIAGRAM OF THE NETL 500-LB/HR COAL COMBUSTION TEST FACILITY



500 LB/HR PILOT COMBUSTOR AND PULSE JET FABRIC FILTER











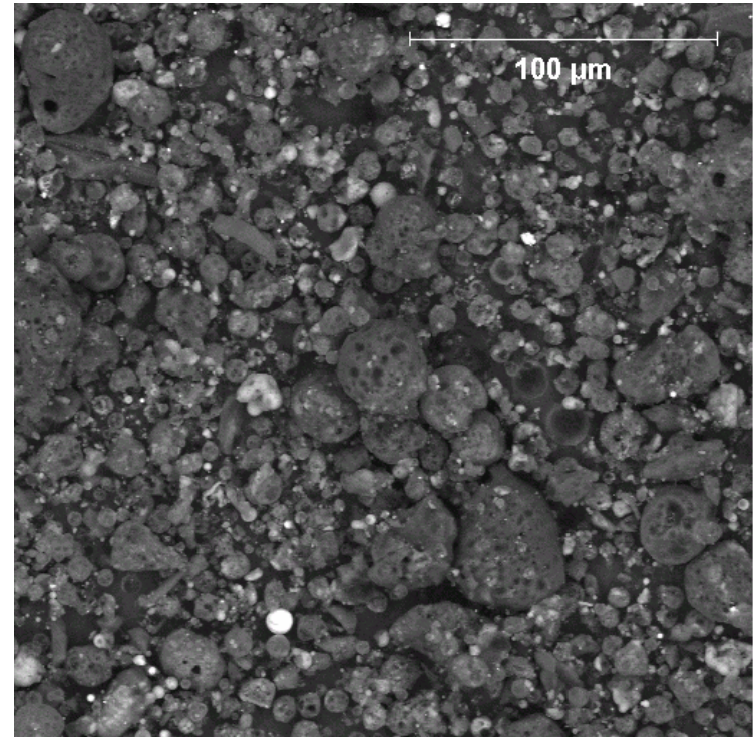
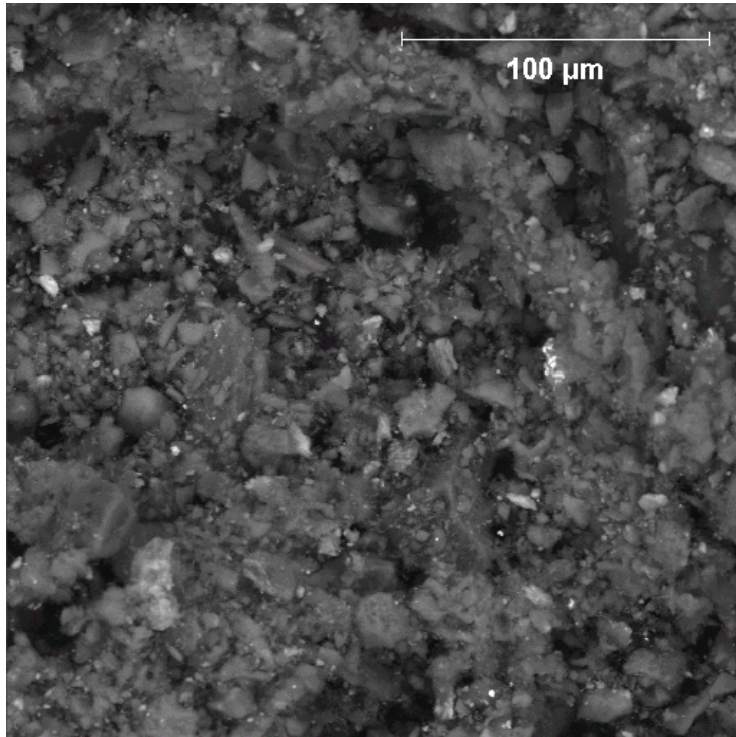




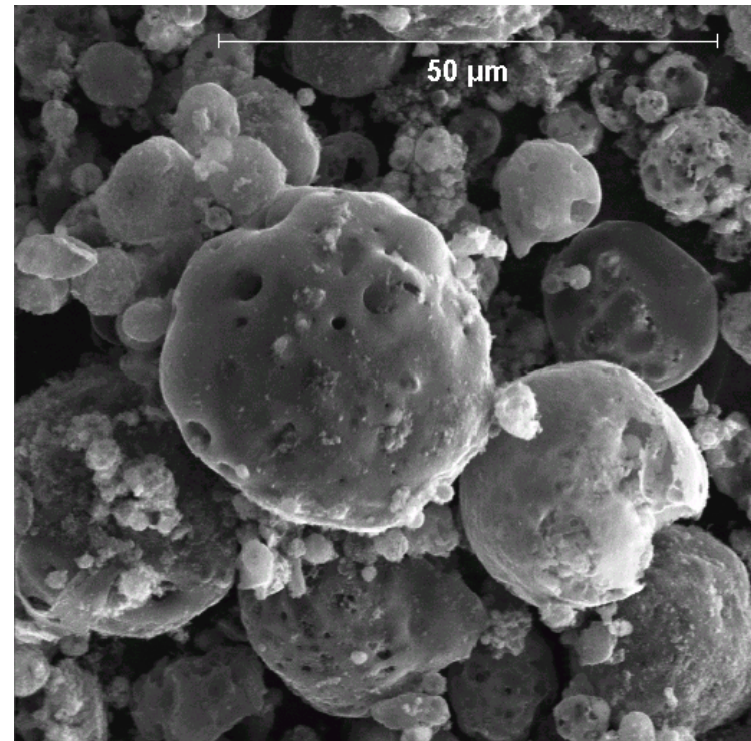
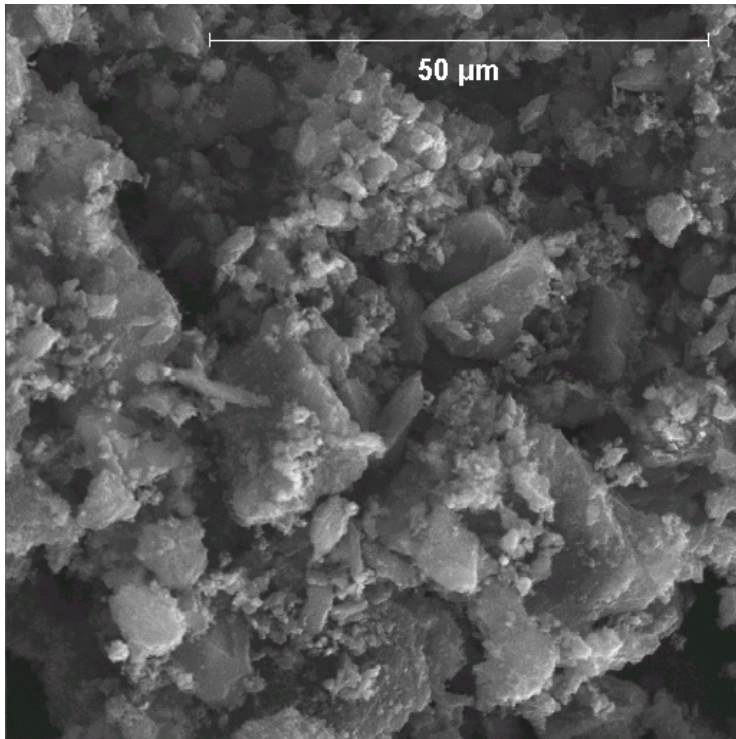
Comparison of Sorbent (Evergreen)

<i>Parameter</i>	<i>CERF Sample</i>	<i>500-lb/hr Sample</i>	<i>Activated Carbon</i>
BET, m²/g	31.2	69.1	481
Carbon Content, wt%	49.8	63.2	66.5
Hg Capacity, mg/g	2.03	1.80	1.61

Norit Darco versus Thief Sample (100micron)



Norit Darco versus Thief Sample (50 micron)

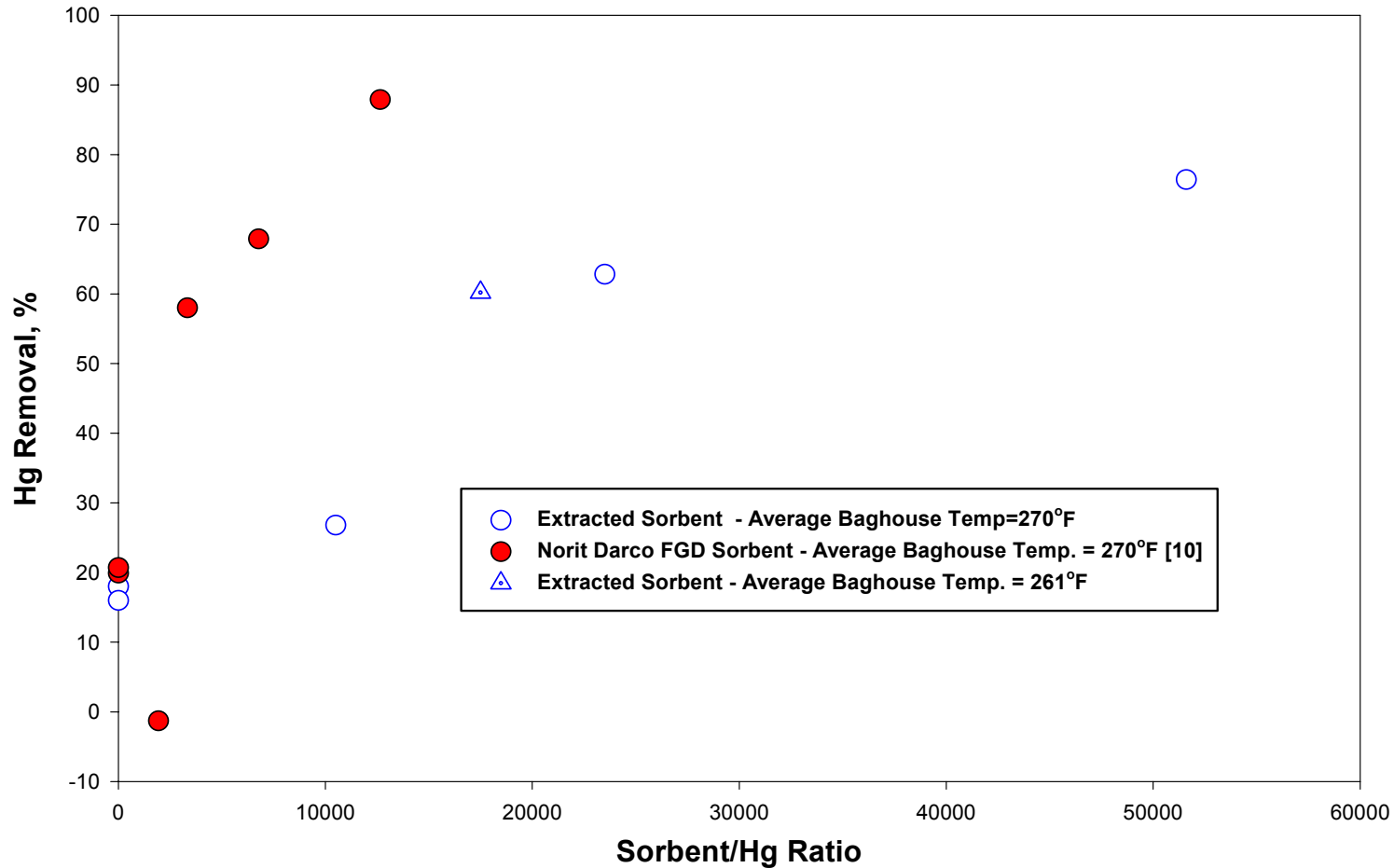


Typical 500-lb/hr Combustor Operating Conditions With Evergreen Coal

- **Coal flow: 360-lb/hr**
- **Duct gas composition:**
 - 7.2% O₂
 - 12.1% CO₂
 - 4.9% H₂O
 - 528ppm SO₂
 - 400ppm NO_x
 - Hg-oxidized 161-μg/min
 - Hg-elemental 23-μg/min
- **Inlet duct temperature: 300°F**
- **Outlet duct temperature: 280°F**
- **Average baghouse temperature: 270°F**
- **Ash loading: 23.8-lb/hr**



Comparison of the Effectiveness of Darco FGD and Thief Sorbent (Evergreen)



Preliminary Data for PRB Coal

Sample	Carbon Content, wt %	Sorbent Injection, lb/mmacf	System Mercury Removal, %
Thief	87-91	14.1	57
Thief	75-84	11.5	82
Thief	50-65	2.3	92
Darco	66.5	2.1	91



CONCLUSIONS

- **An alternate technique to activated carbon injection for Hg removal has been proposed.**
- **Process involves extracting partially combusted coal from the combustor and re-injecting downstream of the air preheater.**
- **As compared to activated carbon, partially combusted coal extracted near burner has:**
 - similar carbon content
 - lower surface area
 - similar elemental mercury capacity

CONCLUSIONS (cont'd)

- **Test results indicate that the technique is promising on the pilot scale.**
- **Optimization in actual combustor requires best extraction location (modeling with coal particle mapping for validation) and good probe design.**
- **Economics appears favorable for near term goal.**
- **Technique patented.**



Mercury Control Technology R&D Program Review Meeting

The GP-254 Process For Photochemical Removal of Mercury From Flue Gas

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Background: GP-254 Process

Discovery

- Sorbent Development
- UV Measurement of Mercury
- AFS
- Unwanted Red-Brown Stains
- Mercuric Oxide
- Serendipity



Photochemical Oxidation of Mercury

- Mercury can absorb and emit 253.7 nm light

- Atomic Absorption (AAS)



- Atomic Emission (AES)



- Atomic Fluorescence (AFS): steps (I) and (II)

- Analytical Basis for CEMs



What is Quenching?

- Intensity of Fluorescent Emission Diminished
- Energy Transfer Due To Collisions
- Function of Size, Shape, and Reactivity
- **Primed for Chemical Reaction (Activation)**
- **Interferes with Ultraviolet Spectroscopy**



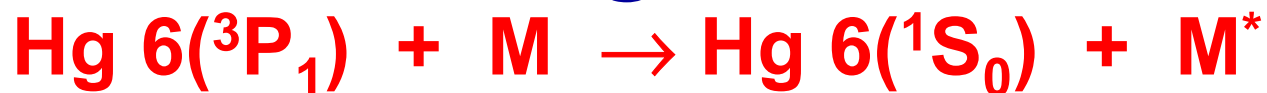
Hg 6 ($^3\text{P}_1$)

Fluorescence

Quenching



Quenching Cross Sections



■ Function of Size, Shape, and Reactivity

<u>Species</u>	<u>Cross Section (cm²)</u>
HCl	37.0×10^{-16}
NO	24.7×10^{-16}
O ₂	13.9×10^{-16}
CO	4.1×10^{-16}
CO ₂	2.5×10^{-16}
H ₂ O	1.0×10^{-16}
N ₂	0.4×10^{-16}

Photochemical Oxidations

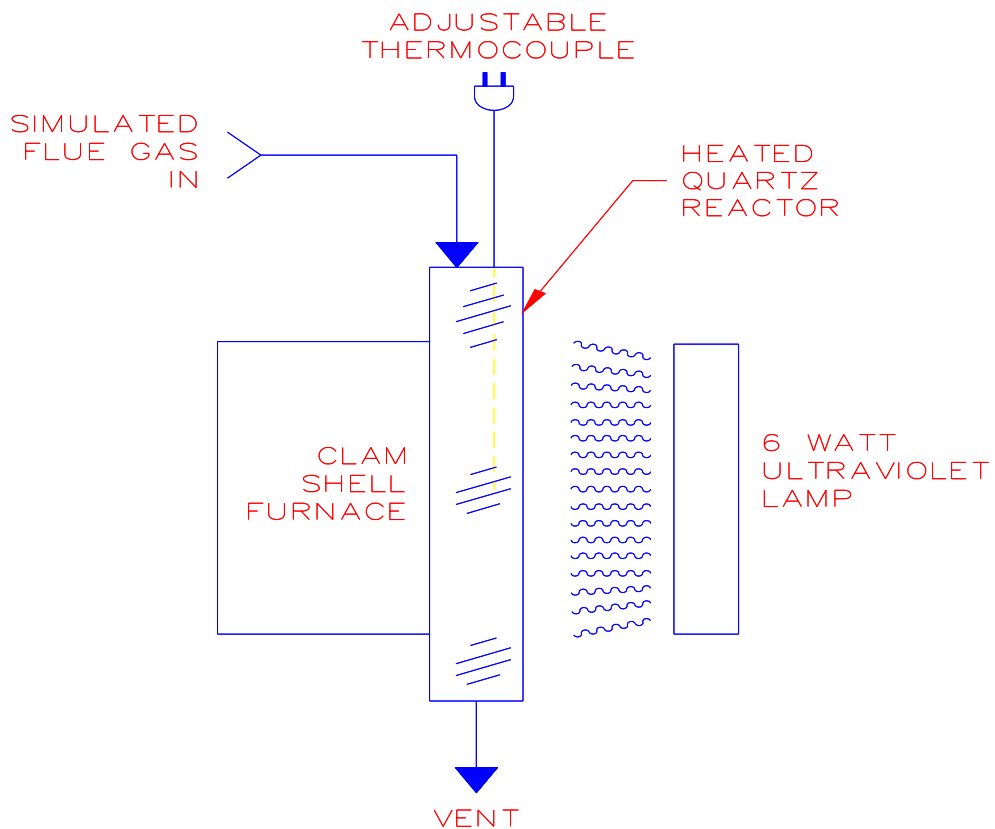
- First described in 1926 by Dickinson and Sherrill (O₂)
- Others discovered by Gunning in 1950s (HCl, H₂O, CO₂)

Relevant Overall Reactions



- Interferes with UV-Based CEMs
- Potential Removal Method

LAB-SCALE PHOTOREACTOR



Photoreactor For Removal of Mercury

Experimental Parameters

- Quartz Photoreactor, 6 Watt UV Lamp
- **Temperatures:** 80°F, 280°F, 350°F
- **Flow-Rate:** 60 ml/min **Reaction Time:** 350 min
- Intensity: 1.4 mW/cm²

Gas Compositions

A: 16% CO₂, 5% O₂, 2000 ppm SO₂,
300 ppb Hg, balance N₂

B: 16% CO₂, 5% O₂, 2000 ppm SO₂,
500 ppm NO, 300 ppb Hg, balance N₂



Results: Photochemical Removal

<u>Gas</u>	<u>T (°F)</u>	<u>Mean Hg Capture (%)</u>
A	350	2.3 ± 2.0
A	280	71.6 ± 30.1
A	80	67.8 ± 28.8
B	280	26.8 ± 11.7

- Removal as Mercuric Oxide/Mercurous Sulfate Stain
- Higher Removals below 300°F
- Limited By Thermal Decomposition of Ozone (300-350°F)
- NO Reduces Removal, Possibly By Consuming Ozone
- Low Energy Consumption
- Potentially Low Operating Costs



Conclusions: Photochemical Oxidation

Method For Mercury Removal

- Obvious Interference For CEMs
- High Levels of Mercury Removal From SFG
- Capture as HgO and Hg_2SO_4
- Enhanced Removal Below 300°F

Conclusions: Photochemical Oxidation

Potential For Better Performance

- Other Oxidants (HCl, H₂O) in Flue Gas
- Promising Process Economics
- Potential For Multi-Pollutant Control
- Pilot-Scale Data Needed
- Low Rank Coals Are of Particular Interest



Plans For FY04

Bench-Scale Photoreactor

- Slipstream of Flue Gas From 500-lb/hr Pilot
- Temperature: 280°F - 350°F
- Effect of Temperature, Radiation Intensity
Residence Time & Composition
- Removals Measured On-Line By CEM
- Impact Upon Other Flue Gas Species
- Determine GP-254 Process Economics

