

# Advances in Microchannel Contactors for Chemical Separations

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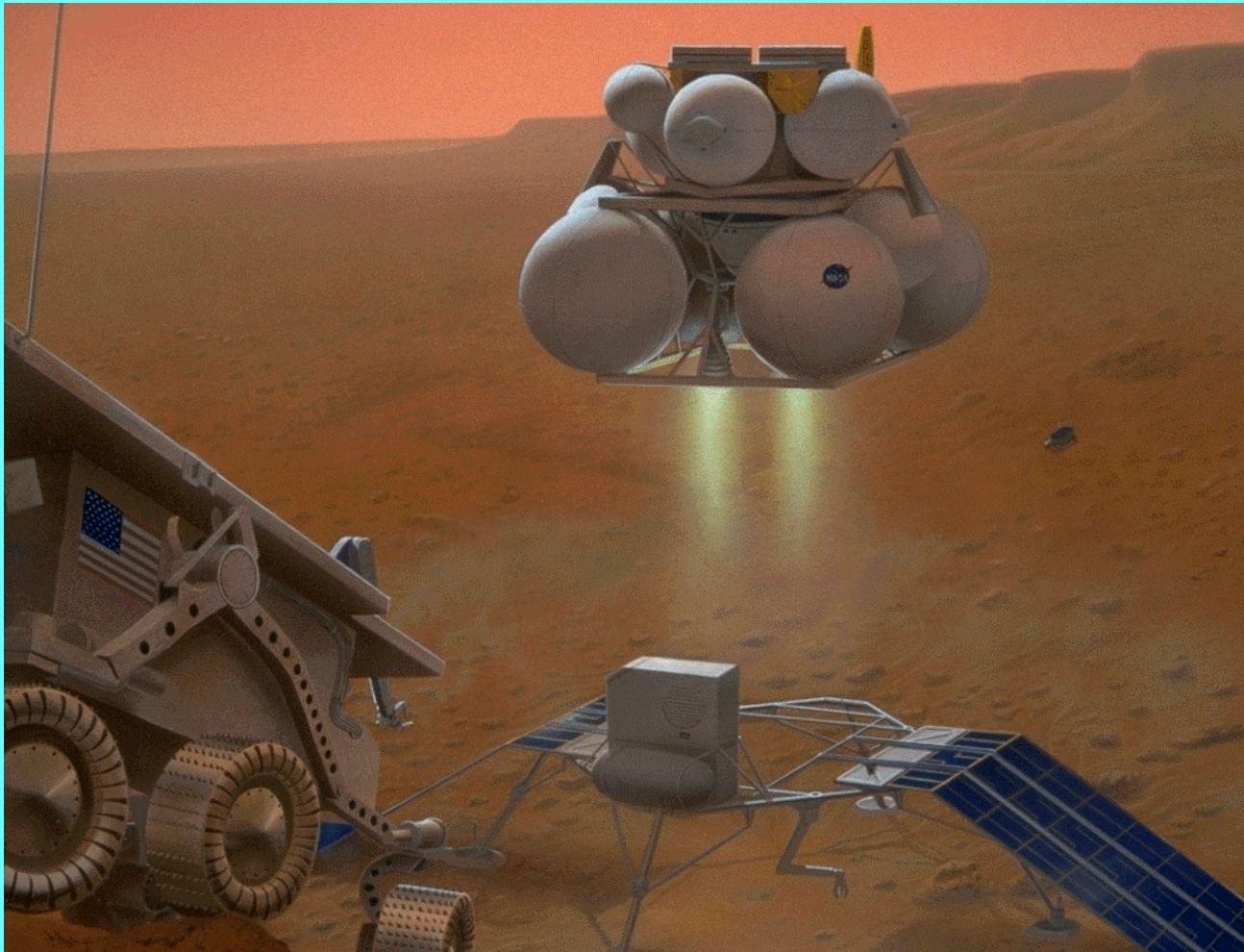
**Battelle**

U.S. Department of Energy  
Pacific Northwest National Laboratory

# Applications

## NASA - In Situ Resource Utilization

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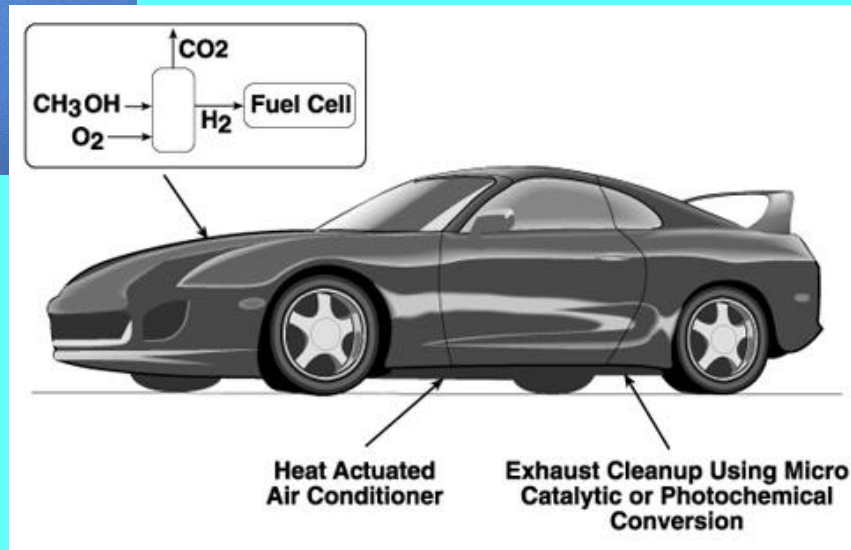
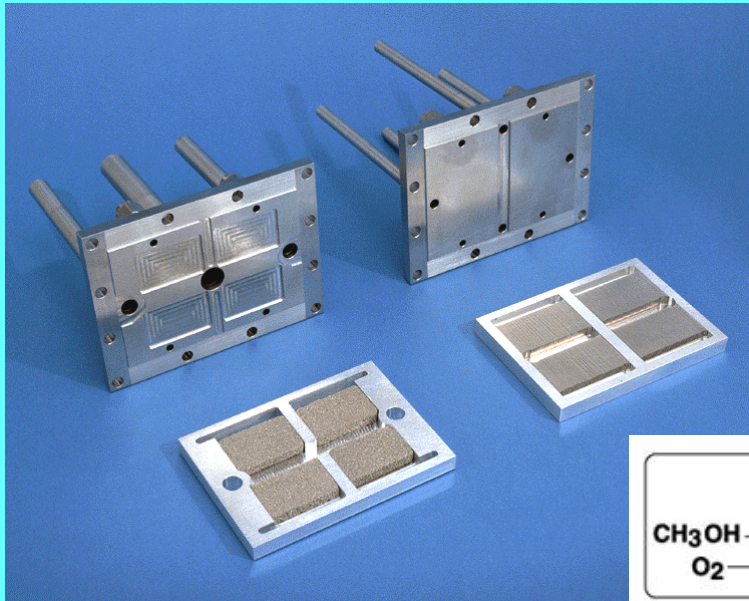
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# Applications

## Onboard Fuel Processing

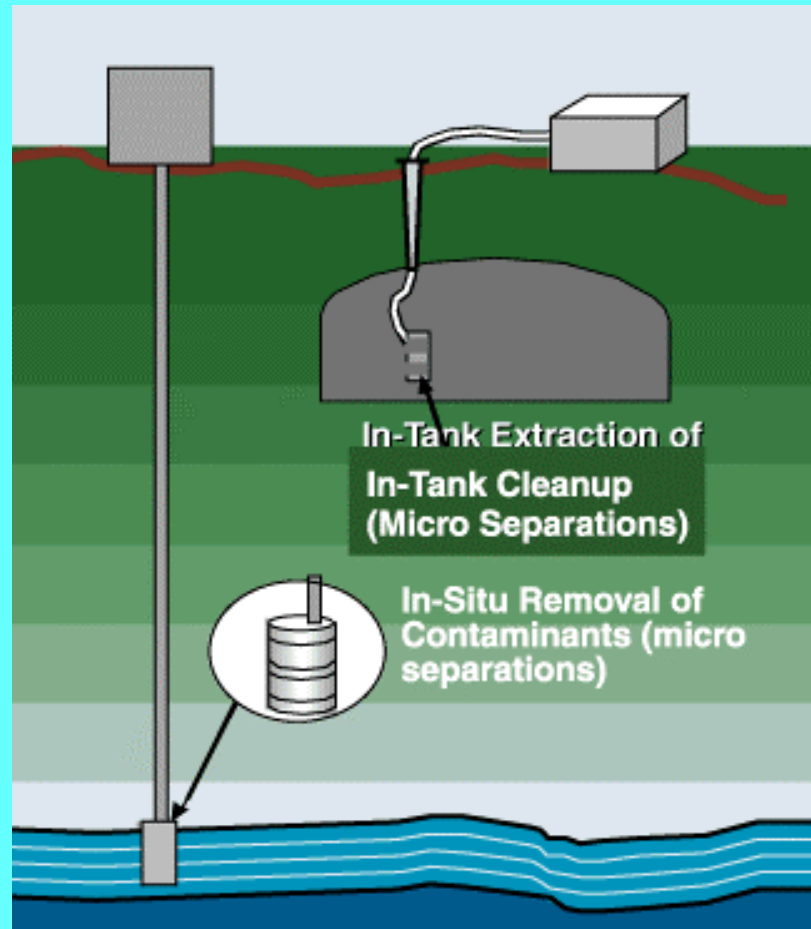
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# Applications

## Waste Processing

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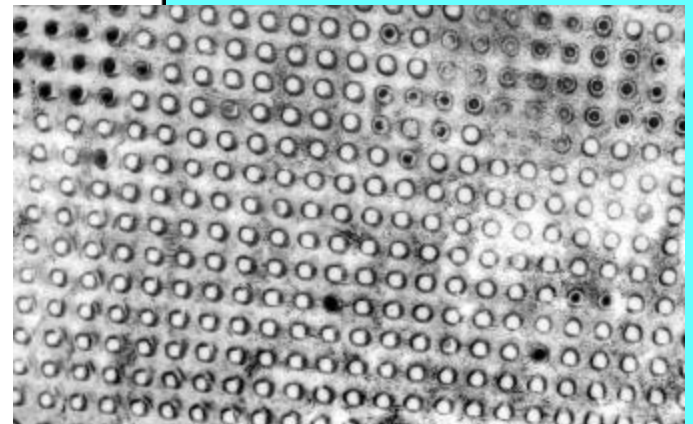
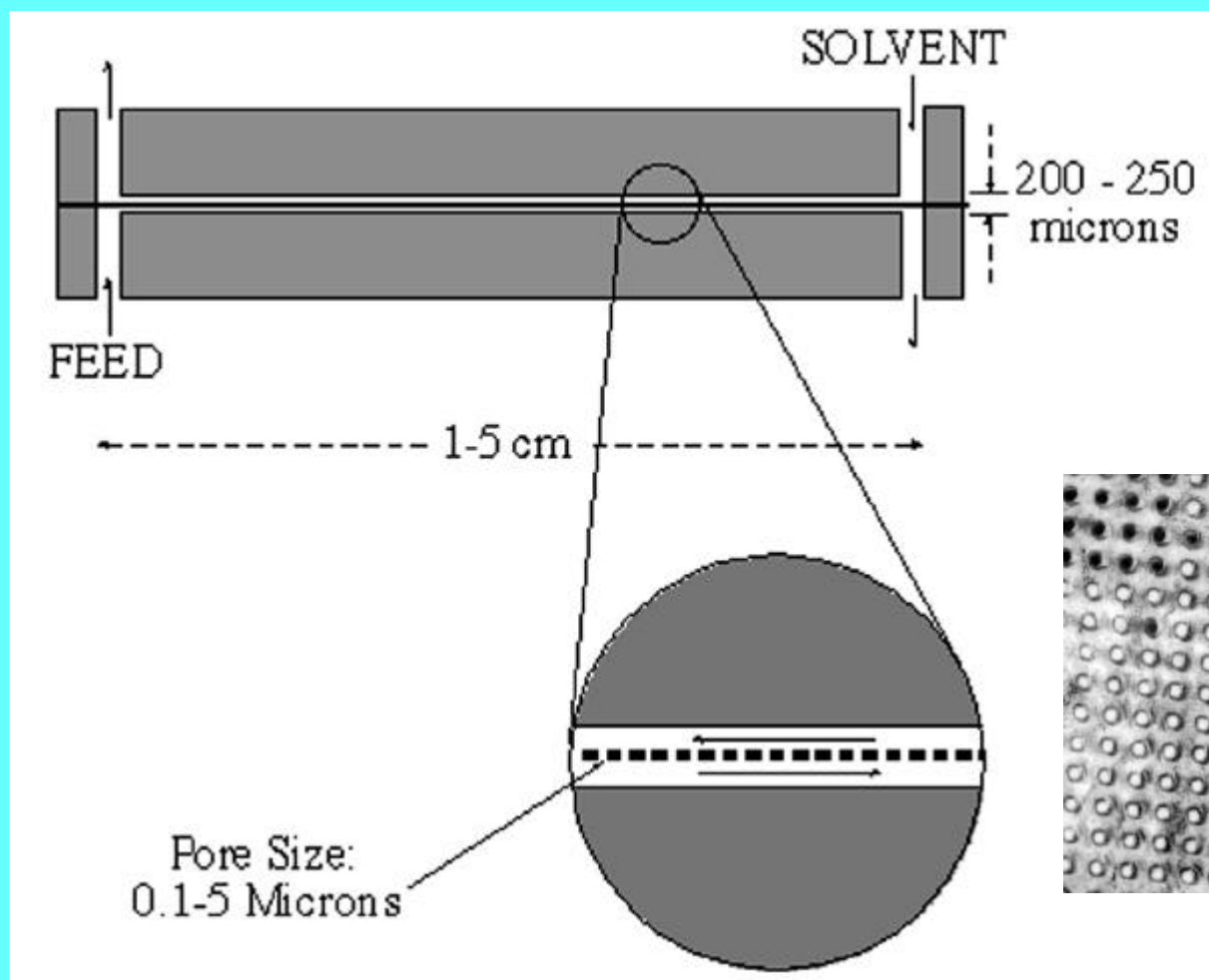
- Microchannel Contactor for Separations

- Hanford Tanks

- Solvent Extraction

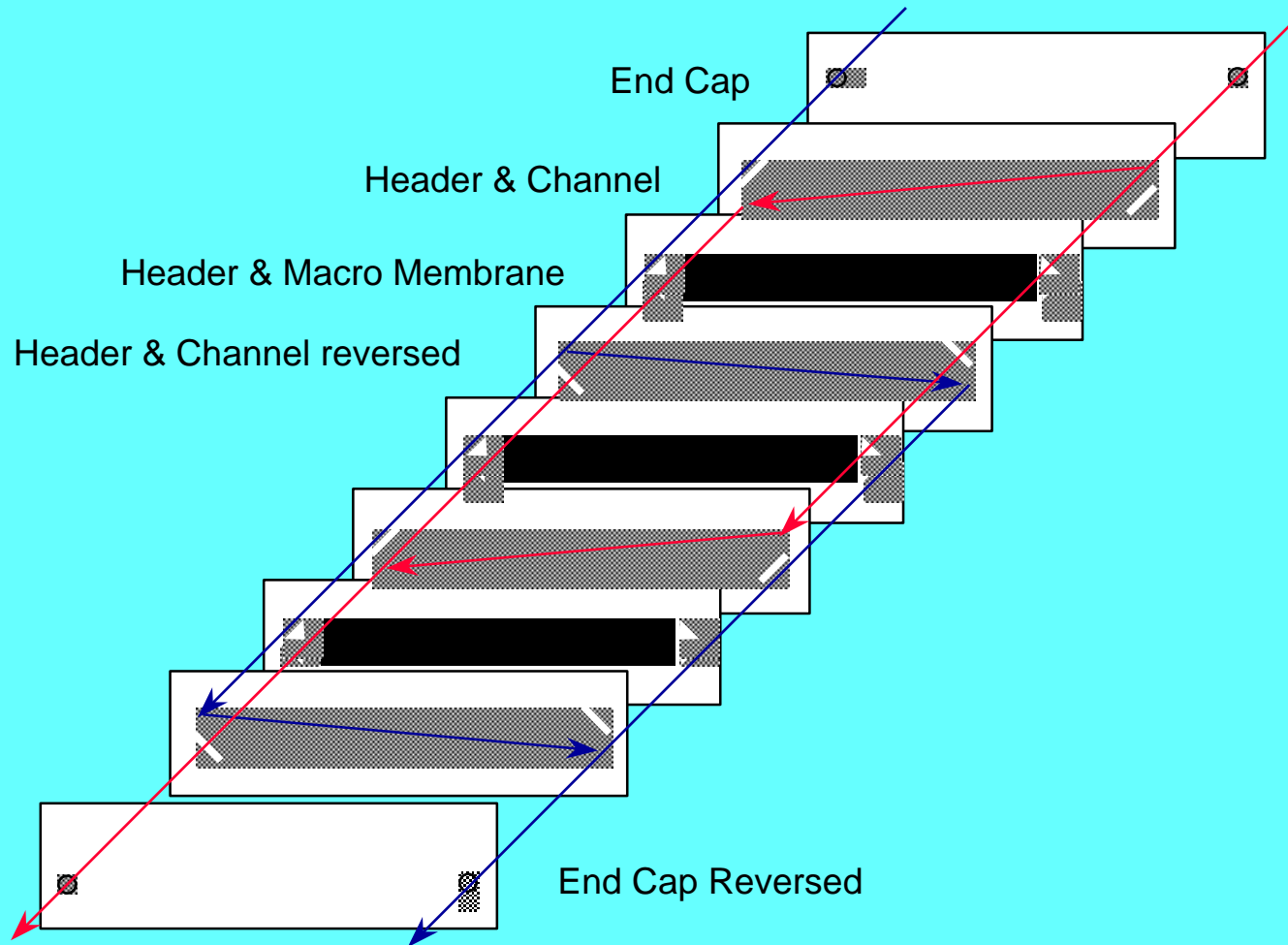
- Summary

# Microchannel Contactor



# Microchannel Architecture

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# Microchemical Processing Advantages

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- High Capacity (throughput per unit hardware volume)
  - Rapid heat transport
  - Rapid mass transport
  - Short residence times
  - Smaller devices to get the job done
- Reduced Capital Cost through Economies of Mass Production
- Compact Size Enables Distributed Processing



# Microcontactor Scaling

- Mass Transfer

$$\frac{1}{Pe_m} = \frac{D_s}{V h} = \frac{w L D_s}{Q h}$$

- Pressure Drop

$$\Delta P \propto \frac{L Q}{w h^3}$$

- Residence Time

$$T_R = \frac{w h L}{Q}$$

- Use constant  $\Delta P$  curves to meet design objectives

<b>h</b>	<b>L</b>	<b>Q</b>	<b><math>\Delta P</math></b>	<b><math>T_R</math></b>	<b><math>1/Pe</math></b>
const	2	1/2	const	4	4
1/2	1/2	1/4	const	const	1/2
1/2	1/4	1/2	const	1/2	const

# Microcontactor Design Approach

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- Design Objectives - Counter-Current Continuous Process
  - Achieve a given number of theoretical stages
  - Minimize size -- Residence time / Number of stages
  - $\Delta P$  Constraint to prevent breakthrough
- Test-case - Acetone Extraction from Water Using 1,1,2-TCA
  - Equilibrium distribution coefficient,  $m_S = C_S/C_R = 2.1$
  - Solvent to feed flow ratio,  $Q_S/Q_F = 0.475$
  - Two contactors
    - 25-micron thick, 26% porosity
    - 10-micron thick, 40% porosity

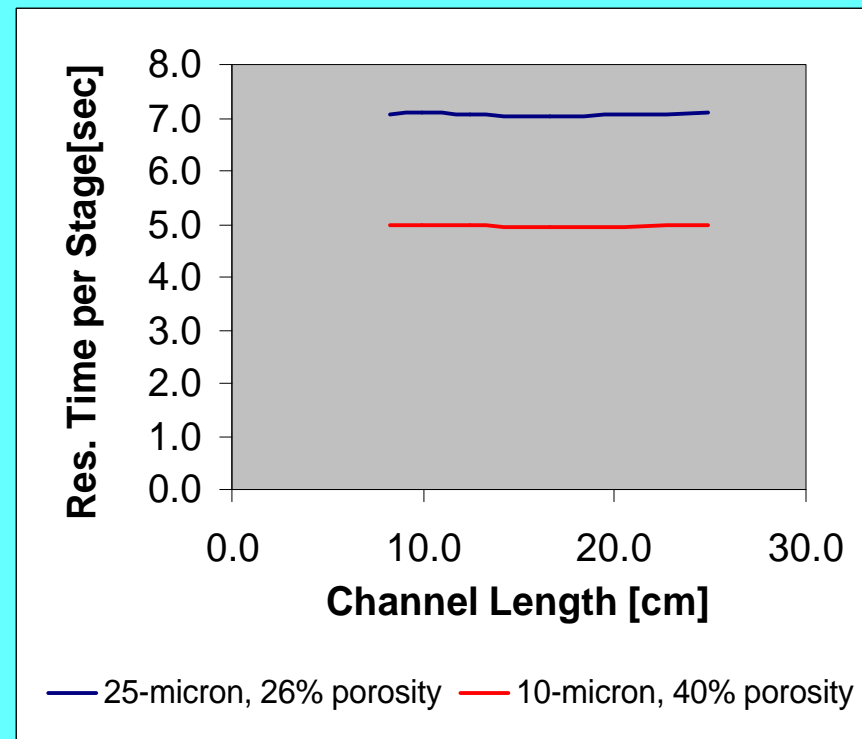
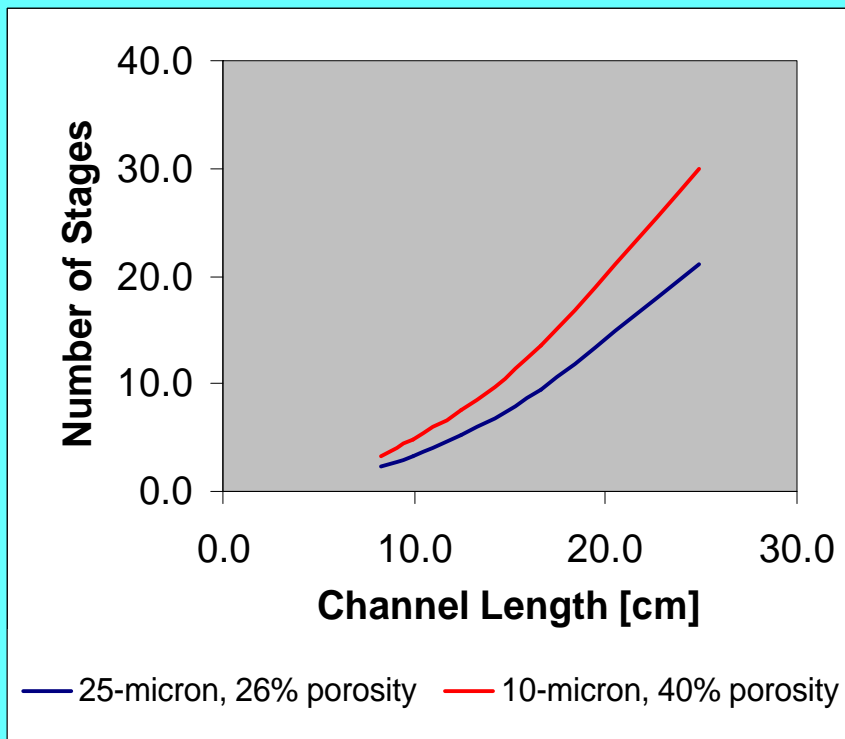
# STEP 1

## Locate Design Point to Accomplish Separation

Constant  $\Delta P = 2$  inches W.C.

Constant channel height = 100 microns

Vary flow rate and channel length inverse proportionally



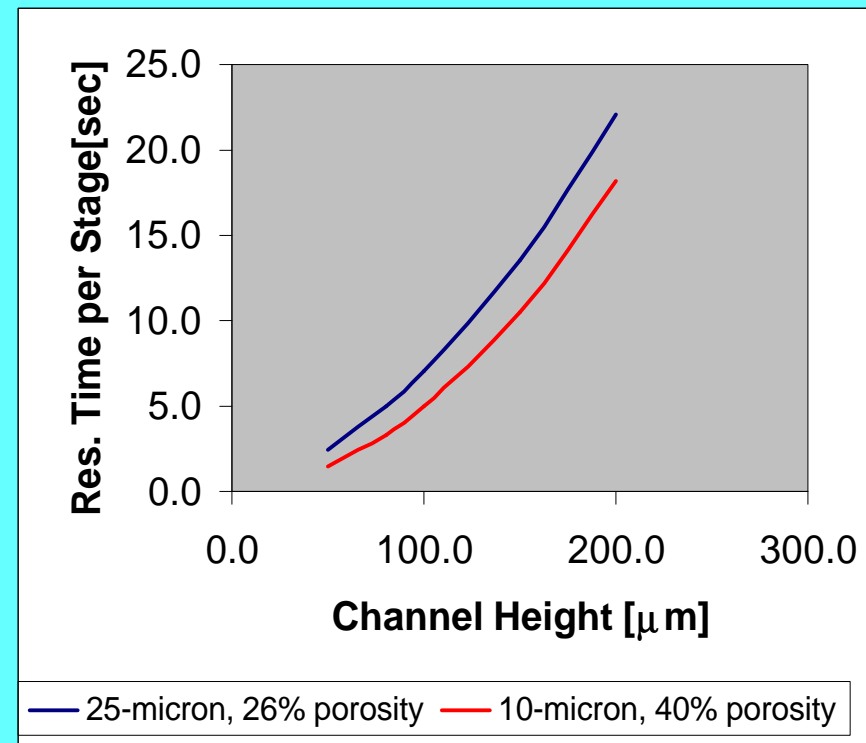
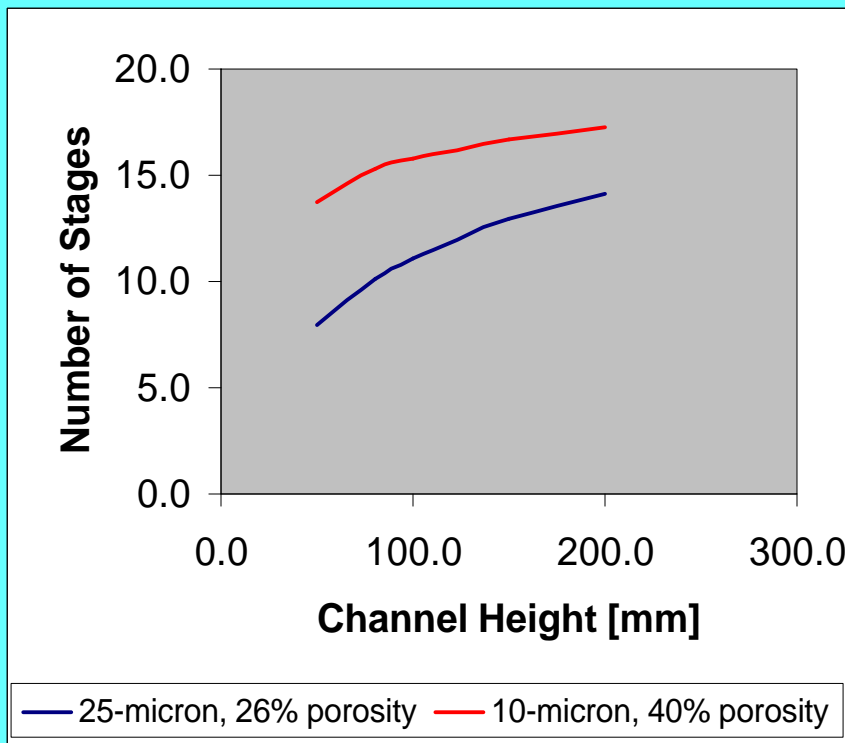
# STEP 2

## Miniaturize Architecture

Constant  $\Delta P = 2$  inches W.C.

Constant Peclet Number

Vary channel height, square root of length, and flow rate proportionally



# How Small?

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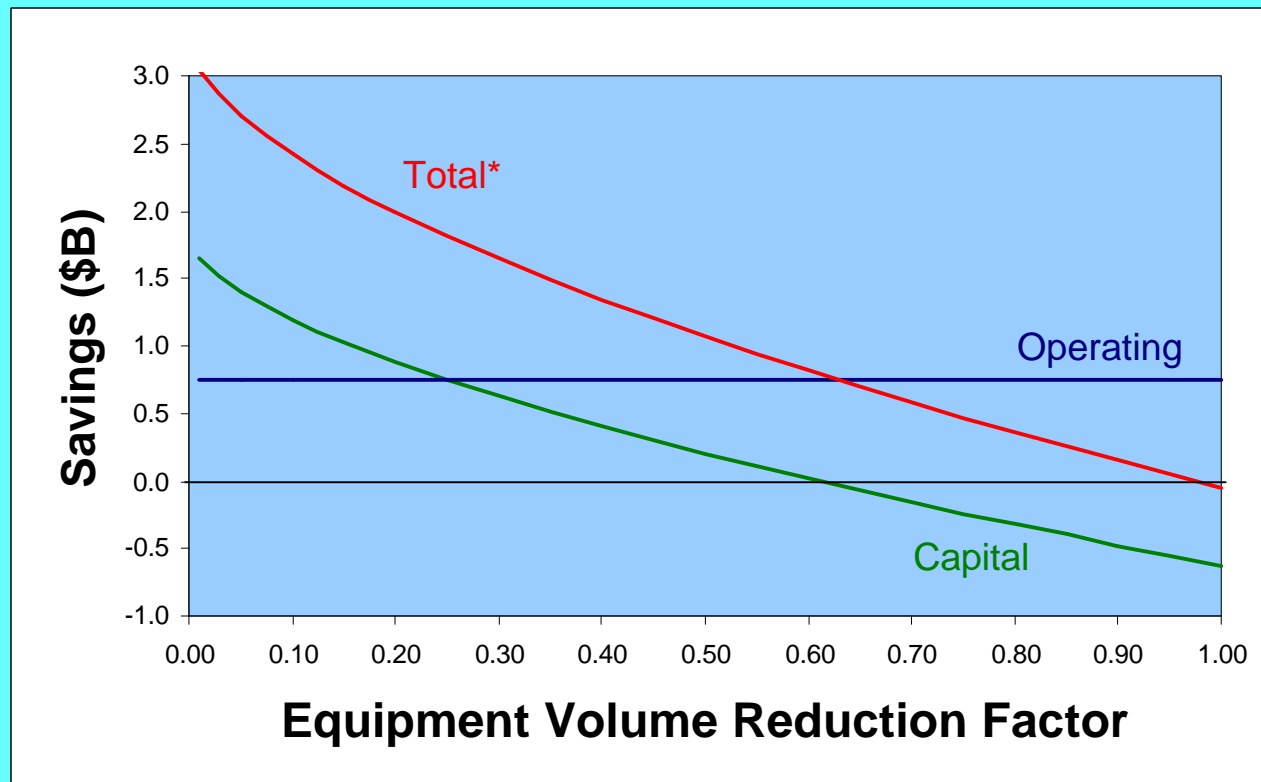
- Progress Toward 1 Second Residence Times per Theoretical Stage
- Acetone Extraction Using 1,1,2-TCA or Toluene:

	Capacity	HETP	T <sub>res</sub> /Stage
	[cm <sup>3</sup> /cm <sup>2</sup> /s]	[cm]	[sec]
Sieve Trays	1	100-250	100-250
Structured Packings	0.8-5	20-180	10-80
Microchannels	0.2	0.25-5	1-20

- Order of Magnitude or More Reduction in Hardware Volume

# Hanford Tank Remediation System Study: Process Intensification with Process Miniaturization

## Cost Savings Relative to TWRS Baseline



\* Total Costs not sum of Operating and Capital; includes fixed and decontamination

# Solvent Extraction

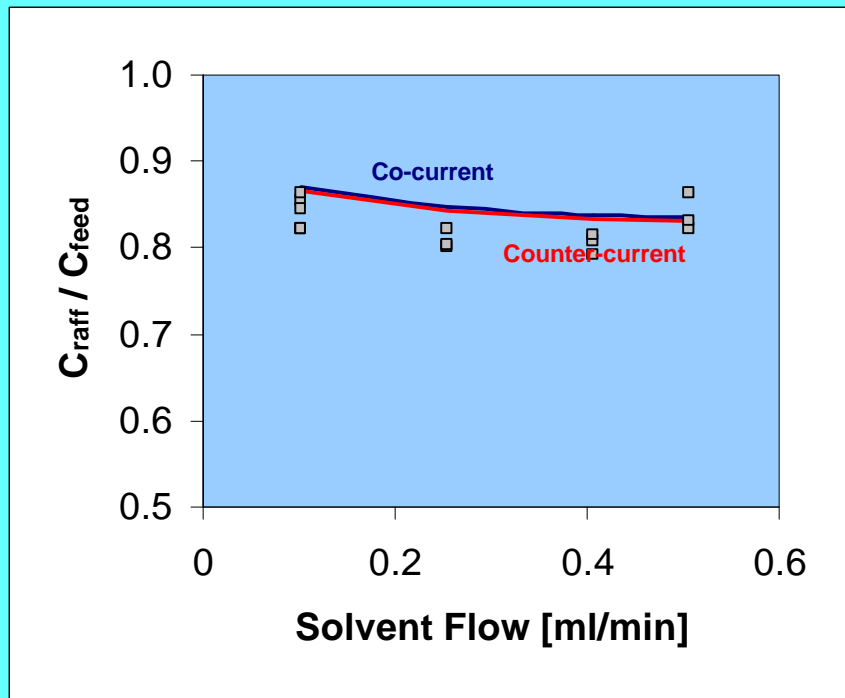
Counter-current

Cyclohexanol extraction from water

Cyclohexane solvent

250-micron channels, 180-micron contactor

Constant feed residence time of 24 seconds



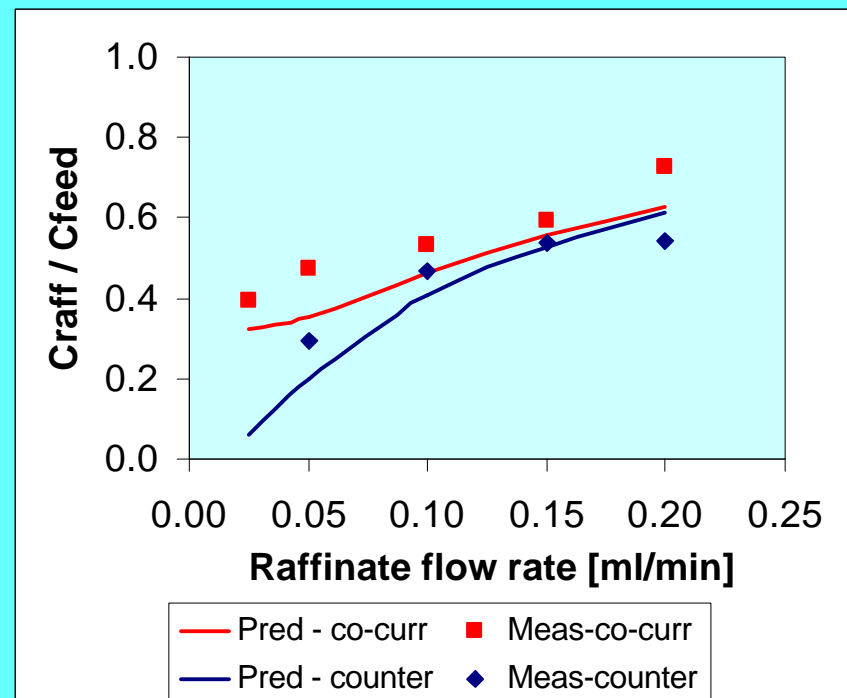
Counter-current

Acetone extraction from water

1,1,2-trichloroethane solvent

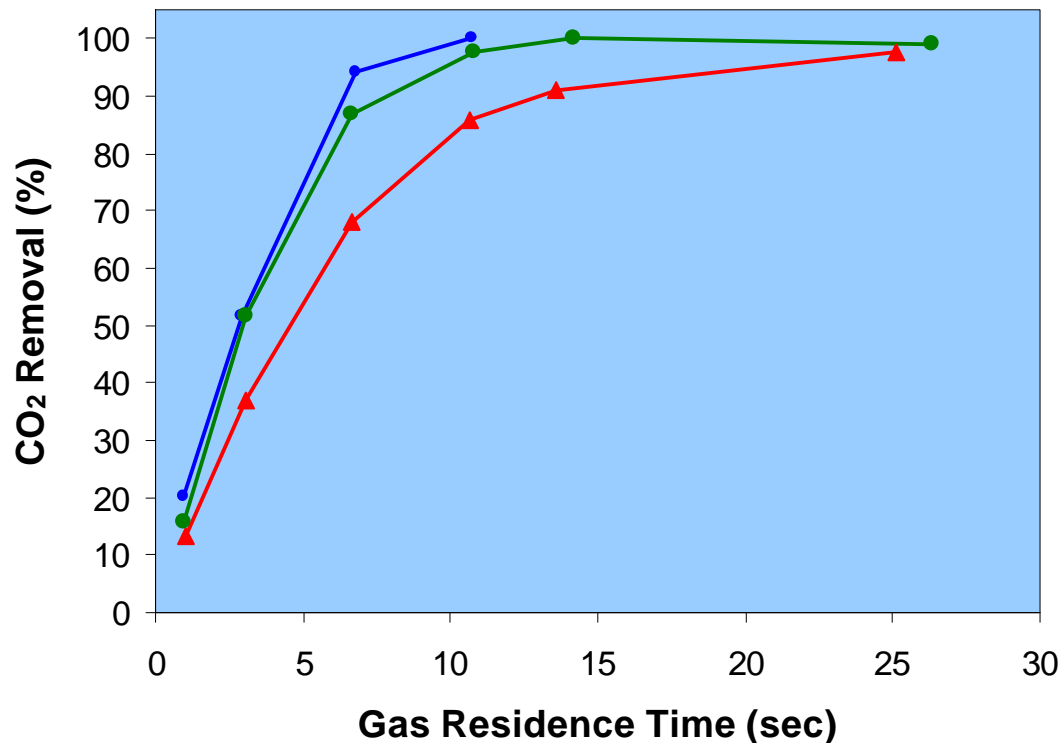
240-micron channels, 180-micron contactor

Solvent and raffinate at equal flow rates



# Gas Absorption

## CO<sub>2</sub> Absorption with DEA Solvent



—●— 20% DEA Solution —▲— 10% DEA Solution —●— 40% DEA Solution

Cocurrent flow through 400-micron channels at 26 sec solvent residence time

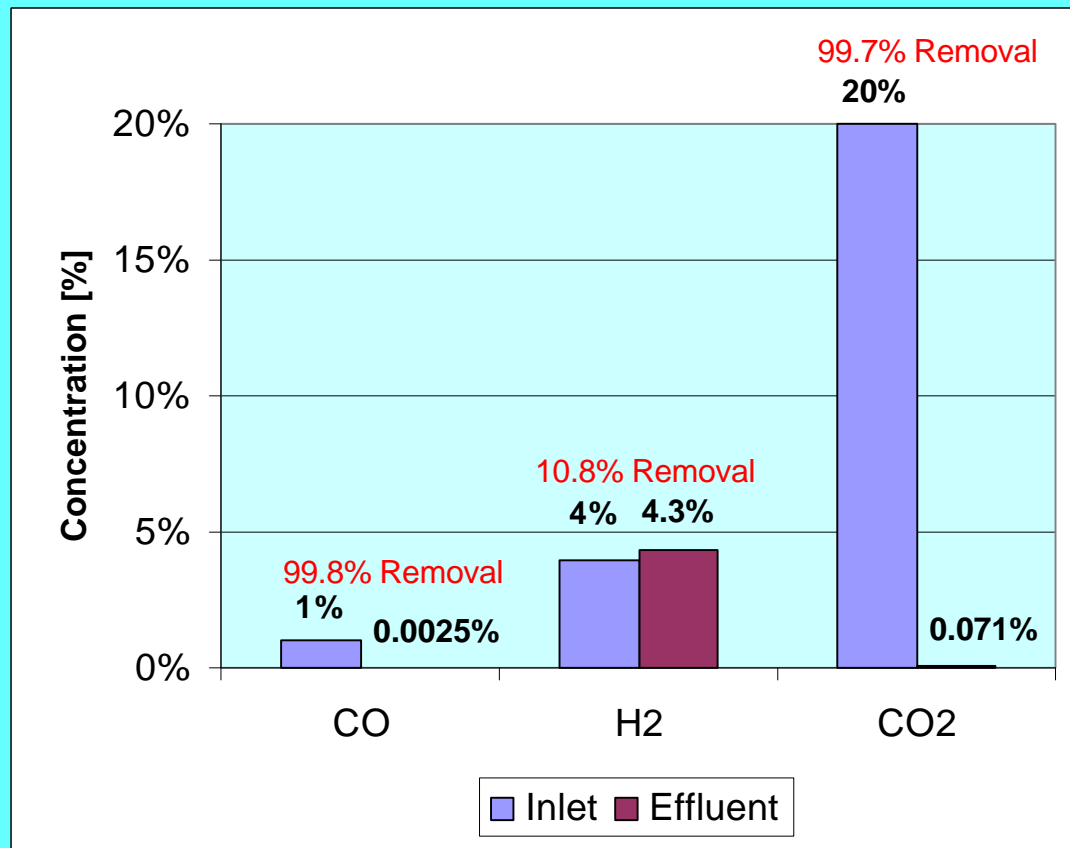
- DEA solvent
- 25% CO<sub>2</sub> and 75% N<sub>2</sub>
- Applications:
  - NASA Mars ISRU
  - Carbon management



# Gas Absorption

## CO Absorption with Copper Ammonia Formate Solvent

Gas residence time = 1.3 sec



Countercurrent flow through 250-micron channels at 36 sec solvent residence time with Teflon membrane

- Copper Ammonia Formate
- 1%CO, % H<sub>2</sub>, 20% CO<sub>2</sub>, 75% N<sub>2</sub>
- Application:
  - Fuel cell feed gas clean-up

# Summary

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- Residence time per theoretical stage is approaching 1 second for chemical separations.
- Microchannel devices have potential for orders of magnitude reduction in hardware volume over conventional technology.
- Microchannel based separations are penetrating markets where size and weight matter.