

# REDUCING NO<sub>x</sub> AND LOI AT THE ST. JOHNS RIVER POWER PARK

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- Introduction
- Description of ABT Opti-Flow™ Fuel Injector
- CFD Modeling
- Post-Retrofit Results
- Summary

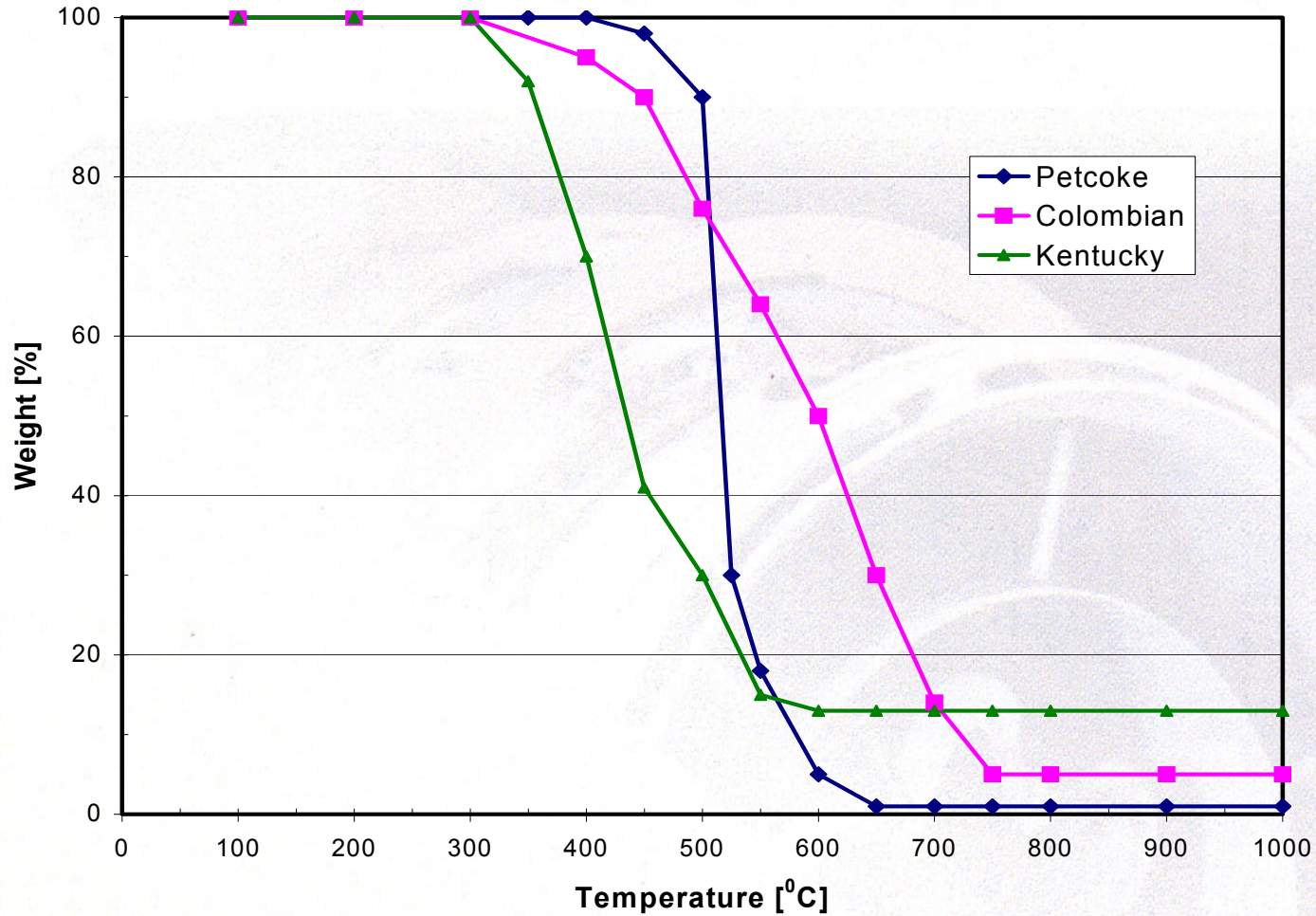
# St. Johns 1 and 2: 670 MW Opposed-Fired

- Fuel: Hard to burn 20% petcoke/  
80% Colombian coal blend
  
- Requirements:
  - » NO<sub>x</sub> guarantee: 0.40 lb/10<sup>6</sup> Btu (*Current limit is 0.5*)
  - » CO: <200 ppm
  - » LOI: <Baseline
  - » Flame stability: Improved turndown
  
- Combustion Modifications: Unit 2 – 8 Mark I low NO<sub>x</sub> fuel injectors\*  
Unit 1 – 28 Mark II low NO<sub>x</sub> fuel injectors\*  
*\* Existing dual registers re-used with modifications*  
Windbox/SA duct modifications
  
- Installation Completed: Unit 2 – March 2002  
Unit 1 – March 2003

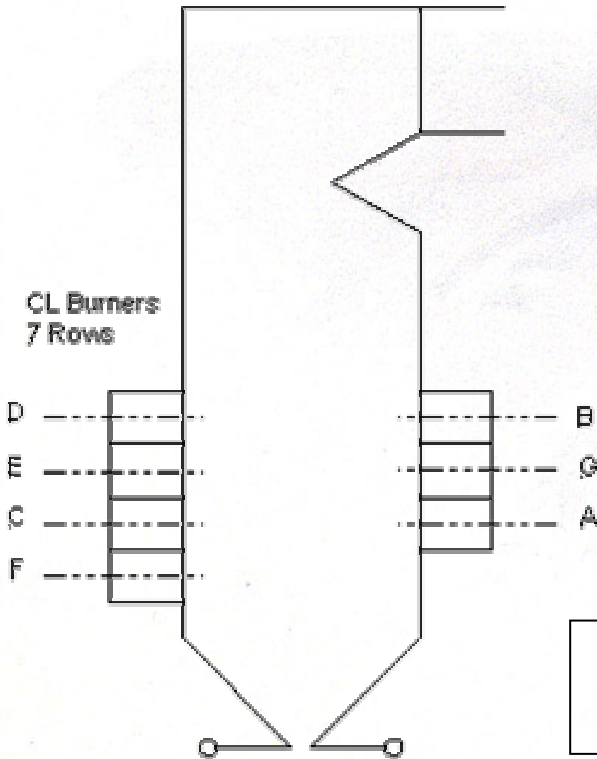
# Fuel Blend Analyses

	Coke	Coal	20/80 Blend
<i>Proximate Analysis (wt%, ar)</i>			
Fixed Carbon	83.92	47.60	<b>54.87</b>
Volatile Matter	8.50	33.40	<b>28.42</b> 1.93 FC/VM
Ash	0.52	7.40	6.02
Moisture	7.06	11.60	10.69
<i>Ultimate Analysis (wt%, ar)</i>			
Carbon	82.22	66.54	69.67
Hydrogen	3.35	4.50	4.28
Oxygen	0.00	7.99	6.40
Nitrogen	1.71	1.32	<b>1.40</b> 1.14 lb/10 <sup>6</sup>
Sulfur	5.14	0.65	1.54
HHV, Btu/lb	14,200	11,800	12,280

# TGA Burning Profiles of Fuels



# St Johns Firing Configuration



- 28 OEM Dual Register Low NO<sub>x</sub> Burners
- 7 Vertical Mills
- 22" O.D. Coal Pipes

**Normal operation with D-Mill out of service  
and SA registers open for simulated OFA**

# St. Johns Pre-Retrofit Conditions:

## Normal Operation with D-Mill Out of Service

	<u>Unit 1</u>	<u>Unit 2</u>
NO <sub>x</sub> , lb/10 <sup>6</sup> Btu	0.46	0.46
CO, ppm	250 - 300	>500
LOI, %	25 – 30	30 – 40

- SA maldistribution: Very high air flow to D-Mill row
- Turndown: Limited to 30% with one mill out of service
- Sidewall corrosion: Localized reducing conditions
- Slagging: Upper furnace slag falls damaged hopper

1. Minimize burner-to-burner stoichiometry imbalance by:
  - » Minimizing imbalances between coal pipes
  - » Equalizing secondary air distribution to burners
2. Maintain good coal fineness for the specific fuel blend
3. Prevent coal roping leaving the burner nozzle
4. Burner must attain a stable, bright flame commencing in the throat.

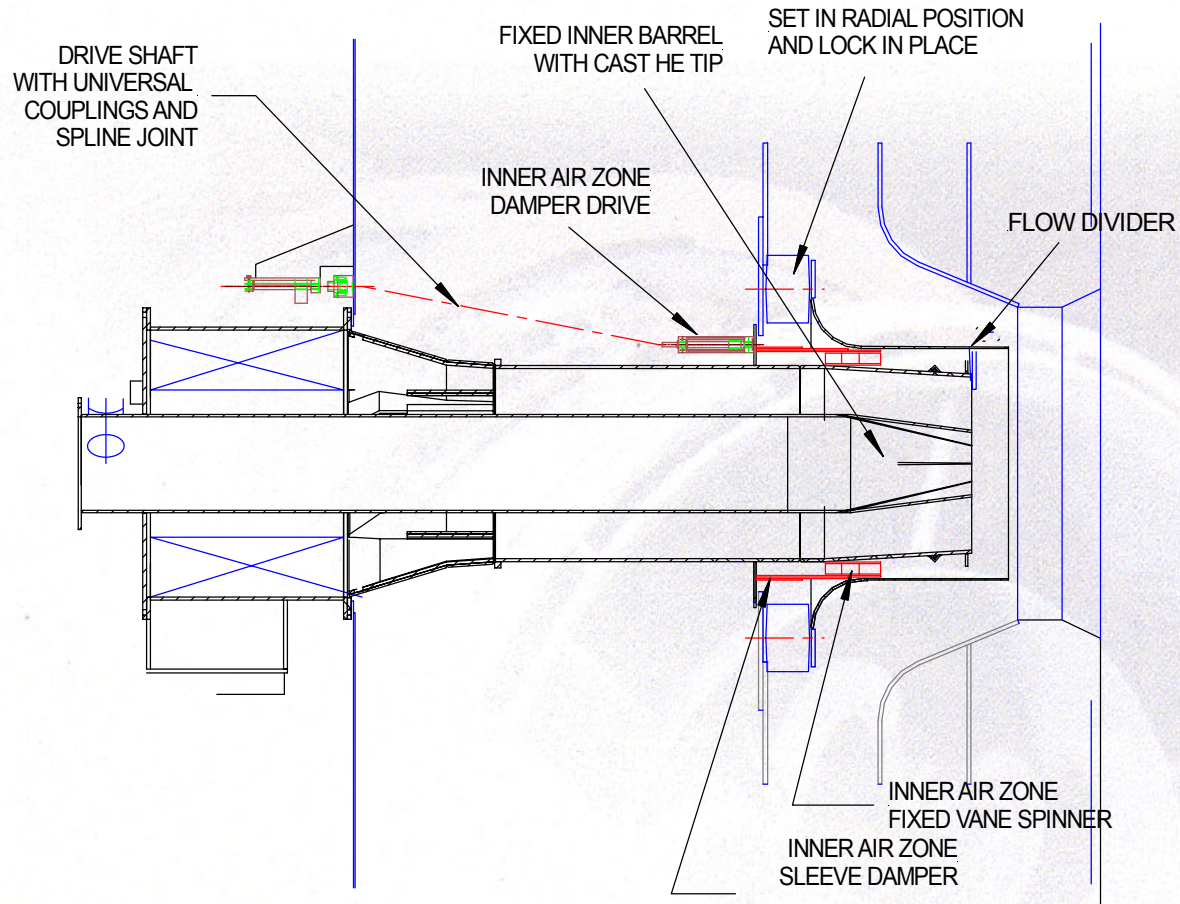


# OPTI-FLOW™ FUEL INJECTOR

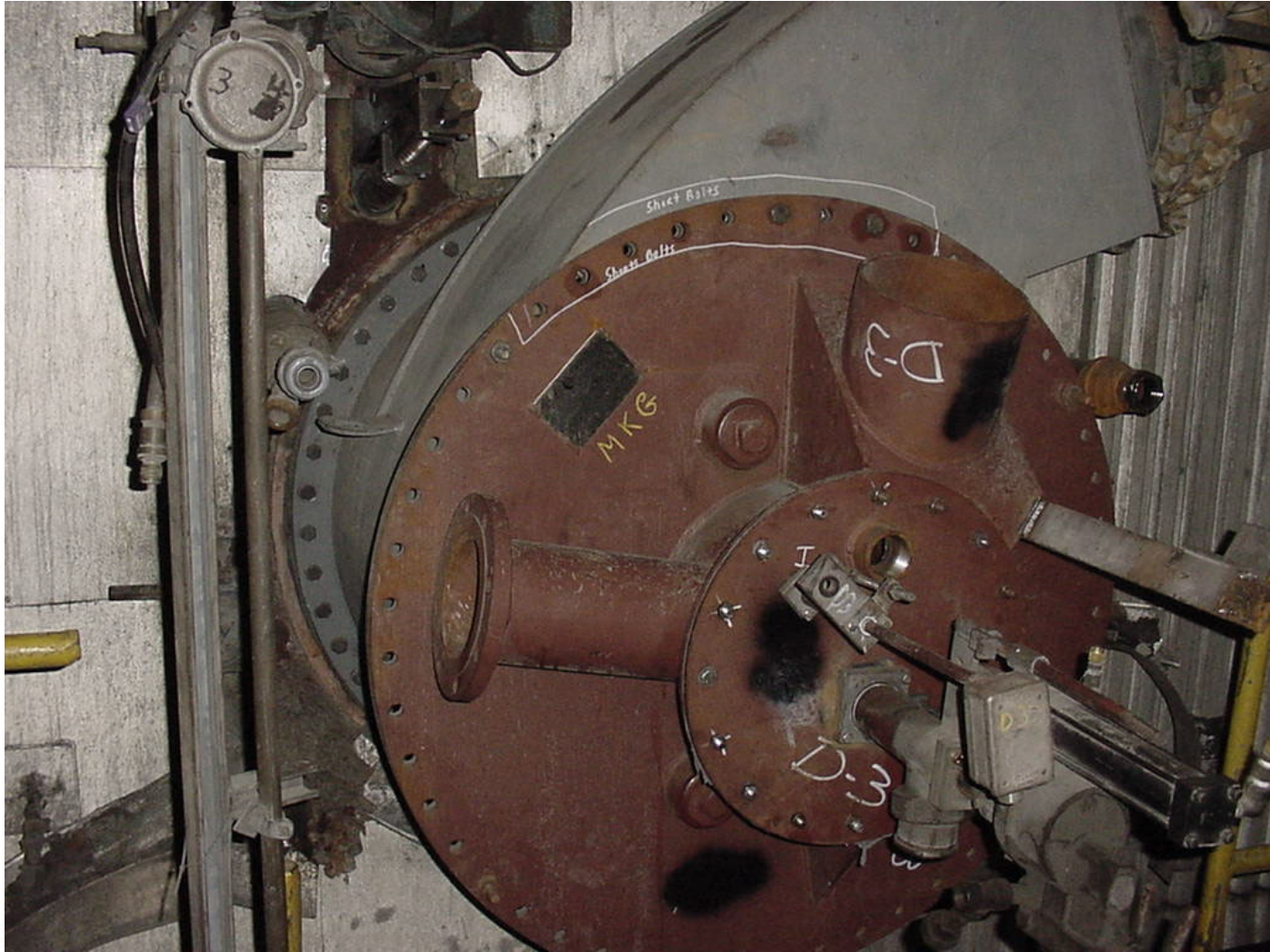
1. Burner Stoichiometry Control:
  - » Coal pipes not balanced  
(Evaluate results and balance coal pipes if needed)
  - » Secondary air balance via windbox/SA duct modifications
2. Guarantees based on as-found coal fineness
3. Fuel injector coal ropes eliminated with ABT de-spin assembly in scroll
4. Opti-Flow™ fuel injector develops stable flame in all burner throats

- Low NO<sub>x</sub> Fuel Injectors
  - » Unit 2: 8 Mark I fuel injectors (front bottom row/rear top row)
  - » Unit 1: 28 Mark II fuel injectors (complete retrofit)
- Windbox Modifications (Units 1 and 2)
  - » Secondary air duct turning vanes
  - » Windbox perforated plates and splitter vanes
- Anti-Corrosion Ports (Unit 1)
- System Models
  - » SA duct/burner windbox (subcontracted to Airflow Sciences)
  - » Furnace (subcontracted to ASC)

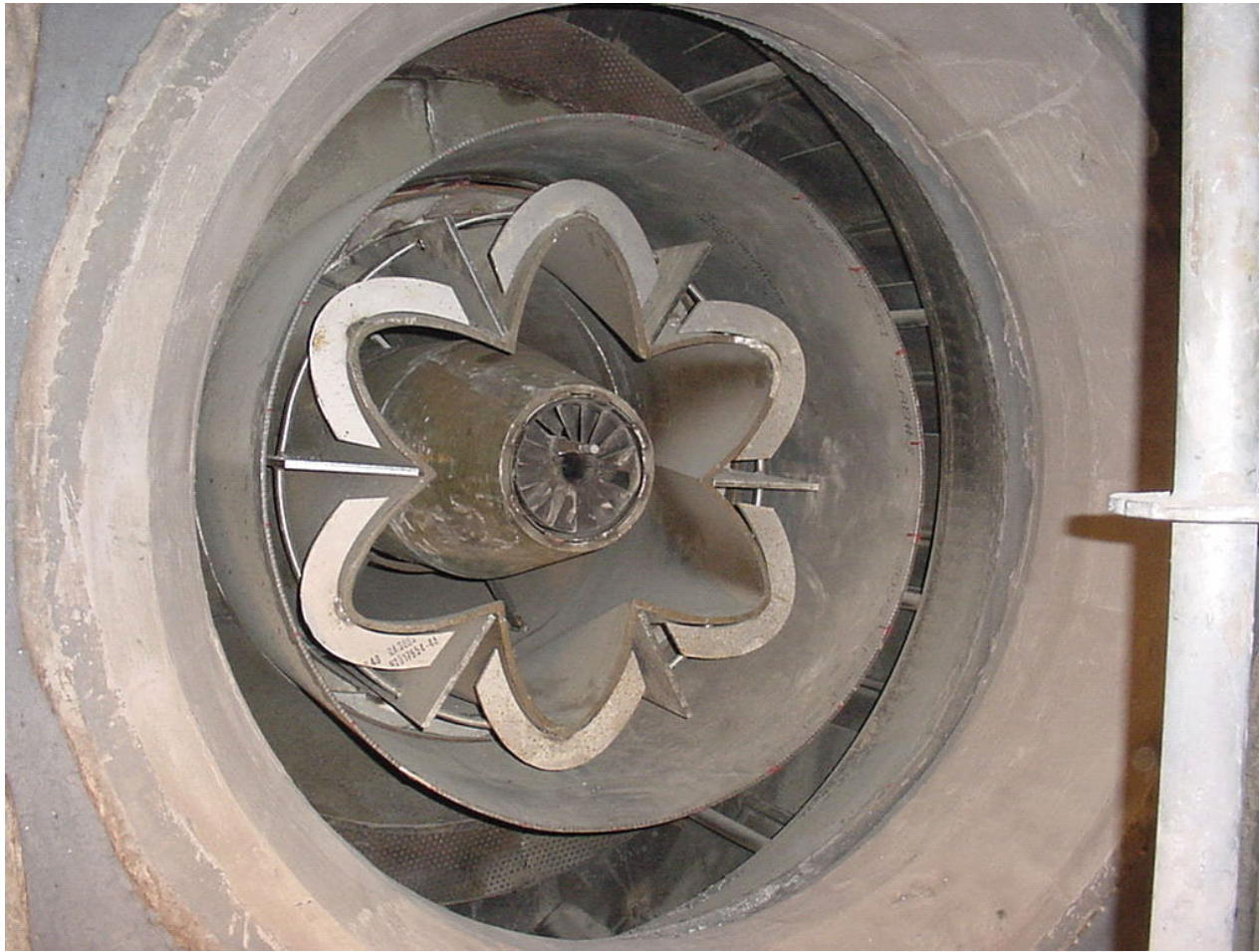
- “Plug-in” assembly with ***existing register used***
- New secondary air flow dividers
- Existing coal feed scrolls modified to include ABT’s de-spin assembly
- New inner secondary air zone damper for Mark II fuel injector (Unit 1)
- Fixed vane swirler for the inner air zone of Mark II fuel injector
- Fixed inner barrel with cast tip for Mark II fuel injector



# St. Johns Unit 1 Burner Front



# St. Johns 1 Fuel Injector Tip



## ABT's Anti-Corrosion Ports (ACP)

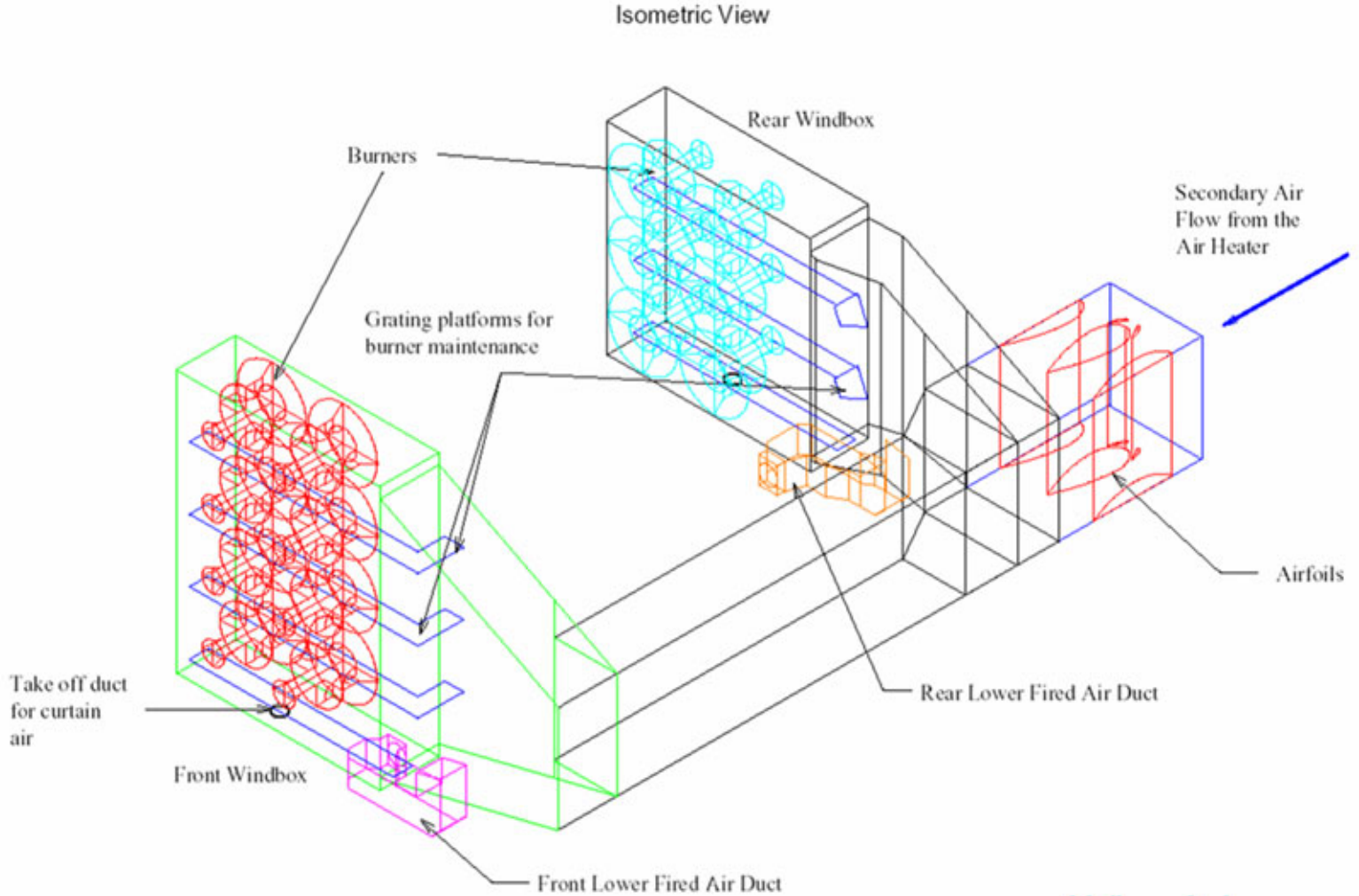
- Circular ports with baffles placed at top burner elevations next to sidewalls within existing windboxes.
- Ports provide a blanket of oxygen along the sidewalls to minimize corrosion from high sulfur fuels.
- Air flow to ACP's controlled by individual sleeve dampers



# CFD MODELING RESULTS

- Burner Secondary Air Flow: Correct maldistribution
  - » Secondary air ducts
  - » Front and rear windboxes
- Furnace Model: ACP location and LFA modifications
  - » CO distribution
  - » O<sub>2</sub> distribution
  - » H<sub>2</sub>S distribution
  - » Temperature

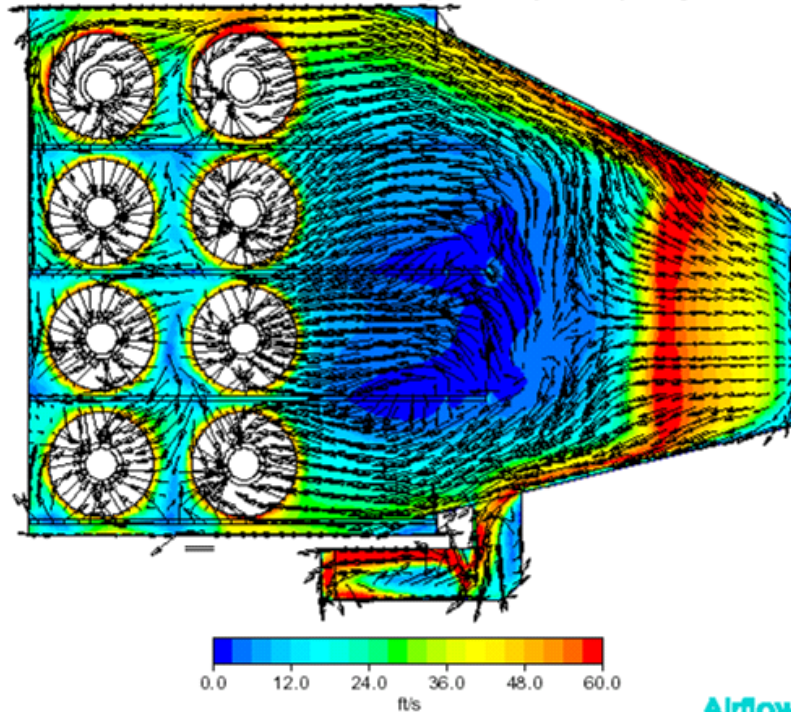
# St. Johns Existing Windboxes Schematic



# CFD Model of St. Johns Front Windbox

3-D Velocity Magnitude Distribution

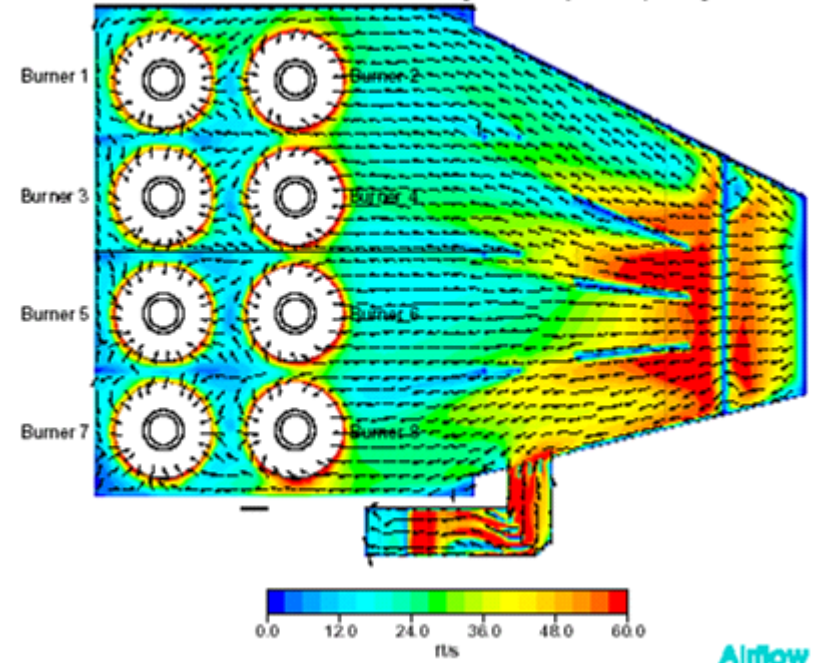
Front Windbox - Vertical Plane Through Secondary Air Damper Registers



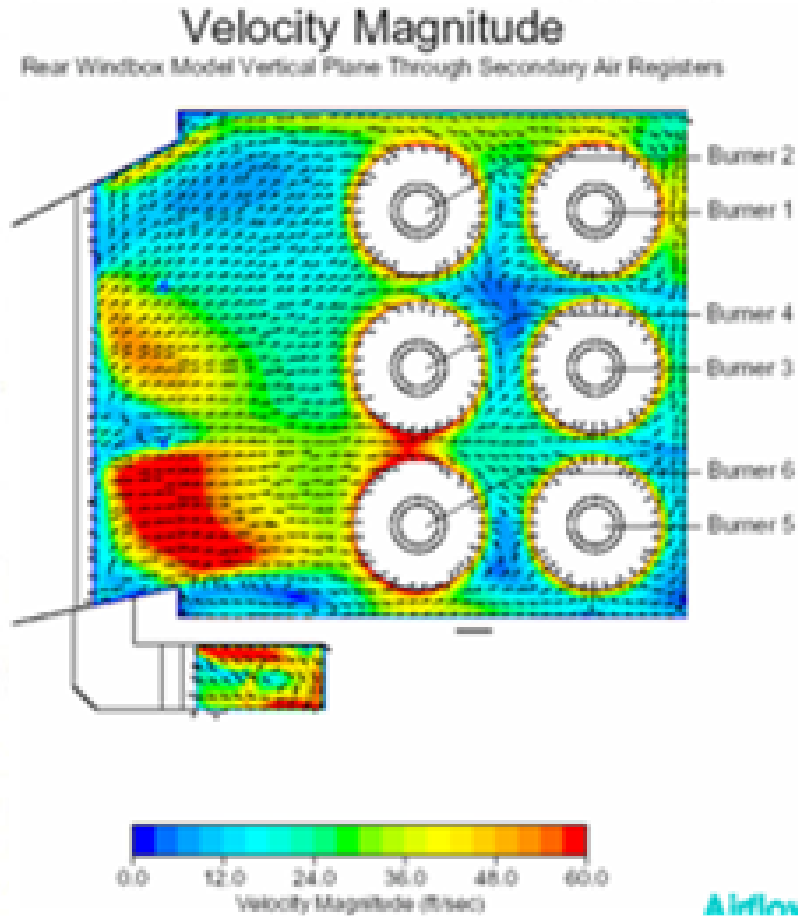
Baseline Air Velocity Distribution

3-D Velocity Magnitude Distribution <sup>70%</sup>

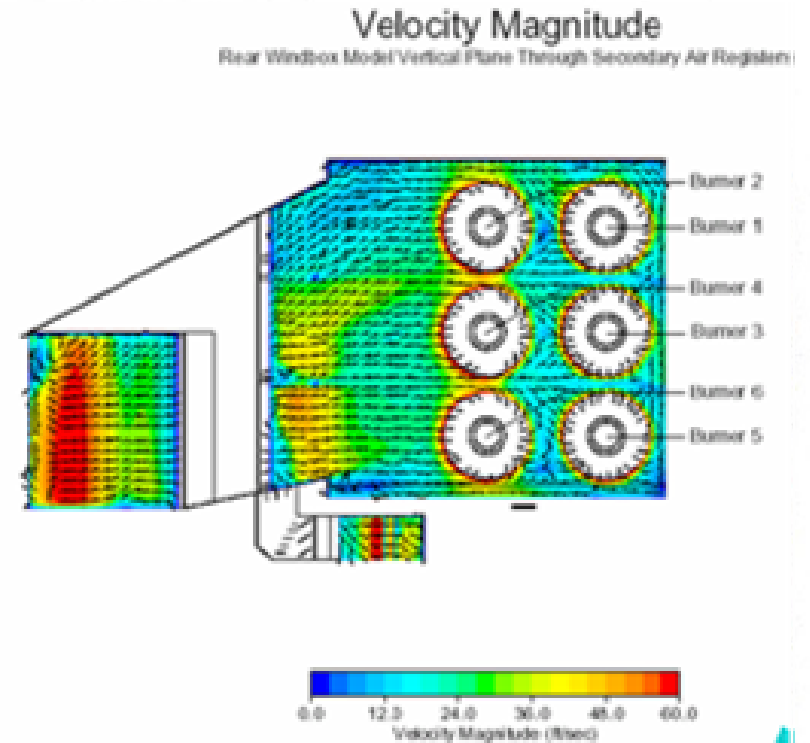
Front Windbox - Vertical Plane Through Secondary Air Damper Registers



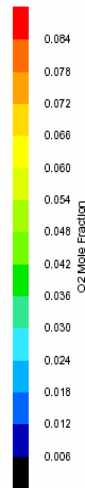
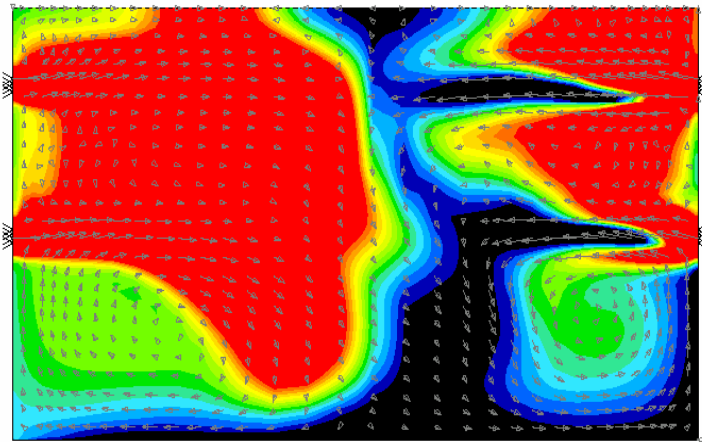
Air Velocity Distribution with Design Modifications



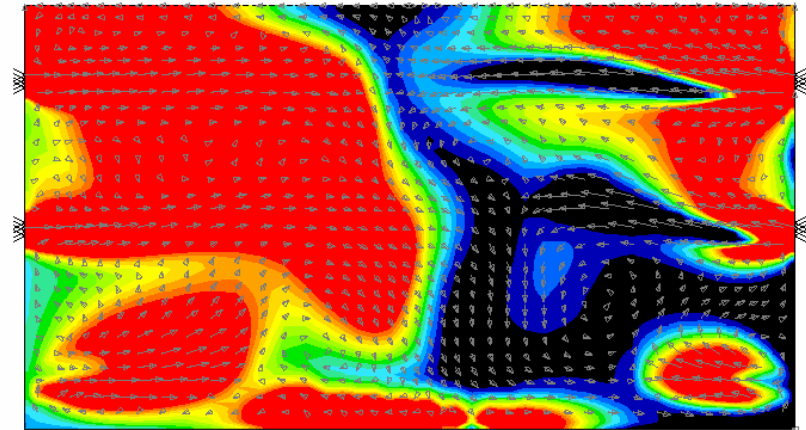
**Baseline Air Velocity Distribution**



**Air Velocity Distribution with Design Modifications**



**Sidewall without ABT Anti-Corrosion System**



**Sidewall with ABT Anti-Corrosion System**

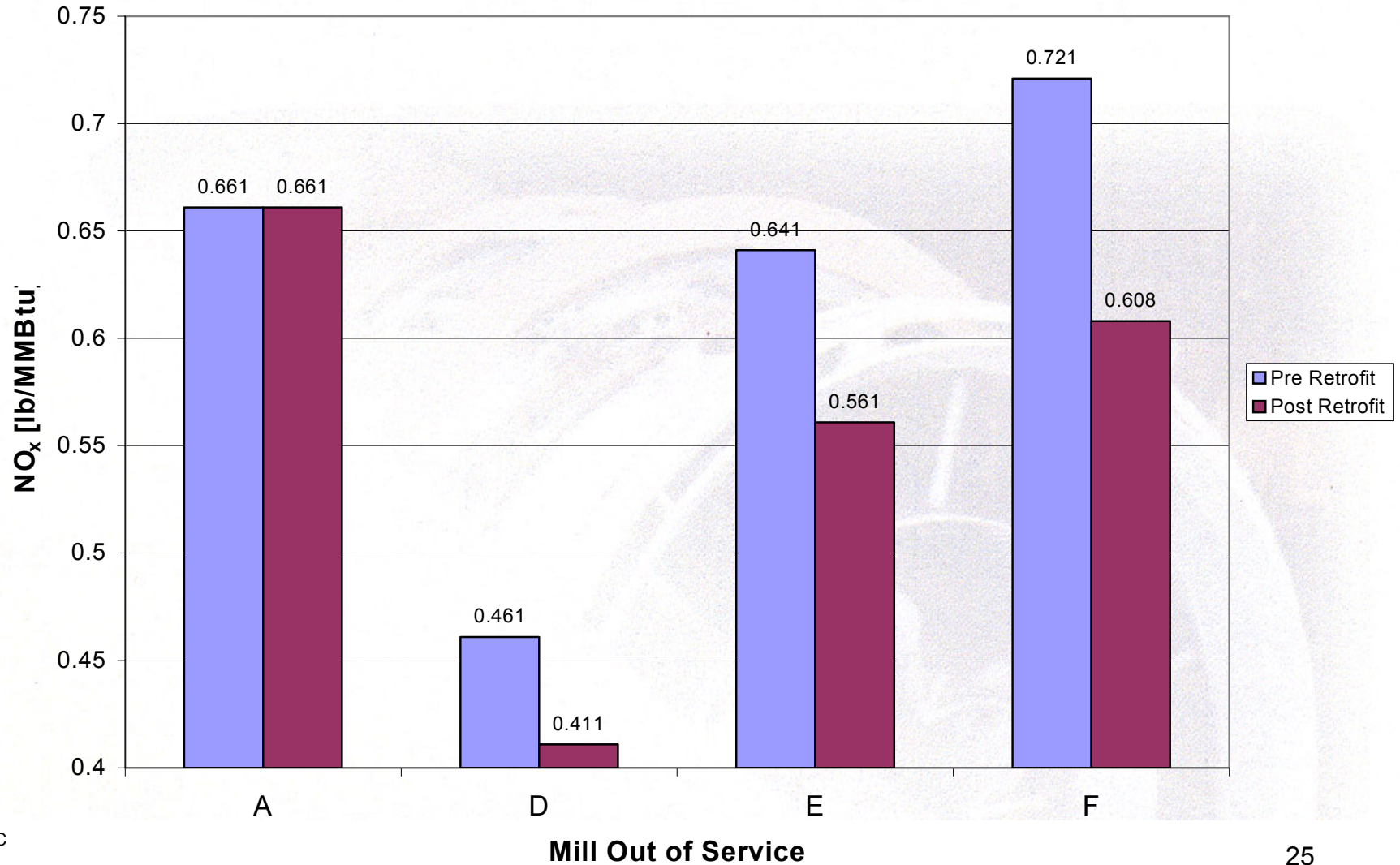
# POST-RETROFIT RESULTS

## St. Johns Unit 2 Results Summary

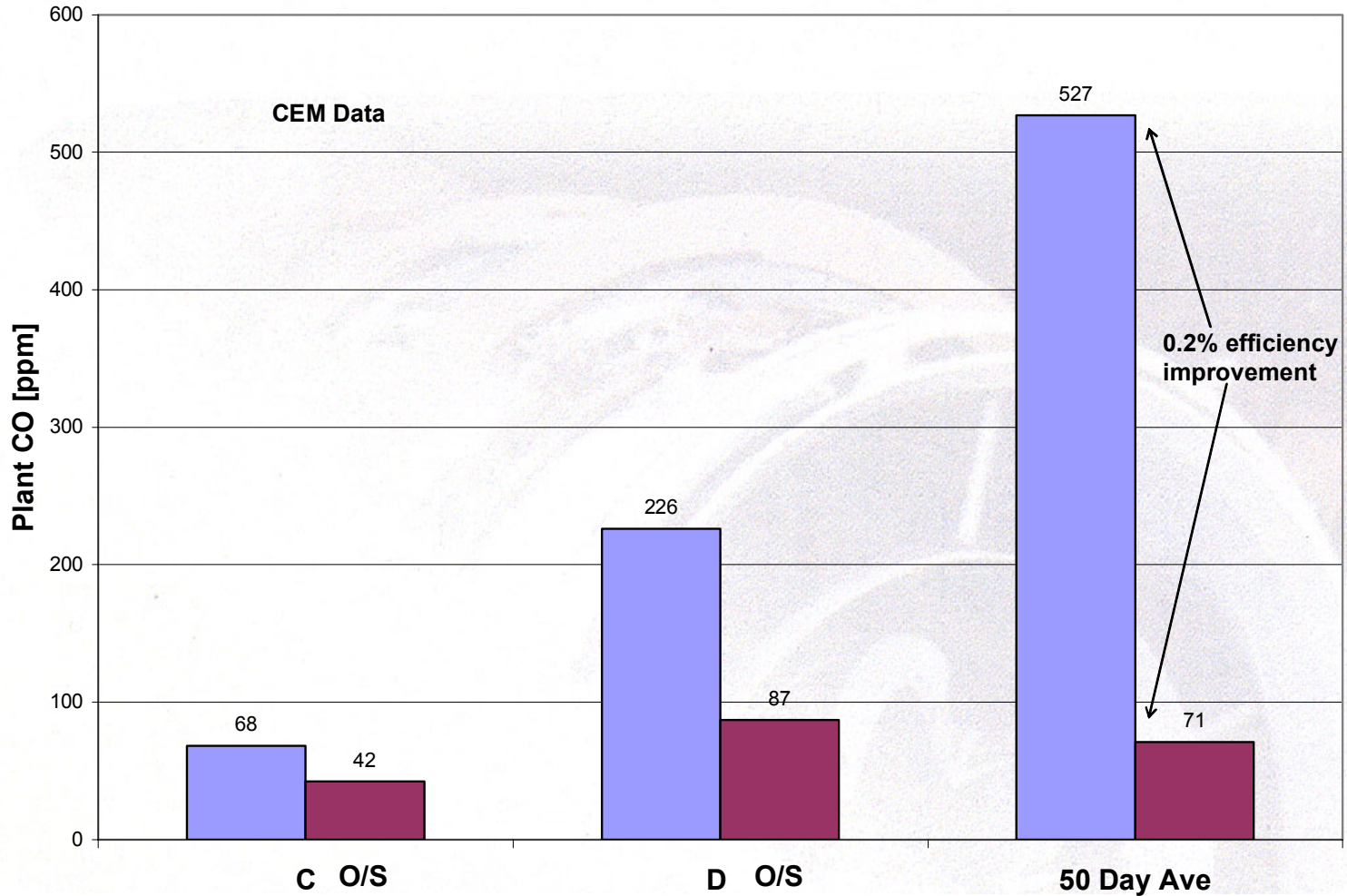
- Moderate NO<sub>x</sub> reduction of approximately 10% for normal operation with only two rows of new ABT fuel injectors
- Significant reduction in CO emissions to less than 100 ppm.
- Reduction in fly ash LOI of approximately 50%
- Improved SA flow distribution allows lower excess air operation (2.5 vs. 3.0%)
- Efficiency improvement of approximately 1% results in annual fuel savings of \$600,000



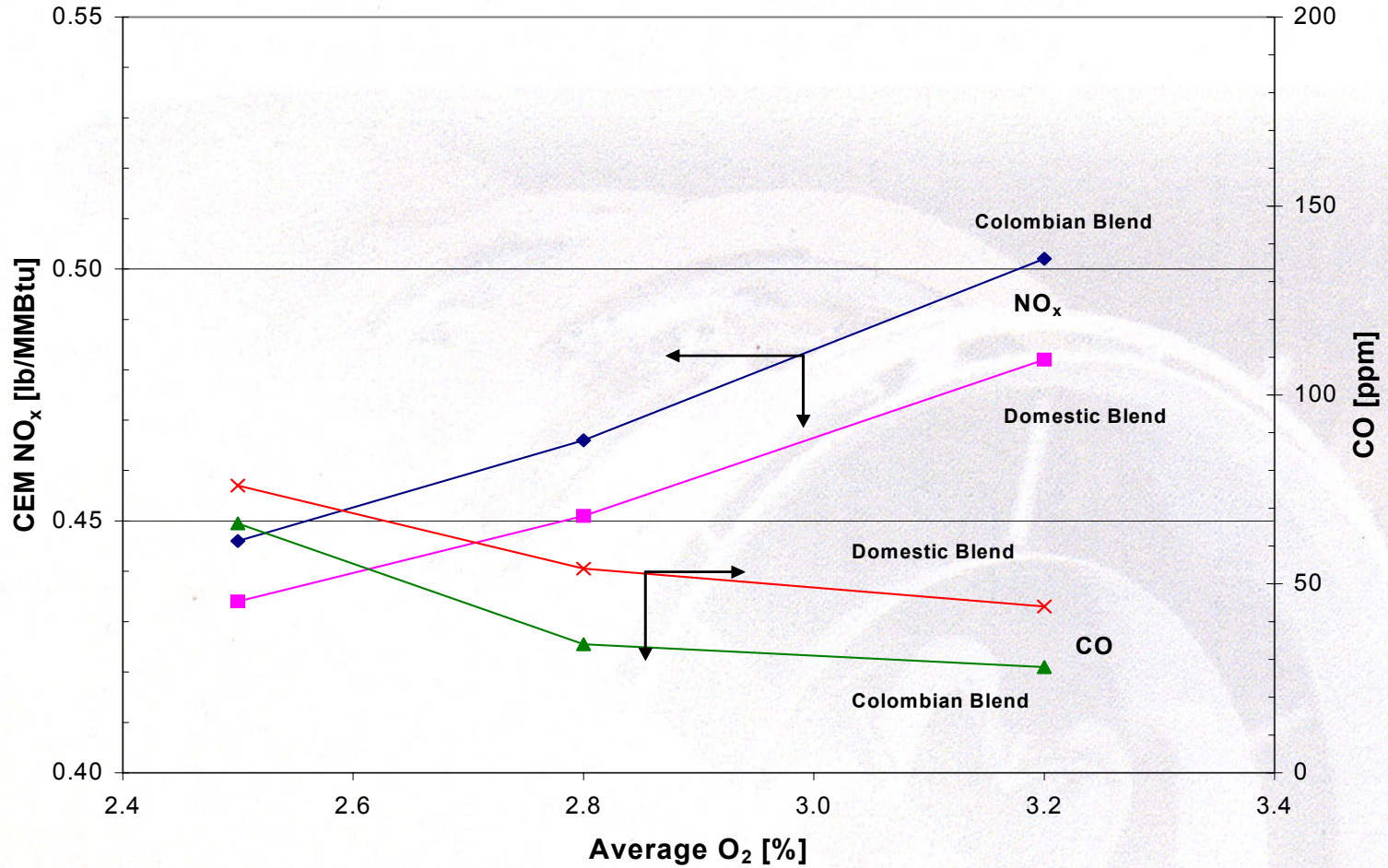
# St. Johns Unit 2 NO<sub>x</sub> Emissions: Post vs. Pre-Retrofit



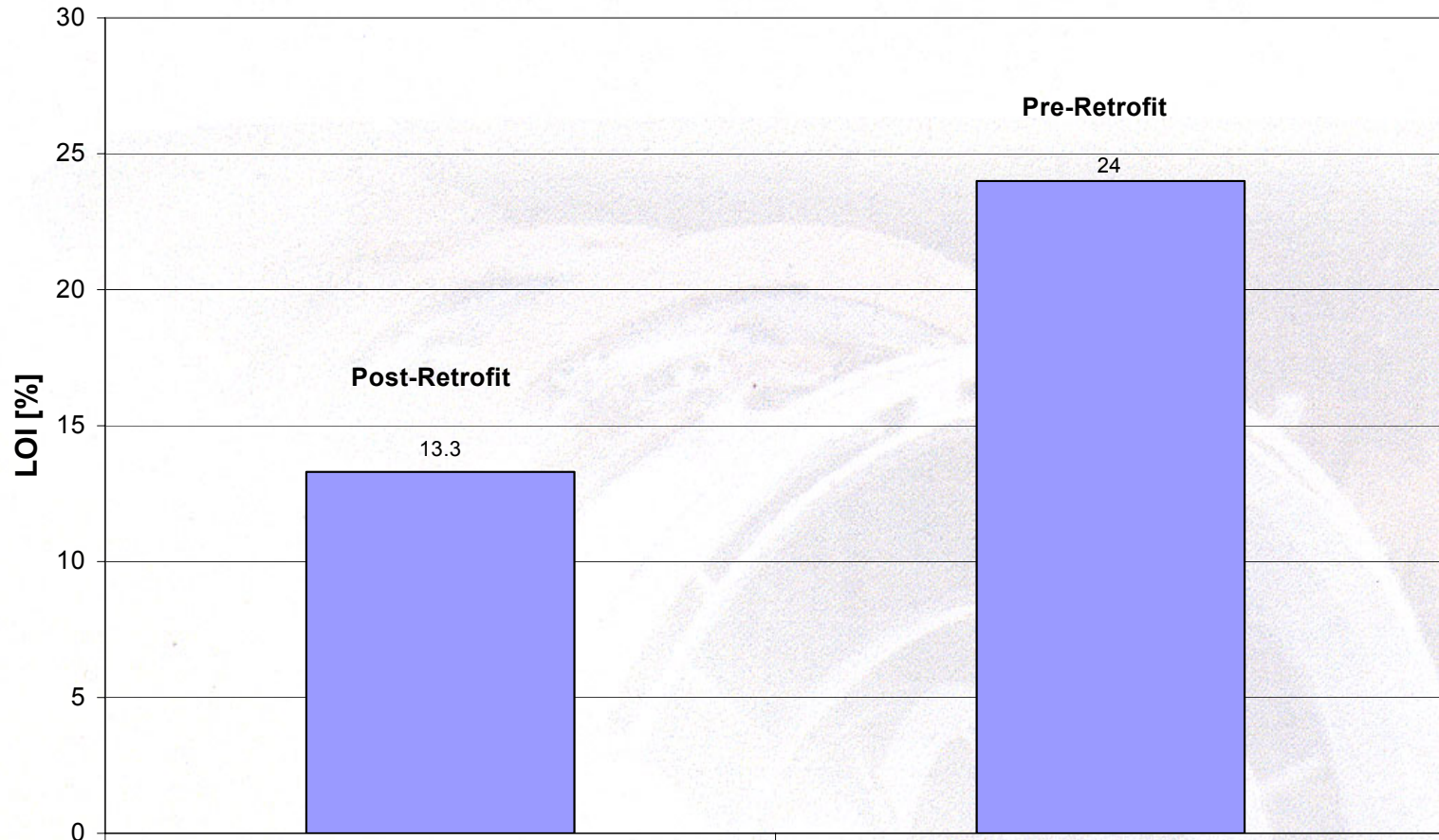
# St. Johns Unit 2 CO Emissions: Post vs. Pre-Retrofit



# St. Johns Unit 2 NO<sub>x</sub> and CO: Post-Retrofit Colombian vs. Domestic Blend



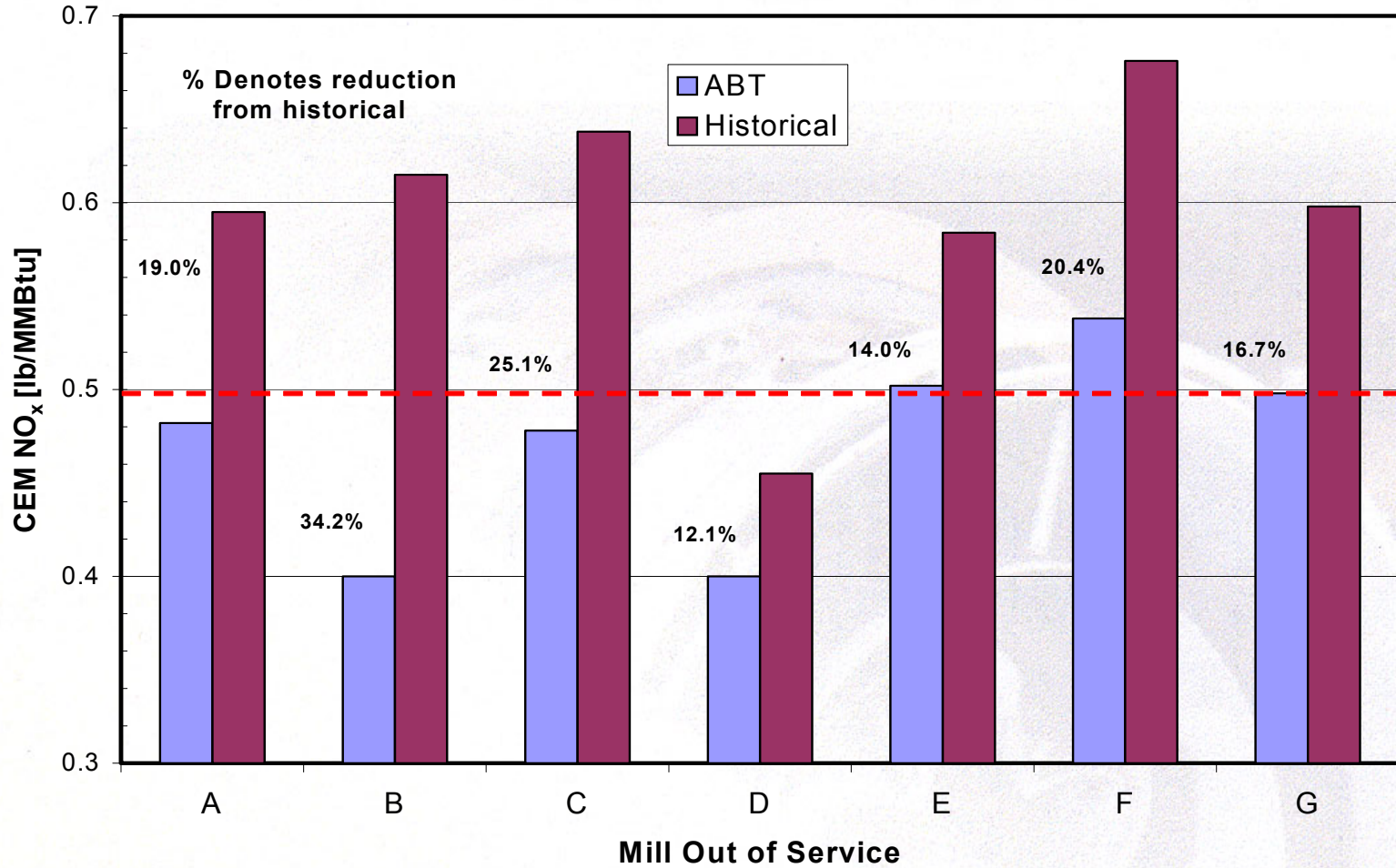
# St. Johns Unit 2 Fly Ash LOI: Post vs. Pre-Retrofit with D-Mill Out of Service



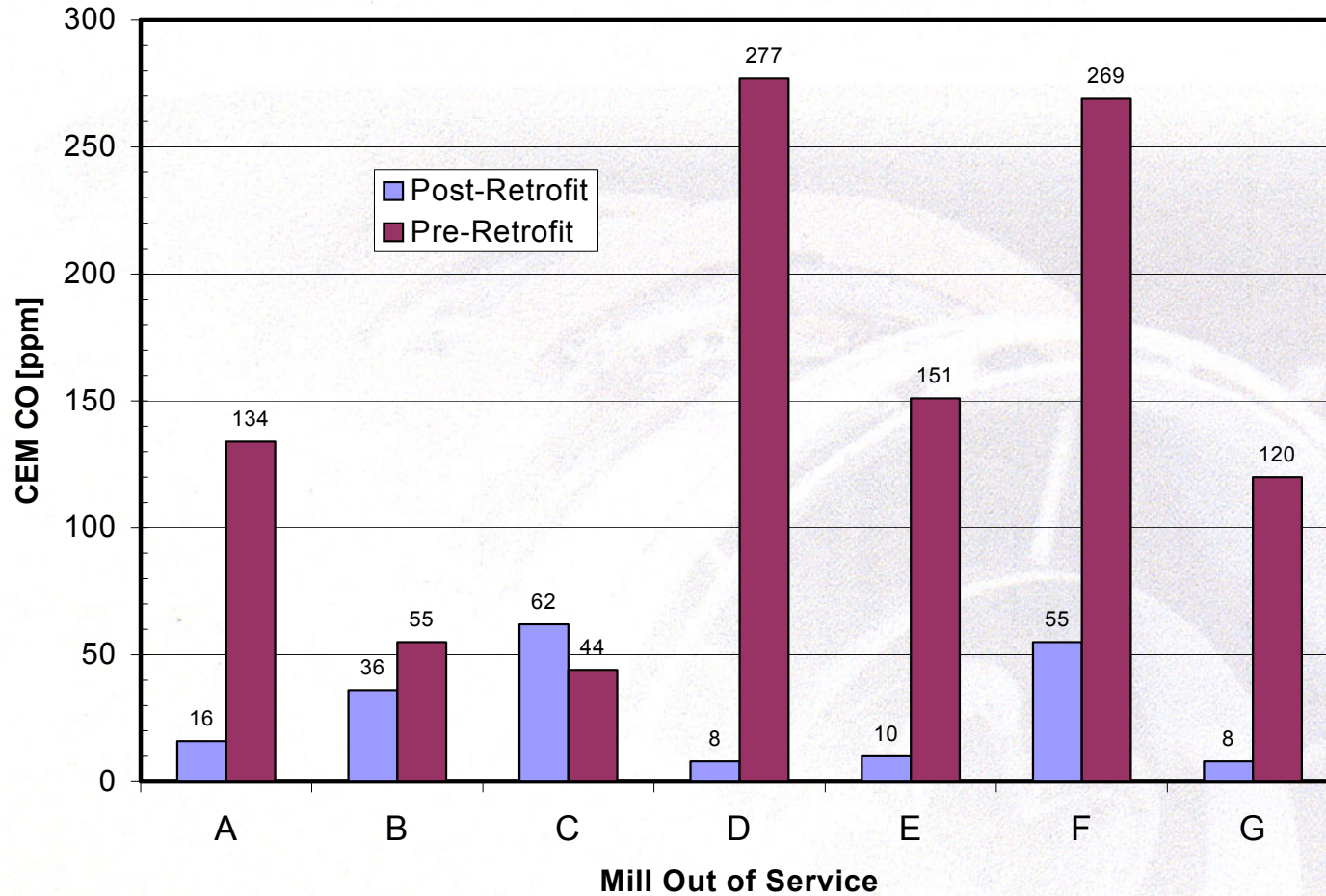
# St. Johns Unit 1 Results Summary

- Average NO<sub>x</sub> reduction > 20% achieved for all mill configurations. Guarantee of 0.4 lb/10<sup>6</sup> Btu met.
- Significant reduction in CO emissions to less than 10 ppm for normal operation with D-Mill out of service
- Fly ash LOI reduced from 30 to 40% range to 15 to 20% range. Lower reduction achieved compared to Unit 2 due to poor mill performance
- Improved flame stability and burner turndown

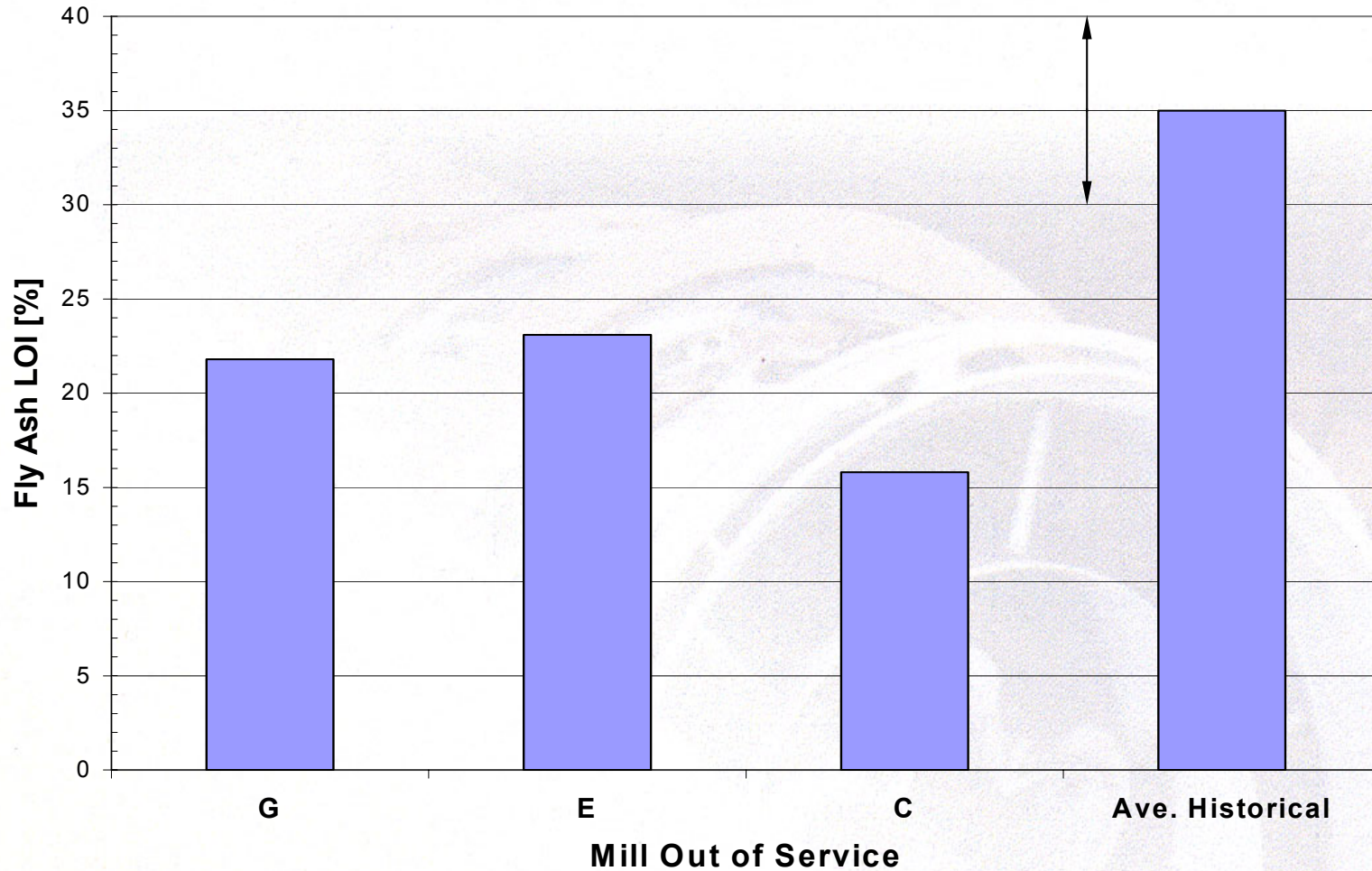
# St. Johns Unit 1 NO<sub>x</sub> Emissions: Post vs. Pre-Retrofit



# St. Johns Unit 1 CO Emissions: Post vs. Pre-Retrofit



# St. Johns Unit 1 Fly Ash LOI: Post vs. Pre-Retrofit





# St. Johns Unit 1 Burner Turndown

- Only 30% turndown to 475 MW could be achieved with the existing OEM burners and one mill out of service
- Turndown to 380 MW has been achieved with the ABT fuel injectors with only one mill out of service
- Improved turndown requires fewer mills taken out of service when dropping load – reducing oil consumption if these mills had to be put back online for unit ramp up.



# ABT Opti-Flow™ Fuel Injector: Unit 1 380 MW





# OEM Fuel Injector: Unit 2 660 MW



## Summary

- For St. Johns Unit 1, a complete retrofit of ABT's fuel injectors has achieved the  $\text{NO}_x$  guarantee of  $0.40 \text{ lb}/10^6 \text{ Btu}$  **while reducing CO and LOI**. Almost all mill configurations can now be used to achieve the  $\text{NO}_x$  limit of  $0.5 \text{ lb}/10^6$  instead of D-Mill only out of service.
- St. Johns Unit 2 has been partially retrofitted with ABT fuel injectors. In the Spring of 2004 a complete fuel injector retrofit and OFA system will be installed.
- CO emissions have been reduced to less than 100 ppm for both units.

## Summary (cont'd)

- LOI has been reduced by 50% for Unit 2 and 35% for Unit 1
- For Unit 1, improved flame stability has resulted in better turndown with a complete retrofit of ABT fuel injectors
- For Unit 1 furnace ACP's have been effective in greatly reducing sidewall CO concentrations as shown by gas measurements (<500 ppm).
- ABT has been the first to demonstrate co-firing petroleum coke in an advanced low NO<sub>x</sub> burner to minimize NO<sub>x</sub>, CO and LOI and attain a 2:1 turndown.