Effects of Fuels/Contaminants on Reforming Catalyst Performance and Durability

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> > presented at

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Program Objectives

- Investigate differences in reforming of gasoline components to
 - identify problem compounds
 - identify beneficial compounds
- Evaluate the effects of fuel constituents and impurities (sulfur) on catalyst stability

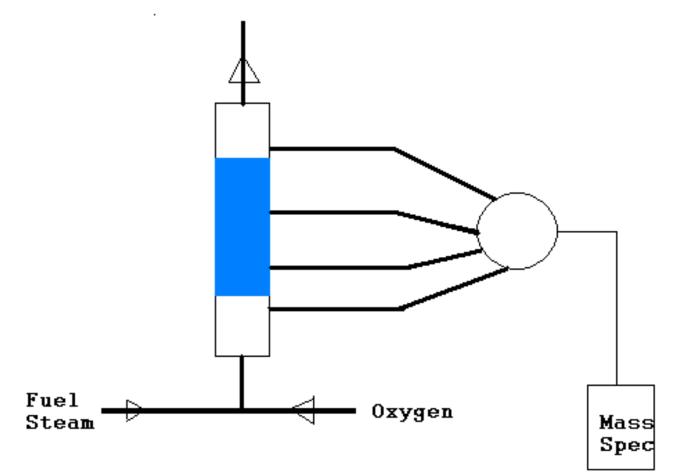
Experimental Approach

- Determine product gas composition dependence on temperature, space velocity
 - test major fuel components individually
 - test minor components, additives, and impurities as isooctane solutions
- Long-term testing (1000h)

- determine poisoning, long-term degradation effects

The short-term test reactor is capable of sampling at various points

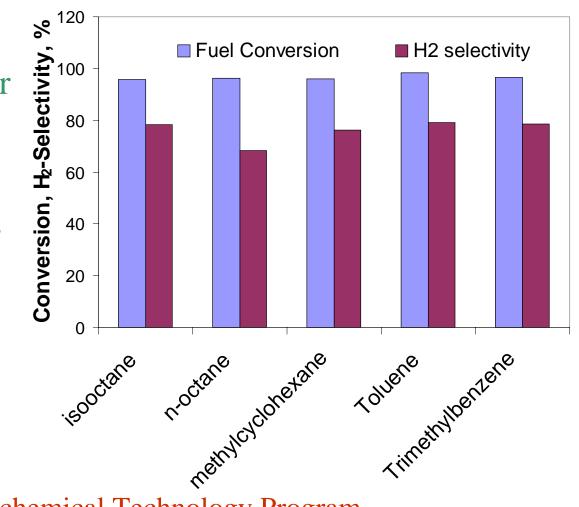
Schematic Diagram of Short Term Test Reactor



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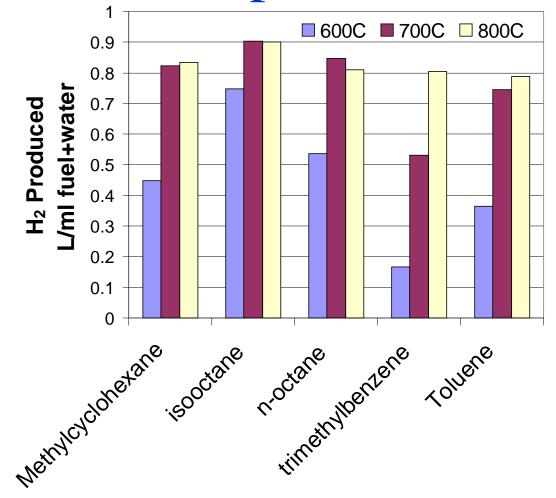
ATR unit can reform all major gasoline substituents at 800°C

- Conversion of all major substituents is >95%
- Hydrogen selectivity is lower for n-octane

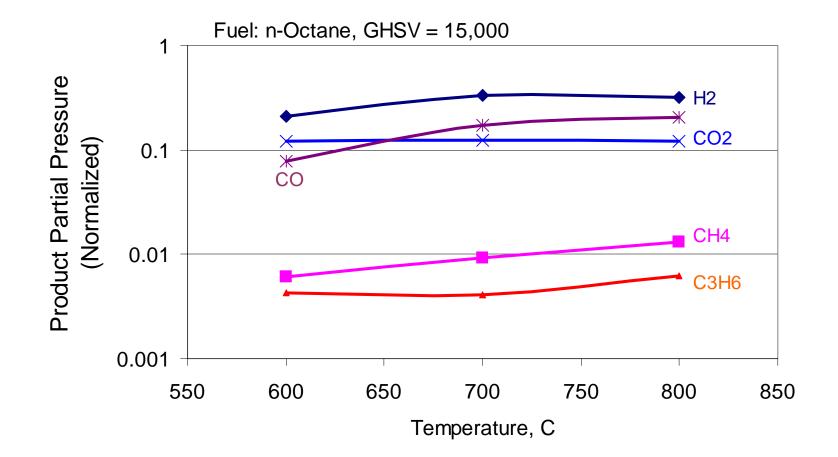


H₂ yield from trimethylbenzene is most sensitive to temperature

- Trimethylbenzene must be reformed at high temperature
- Isooctane reforms better than other components at low temperature



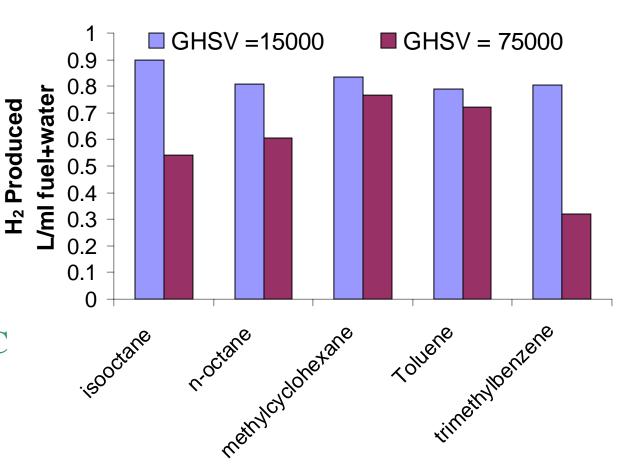
H₂ selectivity from n-octane decreases with increasing temperature



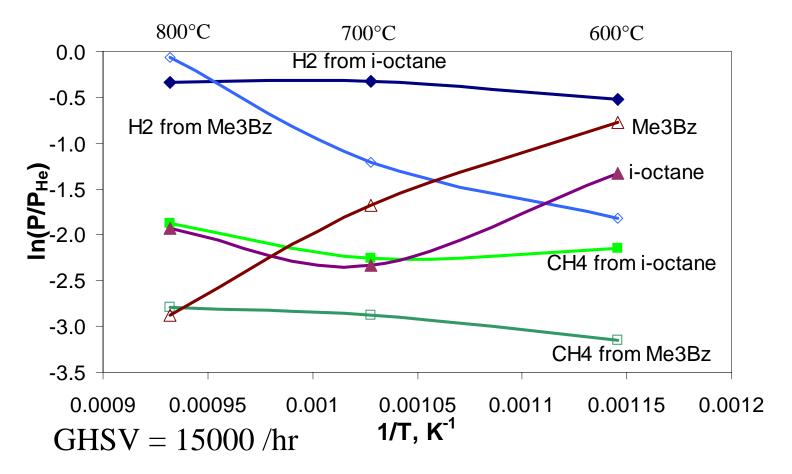
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Hydrogen yield is highest from branched paraffins at low space velocities

- Rate of reforming of trimethylbenzene appears to be slower than that for other components
- methylcyclohexane and toluene appear to react rapidly at 800°C



Trimethylbenzene reforming decreases rapidly with decreasing temperature



Autothermal reforming of major gasoline components have been studied

- All major substituents can be reformed at 800°C
- Trimethylbenzene reforming requires high temperatures and low space velocities
- Methylcyclohexane and toluene can be reformed at high space velocity at 800°C
- Isooctane reforms better than other components at low temperature

Sulfur impurities increased hydrogen yield from ANL catalysts

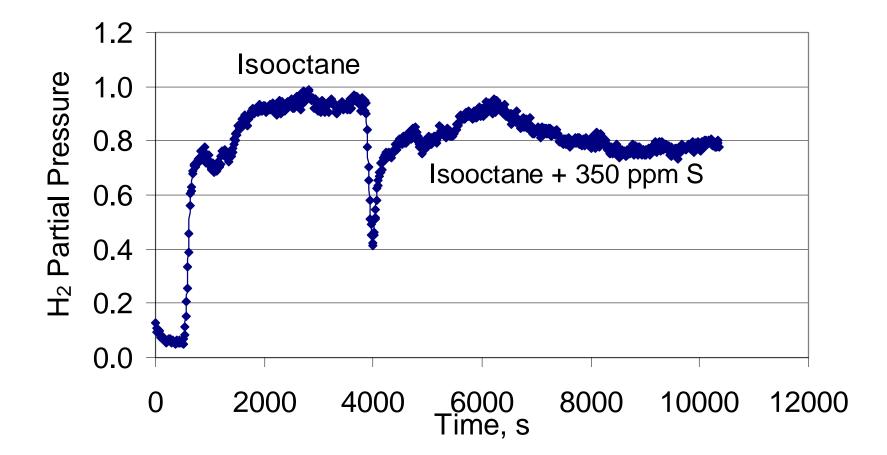
800C, GHSV = 15,000 /hr 60 ANL1 isooctane+1000 wppmS ANL1 pure isooctane 50 ANL2 isooctane+300 wppmS **Gas Composition** % dry, He Free 40 ANL2 pure isooctane 30 20 10 0 %CO %CH4 %CO2 %H2 **Product Gas**

Some sulfur remains on the catalyst

Sulfur in Fuel (wppm)	S on catalyst after reaction (wt.%)
300	0.02
1000	0.04

• Sulfur found in reformate gas as H₂S

Short term tests with sulfur containing fuels show some loss in activity of Ni ATR catalyst



Sulfur containing fuel showed 5% loss in H₂ yield after 1700 hrs

• 750-790°C 45 48h 50ppmS • GHSV= 5169/h40 48h no S Composition (% dry • Benchmark Fuel + S 35 1700h 50 ppm S – (50 wppm) 1000 h no S 30 • 1700h 25 **Results** 20 • No decline in CO_x 15 Gas • ~5% decline in H_2 10 • H₂ selectivity: 88-85% 5 - (40-38% H₂ dry) 0 • More H₂ from fuels with %CO %H2 %CO2 **Product Gas Composition** sulfur

Effects of S impurities are dependent on catalyst

- Sulfur improved hydrogen production from Pt-containing ATR catalyst
- Sulfur poisoned Ni-containing ATR catalyst
- Long-term tests with S impurities indicate little degradation of Argonne Catalyst

Future Work

- Investigate sulfur effects further
 - Sulfur XANES investigation of catalyst at University of Louisiana
 - Investigate kinetics of sulfur effects
- Investigate effects of additives
- Continue collaboration with petroleum companies on future fuel-cell gasoline
- Synergistic effects

Conclusions

- Trimethylbenzene is undesirable in a fuel cell gasoline
 - has lower hydrogen density, requires high temperature, long contact times
- Sulfur effects are dependent on catalyst
 - improves H₂ production from Pt-containing ANL catalyst

Industry Collaborations

• Syntroleum

Evaluated reformability of Fischer-Tropsch fuels

[S. Ahmed, J.P. Kopasz, B.J. Russell, H.L. Tomlinson Proceedings of the 3rd International Fuel Cell Conference, Nagoya, Japan, 1999]

- UOP, BP-Amoco, Exxon-Mobil
 - Continuing discussions on fuel chemistry, future fuels for fuel cells

Responses to Previous Reviewers

- Several reviewers indicated need for further interaction with petroleum industry
 - We now interact with BP-Amoco, Exxon-Mobil, Syntroleum, and UOP on fuels issues
- Too much emphasis on fuels analysis
 - Fuels analyses were needed to identify principal gasoline constituents for current work

Timeline/Milestones

- Program initiated 5/99
- Completed first 1000h test 9/99
- Recommended reference benchmark fuel 10/99
- Completed second long-term test reactor 2/00
- Tests completed on 5 gasoline components 4/00

Timeline/Milestones

- Define alternative fuel blend(s) as standard reformer "gasoline(s)" -7/00
- Test 3 major gasoline additives -7/00
- Complete 1000h tests on four catalysts -7/00
- Identify problem contaminants and constituents in FTP gasoline 9/00