# Microchannel Fuel Processing for Man Portable Power



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# Small Power Systems: Impact on National Security

LAND WARRIOR SOLDIER POWER

| Goals   |            |
|---------|------------|
| 2003    | 270-Wh/kg  |
| 2005    | 1450-Wh/kg |
| 2008    | 3100-Wh/kg |
| 2018-25 | 5900-Wh/kg |

Source: Land Warrior ORD (3 Aug 99), KPP





# Soldier Power: Current Battery Power Sources

| Model      | Туре              | Chemistry          | Gravimetric<br>Energy Density<br>(Whr/kg) | Volumetric<br>Energy Density<br>(Whr/liter) |
|------------|-------------------|--------------------|---|---|
| BA-5847B/U | Primary           | LiSO <sub>2</sub>  | 121                                       | 41  |
| BB-2847/U  | Rechargeable      | Li-Ion             | 68  | 32  |
| BA-x847A/U | Primary (2-Cell)  | LiMnO <sub>2</sub> | 226                                       | 87  |
| Day Pack   | Primary (15-Cell) | LiMnO <sub>2</sub> | 308                                       | 107   |
| Ammo Pack  | Primary (5-Cell)  | LiMnO <sub>2</sub> | TBD                                       | TBD   |

Current battery technology is insufficient for Land Warrior System by 2005!

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# What Energy Source?

|                  | Energy Storage Density |
|------------------|------------------------|
| Energy Source    | (kW-hr/kg)             |
| Diesel           | 13.2                   |
| Advance Battery  | 0.2 - 0.3              |
| Hydrogen Storage |                        |
| Compressed       | 1.0                    |
| Metal Hydride    | 0.5                    |

Conclusion - Liquid hydrocarbon fuels are decisively superior to other energy storage options



# Microchannel Fuel Processing for Fuel Cell Power Systems

**Battery replacement for long duration missions** 



CO2

H2\* Fuel Cell

FP/FC Energy Density:  $2,000 - 4,000 \text{ Wh}_{e}/\text{kg}$ Batteries:  $200 - 300 \text{ Wh}_{e}/\text{kg}$ 



Environmental Measurements 0.01- to 100-W<sub>e</sub> **Battelle** 



Laptops 50 - W<sub>e</sub> Automotive 50-kW<sub>e</sub> U.S. Department of Energy Pacific Northwest National Laboratory

# **Overview**

- Why microtechnology?
- Fuel Processor
  - Conceptual flowsheet
  - Demonstrated components
- Man Portable Power
  - Concept
  - Status



# Why Microtechnology?

### Microscale Advantage

- Reduce *heat transfer* resistance
- Reduce mass transfer resistance

### Component efficiency

- Microtechnology ~ 90% or better
- Conventional technology < microtechnology</li>

### ■ Fuel Processor size (50 kW<sub>e</sub> - Automotive application)

- Microchannel reactor ~ 8 Liters
- Conventional ~ 10x to 100x larger

#### Compact processes need microtechnology



## **Compact Processes:** Highly effective Heat Transfer

Reduce heat transfer resistance using microchannels



## Microchannel Reactors: Enhanced mass transfer reduces process volume



- Transport distance reduced by several orders of magnitude
- Convective vs diffusive transport brings reactants to catalyst

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### **Compact Water Gas Shift Reactor**

$$\begin{array}{l} \text{CO} + \text{H}_2\text{O} \Rightarrow \text{CO}_2 + \text{H}_2 \ (\text{desired}) \\ \Rightarrow \text{CH}_4, \ \text{C(s)} \ (\text{undesired}) \end{array}$$

Conventional technology:

- $\tau = 1 \sec \theta$
- 300 500 °C

**Compact microtechnology:** •  $\tau = 25$  msec

Patent pending

• 300 - 500 °C



### **Compact Water Gas Shift Reactor**



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# **Compact Steam Reformer**



## **Microchannel Fuel Processing**



### **Microchannel Gasoline Vaporizer:** Compact 50-kW<sub>e</sub> (Automotive) Fuel Processor



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- Attributes: Four parallel cells
- Size: 8 cm by 10 cm by 4 cm
- <u>Capacity</u>: Gasoline (~ 300 mL/min)
- Implications: Complete fuel processor system = 8 Liters
- Fabrication: Laminate process
- Pressure drop: DP < 2psi (through microchannels at ~ 1400 SLPM)</p>

# **Microreactor Development**

# ■ 10-W<sub>e</sub> design for butane reforming and WGS





## Steam Reformer: Automotive Fuel Processor

### Iso-octane steam reforming (gasoline simulant)

- $C_8H_{18} + 8H_2O = 8CO + 17H_2$   $DH_r = 1345 \text{ kJ/mol}$
- $CO + H_2O = CO_2 + H_2$  (some high T shift)
- Undesired side/series reactions:
  - $CO+CO = CO_2 + C(s)$
  - Cracking reactions
  - Methane formation

#### • Conditions (conventional hardware):

- Temperature ~ 800C
- Steam : Carbon ~ 6+
- Residence time > 1 sec



# **Iso-octane Steam Reforming:**

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Initial tests – World's First Microchannel Steam Reformer



## Steam Reformer Summary: Isooctane

### Capacity (cell volume 29 cm<sup>3</sup>)

- Initial experiments: 0.5 to 1.0-kW<sub>e</sub> at 1 atm
- Design point: 5-kW<sub>e</sub> at 5 atm

## Range of test conditions

- Residence time: 1.1 to 2.3 milliseconds
- Steam:carbon : 3:1 to 6:1
- Temperature: 630 to 670 C

## Performance

- Conversion = up to 99%, low 90's typical
- $H_2$  Selectivity = 91 to 99%, with H2 content = 67 to 72%
- No degradation observed after 30 hours and 12 thermal cycles
- Implications:
  - Automotive full-scale SR System (50-kW<sub>e</sub>) ~4L



# **Diesel Catalytic Combustion Tests**





# **Diesel Catalytic Combustion** Duration Testing



No sulfur poisoning/coking observed after 50 hours of operation

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# Man Portable Power: System Concept





# **Status: Man Portable Power**

- Demonstrated feasibility of microchannel fuel reforming
- Demonstrated feasibility of microchannel water gas shift
- Demonstrated vaporizers and recuperative heat exchangers

