

## CHAPTER 9

### THE THERMODYNAMIC PROPERTIES OF STEAM

The most widely used tabulation of the properties of steam is that by Keenan and Keyes [1], based on experimental data up to 460°C and 360 atmospheres. Koch [2, 3, 4] has published a table in metric units, ranging from 0° to 550°C and from 0.01 to 300 atmospheres. Goff and Gratch [3] published an accurate table of low-pressure values of properties of water from -160° to 212°F. The recorrelation in 1949 by Keyes [4] of the existing data for steam and the recent experimental data of Kennedy [5] and Kirillin and Rumjanzev [6] prompted a reexamination of the situation. The tables given below are a result of this investigation.

#### Calculation of the Tables

The tables of the compressibility factor and density for steam given here comprise newly calculated values obtained from the thorough correlation by Keyes [4] of all of the then existing data of state. During the course of the calculations, the data of Kennedy [5] were processed with a view of extending the temperature and pressure range of the tables. These data were found too inconsistent at the higher pressures and unreliable at the lower pressures to warrant their use (see figure 9a). In view of this and of the purely empirical nature of the correlation equation used, the tables could not be extended beyond the tabulated range. The data of Kirillin and Rumjanzev are in good agreement with the values of the compressibility factor obtained from the Keyes correlation as is shown in figure 9b.

The data of state have been represented by Keyes [4] by the equations found on page 923 of reference 4. The implicit nature of this equation of state required an iterative procedure which was employed until each of the calculated values became constant to a part in 10,000. The values of the gas imperfection corrections to the heat capacity were calculated from an earlier correlation of Keyes, et al., [7], which is consistent with the PVT representation [4] and which was more amenable to computation. The corrections for enthalpy and entropy were obtained by integration of the above corrections. A fuller discussion of the details of the computation is to be found in the above cited works and in the report of Fano, Hubbell, and Beckett [8].

As a check of the consistency of the independent calculations of compressibility and gas imperfection corrections to the derived properties, the corrections to the free energy function were computed both from the tabulated compressibilities by numerical integration from the equation

$$\frac{F - F^0}{RT} = \int_0^P \frac{Z - 1}{P} dP$$

and from the tabulated entropy and enthalpy. The agreement between the results was very satisfactory, the discrepancies being in the worst case about 2 percent of the correction.

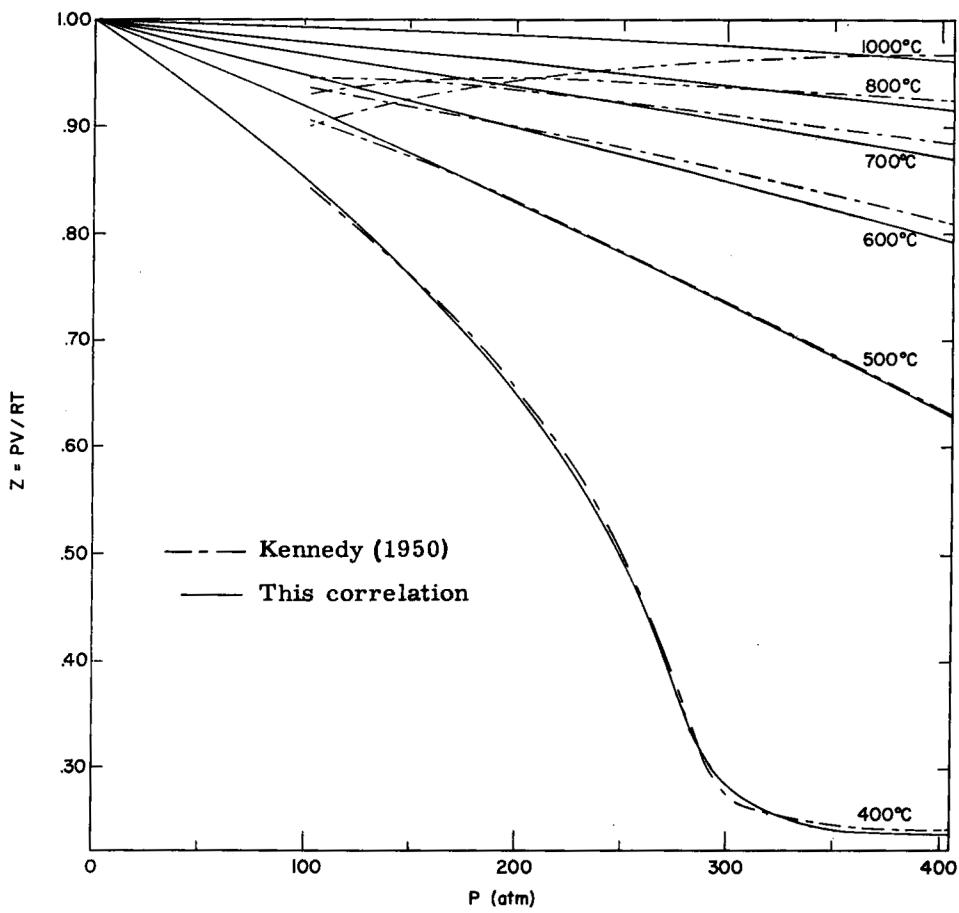


Figure 9a. A comparison of the experimental data of Kennedy [5] with this correlation

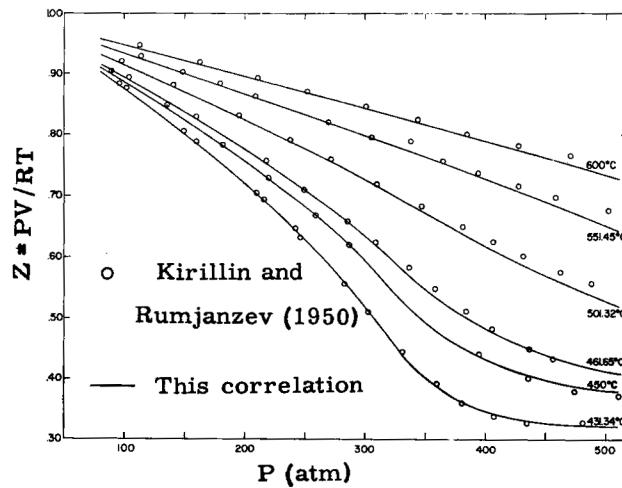


Figure 9b. A comparison of the experimental data of Kirillin and Rumjanzev [6] with this correlation

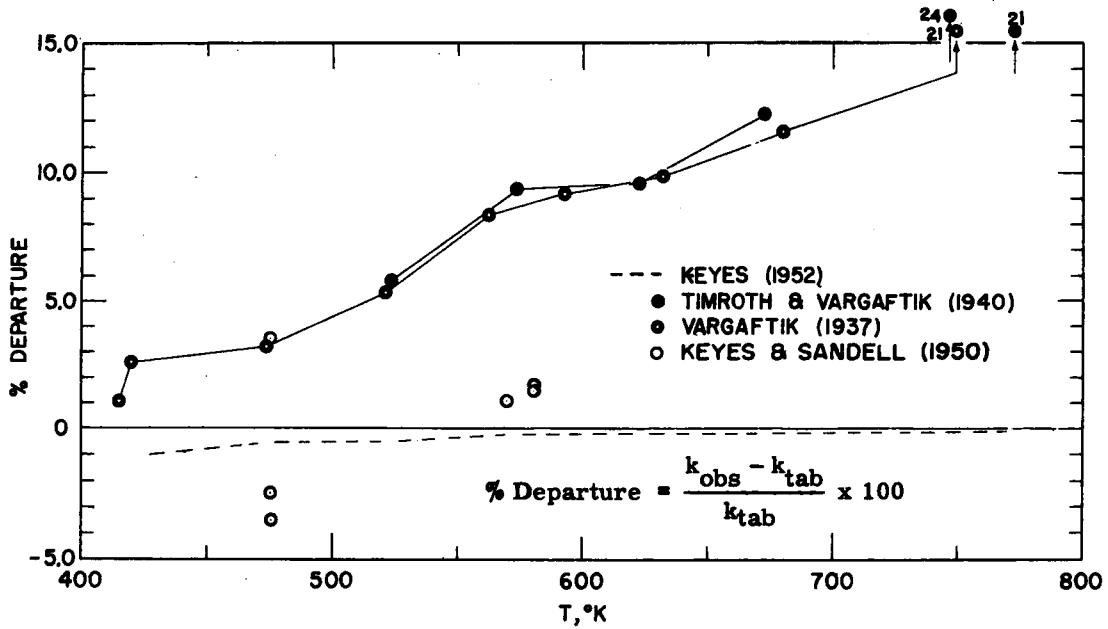


Figure 9c. Departures of low-pressure experimental thermal conductivities from the tabulated values for steam (table 9-7)

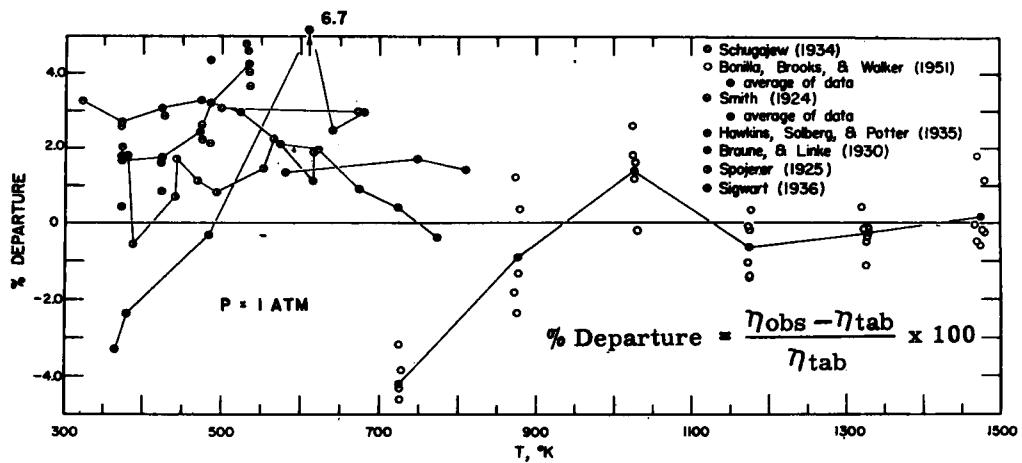


Figure 9d. Departure of low-pressure experimental viscosities from the tabulated values for steam (table 9-6)

The tabulated values of the thermodynamic functions for the ideal gas are those of Friedman and Haar [9]. These authors have calculated the properties of H<sub>2</sub>O to temperatures of 5000°K employing a partition function expanded in closed form. The calculations include first order correction terms for anharmonicity, rotation-vibration interaction, and centrifugal stretching. The calculations are based on the best available molecular constants obtained from extensive spectroscopic measurements by Benedict, Gailor, and Plyler [10, 11] and Benedict, Claassen, and Shaw [12]. The same spectroscopic data were employed by Glatt, Adams, and Johnston [13] in a term-by-term summation over the energy levels of the unexpanded partition function with appropriate rotational cut-off. The agreement of this tabulation with earlier tables [14, 15, 16] is discussed fully by Friedman and Haar [9].

The viscosity and thermal conductivity were computed from the equations given in summary tables 1-B and 1-C. A discussion of the correlation is given by Hilsenrath and Touloukian [17].

The vapor pressures tabulated for the liquid were taken from the tabulation of Osborne, Stimson, and Ginnings [18]. The vapor pressure for ice was taken from the tabulation given by Dorsey [19], who lists values for the critical constants,  $t_c = 374.15^\circ\text{C}$ ,  $p_c = 218.39$  atmospheres, and for the triple point pressure,  $p = 0.00603$  atmospheres.

#### The Consistency and Reliability of the Tables

The accuracy of the tables of thermodynamic functions depends largely on the precision of the correlation of experimental data of state by Keyes [4]. It is estimated that the uncertainty in the values of the compressibility factor (table 9-1) does not exceed a few percent of Z - 1. The values of the density (table 9-2) are equally reliable, since they were computed directly from the compressibility factors. For the derived thermodynamic properties, namely, specific heat (table 9-3), enthalpy (table 9-4), entropy (table 9-5), and free energy function (table 9-8), the uncertainties should be approximately 10 percent of the gas imperfection correction.

The estimated uncertainties in the tabulated ideal-gas values are given in the summary table 1-D.

The tables of compressibility and density are in agreement with values obtained by appropriate interpolation methods from the table of specific volumes given in Keenan and Keyes [1]. The derived quantities, however, disagree by amounts corresponding to the differences between the values of the ideal-gas properties used here and those employed in the steam tables. A comparison of this tabulation with the Collins-Keyes [16] formulation for the ideal-gas specific heat shows table 9-10 to be higher by 0.015 in  $C_p^0/R$  in the temperature region 300° - 500°K.

Comparisons of tables of entropy and enthalpy must take into account the arbitrary values at the reference points for these functions. The reference point used here for both the enthalpy function and entropy is 0°K at which point the values of these properties are taken to be zero.

The tabulated values of thermal conductivity (table 9-7) have an average deviation of 2.1 percent from the observed values reported by Keyes and Sandell [20], whose experimental data extend to 625°K and 150 atmospheres. The tabulated values depart appreciably from data of Vargaftik [21]

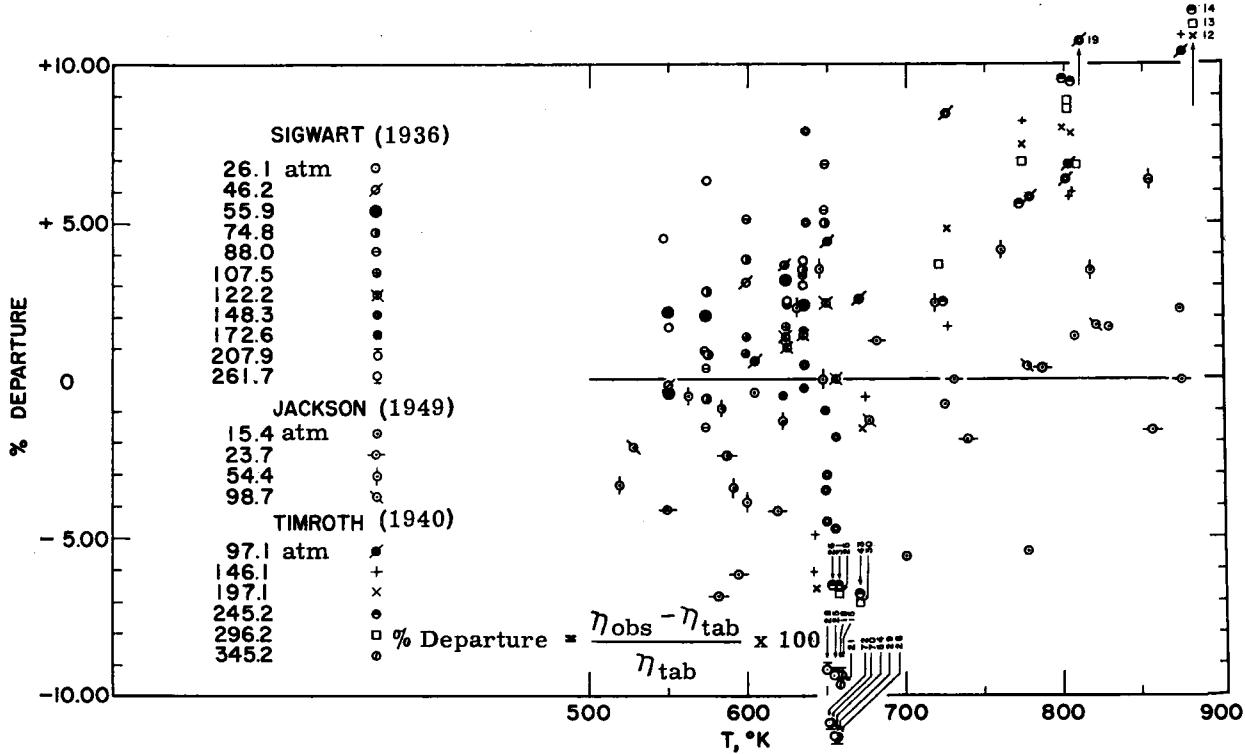


Figure 9e. Departures of high-pressure experimental viscosities from the tabulated values for steam (table 9-6/a)

and Timroth [22]. Figure 9c shows these departures in the low-pressure region (1 atmosphere). The broken line in that figure represents points calculated from the most recent correlation by F. G. Keyes [23].

The departures from the tabulated values of the low-pressure viscosity data for steam are shown in figure 9d to be less than 4 percent. The scatter of the reliable measurements at elevated pressures is higher (approximately 10 percent) as is indicated in figure 9e.

The tables of vapor pressure are thought to be reliable to better than 0.1 percent.

### References

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Table 9-a. VALUES OF THE GAS CONSTANT, R, FOR STEAM

Values of R for Steam for Temperatures in Degrees Kelvin

Pressure Density	atm	kg/cm <sup>2</sup>	mm Hg	lb/in <sup>2</sup>
g/cm <sup>3</sup>	4.55466	4.70660	3461.54	66.9353
mole/cm <sup>3</sup>	82.0567	84.7832	62363.1	1205.91
mole/liter	0.0820544	0.0847809	62.3613	1.20587
lb/ft <sup>3</sup>	0.0729579	0.0753821	55.4480	1.07219
lb mole/ft <sup>3</sup>	1.31441	1.35808	998.952	19.3166

Values of R for Steam for Temperatures in Degrees Rankine

Pressure Density	atm	kg/cm <sup>2</sup>	mm Hg	lb/in <sup>2</sup>
g/cm <sup>3</sup>	2.53037	2.61444	1923.08	37.1863
mole/cm <sup>3</sup>	45.5871	47.1018	34646.2	669.950
mole/liter	0.0455858	0.0471005	34.6452	0.669928
lb/ft <sup>3</sup>	0.0405322	0.0418789	30.8044	0.595661
lb mole/ft <sup>3</sup>	0.730228	0.754489	554.973	10.7314

Table 9-b. CONVERSION FACTORS FOR THE STEAM TABLES

Conversion Factors for Table 9-2

To Convert Tabulated Value of	To	Having the Dimensions Indicated Below	Multiply by
$\rho$ in $\text{g cm}^{-3}$	$\rho$	$\text{mole cm}^{-3}$	.055506
		$\text{g liter}^{-1}$	$1.00003 \times 10^3$
		$\text{lb in}^{-3}$	$3.61275 \times 10^{-2}$
		$\text{lb ft}^{-3}$	62.4283

Conversion Factors for Table 9-4 and 9-10

To Convert Tabulated Value of	To	Having the Dimensions Indicated Below	Multiply by
$(H^{\circ} - E_0^{\circ})/RT_0$	$(H^{\circ} - E_0^{\circ})$ ,	$\text{cal mole}^{-1}$	542.821
$(H - E_0^{\circ})/RT_0$	$(H - E_0^{\circ})$	$\text{cal g}^{-1}$	30.1299
		$\text{joules g}^{-1}$	126.064
		$\text{Btu (lb mole)}^{-1}$	976.437
		$\text{Btu lb}^{-1}$	54.1983

Conversion Factors for Tables 9-3, 9-5, 9-8, and 9-10

To Convert Tabulated Value of	To	Having the Dimensions Indicated Below	Multiply by
$C_p^{\circ}/R$ , $S^{\circ}/R$ ,	$C_p^{\circ}$ , $S^{\circ}$ ,	$\text{cal mole}^{-1} {}^{\circ}\text{K}^{-1}$ (or ${}^{\circ}\text{C}^{-1}$ )	1.98719
$C_p/R$ , $S/R$ ,	$C_p$ , $S$ ,	$\text{cal g}^{-1} {}^{\circ}\text{K}^{-1}$ (or ${}^{\circ}\text{C}^{-1}$ )	0.110301
$-(F^{\circ} - E_0^{\circ})/RT$ ,	$-(F^{\circ} - E_0^{\circ})/T$ ,	$\text{joules g}^{-1} {}^{\circ}\text{K}^{-1}$ (or ${}^{\circ}\text{C}^{-1}$ )	0.461500
$-(F - E_0^{\circ})/RT$	$-(F - E_0^{\circ})/T$	$\text{Btu (lb mole)}^{-1} {}^{\circ}\text{R}^{-1}$ (or ${}^{\circ}\text{F}^{-1}$ )	1.98588
		$\text{Btu lb}^{-1} {}^{\circ}\text{R}^{-1}$ (or ${}^{\circ}\text{F}^{-1}$ )	0.110229

Molecular weight of steam is  $18.016 \text{ g mole}^{-1}$ . Unless otherwise specified, the mole is the gram-mole; the calorie is the thermochemical calorie; and the joule is the absolute joule.

Table 9-b. CONVERSION FACTORS FOR THE STEAM TABLES - Cont.

Conversion Factors for Table 9-6

To Convert Tabulated Value of	To	Having the Dimensions Indicated Below	Multiply by
$\eta$ in poise or $(g \text{ sec}^{-1} \text{ cm}^{-1})$	$\eta$	$\text{kg hr}^{-1} \text{ m}^{-1}$ $\text{slug hr}^{-1} \text{ ft}^{-1}$ $\text{lb sec}^{-1} \text{ ft}^{-1}$ $\text{lb hr}^{-1} \text{ ft}^{-1}$	$3.6000 \times 10^2$ 7.5188 $6.7197 \times 10^{-2}$ $2.4191 \times 10^2$

Conversion Factors for Table 9-7

To Convert Tabulated Value of	To	Having the Dimensions Indicated Below	Multiply by
$k/k_0^{\circ}$	$k$	$\text{cal cm}^{-1} \text{ sec}^{-1} {}^\circ\text{K}^{-1}$ $\text{Btu ft}^{-1} \text{ hr}^{-1} {}^\circ\text{R}^{-1}$ $\text{watts cm}^{-1} {}^\circ\text{K}^{-1}$	$3.789 \times 10^{-5}$ $9.160 \times 10^{-3}$ $1.585 \times 10^{-4}$

Table 9-1. COMPRESSIBILITY FACTOR FOR STEAM

 $Z = PV/RT$ 

$^{\circ}K$	1 atm	10 atm	20 atm	40 atm	$^{\circ}R$
380	.98591	176			684
390	.98767	145			702
400	.98912	120			720
410	.99032	101			738
420	.99133	86			756
430	.99219	75			774
440	.99294	65			792
450	.99359	56			810
460	.99415	50	.93377	671	828
470	.99465	44	.94048	569	846
480	.99509	39	.94617	488	864
490	.99548	35	.95105	423	882
500	.99583	31	.95528	369	900
510	.99614	28	.95897	326	918
520	.99642	25	.96223	288	936
530	.99667	23	.96511	257	954
540	.99690	21	.96768	231	972
550	.99711	19	.96999	208	990
560	.99730	17	.97207	188	1008
570	.99747	16	.97395	170	1026
580	.99763	14	.97565	155	1044
590	.99777	13	.97720	142	1062
600	.99790	12	.97862	130	1080
610	.99802	12	.97992	119	1098
620	.99814	10	.98111	110	1116
630	.99824	10	.98221	102	1134
640	.99834	9	.98323	94	1152
650	.99843	9	.98417	86	1170
660	.99852	8	.98503	81	1188
670	.99860	7	.98584	75	1206
680	.99867	7	.98659	70	1224
690	.99874	6	.98729	66	1242
700	.99880	6	.98795	61	1260
710	.99886	6	.98856	57	1278
720	.99892	5	.98913	54	1296
730	.99897	5	.98967	51	1314
740	.99902	5	.99018	47	1332
750	.99907	4	.99065	45	1350
760	.99911	4	.99110	42	1368
770	.99915	4	.99152	40	1386
780	.99919	4	.99192	37	1404
790	.99923	4	.99229	36	1422
800	.99927	3	.99265	33	1440
810	.99930	3	.99298	32	1458
820	.99933	3	.99330	30	1476
830	.99936	3	.99360	29	1494
840	.99939	3	.99389	27	1512
850	.99942		.99416	.98832	1530
				.97667	

Table 9-1. COMPRESSIBILITY FACTOR FOR STEAM - Cont.

 $Z = PV/RT$ 

$^{\circ}K$	60 atm	80 atm	100 atm	120 atm	$^{\circ}R$				
550	.76634	2397			990				
560	.79031	1983			1008				
570	.81014	1678	.71657	3026	1026				
580	.82692	1441	.74683	2458	1044				
590	.84133	1253	.77141	2053	1062				
600	.85386	1101	.79194	1750	.7180	274	.6214	461	1080
610	.86487	975	.80944	1514	.7454	228	.6675	350	1098
620	.87462	871	.82458	1326	.7682	194	.7025	283	1116
630	.88333	782	.83784	1171	.7876	167	.7308	234	1134
640	.89115	692	.84955	1017	.8043	142	.7542	194	1152
650	.89807	625	.85972	905	.81848	1242	.7736	166	1170
660	.90432	572	.86877	823	.83090	1117	.7902	147	1188
670	.91004	526	.87700	751	.84207	1011	.80493	1316	1206
680	.91530	485	.88451	688	.85218	920	.81809	1185	1224
690	.92015	448	.89139	633	.86138	839	.82994	1074	1242
700	.92463	415	.89772	582	.86977	769	.84068	977	1260
710	.92878	385	.90354	539	.87746	707	.85045	894	1278
720	.93263	358	.90893	498	.88453	652	.85939	819	1296
730	.93621	334	.91391	463	.89105	603	.86758	755	1314
740	.93955	312	.91854	432	.89708	559	.87513	697	1332
750	.94267	291	.92286	402	.90267	520	.88210	645	1350
760	.94558	273	.92688	375	.90787	484	.88855	599	1368
770	.94831	255	.93063	350	.91271	451	.89454	557	1386
780	.95086	241	.93413	329	.91722	421	.90011	519	1404
790	.95327	226	.93742	309	.92143	395	.90530	485	1422
800	.95553	213	.94051	290	.92538	370	.91015	453	1440
810	.95766	200	.94341	273	.92908	348	.91468	425	1458
820	.95966	190	.94614	257	.93256	327	.91893	399	1476
830	.96156	179	.94871	242	.93583	308	.92292	375	1494
840	.96335	169	.95113	229	.93891	290	.92667	354	1512
850	.96504		.95342		.94181		.93021		1530

$^{\circ}K$	120 atm	140 atm	160 atm	180 atm	$^{\circ}R$				
600	.6214	461			1080				
610	.6675	350			1098				
620	.7025	283	.6209	433	1116				
630	.7308	234	.6642	337	.5797	518	1134		
640	.7542	194	.6979	264	.6315	371	.5464	569	1152
650	.7736	166	.7243	218	.6686	289	.6033	395	1170
660	.7902	147	.7461	190	.6975	246	.6428	321	1188
670	.80493	1316	.7651	168	.7221	212	.6749	269	1206
680	.81809	1185	.78194	1495	.7433	187	.7018	231	1224
690	.82994	1074	.79689	1342	.76198	1652	.72492	2016	1242
700	.84068	977	.81031	1212	.77850	1478	.74508	1783	1260
710	.85045	894	.82243	1100	.79328	1332	.76291	1591	1278
720	.85939	819	.83343	1004	.80660	1206	.77882	1430	1296
730	.86758	755	.84347	919	.81866	1099	.79312	1294	1314
740	.87513	697	.85266	845	.82965	1005	.80606	1177	1332
750	.88210	645	.86111	780	.83970	922	.81783	1076	1350
760	.88855	599	.86891	720	.84892	851	.82859	988	1368
770	.89454	557	.87611	669	.85743	785	.83847	909	1386
780	.90011	519	.88280	621	.86528	728	.84756	840	1404
790	.90530	485	.88901	579	.87256	677	.85596	779	1422
800	.91015	453	.89480	540	.87933	630	.86375	723	1440
810	.91468	425	.90020	505	.88563	588	.87098	673	1458
820	.91893	399	.90525	473	.89151	549	.87771	627	1476
830	.92292	375	.90998	444	.89700	514	.88398	587	1494
840	.92667	354	.91442	418	.90214	485	.88985	551	1512
850	.93021		.91860		.90699		.89536		1530

Table 9-1. COMPRESSIBILITY FACTOR FOR STEAM - Cont.

Z = PV/RT

$\gamma$	180 atm	200 atm	220 atm	240 atm	$\gamma$				
640	.5464	569			1152				
650	.6033	395	.5206	504	.3763	1224	1170		
660	.6428	321	.5790	432	.4987	625	.3751	1120	1188
670	.6749	269	.6222	344	.5612	453	.4871	628	1206
680	.7018	231	.6566	287	.6065	360	.5499	459	1224
690	.72492	2016	.6853	245	.6425	298	.5958	366	1242
700	.74508	1783	.70978	2137	.6723	255	.6324	305	1260
710	.76291	1591	.73115	1884	.69785	2220	.6629	260	1278
720	.77882	1430	.74999	1679	.72005	1956	.6889	227	1296
730	.79312	1294	.76678	1508	.73961	1743	.7116	200	1314
740	.80606	1177	.78186	1364	.75704	1565	.7316	178	1332
750	.81783	1076	.79550	1240	.77269	1415	.7494	160	1350
760	.82859	988	.80790	1133	.78684	1287	.7654	145	1368
770	.83847	909	.81923	1099	.79971	1176	.7799	132	1386
780	.84756	840	.82962	957	.81147	1079	.7931	121	1404
790	.85596	779	.83919	885	.82226	994	.8052	110	1422
800	.86375	723	.84804	819	.83220	918	.8162	102	1440
810	.87098	673	.85623	761	.84138	851	.8264	95	1458
820	.87771	627	.86384	708	.84989	790	.8359	87	1476
830	.88398	587	.87092	660	.85779	736	.8446	81	1494
840	.88985	551	.87752	619	.86515	688	.8527	76	1512
850	.89536		.88371		.87203		.8603		1530

$\gamma$	240 atm	260 atm	280 atm	300 atm	$\gamma$				
660	.3751	1120			1188				
670	.4871	628	.3888	952	1206				
680	.5499	459	.4840	604	.4066	805	.3323	931	1224
690	.5958	366	.5444	451	.4871	564	.4254	690	1242
700	.6324	305	.5895	365	.5435	436	.4944	519	1260
710	.6629	260	.6260	305	.5871	356	.5463	413	1278
720	.6889	227	.6565	261	.6227	300	.5876	344	1296
730	.7116	200	.6826	228	.6527	259	.6220	292	1314
740	.7316	178	.7054	202	.6786	227	.6512	254	1332
750	.7494	160	.7256	180	.7013	202	.6766	224	1350
760	.7654	145	.7436	162	.7215	180	.6990	199	1368
770	.7799	132	.7598	147	.7395	162	.7189	179	1386
780	.7931	121	.7745	134	.7557	148	.7368	161	1404
790	.8052	110	.7879	122	.7705	134	.7529	147	1422
800	.8162	102	.8001	113	.7839	124	.7676	134	1440
810	.8264	95	.8114	104	.7963	113	.7810	123	1458
820	.8359	87	.8218	96	.8076	105	.7933	114	1476
830	.8446	81	.8314	89	.8181	97	.8047	105	1494
840	.8527	76	.8403	83	.8278	89	.8152	97	1512
850	.8603		.8486		.8367		.8249		1530

Table 9-2. DENSITY OF STEAM

 $\rho$ 

$^{\circ}K$	1 atm g/cm <sup>3</sup>	10 atm g/cm <sup>3</sup>	20 atm g/cm <sup>3</sup>	40 atm g/cm <sup>3</sup>	$^{\circ}R$
380	.00058604	- 1605			684
390	.00056999	- 1506			702
400	.00055493	- 1419			720
410	.00054074	- 1342			738
420	.00052732	- 1270			756
430	.00051462	- 1208			774
440	.00050254	- 1149			792
450	.00049105	- 1095			810
460	.00048010	- 1045	.00511115 - 1445		828
470	.00046965	- 999	.0049670 - 1327		846
480	.00045966	- 955	.0048343 - 1229		864
490	.00045011	- 916	.0047114 - 1147	.010045 - 317	882
500	.00044095	- 878	.0045967 - 1075	.0097284 - 2851	900
510	.00043217	- 843	.0044892 - 1012	.0094433 - 2598	918
520	.00042374	- 810	.0043880 - 957	.0091835 - 2388	936
530	.00041564	- 779	.0042923 - 907	.0089447 - 2211	.019910 - 740
540	.00040785	- 750	.0042016 - 862	.0087236 - 2062	.019170 - 647
550	.00040035	- 722	.0041154 - 821	.0085174 - 1932	.018523 - 576
560	.00039313	- 697	.0040333 - 784	.0083242 - 1817	.017947 - 518
570	.00038616	- 672	.0039549 - 750	.0081425 - 1717	.017429 - 472
580	.00037944	- 648	.0038799 - 718	.0079708 - 1627	.016957 - 434
590	.00037296	- 626	.0038081 - 689	.0078081 - 1545	.016523 - 402
600	.00036670	- 606	.0037392 - 662	.0076536 - 1472	.016121 - 374
610	.00036064	- 586	.0036730 - 636	.0075064 - 1405	.015747 - 350
620	.00035478	- 567	.0036094 - 613	.0073659 - 1344	.015397 - 329
630	.00034911	- 548	.0035481 - 590	.0072315 - 1286	.015068 - 310
640	.00034363	- 532	.0034891 - 570	.0071029 - 1234	.014758 - 292
650	.00033831	- 516	.0034321 - 550	.0069795 - 1184	.014466 - 278
660	.00033315	- 500	.0033771 - 531	.0068611 - 1140	.014188 - 265
670	.00032815	- 484	.0033240 - 514	.0067471 - 1099	.013923 - 252
680	.00032331	- 471	.0032726 - 497	.0066372 - 1058	.013671 - 242
690	.00031860	- 457	.0032229 - 481	.0065314 - 1022	.013429 - 231
700	.00031403	- 444	.0031748 - 467	.0064292 - 986	.013198 - 222
710	.00030959	- 432	.0031281 - 452	.0063306 - 955	.012976 - 213
720	.00030527	- 420	.0030829 - 439	.0062351 - 923	.012763 - 205
730	.00030107	- 408	.0030390 - 426	.0061428 - 894	.012558 - 197
740	.00029699	- 398	.0029964 - 414	.0060534 - 866	.012361 - 190
750	.00029301	- 386	.0029550 - 402	.0059668 - 839	.012171 - 184
760	.00028915	- 377	.0029148 - 390	.0058829 - 815	.011987 - 177
770	.00028538	- 367	.0028758 - 381	.0058014 - 790	.011810 - 172
780	.00028171	- 358	.0028377 - 369	.0057224 - 768	.011638 - 165
790	.00027813	- 349	.0028008 - 360	.0056456 - 747	.011473 - 161
800	.00027464	- 339	.0027648 - 351	.0055709 - 725	.011312 - 156
810	.00027125	- 332	.0027297 - 341	.0054984 - 706	.011156 - 150
820	.00026793	- 324	.0026956 - 333	.0054278 - 687	.011006 - 147
830	.00026469	- 315	.0026623 - 325	.0053591 - 669	.010859 - 142
840	.00026154	- 309	.0026298 - 316	.0052922 - 651	.010717 - 138
850	.00025845		.0025982	.0052271	1530

Table 9-2. DENSITY OF STEAM - Cont.

 $\rho$ 

$^{\circ}K$	60 atm	80 atm	100 atm	120 atm	$^{\circ}R$				
	g/cm <sup>3</sup>	g/cm <sup>3</sup>	g/cm <sup>3</sup>	g/cm <sup>3</sup>					
550	.031254	- 1489			990				
560	.029765	- 1238			1008				
570	.028527	- 1060	.043003	- 2454	1026				
580	.027467	- 928	.040549	- 1957	1044				
590	.026539	- 826	.038592	- 1627	1062				
600	.025713	- 743	.036965	- 1392	.05096	- 268	.07066	- 595	1080
610	.024970	- 677	.035573	- 1217	.04828	- 218	.06471	- 422	1098
620	.024293	- 621	.034356	- 1080	.04610	- 185	.06049	- 327	1116
630	.023672	- 574	.033276	- 971	.04425	- 160	.05722	- 264	1134
640	.023098	- 531	.032305	- 874	.04265	- 138	.05458	- 218	1152
650	.022567	- 496	.031431	- 798	.041269	- 1233	.05240	- 188	1170
660	.022071	- 466	.030633	- 741	.040036	- 1121	.05052	- 167	1188
670	.021605	- 440	.029292	- 689	.038915	- 1027	.048853	- 1493	1206
680	.021165	- 416	.029203	- 646	.037888	- 948	.047360	- 1352	1224
690	.020749	- 396	.028557	- 606	.036940	- 879	.046008	- 1237	1242
700	.020353	- 376	.027951	- 571	.036061	- 819	.044771	- 1138	1260
710	.019977	- 359	.027380	- 541	.035242	- 767	.043633	- 1053	1278
720	.019618	- 343	.026839	- 512	.034475	- 721	.042580	- 980	1296
730	.019275	- 328	.026327	- 486	.033754	- 680	.041600	- 916	1314
740	.018947	- 314	.025841	- 464	.033074	- 644	.040684	- 860	1332
750	.018633	- 302	.025377	- 443	.032430	- 610	.039824	- 809	1350
760	.018331	- 290	.024934	- 423	.031820	- 579	.039015	- 765	1368
770	.018041	- 279	.024511	- 405	.031241	- 552	.038250	- 724	1386
780	.017762	- 269	.024106	- 388	.030689	- 527	.037526	- 687	1404
790	.017493	- 260	.023718	- 374	.030162	- 504	.036839	- 655	1422
800	.017233	- 251	.023344	- 359	.029658	- 483	.036184	- 623	1440
810	.016982	- 242	.022985	- 346	.029175	- 464	.035561	- 596	1458
820	.016740	- 234	.022639	- 333	.028711	- 445	.034965	- 571	1476
830	.016506	- 227	.022306	- 322	.028266	- 428	.034394	- 547	1494
840	.016279	- 220	.021984	- 310	.027838	- 412	.033847	- 525	1512
850	.016059		.021674		.027426		.033322		1530

Table 9-2. DENSITY OF STEAM - Cont.

 $\rho$ 

$^{\circ}K$	120 atm	140 atm	160 atm	180 atm	$^{\circ}R$				
	g/cm <sup>3</sup>	g/cm <sup>3</sup>	g/cm <sup>3</sup>	g/cm <sup>3</sup>					
600	.07066	- 595			1080				
610	.06471	- 422			1098				
620	.06049	- 327	.07985	- 637	1116				
630	.05722	- 264	.07348	- 466	1134				
640	.05458	- 218	.06882	- 353	1152				
650	.05240	- 188	.06529	- 287	.08083	- 452	.1008	- 76	1170
660	.05052	- 167	.06242	- 246	.07631	- 370	.09315	- 575	1188
670	.048853	- 1493	.05996	- 215	.07261	- 312	.08740	- 459	1206
680	.047360	- 1352	.057808	- 1906	.06949	- 268	.08281	- 380	1224
690	.046008	- 1237	.055902	- 1712	.066814	- 2351	.079009	- 3236	1242
700	.044771	- 1138	.054190	- 1550	.064463	- 2093	.075773	- 2813	1260
710	.043633	- 1053	.052640	- 1416	.062370	- 1881	.072960	- 2483	1278
720	.042580	- 980	.051224	- 1303	.060489	- 1708	.070477	- 2219	1296
730	.041600	- 916	.049921	- 1206	.058781	- 1562	.068258	- 2003	1314
740	.040684	- 860	.048715	- 1121	.057219	- 1439	.066255	- 1825	1332
750	.039824	- 809	.047594	- 1048	.055780	- 1332	.064430	- 1673	1350
760	.039015	- 765	.046546	- 982	.054448	- 1240	.062757	- 1545	1368
770	.038250	- 724	.045564	- 925	.053208	- 1159	.061212	- 1433	1386
780	.037526	- 687	.044639	- 873	.052049	- 1088	.059779	- 1336	1404
790	.036839	- 655	.043766	- 827	.050961	- 1024	.058443	- 1251	1422
800	.036184	- 623	.042939	- 784	.049937	- 967	.057192	- 1174	1440
810	.035561	- 596	.042155	- 747	.048970	- 917	.056018	- 1108	1458
820	.034965	- 571	.041408	- 711	.048053	- 869	.054910	- 1046	1476
830	.034394	- 547	.040697	- 680	.047184	- 827	.053864	- 993	1494
840	.033847	- 525	.040017	- 650	.046357	- 791	.052871	- 943	1512
850	.033322		.039367		.045566		.051928		1530

$^{\circ}K$	180 atm	200 atm	220 atm	240 atm	$^{\circ}R$				
	g/cm <sup>3</sup>	g/cm <sup>3</sup>	g/cm <sup>3</sup>	g/cm <sup>3</sup>					
640	.1130	- 122			1152				
650	.1008	- 76	.1298	- 149	.1975	- 507			1170
660	.09315	- 575	.1149	- 96	.1468	- 183	.2128	- 513	1188
670	.08740	- 459	.1053	- 70	.1285	- 114	.1615	- 206	1206
680	.08281	- 380	.09835	- 547	.1171	- 81	.1409	- 127	1224
690	.079009	- 3236	.09288	- 450	.1090	- 64	.1282	- 92	1242
700	.075773	- 2813	.088380	- 3792	.1026	- 51	.1190	- 70	1260
710	.072960	- 2483	.084588	- 3270	.09749	- 432	.1120	- 58	1278
720	.070477	- 2219	.081318	- 2870	.093169	- 3706	.1062	- 48	1296
730	.068258	- 2003	.078448	- 2553	.089463	- 3242	.1014	- 41	1314
740	.066255	- 1825	.075895	- 2296	.086221	- 2872	.09733	- 358	1332
750	.064430	- 1673	.073599	- 2083	.083349	- 2576	.09375	- 317	1350
760	.062757	- 1545	.071516	- 1905	.080773	- 2332	.09058	- 284	1368
770	.061212	- 1433	.069611	- 1753	.078441	- 2128	.08774	- 256	1386
780	.059779	- 1336	.067858	- 1623	.076313	- 1955	.08518	- 234	1404
790	.058443	- 1251	.066235	- 1511	.074358	- 1806	.08284	- 214	1422
800	.057192	- 1174	.064724	- 1410	.072552	- 1678	.08070	- 198	1440
810	.056018	- 1108	.063314	- 1323	.070874	- 1565	.07872	- 184	1458
820	.054910	- 1046	.061991	- 1245	.069309	- 1466	.07688	- 171	1476
830	.053864	- 993	.060746	- 1174	.067843	- 1378	.07517	- 160	1494
840	.052871	- 943	.059572	- 1114	.066465	- 1300	.07357	- 151	1512
850	.051928		.058458		.065165		.07206		1530

Table 9-2. DENSITY OF STEAM - Cont.

 $\rho$ 

°K	240 atm		260 atm		280 atm		300 atm		°R
	g/cm <sup>3</sup>		g/cm <sup>3</sup>		g/cm <sup>3</sup>		g/cm <sup>3</sup>		
660	.2128	- 513							1188
670	.1615	- 206	.2191	- 457					1206
680	.1409	- 127	.1734	- 214	.2223	- 394	.2915	- 671	1224
690	.1282	- 92	.1520	- 137	.1829	- 213	.2244	- 341	1242
700	.1190	- 70	.1383	- 99	.1616	- 141	.1903	- 205	1260
710	.1120	- 58	.1284	- 76	.1475	- 104	.1698	- 141	1278
720	.1062	- 48	.1208	- 62	.1371	- 81	.1557	- 106	1296
730	.1014	- 41	.1146	- 52	.1290	- 66	.1451	- 84	1314
740	.09733	- 358	.1094	- 45	.1224	- 55	.1367	- 69	1332
750	.09375	- 317	.1049	- 39	.1169	- 48	.1298	- 58	1350
760	.09058	- 284	.1010	- 34	.1121	- 41	.1240	- 50	1368
770	.08774	- 256	.09757	- 308	.1080	- 37	.1190	- 44	1386
780	.08518	- 234	.09449	- 278	.1043	- 33	.1146	- 39	1404
790	.08284	- 214	.09171	- 253	.1010	- 30	.1107	- 34	1422
800	.08070	- 198	.08918	- 233	.09803	- 272	.1073	- 32	1440
810	.07872	- 184	.08685	- 214	.09531	- 248	.1041	- 28	1458
820	.07688	- 171	.08471	- 199	.09283	- 229	.1013	- 27	1476
830	.07517	- 160	.08272	- 185	.09054	- 213	.09862	- 243	1494
840	.07357	- 151	.08037	- 173	.08841	- 197	.09619	- 225	1512
850	.07206		.07914		.08644		.09394		1530

Table 9-3. SPECIFIC HEAT OF STEAM

C<sub>p</sub>/R

°K	1 atm	10 atm	20 atm	40 atm	°R
380	4.462	-64			684
390	4.398	-43			702
400	4.355	-27			720
410	4.328	-16			738
420	4.312	-12			756
430	4.300	-9			774
440	4.291	-7			792
450	4.284	-2			810
460	4.282	5.614	-216		828
470	4.282	3	5.398	-167	846
480	4.285	3	5.231	-132	864
490	4.288	6	5.099	-105	882
500	4.294	7	4.994	-84	900
510	4.301	7	4.910	-68	918
520	4.308	9	4.842	-54	936
530	4.317	9	4.788	-44	954
540	4.326	9	4.744	-36	972
550	4.335	11	4.708	-27	990
560	4.346	11	4.681	-22	1008
570	4.357	10	4.659	-18	1026
580	4.367	12	4.641	-13	1044
590	4.379	12	4.628	-10	1062
600	4.391	13	4.618	-7	1080
610	4.404	12	4.611	-5	1098
620	4.416	13	4.606	-2	1116
630	4.429	13	4.604	-1	1134
640	4.442	12	4.603	1	1152
650	4.454	13	4.604	2	1170
660	4.467	14	4.606	4	1188
670	4.481	14	4.610	5	1206
680	4.495	13	4.615	5	1224
690	4.508	14	4.620	7	1242
700	4.522	13	4.627	7	1260
710	4.535	15	4.634	8	1278
720	4.550	14	4.642	9	1296
730	4.564	14	4.651	8	1314
740	4.578	14	4.659	10	1332
750	4.592	15	4.669	11	1350
760	4.607	14	4.680	10	1368
770	4.621	15	4.690	11	1386
780	4.636	14	4.701	11	1404
790	4.650	15	4.712	12	1422
800	4.665	15	4.724	12	1440
810	4.680	14	4.736	12	1458
820	4.694	15	4.748	12	1476
830	4.709	15	4.760	12	1494
840	4.724	15	4.772	13	1512
850	4.739	15	4.785	13	1530

Table 8-3. SPECIFIC HEAT OF STEAM - Cont.

C<sub>p</sub>/R

°K	40 atm	60 atm	80 atm	100 atm	°R
530	8.041	-609			954
540	7.432	-465			972
550	6.967	-365	10.328	-1197	990
560	6.602	-291	9.131	-805	1008
570	6.311	-237	8.326	-601	1026
580	6.074	-193	7.725	-468	1044
590	5.881	-158	7.257	-371	1062
600	5.723	-132	6.886	-301	1080
610	5.591	-110	6.585	-247	1098
620	5.481	-92	6.338	-203	1116
630	5.389	-78	6.135	-169	1134
640	5.311	-65	5.966	-141	1152
650	5.246	-56	5.825	-121	1170
660	5.190	-46	5.704	-100	1188
670	5.144	-40	5.604	-86	1206
680	5.104	-34	5.518	-73	1224
690	5.070	-27	5.445	-62	1242
700	5.043	-25	5.383	-54	1260
710	5.018	-19	5.329	-45	1278
720	4.999	-16	5.284	-39	1296
730	4.983	-13	5.245	-34	1314
740	4.970	-11	5.211	-29	1332
750	4.959	-8	5.182	-24	1350
760	4.951	-8	5.158	-23	1368
770	4.943	-4	5.135	-17	1386
780	4.939	-2	5.118	-13	1404
790	4.937		5.105	-11	1422
800	4.937	1	5.094	-8	1440
810	4.938	1	5.086	-8	1458
820	4.939	2	5.078	-5	1476
830	4.941	3	5.073	-4	1494
840	4.944	5	5.069	-2	1512
850	4.949	5	5.067	5.192	1530

Table 9-4. ENTHALPY OF STEAM\*

 $(H-E_0)/RT_0$ 

$^{\circ}K$	1 atm	10 atm	20 atm	40 atm	$^{\circ}R$
380	5.482	162			684
390	5.644	160			702
400	5.804	159			720
410	5.963	158			738
420	6.121	158			756
430	6.279	157			774
440	6.436	157			792
450	6.593	157			810
460	6.750	157	6.306	201	828
470	6.907	156	6.507	195	846
480	7.063	157	6.702	189	864
490	7.220	157	6.891	184	882
500	7.377	158	7.075	182	900
510	7.535	157	7.257	178	918
520	7.692	158	7.435	176	936
530	7.850	158	7.611	175	954
540	8.008	159	7.786	173	972
550	8.167	159	7.959	172	990
560	8.326	159	8.131	171	1008
570	8.485	160	8.302	170	1026
580	8.645	160	8.472	169	1044
590	8.805	160	8.641	170	1062
600	8.965	161	8.811	168	1080
610	9.126	162	8.979	169	1098
620	9.288	162	9.148	169	1116
630	9.450	162	9.317	168	1134
640	9.612	163	9.485	169	1152
650	9.775	163	9.654	168	1170
660	9.938	164	9.822	169	1188
670	10.102	164	9.991	169	1206
680	10.266	165	10.160	169	1224
690	10.431	165	10.329	169	1242
700	10.596	166	10.498	170	1260
710	10.762	166	10.668	170	1278
720	10.928	167	10.838	170	1296
730	11.095	167	11.008	170	1314
740	11.262	168	11.178	171	1332
750	11.430	169	11.349	171	1350
760	11.599	169	11.520	171	1368
770	11.768	169	11.691	172	1386
780	11.937	170	11.863	173	1404
790	12.107	171	12.036	172	1422
800	12.278	171	12.208	173	1440
810	12.449	171	12.381	174	1458
820	12.620	172	12.555	174	1476
830	12.792	173	12.729	174	1494
840	12.965	173	12.903	175	1512
850	13.138		13.078	13.011	1530

\* The enthalpy function is divided here by a constant  $RT_0$  where  $T_0 = 273.16^{\circ}K$  ( $491.688^{\circ}R$ ).

Table 9-4. ENTHALPY OF STEAM - Cont.\*

 $(H-E_0^0)/RT_0$ 

$^{\circ}K$	40 atm	60 atm	80 atm	100 atm	$^{\circ}R$
530	6.528	283			954
540	6.811	263			972
550	7.074	248	6.237	355	990
560	7.322	236	6.592	319	1008
570	7.558	227	6.911	293	1026
580	7.785	219	7.204	274	1044
590	8.004	212	7.478	258	1062
600	8.216	207	7.736	247	1080
610	8.432	202	7.983	236	1098
620	8.625	199	8.219	228	1116
630	8.824	196	8.447	222	1134
640	9.020	193	8.669	216	1152
650	9.213	191	8.885	210	1170
660	9.404	189	9.095	207	1188
670	9.593	188	9.302	204	1206
680	9.781	186	9.506	201	1224
690	9.967	185	9.707	198	1242
700	10.152	184	9.905	196	1260
710	10.336	184	10.101	194	1278
720	10.520	183	10.295	193	1296
730	10.703	182	10.488	191	1314
740	10.885	181	10.679	190	1332
750	11.066	182	10.869	190	1350
760	11.248	181	11.059	188	1368
770	11.429	181	11.247	188	1386
780	11.610	181	11.435	187	1404
790	11.791	180	11.622	186	1422
800	11.971	181	11.808	187	1440
810	12.152	181	11.995	186	1458
820	12.333	181	12.181	186	1476
830	12.514	181	12.367	185	1494
840	12.695	181	12.552	186	1512
850	12.876		12.738	12.597	1530

\* The enthalpy function is divided here by a constant  $RT_0$  where  $T_0 = 273.16^{\circ}K$  ( $491.688^{\circ}R$ ).

Table 8-5. ENTROPY OF STEAM

S/R

$^{\circ}\text{K}$	1 atm	10 atm	20 atm	40 atm	$^{\circ}\text{R}$
380	23.628	115			684
390	23.743	111			702
400	23.854	107			720
410	23.961	104			738
420	24.065	101			756
430	24.166	99			774
440	24.265	97			792
450	24.362	94			810
460	24.456	92	21.945	118	828
470	24.548	90	22.063	112	846
480	24.638	88	22.175	106	864
490	24.726	87	22.281	102	882
500	24.813	85	22.383	98	900
510	24.898	84	22.481	95	918
520	24.982	82	22.576	92	936
530	25.064	81	22.668	89	954
540	25.145	79	22.757	87	972
550	25.224	78	22.844	84	990
560	25.302	77	22.928	83	1008
570	25.379	76	23.011	81	1026
580	25.455	75	23.092	79	1044
590	25.530	74	23.171	78	1062
600	25.604	72	23.249	76	1080
610	25.676	72	23.325	75	1098
620	25.748	71	23.400	73	1116
630	25.819	70	23.473	73	1134
640	25.889	69	23.546	71	1152
650	25.958	68	23.617	71	1170
660	26.026	67	23.688	69	1188
670	26.093	66	23.757	68	1206
680	26.159	66	23.825	68	1224
690	26.225	65	23.893	66	1242
700	26.290	64	23.959	66	1260
710	26.354	64	24.025	65	1278
720	26.418	63	24.090	64	1296
730	26.481	62	24.154	63	1314
740	26.543	61	24.217	63	1332
750	26.604	61	24.280	62	1350
760	26.665	61	24.342	61	1368
770	26.726	60	24.403	60	1386
780	26.786	59	24.463	60	1404
790	26.845	58	24.523	60	1422
800	26.903	58	24.583	59	1440
810	26.961	58	24.642	58	1458
820	27.019	57	24.700	57	1476
830	27.076	56	24.757	57	1494
840	27.132	56	24.814	57	1512
850	27.188	55	24.871	56	1530

Table 9-5 ENTROPY OF STEAM - Cont.

S/R

$^{\circ}K$	40 atm		60 atm		80 atm		100 atm		$^{\circ}R$
530	20.837	144							954
540	20.981	132							972
550	21.113	122	20.364	175					990
560	21.235	114	20.539	155					1008
570	21.349	108	20.694	139	20.060	200			1026
580	21.457	102	20.833	128	20.260	170			1044
590	21.559	98	20.961	119	20.430	152	19.880	212	1062
600	21.657	93	21.080	111	20.582	137	20.092	178	1080
610	21.750	90	21.191	105	20.719	126	20.270	157	1098
620	21.840	87	21.296	100	20.845	117	20.427	142	1116
630	21.927	84	21.396	95	20.962	110	20.569	130	1134
640	22.011	82	21.491	91	21.072	104	20.699	120	1152
650	22.093	80	21.582	88	21.176	98	20.819	112	1170
660	22.173	77	21.670	85	21.274	95	20.931	106	1188
670	22.250	76	21.755	83	21.369	90	21.037	100	1206
680	22.326	74	21.838	80	21.459	87	21.137	95	1224
690	22.400	73	21.918	78	21.546	84	21.232	91	1242
700	22.473	72	21.996	76	21.630	81	21.323	88	1260
710	22.545	70	22.072	74	21.711	79	21.411	84	1278
720	22.615	68	22.146	72	21.790	77	21.495	82	1296
730	22.683	68	22.218	72	21.867	75	21.577	80	1314
740	22.751	67	22.290	69	21.942	73	21.657	77	1332
750	22.818	65	22.359	69	22.015	72	21.734	75	1350
760	22.883	65	22.428	67	22.087	70	21.809	73	1368
770	22.948	64	22.495	66	22.157	69	21.882	72	1386
780	23.012	63	22.561	65	22.226	68	21.954	70	1404
790	23.075	62	22.626	64	22.294	66	22.024	69	1422
800	23.137	61	22.690	64	22.360	65	22.093	67	1440
810	23.198	61	22.754	62	22.425	64	22.160	67	1458
820	23.259	60	22.816	62	22.489	64	22.227	65	1476
830	23.319	59	22.878	60	22.553	62	22.292	64	1494
840	23.378	58	22.938	60	22.615	61	22.356	63	1512
850	23.436	58	22.998	59	22.676	61	22.419	62	1530

Table 9-6. VISCOSITY OF STEAM AT ATMOSPHERIC PRESSURE

$^{\circ}\text{K}$	$\eta$	$^{\circ}\text{R}$	$^{\circ}\text{K}$	$\eta$	$^{\circ}\text{R}$
poise $\times 10^{-5}$					
280*	9.09	72	504	900	31.70
300	9.81	72	540	920	32.55
320	10.53	72	576	940	33.39
340	11.25	73	612	960	34.22
360	11.98	72	648	980	35.04
380	12.70	72	684	1000	35.85
400	13.42	72	720	1020	36.65
420	14.14	72	756	1040	37.43
440	14.86	73	792	1060	38.21
460	15.59	72	828	1080	38.97
480	16.31	72	864	1100	39.72
500	17.03	72	900	1120	40.46
520	17.75	72	936	1140	41.18
540	18.47	73	972	1160	41.89
560	19.20	72	1008	1180	42.59
580	19.92	72	1044	1200	43.27
600	20.64	72	1080	1220	43.93
620	21.36	72	1116	1240	44.59
640	22.08	73	1152	1260	45.22
660	22.81	72	1188	1280	45.85
680	23.53	72	1224	1300	46.46
700	24.25	72	1260	1320	47.06
720	24.97	72	1296	1340	47.63
740	25.69	73	1332	1360	48.20
760	26.42	72	1368	1380	48.75
780	27.14	72	1404	1400	49.28
800	27.86	73	1440	1420	49.80
820	28.59	73	1476	1440	50.31
840	29.32	75	1512	1460	50.80
860	30.07	78	1548	1480	51.28
880	30.85	85	1584	1500	51.74
900	31.70		1620		2700

\*Entries below 373.16°K refer to the viscosity of the vapor near the saturation pressure.

Table 9-6/a. VISCOSITY OF STEAM AT ELEVATED PRESSURE

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°K	20 atm		40 atm		60 atm		80 atm		°R
	poises x 10 <sup>-5</sup>		poises x 10 <sup>-5</sup>		poises x 10 <sup>-5</sup>		poises x 10 <sup>-5</sup>		
500	17.17	178							900
550	18.95	180	19.14	176	19.45	167			990
600	20.75	179	20.90	177	21.12	170	21.42	164	1080
650	22.54	180	22.67	179	22.82	178	23.06	172	1170
700	24.34	181	24.46	179	24.60	178	24.78	175	1260
750	26.15	179	26.25	179	26.38	177	26.53	175	1350
800	27.94	184	28.04	183	28.15	182	28.28	181	1440
850	29.78	199	29.87	199	29.97	198	30.09	196	1530
900	31.77	210	31.86	209	31.95	208	32.05	204	1620
950	33.87	205	33.95	204	34.03	204	34.09	207	1710
1000	35.92	196	35.99	196	36.07	196	36.16	195	1800
1050	37.88	190	37.95	190	38.03	189	38.11	188	1890
1100	39.78		39.85		39.92		39.99		1980

°K	100 atm		200 atm		250 atm		300 atm		°R
	poises x 10 <sup>-5</sup>		poises x 10 <sup>-5</sup>		poises x 10 <sup>-5</sup>		poises x 10 <sup>-5</sup>		
600	21.87	147							1080
650	23.34	165	27.90	90					1170
700	24.99	171	27.00	127	29.29	2	34.01	-293	1260
750	26.70	173	28.27	136	29.31	108	31.08	42	1350
800	28.43	179	29.63	150	30.39	140	31.50	111	1440
850	30.22	195	31.13	182	31.79	171	32.61	153	1530
900	32.17	206	32.95	197	33.50	188	34.14	177	1620
950	34.23	202	34.92	194	35.38	188	35.91	180	1710
1000	36.25	195	36.86	189	37.26	184	37.71	178	1800
1050	38.20	188	38.75	182	39.10	179	39.49	176	1890
1100	40.08		40.57		40.89		41.25		1980

Table 9-7. THERMAL CONDUCTIVITY OF STEAM

$^{\circ}\text{K}$	0 atm limit	1 atm	4 atm	7 atm	$^{\circ}\text{R}$	$k/k_0$
300	1.126	47				540
310	1.173	48				558
320	1.221	48				576
330	1.269	49				594
340	1.318	49				612
350	1.367	49				630
360	1.416	49				648
370	1.465	50				666
380	1.515	50	1.547	46		684
390	1.565	50	1.593	48		702
400	1.615	50	1.641	48		720
410	1.665	51	1.689	48		738
420	1.716	51	1.737	49	1.809	756
430	1.767	51	1.786	49	1.850	774
440	1.818	52	1.835	50	1.893	792
450	1.870	51	1.885	50	1.938	810
460	1.921	52	1.935	51	1.985	828
470	1.973	52	1.986	51	2.032	846
480	2.025	52	2.037	51	2.078	864
490	2.077	52	2.088	51	2.125	882
500	2.129	52	2.139	51	2.172	900
510	2.181	52	2.190	52	2.221	918
520	2.233	53	2.242	52	2.271	936
530	2.286	52	2.294	52	2.320	954
540	2.338	53	2.346	52	2.369	972
550	2.391	53	2.398	52	2.419	990
560	2.444	52	2.450	52	2.470	1008
570	2.496	53	2.502	53	2.521	1026
580	2.549	53	2.555	53	2.573	1044
590	2.602	53	2.608	52	2.624	1062
600	2.655	54	2.660	53	2.675	1080
610	2.709	53	2.713	53	2.727	1098
620	2.762	53	2.766	53	2.779	1116
630	2.815	53	2.819	53	2.832	1134
640	2.868	54	2.872	53	2.884	1152
650	2.922	53	2.925	54	2.936	1170
660	2.975	54	2.979	53	2.989	1188
670	3.029	53	3.032	53	3.042	1206
680	3.082	54	3.085	54	3.094	1224
690	3.136	54	3.139	53	3.147	1242
700	3.190	53	3.192	53	3.200	1260
710	3.243	54	3.245	54	3.253	1278
720	3.297	54	3.299	54	3.306	1296
730	3.351	53	3.353	53	3.360	1314
740	3.404	54	3.406	54	3.413	1332
750	3.458	54	3.460	54	3.466	1350
760	3.512	54	3.514	53	3.519	1368
770	3.566	53	3.567	54	3.573	1386
780	3.619	54	3.621	54	3.626	1404
790	3.673	53	3.675	53	3.680	1422
800	3.726		3.728		3.733	1440

Table 9-7. THERMAL CONDUCTIVITY OF STEAM - Cont.

 $k/k_0$ 

$^{\circ}\text{K}$	10 atm	40 atm	70 atm	100 atm	$^{\circ}\text{R}$
450	2.069	31			810
460	2.100	33			828
470	2.133	36			846
480	2.169	38			864
490	2.207	41			882
500	2.248	43			900
510	2.291	44			918
520	2.335	44			936
530	2.379	44			954
540	2.423	44			972
550	2.467	48	2.842	6	990
560	2.515	49	2.848	13	1008
570	2.564	48	2.861	18	1026
580	2.612	48	2.879	23	1044
590	2.660	48	2.902	26	1062
600	2.708	50	2.928	29	1080
610	2.758	50	2.957	34	1098
620	2.808	50	2.991	34	1116
630	2.858	51	3.025	37	1134
640	2.909	50	3.062	39	1152
650	2.959	52	3.101	43	1170
660	3.011	51	3.144	42	1188
670	3.062	52	3.186	43	1206
680	3.114	51	3.229	42	1224
690	3.165	51	3.271	43	1242
700	3.216	53	3.314	47	1260
710	3.269	52	3.361	47	1278
720	3.321	53	3.408	46	1296
730	3.374	52	3.454	47	1314
740	3.426	52	3.501	47	1332
750	3.478	53	3.548	49	1350
760	3.531	53	3.597	49	1368
770	3.584	52	3.646	50	1386
780	3.636	53	3.696	49	1404
790	3.689	52	3.745	49	1422
800	3.741		3.794	3.855	1440

$^{\circ}\text{K}$	150 atm	200 atm	250 atm	300 atm	$^{\circ}\text{R}$
620	5.042	-272			1116
630	4.770	-211			1134
640	4.559	-162	6.338	-482	1152
650	4.397	-126	5.856	-376	1170
660	4.271	-97	5.480	-294	1188
670	4.174	-72	5.186	-229	1206
680	4.102	-54	4.957	-179	1224
690	4.048	-38	4.778	-141	1242
700	4.010	-26	4.637	-110	1260
710	3.984	-15	4.527	-85	1278
720	3.969	-6	4.442	-64	1296
730	3.963	1	4.378	-48	1314
740	3.964	7	4.330	-34	1332
750	3.971	13	4.296	-22	1350
760	3.984	17	4.274	-14	1368
770	4.001	21	4.260	-5	1386
780	4.022	24	4.255	2	1404
790	4.046	27	4.257	7	1422
800	4.073		4.264	4.513	1440

Table 9-8. FREE ENERGY FUNCTION OF STEAM

 $-(F - E_0^0)/RT$ 

$^{\circ}K$	1 atm	10 atm	20 atm	40 atm	$^{\circ}R$
380	19.687	103			684
390	19.790	100			702
400	19.890	98			720
410	19.988	96			738
420	20.084	94			756
430	20.178	92			774
440	20.270	89			792
450	20.359	88			810
460	20.447	87	18.200	81	828
470	20.534	84	18.281	80	846
480	20.618	83	18.361	79	864
490	20.701	82	18.440	78	882
500	20.783	79	18.518	77	900
510	20.862	79	18.595	75	918
520	20.941	77	18.670	75	936
530	21.018	76	18.745	73	954
540	21.094	74	18.818	73	972
550	21.168	73	18.891	71	990
560	21.241	72	18.962	70	1008
570	21.313	71	19.032	70	1026
580	21.384	69	19.102	68	1044
590	21.453	69	19.170	67	1062
600	21.522	67	19.237	67	1080
610	21.589	67	19.304	65	1098
620	21.656	66	19.369	65	1116
630	21.722	64	19.434	63	1134
640	21.786	64	19.497	63	1152
650	21.850	62	19.560	62	1170
660	21.912	62	19.622	61	1188
670	21.974	62	19.683	61	1206
680	22.036	60	19.744	60	1224
690	22.096	59	19.804	59	1242
700	22.155	59	19.863	58	1260
710	22.214	58	19.921	57	1278
720	22.272	57	19.978	57	1296
730	22.329	57	20.035	56	1314
740	22.386	55	20.091	55	1332
750	22.441	55	20.146	55	1350
760	22.496	55	20.201	54	1368
770	22.551	54	20.255	54	1386
780	22.605	53	20.309	53	1404
790	22.658	53	20.362	52	1422
800	22.711	52	20.414	52	1440
810	22.763	52	20.466	51	1458
820	22.815	51	20.517	51	1476
830	22.866	50	20.568	50	1494
840	22.916	50	20.618	50	1512
850	22.966		20.668	49	1530
			19.980	49	19.298

Table 9-8. FREE ENERGY FUNCTION OF STEAM - Cont.

 $-(F - E_0^0)/RT$ 

$^{\circ}K$	40 atm	60 atm	80 atm	100 atm	$^{\circ}R$
530	17.472	64			954
540	17.536	63			972
550	17.599	64	17.267	56	990
560	17.663	64	17.323	58	1008
570	17.727	63	17.381	59	1026
580	17.790	63	17.440	59	1044
590	17.853	63	17.499	59	1062
600	17.916	63	17.558	59	1080
610	17.979	61	17.617	58	1098
620	18.040	61	17.675	58	1116
630	18.101	60	17.733	58	1134
640	18.161	60	17.791	58	1152
650	18.221	59	17.849	57	1170
660	18.280	59	17.906	57	1188
670	18.339	58	17.963	56	1206
680	18.397	58	18.019	56	1224
690	18.455	57	18.075	56	1242
700	18.512	56	18.131	55	1260
710	18.568	56	18.186	54	1278
720	18.624	55	18.240	54	1296
730	18.679	55	18.294	54	1314
740	18.734	54	18.348	53	1332
750	18.788	53	18.401	52	1350
760	18.841	52	18.453	52	1368
770	18.893	53	18.505	52	1386
780	18.946	52	18.557	51	1404
790	18.998	51	18.608	50	1422
800	19.049	51	18.658	50	1440
810	19.100	51	18.708	50	1458
820	19.151	49	18.758	49	1476
830	19.200	49	18.807	49	1494
840	19.249	49	18.856	48	1512
850	19.298		18.904	18.628	1530
				18.416	

Table 9-9. VAPOR PRESSURE OF ICE

T °K	P atm	T °R
154	.0000000001	277.2
155	.0000000003	279.0
156	.0000000003	280.8
157	.0000000003	282.6
158	.0000000004	284.4
159	.0000000005	286.2
160	.0000000008	288.0
161	.0000000009	289.8
162	.000000001	291.6
163	.000000001	293.4
164	.000000001	295.2
165	.000000003	297.0
166	.000000003	298.8
167	.000000004	300.6
168	.000000004	302.4
169	.000000005	304.2
170	.000000007	306.0
171	.000000008	307.8
172	.00000001	309.6
173	.00000001	311.4
174	.00000001	313.2
175	.00000001	315.0
176	.00000003	316.8
177	.00000003	318.6
178	.00000004	320.4
179	.00000004	322.2
180	.00000005	324.0
181	.00000007	325.8
182	.00000008	327.6
183	.00000009	329.4
184	.0000001	331.2
185	.00000013	333.0
186	.00000016	334.8
187	.00000018	336.6
188	.00000022	338.4
189	.00000026	340.2
190	.00000032	342.0
191	.00000037	343.8
192	.00000043	345.6
193	.00000051	347.4
194	.00000061	349.2
195	.00000072	351.0
196	.00000084	352.8
197	.00000099	354.6
198	.0000012	356.4
199	.00000134	358.2
200	.00000158	360.0
201	.00000184	361.8
202	.00000214	363.6
203	.00000249	365.4
204	.00000289	367.2

T °K	P atm	T °R
205	.00000336	369.0
206	.00000388	370.8
207	.00000449	372.6
208	.00000518	374.4
209	.00000597	376.2
210	.00000687	378.0
211	.00000791	379.8
212	.00000905	381.6
213	.0000104	383.4
214	.0000119	385.2
215	.0000137	387.0
216	.0000155	388.8
217	.0000178	390.6
218	.0000203	392.4
219	.0000229	394.2
220	.0000262	396.0
221	.0000296	397.8
222	.0000337	399.6
223	.0000382	401.4
224	.0000432	403.2
225	.0000488	405.0
226	.0000550	406.8
227	.0000621	408.6
228	.0000699	410.4
229	.0000787	412.2
230	.0000883	414.0
231	.0000992	415.8
232	.000111	417.6
233	.000125	419.4
234	.0001397	421.2
235	.0001563	423.0
236	.0001746	424.8
237	.0001948	426.6
238	.0002174	428.4
239	.0002422	430.2
240	.0002696	432.0
241	.0002999	433.8
242	.0003332	435.6
243	.0003700	437.4
244	.000411	439.2
245	.000454	441.0
246	.000504	442.8
247	.000557	444.6
248	.000616	446.4
249	.000682	448.2
250	.000751	450.0
251	.000829	451.8
252	.000913	453.6
253	.00101	455.4
254	.00111	457.2

Table 9-9. VAPOR PRESSURE OF ICE - Cont.

T °K	P atm	T °R
254.0	.00111	457.2
254.5	.00116	458.1
255.0	.00122	459.0
255.5	.00128	459.9
256.0	.001337	460.8
256.5	.001400	461.7
257.0	.001467	462.6
257.5	.001537	463.5
258.0	.001609	464.4
258.5	.001686	465.3
259.0	.001764	466.2
259.5	.001847	467.1
260.0	.001933	468.0
260.5	.002024	468.9
261.0	.002116	469.8
261.5	.002213	470.7
262.0	.002314	471.6
262.5	.002420	472.5
263.0	.002530	473.4
263.5	.002645	474.3
264.0	.002764	475.2
264.5	.002888	476.1
265.0	.003017	477.0
265.5	.003151	477.9
266.0	.003292	478.8
266.5	.003437	479.7
267.0	.003589	480.6
267.5	.003747	481.5
268.0	.003911	482.4
268.5	.004080	483.3
269.0	.004258	484.2
269.5	.004442	485.1
270.0	.004633	486.0
270.5	.004832	486.9
271.0	.005038	487.8
271.5	.005253	488.7
272.0	.005475	489.6
272.5	.005707	490.5
273.0	.005946	491.4

Table 9-9/a. VAPOR PRESSURE OF WATER

T °K	P atm	T °R	T °K	P atm	T °R
274	.006406	477	493.2		
275	.006883	508	495.0	325	.13329
276	.007391	542	496.8	326	.13996
277	.007933	576	498.6	327	.14691
278	.008509	614	500.4	328	.15415
279	.009123	651	502.2	329	.16170
280	.009774	692	504.0	330	.16956
281	.010466	735	505.8	331	.17775
282	.011201	781	507.6	332	.18627
283	.011982	827	509.4	333	.19514
284	.012809	878	511.2	334	.20436
285	.013687	930	513.0	335	.21395
286	.014617	986	514.8	336	.22392
287	.015603	1043	516.6	337	.23428
289	.016646	1104	518.4	338	.24505
290	.017750	1167	520.2	339	.25623
291	.018917	1235	522.0	340	.26785
292	.020152	1305	523.8	341	.27991
293	.021457	1378	525.6	342	.29242
294	.022835	1455	527.4	343	.30541
295	.024290	1535	529.2	344	.31887
296	.025825	1620	531.0	345	.33285
297	.027445	1707	532.8	346	.34733
298	.029152	1800	534.6	347	.36234
299	.030952	1896	536.4	348	.37789
300	.032848	1996	538.2	349	.39400
301	.034844	2101	540.0	350	.41069
302	.036945	2210	541.8	351	.42797
303	.039155	2325	543.6	352	.44586
304	.041480	2444	545.4	353	.46437
305	.043924	2568	547.2	354	.48352
306	.046492	2697	549.0	355	.50333
307	.049189	2822	550.8	356	.52382
308	.052021	2972	552.6	357	.54501
309	.054993	3119	554.4	358	.56690
310	.058112	3270	556.2	359	.58953
311	.061382	3428	558.0	360	.61290
312	.064810	3593	559.8	361	.63705
313	.068403	3764	561.6	362	.66198
314	.072167	3941	563.4	363	.68772
315	.076108	4126	565.2	364	.71430
316	.080234	4317	567.0	365	.74172
317	.084551	4516	568.8	366	.77001
318	.089067	4723	570.6	367	.79920
319	.093790	4939	572.4	368	.82930
320	.098729	515	574.2	369	.86034
321	.10388	539	576.0	370	.89233
322	.10927	563	577.8	371	.92531
323	.11490	587	579.6	372	.95929
324	.12077	613	581.4	373	.99430
	.12690	639	583.2	374	1.0304

Table 9-9/a. VAPOR PRESSURE OF WATER - Cont.

T	P	T	T	P	T		
°K	atm	°R	°K	atm	°R		
375	1.0675	382	675.0	425	4.9338	1325	765.0
376	1.1057	394	676.8	426	5.0663	1352	766.8
377	1.1451	405	678.6	427	5.2015	1382	768.6
378	1.1856	417	680.4	428	5.3397	1410	770.4
379	1.2273	429	682.2	429	5.4807	1440	772.2
380	1.2702	441	684.0	430	5.6247	1470	774.0
381	1.3143	454	685.8	431	5.7717	1500	775.8
382	1.3597	466	687.6	432	5.9217	1531	777.6
383	1.4063	480	689.4	433	6.0748	1563	779.4
384	1.4543	493	691.2	434	6.2311	1595	781.2
385	1.5036	506	693.0	435	6.3906	1626	783.0
386	1.5542	521	694.8	436	6.5532	1660	784.8
387	1.6063	535	696.6	437	6.7192	1693	786.6
388	1.6598	549	698.4	438	6.8885	1727	788.4
389	1.7147	564	700.2	439	7.0612	1760	790.2
390	1.7711	579	702.0	440	7.2372	1796	792.0
391	1.8290	595	703.8	441	7.4168	1830	793.8
392	1.8885	610	705.6	442	7.5998	1867	795.6
393	1.9495	626	707.4	443	7.7865	1902	797.4
394	2.0121	643	709.2	444	7.9767	1939	799.2
395	2.0764	659	711.0	445	8.1706	1976	801.0
396	2.1423	676	712.8	446	8.3682	2014	802.8
397	2.2099	693	714.6	447	8.5696	2051	804.6
398	2.2792	711	716.4	448	8.7747	2091	806.4
399	2.3503	729	718.2	449	8.9838	2130	808.2
400	2.4232	748	720.0	450	9.1968	2170	810.0
401	2.4980	766	721.8	451	9.4138	2210	811.8
402	2.5746	785	723.6	452	9.6348	2250	813.6
403	2.6531	804	725.4	453	9.8598	229	815.4
404	2.7335	824	727.2	454	10.089	234	817.2
405	2.8159	844	729.0	455	10.323	237	819.0
406	2.9003	865	730.8	456	10.560	242	820.8
407	2.9868	885	732.6	457	10.802	246	822.6
408	3.0753	906	734.4	458	11.048	250	824.4
409	3.1659	927	736.2	459	11.298	256	826.2
410	3.2586	950	738.0	460	11.554	259	828.0
411	3.3536	971	739.8	461	11.813	264	829.8
412	3.4507	994	741.6	462	12.077	268	831.6
413	3.5501	1018	743.4	463	12.345	273	833.4
414	3.6519	1042	745.2	464	12.618	279	835.2
415	3.7561	1063	747.0	465	12.897	282	837.0
416	3.8624	1088	748.8	466	13.179	288	838.8
417	3.9712	1114	750.6	467	13.467	292	840.6
418	4.0826	1138	752.4	468	13.759	298	842.4
419	4.1964	1163	754.2	469	14.057	302	844.2
420	4.3127	1189	756.0	470	14.359	307	846.0
421	4.4316	1215	757.8	471	14.666	313	847.8
422	4.5531	1242	759.6	472	14.979	317	849.6
423	4.6773	1269	761.4	473	15.296	323	851.4
424	4.8042	1296	763.2	474	15.619	328	853.2

Table 9-9/a. VAPOR PRESSURE OF WATER - Cont.

T	P	T	T	P	T	T	
°K	atm	°R	°K	atm	°R	°R	
475	15.947	334	855.0	525	40.490	684	945.0
476	16.281	339	856.8	526	41.174	692	946.8
477	16.620	344	858.6	527	41.866	700	948.6
478	16.964	350	860.4	528	42.566	710	950.4
479	17.314	356	862.2	529	43.276	719	952.2
480	17.670	361	864.0	530	43.995	728	954.0
481	18.031	367	865.8	531	44.723	737	955.8
482	18.398	372	867.6	532	45.460	746	957.6
483	18.770	379	869.4	533	46.206	756	959.4
484	19.149	384	871.2	534	46.962	766	961.2
485	19.533	391	873.0	535	47.728	774	963.0
486	19.924	396	874.8	536	48.502	784	964.8
487	20.320	402	876.6	537	49.286	793	966.6
488	20.722	409	878.4	538	50.079	804	968.4
489	21.131	415	880.2	539	50.883	813	970.2
490	21.546	421	882.0	540	51.696	824	972.0
491	21.967	428	883.8	541	52.520	833	973.8
492	22.395	433	885.6	542	53.353	843	975.6
493	22.828	441	887.4	543	54.196	853	977.4
494	23.269	447	889.2	544	55.049	864	979.2
495	23.716	453	891.0	545	55.913	874	981.0
496	24.169	460	892.8	546	56.787	884	982.8
497	24.629	466	894.6	547	57.671	894	984.6
498	25.095	474	896.4	548	58.565	906	986.4
499	25.569	481	898.2	549	59.471	916	988.2
500	26.050	487	900.0	550	60.387	927	990.0
501	26.537	495	901.8	551	61.314	937	991.8
502	27.032	501	903.6	552	62.251	948	993.6
503	27.533	508	905.4	553	63.199	960	995.4
504	28.041	516	907.2	554	64.159	971	997.2
505	28.557	523	909.0	555	65.130	982	999.0
506	29.080	530	910.8	556	66.112	993	1000.8
507	29.610	538	912.6	557	67.105	1004	1002.6
508	30.148	545	914.4	558	68.109	1016	1004.4
509	30.693	553	916.2	559	69.125	1028	1006.2
510	31.246	560	918.0	560	70.153	1039	1008.0
511	31.806	568	919.8	561	71.192	1050	1009.8
512	32.374	575	921.6	562	72.242	1063	1011.6
513	32.949	584	923.4	563	73.305	1074	1013.4
514	33.533	592	925.2	564	74.379	1087	1015.2
515	34.125	599	927.0	565	75.466	1099	1017.0
516	34.724	608	928.8	566	76.565	1110	1018.8
517	35.332	615	930.6	567	77.675	1123	1020.6
518	35.947	624	932.4	568	78.798	1136	1022.4
519	36.571	632	934.2	569	79.934	1148	1024.2
520	37.203	641	936.0	570	81.082	1161	1026.0
521	37.844	649	937.8	571	82.243	1174	1027.8
522	38.493	657	939.6	572	83.417	1186	1029.6
523	39.150	666	941.4	573	84.603	1199	1031.4
524	39.816	674	943.2	574	85.802	1212	1033.2

Table 9-9/a. VAPOR PRESSURE OF WATER - Cont.

T °K	P atm	T °R	T °K	P atm	T °R
575	87.014	1226	1035.0	610	138.55
576	88.240	1238	1036.8	611	140.31
577	89.478	1251	1038.6	612	142.09
578	90.729	1266	1040.4	613	143.88
579	91.995	1279	1042.2	614	145.70
580	93.274	1292	1044.0	615	147.53
581	94.566	1306	1045.8	616	149.38
582	95.872	1319	1047.6	617	151.25
583	97.191	1334	1049.4	618	153.14
584	98.525	1349	1051.2	619	155.05
585	99.874	137	1053.0	620	156.98
586	101.24	137	1054.8	621	158.93
587	102.61	139	1056.6	622	160.90
588	104.00	141	1058.4	623	162.89
589	105.41	142	1060.2	624	164.90
590	106.83	144	1062.0	625	166.93
591	108.27	145	1063.8	626	168.98
592	109.72	146	1065.6	627	171.05
593	111.18	148	1067.4	628	173.14
594	112.66	150	1069.2	629	175.26
595	114.16	151	1071.0	630	177.39
596	115.67	153	1072.8	631	179.55
597	117.20	155	1074.6	632	181.74
598	118.75	156	1076.4	633	183.94
599	120.31	157	1078.2	634	186.17
600	121.88	159	1080.0	635	188.43
601	123.47	161	1081.8	636	190.71
602	125.08	162	1083.6	637	193.01
603	126.70	164	1085.4	638	195.33
604	128.34	166	1087.2	639	197.68
605	130.00	168	1089.0	640	200.06
606	131.68	169	1090.8	641	202.47
607	133.37	171	1092.6	642	204.91
608	135.08	172	1094.4	643	207.38
609	136.80	175	1096.2	644	209.87
			645	212.40	256 1161.0
			646	214.96	260 1162.8
			647	217.56	1164.6

Table 9-10 IDEAL-GAS THERMODYNAMIC FUNCTIONS FOR STEAM

$\frac{C_p}{R}$	$\frac{(H^\circ - E_0^\circ)^*}{RT_0}$	$\frac{-(F^\circ - E_0^\circ)}{RT}$	$\frac{S^\circ}{R}$	$^{\circ}R$
50	4.0072	- 9	.7149	1467
60	4.0063	- 4	.8616	1467
70	4.0059	- 2	1.0083	1466
80	4.0057		1.1549	1467
90	4.0057	1	1.3016	1466
100	4.0058	2	1.4482	1467
110	4.0060	2	1.5949	1466
120	4.0062	3	1.7415	1467
130	4.0065	3	1.8882	1467
140	4.0068	4	2.0349	1466
150	4.0072	4	2.1815	1468
160	4.0076	4	2.3283	1467
170	4.0080	6	2.4750	1467
180	4.0086	7	2.6217	1468
190	4.0093	9	2.7685	1468
200	4.0102	11	2.9153	1468
210	4.0113	14	3.0621	1469
220	4.0127	18	3.2090	1469
230	4.0145	21	3.3559	1470
240	4.0166	25	3.5029	1471
250	4.0191	30	3.6500	1472
260	4.0221	36	3.7972	1473
270	4.0257	40	3.9445	1474
280	4.0297	46	4.0919	1476
290	4.0343	51	4.2395	1478
300	4.0394	57	4.3873	1480
310	4.0451	63	4.5353	1482
320	4.0514	68	4.6835	1484
330	4.0582	73	4.8319	1487
340	4.0655	78	4.9806	1490
350	4.0733	83	5.1296	1493
360	4.0816	88	5.2789	1495
370	4.0904	92	5.4284	1500
380	4.0996	96	5.5784	1502
390	4.1092	100	5.7286	1506
400	4.1192	547	5.8792	1589
450	4.1739	606	6.6381	7695
500	4.2345	644	7.4076	7809
550	4.2989	670	8.1885	7930
600	4.3659	691	8.9815	8055
650	4.4350	709	9.7870	8182
700	4.5059	726	10.6052	8314
750	4.5785	740	11.4366	8448
800	4.6525	753	12.2814	8585
850	4.7278	760	13.1399	8723
900	4.8038	766	14.0122	8863
950	4.8804	765	14.8985	9004
1000	4.9569	761	15.7989	9143
1050	5.0330	754	16.7132	9281
1100	5.1084	742	17.6413	9419
1150	5.1826	729	18.5832	9553

\* The enthalpy function is divided here by a constant  $RT_0$  where  $T_0 = 273.16^\circ\text{K}$  ( $491.688^\circ\text{R}$ ).

Table 9-10 IDEAL-GAS THERMODYNAMIC FUNCTIONS FOR STEAM - Cont.

$^{\circ}\text{K}$	$\frac{C_p}{R}$	$(H^\circ - E_0^\circ)^*$		$-(F^\circ - E_0^\circ)$		$\frac{S^\circ}{R}$	$^{\circ}\text{R}$
		$\frac{RT_0}{R}$		$\frac{RT}{R}$			
1200	5.2555	1405	19.5385	19499	24.4569	3587	28.9046
1300	5.3960	1326	21.4884	19999	24.8156	3371	29.3308
1400	5.5286	1240	23.4883	20470	25.1527	3185	29.7356
1500	5.6526	1152	25.5353	20907	25.4712	3022	30.1213
1600	5.7678	1065	27.6260	21312	25.7734	2879	30.4899
1700	5.8743	982	29.7572	21688	26.0613	2751	30.8428
1800	5.9725	903	31.9260	22091	26.3364	2636	31.1814
1900	6.0628	832	34.1291	22350	26.6000	2532	31.5067
2000	6.1460	764	36.3641	22641	26.8532	2438	31.8199
2100	6.2224	704	38.6282	22910	27.0970	2350	32.1216
2200	6.2928	648	40.9192	23158	27.3320	2271	32.4127
2300	6.3576	598	43.2350	23385	27.5591	2196	32.6939
2400	6.4174	553	45.5735	23596	27.7787	2128	32.9657
2500	6.4727	511	47.9331	23789	27.9915	2063	33.2288
2600	6.5238	474	50.3120	23971	28.1978	2004	33.4837
2700	6.5712	441	52.7091	24139	28.3982	1948	33.7308
2800	6.6153	410	55.1230	24293	28.5930	1894	33.9706
2900	6.6563	382	57.5523	24439	28.7824	1845	34.2035
3000	6.6945	691	59.9962	49273	28.9669	3552	34.4298
3200	6.7636	608	64.9235	49748	29.3221	3382	34.8641
3400	6.8244	538	69.8983	50168	29.6603	3229	35.2760
3600	6.8782	481	74.9151	50539	29.9832	3091	35.6676
3800	6.9263	431	79.9690	50872	30.2923	2964	36.0408
4000	6.9694	389	85.0562	51173	30.5887	2848	36.3972
4200	7.0083	353	90.1735	51444	30.8735	2740	36.7382
4400	7.0436	322	95.3179	51691	31.1475	2642	37.0651
4600	7.0758	295	100.4870	51917	31.4117	2550	37.3789
4800	7.1053	272	105.6787	52124	31.6667	2464	37.6807
5000	7.1325		110.8911		31.9131		37.9713

\* The enthalpy function is divided here by a constant  $RT_0$  where  $T_0 = 273.16^\circ\text{K}$  ( $491.688^\circ\text{R}$ ).