## An Investigation of Site-Specific Factors for Retrofitting Recirculating Cooling Towers at Existing Power Plants

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## **Table of Contents**

Section	Title	Page
	List of Tables	ii
	List of Figures	ii
	List of Acronyms and Abbreviations	iii
	Glossary	iv
1	Introduction	1-1
2	Site Descriptions	2-1
3	Methodology	3-1
	3.1 Technical Considerations	3-1
	3.2 Cost Estimating and Economic Considerations	3-8
	3.2.1 Cost Estimating	3-8
	3.2.2 Economic Considerations	3-8
4	Results	4-1
	4.1 Discussion of Results	4-1
	4.2 Capital Cost and Operating Cost Results	4-3
5	Conclusions	5-1

Appendix A, Capital Cost Estimate (14 pages)

Appendix B, O&M Cost Estimate (14 pages)

Appendix C, January 22, 2003 Addendum (12 pages)

## List of Tables

Table	Title	Page
3-1	Seasonal Average Temperatures	3-6
3-2	Plant Design Bases	3-7
3-3	Condenser and Cooling Tower Design Parameters	3-7
4-1	Energy Flow Comparison	4-1
4-2	Evaluation Results – Plant Output Effects	4-2
4-3	Evaluation Results – Technical Parameters	4-4
4-4	Summary of Capital and Operating Costs – All Plants	4-5

## **List of Figures**

<u>Figure</u>	Title	Page
2-1	Aerial Photograph, Vicinity of Surry Site, with Proposed Cooling Towers Superimposed	2-4
2-2	Map, Vicinity of Surry Site	2-5
2-3	Aerial Photograph, Vicinity of Hudson Site, with Proposed Cooling Towers Superimposed	2-6
2-4	Map, Vicinity of Hudson Site	2-7
2-5	Aerial Photograph, Vicinity of Barney Davis Site, with Proposed Cooling Towers Superimposed	2-8
2-6	Map, Vicinity of Barney Davis Site	2-9
2-7	Aerial Photograph, Vicinity of Big Bend Site, with Proposed Cooling Towers Superimposed	2-10
2-8	Map, Vicinity of Big Bend Site	2-11
3-1	Existing Once-Through Cooling Schematic	3-2
3-2	Proposed Retrofit Cooling Tower Schematic	3-2
3-3	Cooling Tower Cell Arrays (Plan View)	3-3

## List of Acronyms and Abbreviations

AFDC	allowance for funds used during construction
Avg.	average
bhp	brake horsepower
Btu	British thermal unit
C.F.	capacity factor
CM	construction management
COE	cost of electricity
СТ	cooling tower
CW	circulating water
DOE	U.S. Department of Energy
EPA	U.S. Environmental Protection Agency
°F	degrees Fahrenheit
FTE	full time equivalent
gpm	gallons per minute
h	hour
hp	horsepower
kW	kilowatt
kWe	kilowatt electric
kWh	kilowatt hour
lb	pound
LP	low pressure
MM	million
MW	megawatt
MW <sub>e</sub>	megawatt electric
MWh	megawatt hour
MWt	megawatt thermal
NETL	National Energy Technology Laboratory
No.	number
O&M	operating and maintenance
OH	overhead
psia	pounds per square inch atmospheric
psig	pounds per square inch gauge
USGS	U.S. Geological Survey
Yr.	year

### Glossary

**AFDC** – Allowance for Funds used During Construction; a monthly allowance for interest paid on monies spent during the construction phase of a project.

**Capacity factor** – Actual power generated, in kilowatt hours, compared to the maximum power that could be generated over a defined time period, usually all year.

**Cell array** – A geometric arrangement of cooling tower cells.

**Circulating water system** – A cooling water system that circulates cold water to the steam condenser and hot water to a cooling tower for cooling.

**Condensing backpressure** – The pressure at which steam condenses inside the condenser.

**Cooling tower** – A heat exchanger transferring waste heat from circulating water to the atmosphere.

**Cooling tower retrofit** – Adding a cooling tower to a site that does not already incorporate one.

**Cooling tower temperature range** – The difference in temperature between the hot water entering and the cold water leaving the cooling tower.

**Dew point** – The dry-bulb temperature at which condensation begins if an air-vapor mixture is cooled at constant pressure.

**Double-flow LP cylinder** – A low-pressure turbine section comprising two expansion flow paths.

**Drift eliminators** – Devices in a cooling tower that capture droplets of water in the airflow leaving the tower, preventing their discharge to the atmosphere.

**Dry Bulb Temperature** - The temperature of ambient air as measured by a standard thermometer or other similar device.

**Energy Penalty** - The loss of electricity generating capacity incurred when a cooling system is unable to perform at design efficiency. The energy penalty is associated with insufficient cooling of the turbine exhaust steam and usually is manifested by an increase in steam turbine back pressure. This study expresses the penalty as "the percentage of plant output," or phrased differently, "the percentage of additional energy that would have to be used to generate the same amount of electricity." In this study, the energy penalty also includes additional power needed for pumps and fans in cooling tower systems.

**Evaporative cooling tower** – A heat exchanger transferring waste heat from circulating water to the atmosphere, which uses evaporation of water as a means of heat transfer.

**Last-stage blades** – The last stage of turbine blades in the steam expansion flow path of a steam turbine.

**Mean ambient wet bulb data** – Statistical mean, or average, of discrete ambient wet bulb temperature data.

**Mechanical draft evaporative cooling tower** – An evaporative cooling tower using a motordriven fan to propel a stream of air through the tower.

**Once-through cooling water system** – A cooling water system that does not recirculate the water. The water flows from the intake to the heat load and then to the discharge in a direct path.

**Parasitic power losses** – See plant auxiliary load below.

**Plant auxiliary loads** – Electrical power requirements of auxiliary equipment necessary to support operation of the plant.

**Plume abatement** – A means of reducing the visual and local environmental impacts (fog, icing) of the plume of saturated air leaving an evaporative cooling tower.

**Power block** – Major buildings and structures comprising the power plant; typically includes the boiler (reactor building in the case of a nuclear plant), steam turbine, particulate control device (electrostatic precipitator or baghouse), wet scrubber (if included), draft equipment (fans), ducting, and stack. Other equipment and structures may be included, if contiguous with the boiler and turbine buildings.

**Pultruded** – A continuous molding manufacturing process utilizing glass or fibrous reinforcement in a polyester or vinyl ester resin matrix.

**Recirculating wet cooling tower** – Same as an evaporative cooling tower.

**Regenerative feedwater heating** – The use of steam extracted from different locations in the steam turbine, steam expansion flow path to progressively heat condensate and feedwater.

**Spray deck** – The horizontal deck surface of a cooling tower where the cooling water is released via spray nozzles to drain downward by gravity, and be cooled by evaporation as it falls to the basin below.

**Steam condensing enthalpy** – A measure of the thermal energy released by the steam as it condenses.

**Steam cycle performance** – Thermal performance of the steam thermodynamic cycle.

**Subcritical steam generator** – A device generating steam at subcritical pressure and temperature (less than 3,208 psia/705 °F).

**Supercritical steam generator** – A device generating steam at supercritical pressure and temperature (greater than 3,208 psia/705 °F).

**Turbine generator** – A steam turbine and electric generator set. The steam turbine provides the motive power to drive the electric generator, which produces electricity.

**Wet bulb temperature** – The temperature of ambient air as measured by a thermometer in which the bulb is kept moistened and ventilated. The resulting measurement equates to the dynamic equilibrium temperature attained by a water surface when the rate of heat transfer to the surface by convection equals the rate of mass transfer away from the surface by evaporation. The wet bulb temperature is the lowest temperature at which evaporation can occur for specific ambient conditions (dry bulb temperature and relative humidity).

## **1. INTRODUCTION**

The protection of aquatic organisms found in the water bodies of the United States has been an important focus of environmental regulations in the United States. In 1972, Congress enacted section 316(b) of the Clean Water Act addressing the withdrawal of cooling water from surface water bodies. The congressional language mandated that:

"Any standard established pursuant to section 301 or section 306 of this Act and applicable to a point source shall require that the location, design, construction, and capacity of cooling water intake structures reflect the best technology available for minimizing adverse environmental impact."

The U.S. Environmental Protection Agency (EPA) promulgated final section 316(b) regulations in 1976. However, in 1979, EPA formally withdrew its section 316(b) regulations as a result of a successful Federal court challenge initiated by a consortium of 58 utilities. Over the past 20 years, in the absence of Federal guidelines, many States have adopted their own regulations with respect to the implementation of section 316(b) requirements regarding cooling water intake structures. In many cases, the States had adopted a site-specific approach to determine what constitutes best technology available for minimizing adverse environmental impact.

The regulatory environment had changed by 1995 when the U.S. District Court, Southern District of New York, entered a Consent Decree between the EPA and the Hudson Riverkeeper that obligated the Agency to issue cooling water intake structure regulations within 7 years. The Consent Decree was modified on November 21, 2000 to: a) finalize new facility regulations by November 9, 2001 (Phase I); b) propose existing source large utility and non-utility power producer regulations by February 28, 2002 and issue final regulations by August 28, 2003 (Phase II); and c) propose regulations by June 15, 2003 and issue final regulations by December 15, 2004 for other existing facilities not covered in b) above (Phase III).

EPA's Phase II proposal addressing existing facilities has been released and can be found at <u>http://www.epa.gov/waterscience/316b/</u>. As currently written, the proposal presents several options under consideration for the final rule. One of the options suggests that existing, once-through cooled facilities be required – based on water body type and intake flow capacity – to retrofit with recirculating wet cooling towers as a method to meet reductions in organism impingement and entrainment. EPA estimates that this option would affect 50 to 60 existing steam-condensing power generation facilities.

When considering a recirculating wet cooling tower retrofit to an existing once-through cooled facility, there are several significant site-specific issues and assumptions that must be fully analyzed a priori. Among these issues are effect on turbine performance, increased plant parasitic power losses, land space consideration, tower size and type, permitting restrictions, tower plume and noise abatement, and tower drift loss control, just to name a few. The purpose of this report is to evaluate the feasibility of a wet recirculating cooling tower retrofit at four existing steam-condensing power plants with respect to the aforementioned issues. The plants that were evaluated are the Surry Power Station (nuclear, Units 1 and 2), Hudson Generating

Station (Unit 1/gas, Unit 2/coal), Barney M. Davis Power Station (natural gas, Units 1 and 2), and Big Bend Station (coal, Units 1, 2, 3, and 4). These plants were studied because of their representative fuel type and their geographic location, which underscored the very site-specific nature of the wet recirculating cooling tower retrofit option.

## 2. SITE DESCRIPTIONS

The four plants selected for evaluation of a potential evaporative cooling tower retrofit are briefly described below. These sites were chosen because they represent the class of power plants that could be candidates for cooling tower retrofits and encompass the range of site specific issues that may need to be addressed. They represent all fuel types and have significantly different geographic locations. An aerial photograph and map of the surrounding area for each site are included in the back of this section of the report (Figure 2-1 through Figure 2-8). The selected plants are:

- Surry Power Station (Surry County, Virginia), Units 1 and 2
- Hudson Generating Station (Jersey City, New Jersey), Units 1 and 2
- Barney M. Davis Power Station (Corpus Christi, Texas), Units 1 and 2
- Big Bend Station (Tampa Bay, Florida), Units 1, 2, 3, and 4

A sketch of a proposed cooling tower arrangement has been prepared for each site, and is superimposed on the aerial photograph for each site. The site descriptions make reference to nearby facilities such as airports, highways, tourist attractions, etc. The presence of these site-specific features must be taken into account when considering the siting of evaporative cooling towers, since these towers can cause local fogging, icing, deposition of droplets containing dissolved solids, or have other impacts such as noise, or interpose high structures in the path of an approach to an airport. It is important to recognize the inextricable tie between these cooling tower siting challenges and the potential for increased capital/operating costs to overcome them.

#### Surry Power Station, Units 1 and 2

Surry Unit 1 and Unit 2 are identical nuclear power plants, based on Westinghouse pressurized water reactors generating a nominal 848 MW<sub>e</sub> each. Each turbine generator has two double-flow low-pressure (LP) cylinders with 44-inch last-stage blades. Unit 1 was placed in service in December 1972 and Unit 2 in May 1973.

The site is on a point of land called Gravel Neck, which projects into the James River in Surry County, Virginia. The river is brackish. Both units share a common cooling water intake canal that is approximately 2 miles long. The cooling water is pumped from the James River into the intake canal, and a common discharge canal returns the water from the plant.

The immediate area around the plant power block is surrounded by structures or the cooling water intake and discharge canals. The most likely available vacant space for siting cooling towers that is accessible to both cooling water canals is southeast of the plant.

The Surry site is approximately 6 miles south and across the James River from the Jamestown National Historic Site. The Williamsburg Jamestown airport is 8 miles north of the site, and the Felker Army Airfield is 6 miles southeast. State parks and wetland areas surround the site. *Based on this preliminary analysis, it appears as though cooling tower plume abatement design measures may not be a requirement at the Surry site.* 

#### Hudson Generating Station, Units 1 and 2

Hudson Station comprises two fossil-fuel-fired units. Hudson Unit 1 has a nominal 455 MW gas-fired supercritical steam generator with a turbine generator that has two double-flow LP cylinders with 28-inch last-stage blades. Hudson Unit 2, rated at a nominal 660 MW, has a coal-fired supercritical steam generator and a turbine with three double-flow LP cylinders with 28-inch last-stage blades. Unit 1 was placed in service in December 1964 and Unit 2 in December 1968.

The site is on the east shore of the Hackensack River on the outskirts of Jersey City, New Jersey. The river is brackish. There is an intake canal for the cooling water. The cooling water discharge appears to be on the river's edge downstream of the plant.

The immediate area around the power blocks for the two units is surrounded by the river on one side, the coal handling and storage facilities below, the substation above, and fuel oil storage facilities on the other side. The most likely large vacant area that can accommodate all the cooling towers in the same location is north of the plant across the railroad tracks.

The Hudson site is approximately <sup>1</sup>/<sub>2</sub> mile south of the New Jersey Turnpike, <sup>3</sup>/<sub>4</sub> mile south of the Secaucus Railroad Station and <sup>1</sup>/<sub>2</sub> mile south of Amtrak tracks. Various Conrail tracks are immediately adjacent to the site on three sides. The plant is <sup>1</sup>/<sub>2</sub> mile north of Newark Avenue and the Pulaski Skyway (Route 9) and has warehouse storage sites on its immediate southern end. *The Hudson plant was deemed to require plume abatement design measures, based on its proximity to roads and its general location in a heavily urban setting.* 

#### Barney M. Davis Power Station, Units 1 and 2

Barney Davis Station comprises two natural-gas-fired steam plants. Unit 1 has a nominal 353 MW gas-fired subcritical steam generator with a turbine generator that has one double-flow LP cylinder with 28-inch last-stage blades. Unit 2 has a nominal 351 MW gas-fired steam generator with a turbine that has one double-flow LP cylinder with 30-inch last-stage blades. Unit 1 was placed in service in May 1974 and Unit 2 in June 1976.

The site is approximately 1 mile inland from upper Laguna Madre, which is on the Gulf coast of Texas, just south of Corpus Christi. The seawater intake is at the end of the 1-mile-long canal to Laguna Madre. The plant discharges into the Oso Bay, which is attached to Corpus Christi Bay.

The power blocks are fairly unencumbered by surrounding facilities. The best choice for the cooling towers appears to be along the intake canal since this affords the efficient use of the existing intake canal for returning the water to the existing circulating water pumps.

The Barney Davis site is approximately 1.5 miles south of Waldron U.S. Navy Airfield, 5.5 miles south of Corpus Christi Naval Air Station, 5 miles south of State Route 358, and 15 miles south of Interstate Route 37. The area surrounding the site appears not to be heavily populated, with fish hatcheries on the northwest being one of the closest identifiable features. *Based on this preliminary analysis, it appears as though cooling tower plume abatement design measures may not be a requirement at the Barney Davis site.* 

#### **Big Bend Station**, Units 1, 2, 3, and 4

Big Bend Station comprises four coal-fired steam plants. Units 1, 2, and 3 each have nominal 446 MW coal-fired subcritical steam generators. Units 1 and 2 each have a turbine generator with one double-flow LP cylinder with 31-inch last-stage blades. Unit 3 has a turbine with one double-flow LP cylinder with 33.5-inch last-stage blades. Unit 4 has a nominal 486 MW coal-fired steam generator with a turbine that has two double-flow LP cylinders with 26-inch last-stage blades. Unit 1 was placed in service in October 1970, Unit 2 in April 1973, Unit 3 in June 1976, and Unit 4 in February 1985.

The site is located on the lower Hillsborough Bay near Tampa Bay, Florida. The four units appear to share a common seawater intake canal north of the plants and discharge back into the bay south of the plants.

The power blocks are surrounded by the intake canal and bay on the north and south, the coal handling and storage facilities on the west, and other support facilities on the east side so that there is virtually no vacant area immediately adjacent to the power blocks. The best available vacant space appears to be on the strip of land on the north side of the intake canal. The length of this strip of land appears to be sufficient to accommodate the use of inline towers for all four units without having to place any in parallel rows.

The Big Bend site is approximately 1.5 miles north of the Apollo Beach marina, 6 miles southeast of McDill Air Force Base, 1 mile west of the Tamlani Trail highway, and 3 miles west of Interstate Route 75. *Based on this preliminary analysis, it appears as though cooling tower plume abatement design measures may not be a requirement at the Big Bend site.* 



Figure 2-1 Aerial Photograph, Vicinity of Surry Site, with Proposed Cooling Towers Superimposed

Figure 2-2 Map, Vicinity of Surry Site





Figure 2-3 Aerial Photograph, Vicinity of Hudson Site, with Proposed Cooling Towers Superimposed

Scale



Figure 2-4 Map, Vicinity of Hudson Site



Figure 2-5 Aerial Photograph, Vicinity of Barney Davis Site, with Proposed Cooling Towers Superimposed



Figure 2-6 Map, Vicinity of Barney Davis Site



Figure 2-7 Aerial Photograph, Vicinity of Big Bend Site, with Proposed Cooling Towers Superimposed



Figure 2-8 Map, Vicinity of Big Bend Site

## **3. METHODOLOGY**

#### 3.1 TECHNICAL CONSIDERATIONS

Evaluation of the retrofit of evaporative cooling towers to existing power plants was based on certain assumptions. For this study, the retrofit design was configured to minimize the impact on the existing steam turbine and condenser. This minimizes capital costs and the potential for lengthy plant outages, both of which would add a significant cost penalty to the retrofit. The design approach taken maintains intact the major part of the plant circulating water system, including the circulating water pumps and intake structure, piping from the pumps to the condenser, the condenser itself, and much of the discharge piping from the condenser.

If new pumps with higher discharge pressure were employed to replace the existing circulating water pumps, the system pressure might be higher than the pressure capability of the condenser, which would necessitate expensive modifications or replacement of the condenser. The original circulating water flow and condenser range (temperature rise) were maintained to keep tube velocity at the original design value to minimize fouling. This has the added effect of minimizing the impact of the cooling tower retrofit on condensing backpressure, and thus on turbine generator output. The penalty in added auxiliary load caused by higher than optimum circulating water flow rate is minimized by the fact that modern cooling tower designs have a spray deck height that is significantly lower than previous generations of cooling tower designs. Typical once-through circulating water system designs utilize a condenser temperature rise of between 12 °F and 15 °F, whereas cooling-tower-based systems use a temperature rise of about 20 °F or higher.

The modifications to the plant involve interception of the condenser discharge piping at an appropriate location and installation of a wet pit with vertical booster pumps. These booster pumps provide the added head required to lift the water up to the cooling tower spray deck, and to compensate for added piping pressure losses and for any differential in elevation between the new pumping station and the cooling towers. Two schematic diagrams showing a typical plant configuration pre- and post-retrofit are presented as Figure 3-1 and Figure 3-2.

The retrofit design is based on the use of mechanical draft evaporative cooling towers of modern counter flow design, using film type fill. The cooling tower for each plant is comprised of a series of cells constructed of pultruded fiberglass for the linear arrays used at Hudson, Barney Davis, and Big Bend. Each cell is 66 feet square, with a deck height of 40 feet, and equipped with a 250 hp 1,800 rpm totally enclosed, fan cooled, motor driving the fan through a speed-reducing gearbox. Each cell is equipped with high-efficiency drift eliminators, to limit drift to 0.0005 percent or less. The clustered cell arrangement used at Surry utilizes a concrete structure. Cell dimensions, fan horsepower, and other details of construction are similar to those in the fiberglass cells used at the other sites.

Figure 3-3 provides an illustration (plan view) of the cooling tower cell arrays for each of the four sites evaluated. These cell arrays were chosen to efficiently use available land. The tower views are all presented at the same scale.



Figure 3-1 Existing Once-Through Cooling Schematic



#### Figure 3-3 Cooling Tower Cell Arrays (Plan View)



The need for plume abatement was evaluated for each of the four plants evaluated herein. Of the four plants, only the Hudson plant was deemed to require plume abatement design measures, based on its proximity to a road and its general location in a heavily urban setting.

The cooling tower for the Hudson plant application is equipped with a plume abatement feature, which comprises a finned tube coil mounted on top of the fan deck. The hot circulating water returning from the condenser passes through the coils first, and is cooled approximately 4 °F before exiting the coil and being routed to the spray nozzles above the fill. The fin tube coils are mounted to provide a parallel flow path with respect to the air that flows through the fill. The air streams mix in the fan exhaust; the mixed dry and humid air has a lower dewpoint, resulting in reduction in visibility of the plume and mitigation of the potential for local fogging and icing of nearby surfaces and structures. The other three plants evaluated in this study are not provided with plume abatement design features, based on the specific layout and location of each plant. If cooling tower retrofit becomes a reality for any of these plants, a more detailed study must be undertaken to thoroughly evaluate local conditions. The plume abatement feature is regulated by valves and dampers, and is only used when ambient conditions warrant. This type of plume abatement feature adds significantly to the cost of a cooling tower, potentially doubling the cost of the tower.

To accommodate the short time period available to perform the study and the lack of detailed information regarding the plant design conditions, the following simplifications or assumptions were made:

- The circulating water (CW) temperature rise across the condenser was assumed to be 15 °F.
   From our experience, this value is typical for many of the plants. Since the condenser temperature rise is equal to the range for the cooling tower, the cooling tower range is thus also set at 15 °F.
- Where plant data on the circulating water flow to the condenser was not available (only Surry data were), the flow was calculated using the assumed condenser rise of 15 °F, an assumed steam flow to the condenser of approximately 65 percent of the plant rated steam flow at the throttle, and a steam condensing enthalpy of 1000 Btu/lb. The percentage (65 percent) of plant rated steam flow to the condenser is based on previous experience with steam cycles using regenerative feedwater heating. The other 35 percent of the throttle steam flow is extracted from the steam turbine at various locations for feedwater heating and deaeration.
- The condenser backpressure was determined by using an assumed terminal temperature difference of 5 °F for the nuclear unit and 8 °F for the fossil units. The assumed terminal temperature differences were considered from experience to be typical values for condenser design.
- Seasonal average temperatures (cooling water and ambient wet bulb) were used to evaluate the impact of differences in condenser backpressure due to the introduction of a cooling tower into the circulating water system. Cooling water temperatures were based on available data from observation and recording stations for sites close to the plants. Likewise, the mean ambient wet bulb temperature data came from airports near the sites that record annual

weather data. Monthly averages for at least the last 5 years of data were calculated and then combined into spring, summer, fall, and winter seasonal averages. Time did not permit a more detailed or exhaustive study of this type of data.

- The return cooling water temperatures from the cooling towers at various seasonal average mean wet bulb temperatures were estimated using a tower manufacturer's performance curve for the specified design duty and range. Although the sites had different design wet bulb temperatures (74, 77, 78, and 79 °F), a performance curve based on a design wet bulb temperature of 77 °F was used for all sites in determining the return water temperatures for the various seasonal temperature conditions. This approach was suggested by the tower manufacturer since the effect of the tower design wet bulb temperature is minimal. The site design wet bulb temperature was selected using standard air conditioning design values for temperatures that are exceeded no more than 2 percent of the total hours during a normal summer.
- Curves for LP turbine exhaust pressure correction to the plant output or heat rate were
  matched to turbines with a similar number of LP flow paths and last-stage blade length, as
  listed later in Table 3-2 (page 3-7). However, because of the lack of plant data for each unit,
  predictions of the loss of generation capability due to variations in condenser backpressure
  (due to the introduction of cooling towers) may not be exact, but are typical for plants with a
  similar type of LP turbine.
- The cooling towers were located on the best available vacant area on each site and as close as possible to the power blocks. Vacant areas were determined from USGS site aerial maps that were not necessarily current nor detailed enough to verify all obstacles to installation of towers or piping. Piping lengths were estimated using the assumed tower locations and routings that avoided existing facilities as best as could be determined from the aerial maps.
- Cooling tower blowdown is required to maintain the required quality of the recirculated water and was assumed to be at a flow that would result in a doubling of the concentration of total dissolved solids in the original feedwater. Blowdown containing twice the amount of total dissolved solids of the makeup water is considered typical for seawater cooling tower applications. Based on experience at other sites, treatment of blowdown, other than addition of chemicals to remove chlorine (if used for biological growth control), is not required. Therefore, no treatment plant or extensive equipment is expected for processing the cooling tower blowdown before discharge. Specific site conditions or local restrictions may require more extensive treatment.

A summary of cooling water temperatures (pre- and post-retrofit) is presented in Table 3-1. Although cooling water temperatures increase by 10 °F to 20 °F by adding the cooling towers, this increase does not appear to impact electricity generation to a significant extent (i.e., the annual energy penalty is less than 2 percent) at three of the four plant sites evaluated. Cooling tower retrofit impacts on steam cycle performance, such as reduced generating output, were estimated by using manufacturer's steam turbine performance characteristics for machines that have the same configuration as found in each of the cases evaluated.

	Surry	Hudson	Barney Davis	Big Bend
Seasonal Avg. Ambient Mean Wet Bulb Temp, °F				
Spring	58	46	66	65
Summer	77	66	77	76
Fall	62	52	68	69
Winter	42	31	54	56
Seasonal Avg. River/Bay Water Temp, °F				
Spring	60	51	74	75
Summer	83	75	86	84
Fall	67	58	74	78
Winter	41	36	56	66
Seasonal Avg. CT Return Cold Water Temp, °F				
Spring	72	65	77	77
Summer	85	77	85	84
Fall	75	68	78	79
Winter	62	58	70	71

Table 3-1Seasonal Average Temperatures

Based on available data, it was judged that the steam turbines installed in three of the plants evaluated (Surry, Barney Davis, and Big Bend) do not have sufficiently large last-stage blading to effectively expand the steam to backpressures consistent with condensing temperatures typically achieved with once-through cooling. In theory, reducing cooling water temperature reduces condensing backpressure and increases power output. However, in three of the specific cases evaluated here, the steam turbine generator cannot effectively utilize the reduced condensing backpressure. Only one of the four plants evaluated, Hudson Generating Station, appears to use a turbine design that can effectively utilize lower cooling water temperatures achieved with once-through cooling. A cooling tower retrofit at this plant would increase condensing backpressure (relative to once-through cooling), and thus reduce generation output. This is discussed further in Section 4.1, Discussion of Technical Results.

Principal design parameters for each plant evaluated are summarized in Table 3-2. The condenser and cooling tower design parameters selected for each plant evaluated in this study are presented in Table 3-3.

	Surry 1	Surry 2	Hudson 1	Hudson 2	Barney Davis 1	Barney Davis 2	Big Bend 1	Big Bend 2	Big Bend 3	Big Bend 4
Gross MWe	848	848	455	660	353	351	446	446	446	486
Fuel Type	Nuclear	Nuclear	Gas	Coal	Gas	Gas	Coal	Coal	Coal	Coal
Boiler	PWR	PWR	Supercritical	Supercritical	Subcritical	Subcritical	Subcritical	Subcritical	Subcritical	Subcritical
Steam Press, psig	733	733	3500	3500	2000	2000	2400	2400	2400	24000
Steam Temp, °F	511	511	1000	1000	1000	1000	1000	1000	1000	1000
Reheat Temp, °F	483	483	1025/1050	1025/1050	1000	1000	1000	1000	1000	1000
Steam Flow, million lb/h	10	10	2.5	3.9	2.4	2.4	2.9	2.9	3.1	3.3
Turbine Manufacturer/ LP Configuration	Westing- house/ TC4F44	Westing- house/ TC4F44	Westing- house/ TC4F28	Westing- house/ TC6F28	Westing- house/ TC2F28	GE/ TC2F30	Westing- house/ TC2F31	Westing- house/ TC2F31	GE/ TC2F33.5	GE/ TC4F26
Commercial Operation Date	12/72	5/73	12/64	12/68	5/74	6/76	10/70	4/73	6/76	2/85
Circulating Water Source	Brackish	Brackish	Brackish	Brackish	Seawater	Seawater	Seawater	Seawater	Seawater	Seawater

Table 3-2
<b>Plant Design Bases</b>

Table 3-3
<b>Condenser and Cooling Tower Design Parameters</b>

	Surry 1	Surry 2	Hudson 1	Hudson 2	Barney Davis 1	Barney Davis 2	Big Bend 1	Big Bend 2	Big Bend 3	Big Bend 4
Condenser/CT Duty, MMBtu/h	6,300	6,300	1,630	2,570	1,600	1,600	1,910	1,910	2,020	2,150
Assumed Condenser/ CT Range, °F	15	15	15	15	15	15	15	15	15	15
Assumed Condenser Terminal Temperature Difference, °F	5	5	8	8	8	8	8	8	8	8
CW Flow, gpm	840,000	840,000	220,000	340,000	214,000	214,000	256,000	256,000	270,000	288,000
CT Design Wet Bulb, °F	77	77	74	74	79	79	78	78	78	78
CT Design Approach, °F	8	8	8	8	8	8	8	8	8	8

#### 3.2 COST ESTIMATING AND ECONOMIC CONSIDERATIONS

#### 3.2.1 COST ESTIMATING

Separate cost estimates have been developed for each power plant unit and with total costs calculated for each site. The cost estimates are for a completed retrofit for each facility, with all-new construction and normally supplied services, including indirect costs and contingencies.

The format of each estimate has been arranged to show major cost components and their relative importance. Cost components are not arranged in any particular order of importance. Equipment costs are broken out separately and contain bulk material items. Labor costs cover site craft personnel and associated contractor markups, employee benefits, and supporting supervision, administration, and home office support. Union labor or equivalent prevailing wage rates are implied. No attempt has been made to convert or adjust labor costs for particular areas of the country.

Vendor quotes have been incorporated for major items such as cooling towers, circulating water pipes, and cooling tower pumps on a generic basis due to the lack of specific site design information. Lengths of circulating water piping were scaled from the design sketches superimposed on the aerial photos presented in Section 2. Labor costs associated with these items have been made based on experience with similar items at other sites. Allowances for costs of other items such as demolition, foundations and structures, instruments and controls, electrical, and chemical treatment were made from prior similar estimates.

Allowances for indirect costs have been included in each of the estimates based upon percentage factors. These include temporary construction services and facilities, engineering, construction management, and other professional services, owner costs, and a contingency. An allowance of 20 percent for contingencies has been included since these are existing sites and many interferences are expected. No allowances for escalation or for funds used during construction (AFDC) have been included, as there are no schedule dates considered in this study.

Costs are presented at 2002 levels in thousands of dollars for each category and also dollars per kilowatt. The overall accuracy of the estimates is expected to be  $\pm 40$  percent due to the conceptual nature of the design, in accordance with the Association for the Advancement of Cost Engineering International (AACEI) guidelines. Variances beyond these ranges are possible but not likely.

#### **3.2.2** ECONOMIC CONSIDERATIONS

Separate estimates of changes in operating and maintenance (O&M) costs caused by conversion to cooling towers at each plant have been prepared. An attempt has been made to include all major cost components for each plant.

For most of the plants it is expected that existing personnel can absorb some of the added duties that will be required to operate and maintain the new cooling system equipment. The skill level,

average salaries, burdens, and overhead rates are used to estimate the cost of additional personnel that would be required (see Appendix B).

Supplies have been estimated mostly for the chemicals required for treatment of the makeup water, treatment of the cooling towers and basins, and treatment of blowdown flows prior to their discharge. The costs are similar to those needed in a new fossil plant on a per kilowatt basis.

Maintenance costs have been estimated on a percentage basis of new construction costs. The percentage chosen is an average of the various components involved. For instance, the cooling towers will have a higher percentage of maintenance than the circulating water piping. The costs will vary by year and thus an average value is shown.

The worksheets in Appendix A show the estimated power quantities and costs of the new cooling tower equipment and related systems. Allowances have been made for motor sizes, capacity factors of the existing plant, and the interchange rate for the region. These are new auxiliary loads for the existing plants.

An additional calculation has been made to account for the expected change in plant efficiency due to different cooling water temperatures during the year and their resulting impact on the condenser and turbine operations. The values shown are the average energy penalty over four different seasons of the year.

O&M costs have been grouped into two categories: fixed and variable annual costs. The way that the O&M costs were assigned to each category is described in the worksheets provided in Appendix B.

## 4. RESULTS

#### 4.1 DISCUSSION OF RESULTS

The results of the study indicate that cooling tower retrofits are technically feasible at three of the four plants evaluated: Surry Nuclear Power Plant, Big Bend, and Barney Davis. The addition of cooling towers at the Hudson plant is considered feasible on a provisional basis; serious issues remain that require evaluation. These issues relate to availability of land to locate the cooling towers and route the large-diameter circulating water piping. The requirement for plume abatement at this site exacerbates the space issues, since the plume abatement requirement imposes restrictions on the cooling tower cell array configuration. Towers with plume abatement features added cannot be spaced as closely as towers without this feature.

From an economic perspective, the addition of cooling towers to the evaluated plants poses a significant added cost, both as one-time capital costs and an ongoing increase in the cost of production of electricity. The added costs range from an estimated  $128/kW_e$  for the Surry plant to  $65/kW_e$  at the Hudson plant. The cost of adding cooling towers to nuclear units is significantly higher, on a unit basis, compared to a fossil plant. This is due to the much higher heat rejection to the condenser in a nuclear unit relative to that of a fossil unit, which rejects a significant amount of waste heat to the atmosphere via the stack. Table 4-1 compares the heat rejection at Surry with a typical fossil unit. Note that the heat transfer to the condenser for each of the Surry nuclear units is more than  $1\frac{1}{2}$  times greater per kilowatt of electricity produced.

Plant	Surry Power Station (Nuclear)	Typical Fossil Unit
Efficiency	33.3%	37.5%
Energy Input, MWt	2,550	1,133
Heat to Condenser, MWt	1,650	510
Heat to Stack, MWt	0	149.5
Energy at Generator Terminals, $MW_e$	900	422
Auxiliary Load, MWe	50	24.5
Net Plant Output, MWe	850	397.5
Condenser Heat Rejection/ Net Electric Generation, MWt/MWe	2.0	1.28

Table 4-1Energy Flow Comparison

The annual energy penalty caused by the installation of cooling towers at these four existing plants (see Table 4-2) is estimated to be between 1.1 and 2.1 percent of the power plant output. This loss in salable power (annual energy penalty) is due to increases in condensing backpressure and auxiliary load (cooling tower boost pumps and fans).

	Surry 1	Surry 2	Hudson 1	Hudson 2	Barney Davis 1	Barney Davis 2	Big Bend 1	Big Bend 2	Big Bend 3	Big Bend 4
Gross MWe	848	848	455	660	353	353	446	446	446	486
Generation Capability Impact, MW:										
Spring			0.5	0.8	0.1	.01				1.0
Summer	0.8	0.8	0.5	0.8						
Fall			0.5	0.8	0.2	0.2				0.5
Winter			0.5	0.7						0.5
Yearly Average	0.2	0.2	0.5	0.78	0.08	0.08	0	0	0	0.5
Auxiliary Load Impact, MW:										
Cooling Tower Pumps	7.46	7.46	1.91	2.98	1.91	1.91	2.57	2.57	2.73	2.90
Cooling Tower Fans	9.94	9.94	2.49	3.98	2.49	2.49	2.90	2.90	3.15	3.31
Makeup Water Pumps	0.21	0.21	0.06	0.10	0.06	0.06	0.08	0.08	0.08	0.08
Miscellaneous	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.05
Net Impact on Salable Power, Loss in MW	17.86	17.86	5.01	7.89	4.59	4.59	5.60	5.60	6.01	6.84
Net Impact on Salable Power, Loss in %	2.1	2.1	1.1	1.2	1.3	1.3	1.3	1.3	1.3	1.4

Table 4-2Evaluation Results – Plant Output Effects

The auxiliary power requirements for booster pumps and cooling tower fans associated with the cooling tower retrofits are significant in all four of the cases evaluated accounting for 90 to 100 percent of the estimated annual energy penalty.

In contrast, decreased plant generation output due to condenser/turbine effects of the new cooling systems is smaller than originally anticipated. Surry's capacity decrement due to the new cooling temperatures (and not new plant auxiliary loads) is only 0.002 percent or 200 kW per unit. The losses at Barney Davis and Big Bend are equally small. The Hudson plant can anticipate a loss of almost 0.7 percent, or 7,500 kW<sub>e</sub> for both units combined. However, the decrease in net plant generation output due to increased auxiliary load is much more significant, and ranges from about 1 percent for the fossil units to about 2 percent for the nuclear units (Surry).

Decreases in the performance of the steam turbines because of the change from once-through cooling to recirculated cooling water were a minor contributor to the overall energy penalty due to the factors listed below.

- First, it appears that most of the plants evaluated (except Hudson) were designed with relatively high turbine exhaust velocities. Operation on a cooling tower would shift the condensing backpressure up, and exhaust velocity down. The reduction in exhaust velocity results in lower exhaust power losses, which tends to mitigate, but not completely compensate for, any reduction in generation output caused by the higher backpressure.
- Second, the cooling tower retrofits were designed with the same condenser temperature rise (nominally 15 °F). This tends to maintain low condensing backpressures, relative to units operating with higher temperature rises.
- Third, the cooling water temperatures for the original once-through cooling water systems tend to be high; cooling water from an evaporative tower designed with a typical design basis approach (difference in temperature between cold water temperature leaving the tower and the ambient wet bulb temperature) was relatively close to the once-through cooling water temperature during the summer months. During winter, spring, and fall the differences in cold water temperatures available to the plant condensers tend to diverge (between once-through vs. cooling tower cases of each plant). However, the Surry, Barney Davis, and Big Bend plants are not significantly impacted by increased cooling water temperatures over the range of temperatures encountered in the study due to turbine characteristics referred to above.

Technical parameters describing the retrofit cooling towers and circulating water piping for each unit that was evaluated are presented in Table 4-3.

#### 4.2 CAPITAL COST AND OPERATING COST RESULTS

From an economic perspective, the retrofit of cooling towers to the evaluated plants poses a significant added cost, both as one-time capital costs and an ongoing increase in the cost of production of electricity.

	Surry 1	Surry 2	Hudson 1	Hudson 2	Barney Davis 1	Barney Davis 2	Big Bend 1	Big Bend 2	Big Bend 3	Big Bend 4
CW Pipe Diameter, in.	144	144	108	120	108	108	120	120	120	120
Length of CW Pipe, ft	12,000	12,000	4,000	4,000	4,000	4,000	7,000	7,000	7,000	7,000
Total CT Pump Flow, gpm	840,000	840,000	220,000	340,000	214,000	214,000	256,000	256,000	270,000	288,000
CT Pump Head, ft	35	35	35	35	35	35	40	40	40	40
Total CT Pump Horsepower, bhp	9,000	9,000	2,300	3,600	2,300	2,300	3,100	3,100	3,300	3,500
CT Makeup Water Flow, gpm	20,000	20,000	6,000	9,000	6,000	6,000	7,000	7,000	7,000	7,000
CT Makeup Water Pump Horsepower, bhp	250	250	75	125	75	75	100	100	100	100
Number of Modular 60 ft x 66 ft CT Cells	4 clusters of 12	4 clusters of 12	12	19	12	12	14	14	15	16
CT Total Fan, bhp	12,000	12,000	3,000	4,800	3,000	3,000	3,500	3,500	3,800	4,000
Plume Abatement	No	No	Yes	Yes	No	No	No	No	No	No
Cell Arrangement	Cluster	Cluster	Inline	Inline	Inline	Inline	Inline	Inline	Inline	Inline
CT Plan Area, L (ft) x W (ft)	4 clusters at 250 x 250	4 clusters at 250 x 250	726 x 66	1150 x 66	726 x 66	726 x 66	847 x 66	847 x 66	908 x 66	968 x 66

Table 4-3Evaluation Results – Technical Parameters

A summary of the results of the assessment of capital costs and other economic considerations is shown on Table 4-4.

Plant Name	Unit No.	Capital Costs, \$/kW	Fixed Oper. Costs, \$/MW	Variable Oper. Costs <sup>1</sup> , \$/MWh	Annual Energy Penalty <sup>2</sup> , %
Surry Nuclear Plant	1	\$128	\$655	\$0.885	2.1
	2	\$128	\$655	\$0.885	2.1
	Total	\$128	\$655	\$0.885	2.1
Big Bend	1	\$75	\$411	\$0.617	1.3
	2	\$75	\$411	\$0.617	1.3
	3	\$77	\$418	\$0.642	1.3
	4	\$72	\$391	\$0.636	1.4
	Total	\$75	\$407	\$0.628	1.3
Barney Davis	1	\$67	\$371	\$0.623	1.3
	2	\$67	\$373	\$0.625	1.3
	Total	\$67	\$372	\$0.624	1.3
Hudson	1	\$68	\$371	\$0.540	1.1
	2	\$65	\$347	\$0.558	1.2
	Total	\$66	\$357	\$0.551	1.2

 Table 4-4

 Summary of Capital and Operating Costs – All Plants

Notes:

<sup>1</sup> Includes cost of added electric power consumption for new pumps and cooling tower fans.

<sup>2</sup> Energy penalty shown includes condenser backpressure effect on generation and the reduction in salable power due to increased auxiliary load.

Detailed capital cost estimates for each unit and plant are contained in Appendix A. The total cost per plant ranges from \$23 million to \$108 million or from \$65 per kW to \$128 per kW. As expected, the Surry Nuclear Plant has the highest cost due to its large (848 MW) size per unit and high rate of heat rejection. However, two additional factors contributed to the high cost of this plant: the use of clustered cooling towers to minimize the required land space and distance of the towers from the plant, and, secondly, the long runs of circulating water pipes to the available open areas for the towers.

The costs to retrofit cooling towers at the fossil units are relatively close to each other at \$65 to \$77 per kW. The installed cost of both the cooling towers and the circulating water pipe account for approximately 60 percent of the direct costs. The foundations and structures account for almost another 20 percent of direct costs.

The Hudson site cost estimate includes plume abatement technology and costs due to its location. This factor increases the cost of the towers by about 100 percent or an additional \$12 million of
direct costs. This had the effect of increasing the total capital cost of the installation by 22.5 percent. The Barney Davis, Surry, and Big Bend sites were not determined to need plume abatement due to their location.

The detailed calculations for annual O&M costs associated with cooling towers for each unit and plant are contained in Appendix B. Operating costs for each of the nuclear units is expected to increase about \$5.8 million per year. About 60 percent of this increase is for new auxiliary power requirements to run pumps and fans. The remaining 40 percent is for additional operators and supplies. About 90 percent of the O&M costs are considered variable costs.

Operating costs for each of the fossil units is expected to increase by about \$1.5 to \$2.0 million per year. About 50 percent of the new costs are for new plant auxiliary loads for fans and pumping. About 90 percent of the fossil O&M costs are for variable costs.

If construction of the retrofit cooling tower system would require an extended outage, costs could increase significantly. However, it is the opinion of the Parsons engineering staff that construction and startup of new cooling tower systems at the Surry and Barney Davis sites would not result in extended outages. With proper planning and coordination with other planned outages, cutover from the older cooling systems to the new cooling towers could be accomplished without loss of generating time. This has been the experience with other plants. Therefore, the analysis shows no cost penalty for extended outages at this time.

The situation is less certain at the Hudson and Big Bend sites. The configuration of the existing site for each of these two cases makes it difficult to assess the need for extended construction outages without more detailed site information and study.

The data presented in Appendix B of this report reflect no outage. However, should it be determined upon further review and a more detailed analysis of system locations, that an extraordinary outage will be required as part of a cooling tower retrofit, the following loss of revenues can be expected <u>per plant</u> (i.e., all units) per month:

- Surry... \$30 million per month
- Hudson... \$16 million per month
- Barney Davis... \$11 million per month
- Big Bend... \$28 million per month

To determine these losses in revenues, a conservative assumption of \$0.030/kWh was used as the value of the lost power generation each plant would suffer as a result of an extended cooling tower retrofit outage. The calculation was also based on each plant's peak net summer power output.

## 5. CONCLUSIONS

The conclusions reached from this study based on assumptions about, and analysis of, four "real world" power plants indicate that the retrofit of evaporative cooling towers to an electric generating plant, fossil or nuclear, imposes a significant burden in terms of capital costs (\$65 to \$128 per kW) and loss of net generation output (1.1 to 2.1 percent of plant electricity generation). The capital cost expenditure reflects the cost of the cooling towers, circulating water piping, and related ancillary items such as added circulating water booster and makeup pumps. The loss of salable power is due to the added auxiliary electrical load, and for certain plants, a decrement in electric generation caused by operation at higher condensing backpressures.

Operating costs are estimated to increase about \$5.8 million per year for the nuclear unit studied and about \$1.5 to \$2.0 million per year for the fossil energy units studied. More than half of the increase in operating costs is for new auxiliary power requirements to run new pumps and cooling tower fans.

The loss of revenue due to an extended outage to accommodate a cooling tower retrofit is a potential issue. In the current study, two plants (Surry and Barney Davis) appear to be able to avoid an extension to a normal annual outage to enable the changeover to be accomplished; the other two plants (Hudson and Big Bend) have more restrictive site arrangements and may require outage extensions.

When considering a recirculating wet cooling tower retrofit to an existing once-through cooled facility, there are several significant site-specific issues and assumptions that must be fully analyzed a priori. Among these issues are effect on turbine performance, increased plant parasitic power losses, land space consideration, tower size and type, permitting restrictions, tower plume and noise abatement, and tower drift loss control.

A series of these assumptions was made to facilitate the analysis of a prospective cooling tower retrofit at the four power plant sites documented in this study. These assumptions were based on the collective experience of the Parsons engineering staff, drawing on a large number of power plant design experiences spanning the last several decades. Changes to these assumptions will affect the detailed performance and cost data presented herein, but will most likely not affect the validity of the conclusions expressed. The effect of deviations from each assumption is briefly discussed below:

### Cooling Water Temperature Rise

The assumption made in this study was to maintain the original temperature rise of 15 °F. If the cooling tower retrofit were to be based on a value of 20 °F, for example (a value typically used in new power plant cooling tower installations), the capital cost of the cooling tower might decrease somewhat, but generation output might also be diminished. A more detailed study, beyond the scope of the present effort, is required to select the optimum design value.

### Steam Flow to Condenser

A typical value for the fraction of throttle steam flow passed to the condenser after expansion in the steam turbine of 65 percent was assumed. Variations of plus or minus 10 percent in this flow rate are not expected to change any of the results of this study. Larger changes would require evaluation on an individual plant basis.

### Seasonal Average Temperatures for Cooling Water and Ambient Wet Bulb Temperatures

The use of seasonal average temperatures instead of monthly averages is not expected to impact the results developed by this study.

### Steam Turbine Exhaust Pressure Correction

The steam turbine exhaust physical design parameters coupled with condensing steam flow rates have a significant impact on steam turbine generator electric output and plant efficiency. The estimate of performance impacts due to cooling tower retrofits presented in this report is based on the assumption that the reported turbine configuration is correct for each plant. Changes in turbine configuration used in this study to alternate configurations (number of low-pressure flow paths and/or last-stage blade lengths) could have a significant impact on the predicted change in generation output.

### Cooling Tower Siting

For this study, the cooling towers were sited on the closest available open land near the steam turbine generator building. If these lands were not suitable or available, and the towers were located further away, piping costs would increase.

#### Cooling Tower Blowdown

The report assumes that extensive and/or expensive treatment of cooling tower blowdown is not required. If specific site conditions mandate high degrees of treatment for the blowdown, the capital and operating costs of the retrofit will increase, but are not expected to increase to a level that will compromise the overall economics of the cooling tower retrofit.

Overall, any requirement to retrofit closed circuit cooling towers to plants that now utilize oncethrough cooling could have significant operational and financial impacts. If the motivation for this change is due to water intake concerns, other engineering solutions that modify the inlet designs should be investigated.

# **APPENDIX A**

# CAPITAL COST ESTIMATE

	Parsons Corporation <b>Client:</b> U.S. DOE NETL <b>Project:</b> Proposed Section 316b Coc	ling Tower Retrofi	its	Date: Proj. No.	1/31/2002 50802
	CAPITAL COST ESTIMATE	2002 Dollars X 10	000	Conceptual	
	Surry Nuclear Power Plant - Unit #1 -	848 MW	848	MW	
Acct No.	Item/Description	Equip Cost	Labor Cost	Total <b>Cost</b>	Avg. \$/KW
1	Demolition & Sitework	\$50	\$450	\$500	1
2	Foundations & Structures	\$2,940	\$6,860	\$9,800	12
3	Cooling Towers ( clustered)	\$28,800	\$9,600	\$38,400	45
4	Mechanical Equipment	\$3,300	\$660	\$3,960	5
5	Piping Systems	\$8,294	\$12,442	\$20,736	24
6	Instruments & Controls	\$500	\$500	\$1,000	1
7	Accessory Electrical Systems	\$2,500	\$2,500	\$5,000	6
8	Chemical Treatment	\$500	\$500	\$1,000	1
9	Miscellaneous	\$500	\$500	\$1,000	1
10	Open	\$0	\$0	\$0	0
11	Open	\$0	\$0	\$0	0
12	Open	\$0	\$0	\$0	0
13	Open	\$0	\$0	\$0	0
14	Open	\$0	\$0	\$0	0
	SUBTOTAL DIRECT COST	\$47,384	\$34,012	\$81,396	96
INDIRE	CT COSTS				0
	Temporary Construction Services and	Facilities		1,628	2
	ENGINEERING, CM, PROFESSION	AL SERVICES		6,512	8
	OWNER COSTS			814	1
	SUBTOTAL INDIRECT COST			8,954	11
	CONTINGENCY @ _20%			18,070	21
	ESCALATION @0% PER YE	EAR		0	0
	AFDC0% FOR0YEAR	S		0	0
		TOTAL COST		108,419	128
	Accuracy =+/- 40%				Page 1

### **APPENDIX A – CAPITAL COST ESTIMATE**

	Parsons Corporation <b>Client:</b> U.S. DOE NETL <b>Project:</b> Proposed Section 316b Coc	bling Tower Retrof	its	Date: Proj. No.	1/31/2002 50802	
	CAPITAL COST ESTIMATE	2002 Dollars X 10	000	Conceptual		
	Surry Nuclear Power Plant - Unit # 2 -	- 848 MW	848	MW		
Acct No.	Item/Description	Equip Cost	Labor Cost	Total <b>Cost</b>		Avg. \$/KW
1	Demolition & Sitework	50	450	500		1
2	Foundations & Structures	\$2,940	\$6,860	9,800		12
3	Cooling Towers ( clustered)	\$28,800	\$9,600	38,400		45
4	Mechanical Equipment	\$3,300	\$660	3,960		5
5	Piping Systems	\$8,294	\$12,442	20,736		24
6	Instruments & Controls	500	500	1,000		1
7	Accessory Electrical Systems	2,500	2,500	5,000		6
8	Chemical Treatment	500	500	1,000		1
9	Miscellaneous	500	500	1,000		1
10	Open	0	0	0		0
11	Open	0	0	0		0
12	Open	0	0	0		0
13	Open	0	0	0		0
14	Open	0	0	0		0
	SUBTOTAL DIRECT COST	47,384	34,012	81,396		96
INDIRE	CT COSTS					0
	Temporary Construction Servicesand	Facilities		1,628		2
	ENGINEERING+B44, CM, PROFESS	SIONAL SERVICE	S	6,512		8
	OWNER COSTS			814		1
	SUBTOTAL INDIRECT COST			8,954		11
	CONTINGENCY @ _20%			18,070		21
	ESCALATION @0% PER YE	EAR		0		
	AFDC0% FOR0YEAR	S		0		0
		TOTAL COST		108,419		128
	Accuracy =+/- 40%				Page 2	

	Parsons Corporation <b>Client:</b> U.S. DOE NETL <b>Project:</b> Proposed Section 316b Coc	ling Tower Retrofi	ts	Date: Proj. No.	1/31/2002 50802
	CAPITAL COST ESTIMATE	2002 Dollars X 10	00	Conceptual	
	Surry Nuclear Power Plant Both Units #1 & #2 - 848 MW Each		1,696	MW	
Acct No.	Item/Description	Equip Cost	Labor Cost	Total <b>Cost</b>	Avg. \$/KW
1	Demolition & Sitework	100	900	1,000	1
2	Foundations & Structures	5,880	13,720	19,600	12
3	Cooling Towers ( clustered)	57,600	19,200	76,800	45
4	Mechanical Equipment	6,600	1,320	7,920	5
5	Piping Systems	16,589	24,883	41,472	24
6	Instruments & Controls	1,000	1,000	2,000	1
7	Accessory Electrical Systems	5,000	5,000	10,000	6
8	Chemical Treatment	1,000	1,000	2,000	1
9	Miscellaneous	1,000	1,000	2,000	1
10	Open	0	0	0	0
11	Open	0	0	0	0
12	Open	0	0	0	0
13	Open	0	0	0	0
14	Open	0	0	0	0
	SUBTOTAL DIRECT COST	94,769	68,023	162,792	96
INDIRE	CT COSTS				0
	Temporary Construction Servicesand	Facilities		3,256	2
	ENGINEERING, CM, PROFESSION	AL SERVICES		13,023	8
	OWNER COSTS			1,628	1
	SUBTOTAL INDIRECT COST			17,907	11
	CONTINGENCY @ _20%			36,140	21
	ESCALATION @0% PER YE	EAR		0	0
	AFDC0% FOR0YEAR	S		0	0
		TOTAL COST		216,839	128
	Accuracy =+/- 40%				Page 3

	Parsons Corporation <b>Client:</b> U.S. DOE NETL <b>Project:</b> Proposed Section 316b Coc	ling Tower Retrof	ïits	Date: Proj. No.	1/31/2002 50802
	CAPITAL COST ESTIMATE	2002 Dollars X 1	000	Conceptual	
	Big Bend Coal Fired Power Plant - Ur	iit #1 - 446 MW	446	MW	
Acct No.	Item/Description	Equip Cost	Labor Cost	Total <b>Cost</b>	Avg. \$/KW
1	Demolition & Sitework	25	225	250	1
2	Foundations & Structures	1,170	2,730	3,900	9
3	Cooling Towers	4,200	1,400	5,600	13
4	Mechanical Equipment	1,190	238	1,428	3
5	Piping Systems	\$4,032	\$6,048	10,080	23
6	Instruments & Controls	250	250	500	1
7	Accessory Electrical Systems	1,250	1,250	2,500	6
8	Chemical Treatment	250	250	500	1
9	Miscellaneous	250	250	500	1
10	Open	0	0	0	0
11	Open	0	0	0	0
12	Open	0	0	0	0
13	Open	0	0	0	0
14	Open	0	0	0	0
	SUBTOTAL DIRECT COST	12,617	12,641	25,258	57
INDIRE	CT COSTS				0
	Temporary Construction Services and	Facilities		505	1
	ENGINEERING, CM, PROFESSION	AL SERVICES		2,021	5
	OWNER COSTS			253	1
	SUBTOTAL INDIRECT COST			2,778	6
	CONTINGENCY @ _20%			5,607	13
	ESCALATION @0% PER YE	EAR		0	0
	AFDC0% FOR0YEAR	S		0	0
		TOTAL COST		33,644	0 75
	Accuracy =+/- 40%		Page 1		

	Parsons Corporation <b>Client:</b> U.S. DOE NETL <b>Project:</b> Proposed Section 316b Coc	ling Tower Retrofi	ts	Date: Proj. No.	1/31/2002 50802
	CAPITAL COST ESTIMATE	2002 Dollars X 10	000	Conceptual	
	Big Bend Coal Fired Power Plant - Ur	nit #2 - 446 MW	446	MW	
Acct No.	Item/Description	Equip Cost	Labor Cost	Total <b>Cost</b>	Avg. \$/KW
1	Demolition & Sitework	25	225	250	1
2	Foundations & Structures	1,170	2,730	3,900	9
3	Cooling Towers	4,200	1,400	5,600	13
4	Mechanical Equipment	1,190	238	1,428	3
5	Piping Systems	\$4,032	\$6,048	10,080	23
6	Instruments & Controls	250	250	500	1
7	Accessory Electrical Systems	1,250	1,250	2,500	6
8	Chemical Treatment	250	250	500	1
9	Miscellaneous	250	250	500	1
10	Open	0	0	0	0
11	Open	0	0	0	0
12	Open	0	0	0	0
13	Open	0	0	0	0
14	Open	0	0	0	0
	SUBTOTAL DIRECT COST	12,617	12,641	25,258	57
INDIRE	CT COSTS				0
	Temporary Construction Servicesand	Facilities		505	1
	ENGINEERING+B44, CM, PROFESS	SIONAL SERVICE	S	2,021	5
	OWNER COSTS			253	1
	SUBTOTAL INDIRECT COST			2,778	6
	CONTINGENCY @ _20%			5,607	13
	ESCALATION @0% PER YE	EAR		0	
	AFDC0% FOR0YEAR	S		0	0
		TOTAL COST		33,644	75
	Accuracy =+/- 40%				Page 2

	Parsons Corporation Client:U.S. DOE NETL Project: Proposed Section 316b Coc	ling Tower Retrof	its	Date: Proj. No.	1/31/2002 50802
	CAPITAL COST ESTIMATE	2002 Dollars X 1	000	Conceptual	
	Big Bend Coal Fired Power Plant - Ur	446	MW		
Acct No.	Item/Description	Equip Cost	Labor Cost	Total <b>Cost</b>	Avg. \$/KW
1	Demolition & Sitework	25	225	250	1
2	Foundations & Structures	1,200	2,800	4,000	9
3	Cooling Towers	4,500	1,500	6,000	13
4	Mechanical Equipment	1,190	238	1,428	3
5	Piping Systems	\$4,032	\$6,048	10,080	23
6	Instruments & Controls	250	250	500	1
7	Accessory Electrical Systems	1,250	1,250	2,500	6
8	Chemical Treatment	250	250	500	1
9	Miscellaneous	250	250	500	1
10	Open	0	0	0	0
11	Open	0	0	0	0
12	Open	0	0	0	0
13	Open	0	0	0	0
14	Open	0	0	0	0
	SUBTOTAL DIRECT COST	12,947	12,811	25,758	58
INDIRE	CT COSTS				0
	Temporary Construction Services and	Facilities		515	1
	ENGINEERING, CM, PROFESSION	AL SERVICES		2,061	5
	OWNER COSTS			258	1
	SUBTOTAL INDIRECT COST			2,833	6
	CONTINGENCY @ _20%			5,718	13
	ESCALATION @0% PER YE	EAR		0	0
	AFDC0% FOR0YEAR	S		0	0
		TOTAL COST		34,310	77
	Accuracy =+/- 40%				Page 3

	Parsons Corporation <b>Client:</b> U.S. DOE NETL <b>Project:</b> Proposed Section 316b Coc	oling Tower Retrofi	ts	Date: Proj. No.	1/31/2002 50802
	CAPITAL COST ESTIMATE	2002 Dollars X 10	00	Conceptual	
	Big Bend Coal Fired Power Plant - Ur	nit #4 - 486 MW	486	MW	
Acct No.	Item/Description	Equip Cost	Labor Cost	Total <b>Cost</b>	Avg. \$/KW
1	Demolition & Sitework	25	225	250	1
2	Foundations & Structures	1,230	2,870	4,100	8
3	Cooling Towers	4,800	1,600	6,400	13
4	Mechanical Equipment	1,190	238	1,428	3
5	Piping Systems	\$4,032	\$6,048	10,080	21
6	Instruments & Controls	250	250	500	1
7	Accessory Electrical Systems	1,250	1,250	2,500	5
8	Chemical Treatment	250	250	500	1
9	Miscellaneous	250	250	500	1
10	Open	0	0	0	0
11	Open	0	0	0	0
12	Open	0	0	0	0
13	Open	0	0	0	0
14	Open	0	0	0	0
	SUBTOTAL DIRECT COST	13,277	12,981	26,258	54
INDIRE	CT COSTS				0
	Temporary Construction Servicesand	Facilities		525	1
	ENGINEERING+B44, CM, PROFESS	SIONAL SERVICE	3	2,101	4
	OWNER COSTS			263	1
	SUBTOTAL INDIRECT COST			2,888	6
	CONTINGENCY @ _20%			5,829	12
	ESCALATION @0_% PER YE	EAR		0	0
	AFDC0% FOR0YEAR	S		0	0
		TOTAL COST		34,976	72
1	Accuracy =+/- 40%				Page 4

	Parsons Corporation <b>Client:</b> U.S. DOE NETL <b>Project:</b> Proposed Section 316b Coc	ling Tower Retrof	its	Date: Proj. No.	1/31/2002 50802
	CAPITAL COST ESTIMATE	2002 Dollars X 10	000	Conceptual	
	Big Bend Coal Fired Power Plants - Unit #1, #2, #3 @ 446 MW & #4 @ 48	36 MW	1,824	MW	
Acct No.	Item/Description	Equip Cost	Labor Cost	Total <b>Cost</b>	Avg. \$/KW
1	Demolition & Sitework	100	900	1,000	1
2	Foundations & Structures	4,770	11,130	15,900	9
3	Cooling Towers	17,700	5,900	23,600	13
4	Mechanical Equipment	4,760	952	5,712	3
5	Piping Systems	16,128	24,192	40,320	22
6	Instruments & Controls	1,000	1,000	2,000	1
7	Accessory Electrical Systems	5,000	5,000	10,000	5
8	Chemical Treatment	1,000	1,000	2,000	1
9	Miscellaneous	1,000	1,000	2,000	1
10	Open	0	0	0	0
11	Open	0	0	0	0
12	Open	0	0	0	0
13	Open	0	0	0	0
14	Open	0	0	0	0
	SUBTOTAL DIRECT COST	51,458	51,074	102,532	56
INDIRE	CT COSTS				0
	Temporary Construction Servicesand	Facilities		2,051	1
	ENGINEERING, CM, PROFESSION	AL SERVICES		8,203	4
	OWNER COSTS			1,025	1
	SUBTOTAL INDIRECT COST			11,279	6
	CONTINGENCY @ _20%			22,762	12
	ESCALATION @0_% PER YI	EAR		0	0
	AFDC0% FOR0YEAR	S		0	0
		TOTAL COST		136,573	75
	Accuracy =+/- 40%				Page 5

	Parsons Corporation Client:U.S. DOE NETL Project: Proposed Section 316b Cooling	Tower Retrofits		Date: Proj. No.	1/31/2002 50802
	CAPITAL COST ESTIMATE	2002 Dollars X 10	00	Conceptual	
	Barney Davis Gas Fired Power Plant - Unit	#1 - 353 MW	353	MW	
Acct No.	Item/Description	Equip Cost	Labor Cost	Total Cost	Avg. \$/KW
1	Demolition & Sitework	20	180	200	1
2	Foundations & Structures	960	2,240	3,200	9
3	Cooling Towers	3,600	1,200	4,800	14
4	Mechanical Equipment	920	184	1,104	3
5	Piping Systems	2,074	3,110	5,184	15
6	Instruments & Controls	200	200	400	1
7	Accessory Electrical Systems	1,000	1,000	2,000	6
8	Chemical Treatment	200	200	400	1
9	Miscellaneous	200	200	400	1
10	Open	0	0	0	0
11	Open	0	0	0	0
12	Open	0	0	0	0
13	Open	0	0	0	0
14	Open	0	0	0	0
	SUBTOTAL DIRECT COST	9,174	8,514	17,688	50
INDIREC	T COSTS				0
	Temporary Construction Services and Facili	ties		354	1
	ENGINEERING, CM, PROFESSIONAL SEF	RVICES		1,415	4
	OWNER COSTS			177	1
	SUBTOTAL INDIRECT COST			1,946	6
	CONTINGENCY @ _20%			3,927	11
	ESCALATION @0% PER YEAR			0	0
	AFDC0% FOR0YEARS			0	0
		TOTAL COST		23,560	67
	Accuracy =+/- 40%				Page 1

	Parsons Corporation Client:U.S. DOE NETL Project: Proposed Section 316b Cooling	Tower Retrofits		Date: Proj. No.	1/31/2002 50802
	CAPITAL COST ESTIMATE	2002 Dollars X 100	00	Conceptual	
	Barney Davis Gas Fired Power Plant - Unit #	MW			
Acct No.	Item/Description	Equip Cost	Labor Cost	Total <b>Cost</b>	Avg. \$/KW
1	Demolition & Sitework	20	180	200	1
2	Foundations & Structures	960	2,240	3,200	9
3	Cooling Towers	3,600	1,200	4,800	14
4	Mechanical Equipment	920	184	1,104	3
5	Piping Systems	2,074	3,110	5,184	15
6	Instruments & Controls	200	200	400	1
7	Accessory Electrical Systems	1,000	1,000	2,000	6
8	Chemical Treatment	200	200	400	1
9	Miscellaneous	200	200	400	1
10	Open	0	0	0	0
11	Open	0	0	0	0
12	Open	0	0	0	0
13	Open	0	0	0	0
14	Open	0	0	0	0
	SUBTOTAL DIRECT COST	9,174	8,514	17,688	50
INDIREC	T COSTS				0
	Temporary Construction Servicesand Facilit	ies		354	1
	ENGINEERING+B44, CM, PROFESSIONAL	L SERVICES		1,415	4
	OWNER COSTS			177	1
	SUBTOTAL INDIRECT COST			1,946	6
	CONTINGENCY @ _20%			3,927	11
	ESCALATION @0% PER YEAR			0	
	AFDC0% FOR0YEARS			0	0
		TOTAL COST		23,560	67
	Accuracy =+/- 40%				Page 2

	Parsons Corporation Client:U.S. DOE NETL Project: Proposed Section 316b Cooling	Tower Retrofits		Date: Proj. No.	1/31/2002 50802
	CAPITAL COST ESTIMATE	2002 Dollars X 10	00	Conceptual	
	Barney Davis Gas Fired Power Plants - Unit #1 @ 353 MW & #2 @ 351 MW		704	MW	
Acct No.	Item/Description	Equip Cost	Labor Cost	Total <b>Cost</b>	Avg. \$/KW
1	Demolition & Sitework	40	360	400	1
2	Foundations & Structures	1,920	4,480	6,400	9
3	Cooling Towers	7,200	2,400	9,600	14
4	Mechanical Equipment	1,840	368	2,208	3
5	Piping Systems	4,147	6,221	10,368	15
6	Instruments & Controls	400	400	800	1
7	Accessory Electrical Systems	2,000	2,000	4,000	6
8	Chemical Treatment	400	400	800	1
9	Miscellaneous	400	400	800	1
10	Open	0	0	0	0
11	Open	0	0	0	0
12	Open	0	0	0	0
13	Open	0	0	0	0
14	Open	0	0	0	0
	SUBTOTAL DIRECT COST	18,347	17,029	35,376	50
INDIREC	T COSTS				0
	Temporary Construction Servicesand Facilit	ies		708	1
	ENGINEERING, CM, PROFESSIONAL SE	RVICES		2,830	4
	OWNER COSTS			354	1
	SUBTOTAL INDIRECT COST			3,891	6
	CONTINGENCY @ _20%			7,853	11
	ESCALATION @0% PER YEAR			0	0
	AFDC0% FOR0YEARS			0	0
		TOTAL COST		47,121	67
	Accuracy =+/- 40%				Page 3

	Parsons Corporation <b>Client:</b> U.S. DOE NETL <b>Project:</b> Proposed Section 316b Coc	bling Tower Retrofi	ts	Date: Proj. No.	1/31/2002 50802
	CAPITAL COST ESTIMATE	2002 Dollars X 10	000	Conceptual	
	Hudson Gas Fired Power Plant - Unit	#1 - 455 MW	455	MW	
Acct No.	Item/Description	Equip Cost	Labor Cost	Total <b>Cost</b>	Avg. \$/KW
1	Demolition & Sitework	25	225	250	1
2	Foundations & Structures	1,110	2,590	3,700	8
3	Cooling Towers w/ Plume Abate.	7,200	2,400	9,600	21
4	Mechanical Equipment	920	184	1,104	2
5	Piping Systems	2,074	2,333	4,406	10
6	Instruments & Controls	250	250	500	1
7	Accessory Electrical Systems	1,250	1,250	2,500	5
8	Chemical Treatment	250	250	500	1
9	Miscellaneous	250	250	500	1
10	Open	0	0	0	0
11	Open	0	0	0	0
12	Open	0	0	0	0
13	Open	0	0	0	0
14	Open	0	0	0	0
	SUBTOTAL DIRECT COST	13,329	9,732	23,060	51
INDIRE	CT COSTS				0
	Temporary Construction Services and	d Facilities		461	1
	ENGINEERING, CM, PROFESSION/	AL SERVICES		1,845	4
	OWNER COSTS			231	1
	SUBTOTAL INDIRECT COST			2,537	6
	CONTINGENCY @ _20%			5,119	11
	ESCALATION @0% PER YI	EAR		0	0
	AFDC0% FOR0YEAR	S		0	0
		TOTAL COST		30,716	68
	Accuracy =+/- 40%				Page 1

	Parsons Corporation Client:U.S. DOE NETL Project: Proposed Section 316b Coc	bling Tower Retrofi	ts	Date: Proj. No.	1/31/2002 50802		
	CAPITAL COST ESTIMATE	2002 Dollars X 10	000	Conceptual			
	Hudson Coal Fired Power Plant - Unit	t #2 - 660 MW	660	MW			
Acct No.	Item/Description	Equip Cost	Labor Cost	Total <b>Cost</b>	Avg. \$/KW		
1	Demolition & Sitework	30	300	330	1		
2	Foundations & Structures	1,620	3,780	5,400	8		
3	Cooling Towers w/ Plume Abate.	11,400	3,800	15,200	23		
4	Mechanical Equipment	1,260	252	1,512	2		
5	Piping Systems	2,304	2,592	4,896	7		
6	Instruments & Controls	300	300	600	1		
7	Accessory Electrical Systems	1,500	1,500	3,000	5		
8	Chemical Treatment	300	300	600	1		
9	Miscellaneous	300	300	600	1		
10	Open	0	0	0	0		
11	Open	0	0	0	0		
12	Open	0	0	0	0		
13	Open	0	0	0	0		
14	Open	0	0	0	0		
	SUBTOTAL DIRECT COST	19,014	13,124	32,138	49		
INDIRE	CT COSTS				0		
	Temporary Construction Servicesand	Facilities		643	1		
	ENGINEERING+B44, CM, PROFESS	SIONAL SERVICE	S	2,571	4		
	OWNER COSTS		321	0			
	SUBTOTAL INDIRECT COST		3,535	5			
	CONTINGENCY @ _20%		7,135	11			
	ESCALATION @0% PER YI	ESCALATION @0 PER YEAR					
	AFDC0% FOR0YEAR		0	0			
		TOTAL COST		42,808	65		
	Accuracy =+/- 40%				Page 2		

	Parsons Corporation <b>Client:</b> U.S. DOE NETL <b>Project:</b> Proposed Section 316b Coc	bling Tower Retrofit	S	Date: Proj. No.	1/31/2002 50802
	CAPITAL COST ESTIMATE	2002 Dollars X 10	00	Conceptual	
	Hudson Power Plants - Unit #1 Gas @ 455 MW & #2 Coal (	@ 660 MW	1,115	MW	
Acct No.	Item/Description	Equip Cost	Labor Cost	Total <b>Cost</b>	Avg. \$/KW
1	Demolition & Sitework	55	525	580	1
2	Foundations & Structures	2,730	6,370	9,100	8
3	Cooling Towers w/ Plume Abate.	18,600	6,200	24,800	22
4	Mechanical Equipment	2,180	436	2,616	2
5	Piping Systems	4,378	4,925	9,302	8
6	Instruments & Controls	550	550	1,100	1
7	Accessory Electrical Systems	2,750	2,750	5,500	5
8	Chemical Treatment	550	550	1,100	1
9	Miscellaneous	550	550	1,100	1
10	Open	0	0	0	0
11	Open	0	0	0	0
12	Open	0	0	0	0
13	Open	0	0	0	0
14	Open	0	0	0	0
	SUBTOTAL DIRECT COST	32,343	22,856	55,198	50
INDIRE	CT COSTS				
	Temporary Construction Servicesand	Facilities		1,104	1
	ENGINEERING, CM, PROFESSION	AL SERVICES		4,416	4
	OWNER COSTS			552	0
	SUBTOTAL INDIRECT COST			6,072	5
	CONTINGENCY @ _20%			12,254	11
	ESCALATION @0% PER YI	EAR		0	0
	AFDC0% FOR0YEAR		0	0	
		TOTAL COST		73,524	66
	Accuracy =+/- 40%				Page 3

# **APPENDIX B**

# **O&M COST ESTIMATE**

	Parsons Corporation Client:_U.S. D Project: Propo	OOE NETL sed Section 316b Coolir	ng Tower Re	trofits			Date: Proj. No.	1/31/2002 50802
	O & M COST I	ESTIMATE	2	2002 Dollars			Conceptual	
	Surry Nuclear	Power Plant - Unit #1 - 8	48 MW			848	MW	
Α.	Operators	Туре	No - FTE	\$/ Yr	Burden	ОН	Annual Cost	
		Unskilled	0.2	\$20,000	0.5	0.25	\$7,500	
		Skilled	0.1	\$30,000	0.5	0.25	\$5,625	
		Supv	0	\$40,000	0.5	0.25	\$0 \$0	
		Admin	0	\$20,000	0.5 Subtotal	0.25	13 125	
							,.=0	
В.	Supplies	Makeup & Water Treat	ment Chemi	icals @ \$1.50/	KW-Yr		\$1,081,200	
C.	Maintenance	Conital Cost of Now Fr	Based on the	e capital cost o	of added equ	uipment.	¢400.440.470	
		Annual Percent of Can	juipment (se ital Cost	e estimate)			φ106,419,472 1.0%	
		Annual Maintenace Co	ists ( both m	aterials & labo	r)		\$1,084,195	
D.	Increased Pov	wer Requirements (plar	nt auxiliary	load)	0.5	ф Илан		
		Load	Units	Kw/Unit	C.F.	\$/Kwh	Annual Cost	
		Cooling Tower Pumps	4	1,865	0.85	\$0.030	\$1,666,415	
		Makeup Water Pumps	1	250	0.85	\$0.030 ¢0.030	\$55,845	
		Missellensous	48	207	0.85	\$0.030 ¢0.020	\$2,220,397	
		wiscellarieous	I	50	Subtotal	φ0.030	\$3.953.826	
E.	Decreased Ra	ting or Net Output of t	he Plant (at	the generator	r terminals)	\$/Kwh	Annual Cost	
			1	200	0.85	\$0.030	\$11 169	
		Percent of Capacity	·	0.02%	0.00	ψ0.000	ψ11,100	
F.	Fixed Annual (100% Operato	O & M Costs ors and 50% of Maint)		\$555,222	or	\$655	per MW	
G.	Variable O & I (50% Maint & 7	<b>M Costs</b> 100% Supplies & 100% /	Aux Load an	\$5,588,292 id 100% Decre	or ased Rating	\$0.885 g)	per MWh	
н.	Dispatch Pena	alty - One Time During	Constructio	on	0.5	<b>•</b> #4		
		Load	Months	Kw/Unit		\$/Kwh	Annual Cost	
		Overall Plant	U	848,000	0.85	<b>ъ</b> 0.030	\$0	
								Page 4

### **APPENDIX B – O&M COST ESTIMATE**

	Parsons Corporation Client:_U.S. E Project: Propo	OOE NETL sed Section 316b Coolir	ng Tower Re	trofits			Date: Proj. No.	1/31/2002 50802
	O & M COST I	ESTIMATE	2	2002 Dollars			Conceptual	
	Surry Nuclear	Power Plant - Unit # 2 - 8	348 MW			848	MW	
Α.	Operators	Туре	No - FTE	\$/ Yr	Burden	ОН	Annual Cost	
		Unskilled	0.2	\$20,000	0.5	0.25	\$7,500	
		Skilled	0.1	\$30,000	0.5	0.25	\$5,625	
		Supv	0	\$40,000	0.5	0.25	\$U \$0	
		Admin	0	φ20,000	0.0 Subtotal	0.25	⊅0 12 125	
					Subiolai		15,125	
В.	Supplies	Makeup & Water Treat	ment Chem	icals @ \$1.50/	KW-Yr		\$1,081,200	
C.	Maintenance	Capital Cost of New Ed	Based on th quipment (se	e capital cost o ee estimate)	f added equ	uipment.	\$108,419,472	
		Annual Maintenace Co	sts ( both m	aterials & labo	r)		\$1,084,195	
D. E.	Increased Pov	wer Requirements (plan Load Cooling Tower Pumps Makeup Water Pumps Cooling Tower Fans Miscellaneous	nt auxiliary Units 4 1 48 1 1	load) Kw/Unit 1,865 250 207 50 the generator	C.F. 0.85 0.85 0.85 0.85 Subtotal	\$/Kwh \$0.030 \$0.030 \$0.030 \$0.030	Annual Cost \$1,666,415 \$55,845 \$2,220,397 \$11,169 \$3,953,826	
			Units	KW/Unit	0.F.	\$/KWN	Annual Cost	
		Percent of Capacity	I	0.02%	0.05	φ0.030	\$11,109	
F.	Fixed Annual (100% Operato	O & M Costs ors and 1/2 of Maint)		\$555,222	or	\$655	per MW	
G.	Variable O & I (50% Maint & 7	<b>II Costs</b> 100% Supplies & 100% /	Aux Load ar	\$5,588,292 nd 100% Decre	or ased Rating	\$0.885 g)	per MWh	
Н.	Dispatch Pena	alty - One Time During	Constructio	on Kw/l loit	C F	¢/Kwb	Appual Cost	
			NOTITIS	848.000	0.F.	\$/ NWI		
			Ŭ	,				Page 5

	Parsons Corporation Client:_U.S. D Project: Propo	OOE NETL sed Section 316b Coolii	ng Tower Re	etrofits			Date: Proj. No.	1/31/2002 50802
	O & M COST E	ESTIMATE		2002 Dollars			Conceptual	
	Surry Nuclear Both Units #1 8	Power Plant & #2 - 848 MW Each				1,696	MW	
Α.	Operators	Туре	No - FTE	\$/ Yr	Burden	OH	Annual Cost	
		Unskilled	0.4	\$20,000	0.5	0.25	\$15,000	
		Sunv	0.2	\$30,000	0.5	0.25	φ11,250 \$0	
		Admin	0	\$20,000	0.5	0.25	\$0 \$0	
			Ũ	<i><i><b>Q</b></i>=0,000</i>	Subtotal	0.20	26,250	
В.	Supplies	Makeup & Water Trea	tment Cherr	nicals @ \$1.50/	KW-Yr		\$2,162,400	
C.	Maintenance	Capital Cost of New E	Based on th quipment (s	ne capital cost o ee estimate)	f added equ	ipment.	\$216,838,944	
		Annual Percent of Cap	oital Cost		A		1.0%	
		Annual Maintenace Co	osts ( both n	naterials & laboi	r)		\$2,168,389	
D.	Increased Pov	wer Requirements (pla Load Cooling Tower Pumps Makeup Water Pumps Cooling Tower Fans	nt auxiliary Units 8 2 96	r <b>load)</b> Kw/Unit 1,865 250 207	C.F. 0.85 0.85 0.85	\$/Kwh \$0.030 \$0.030 \$0.030	Annual Cost \$3,332,830 \$111,690 \$4 440 794	
		Miscellaneous	2	50	0.85	\$0.030	\$22,338	
				:	Subtotal		\$7,907,652	
E.	Decreased Ra	ting or Net Output of t	<b>he Plant (a</b> t	t the generator Kw/Unit	terminals)	\$/Kwh	Annual Cost	
		Overall Plant	1	400	0.85	\$0.030	\$22,338	
		Percent of Capacity	·	0.02%			<i> </i>	
F.	Fixed Annual (100% Operato	O & M Costs ors and 1/2 of Maint)		\$1,110,445	or	\$655	per MW	
G.	Variable O & I (50% Maint & 7	<b>II Costs</b> 100% Supplies 100% At	ux Load and	\$11,176,585 100%Decrease	or ed Rating)	\$0.885	per KW	
н.	Dispatch Pena	alty - One Time During	Constructi	ion Kw/Lloit	CE	¢/Kwb	Annual Cost	
		Overall Plant	0	1.696.000	0.85	\$0.030	\$0	
								Page 6

	Client:_U.S. D Project Propos	OE NETL sed Section 316b Coolin	g Tower Ret	trofits			Date: Proj. No.	1/31/2002 50802
	O & M COST	ESTIMATE	:	2002 Dollars			Conceptual	
	Big Bend Coal	Fired Power Plant - Unit	: #1 - 446 M	W		446	MW	
Α.	Operators	Туре	No - FTE	\$/ Yr	Burden	он	Annual Cost	
		Unskilled Skilled Supv Admin	0.25 0.1 0 0	\$20,000 \$30,000 \$40,000 \$20,000	0.5 0.5 0.5 0.5 Subtotal	0.25 0.25 0.25 0.25	\$9,375 \$5,625 \$0 \$0 15,000	
В.	Supplies	Makeup & Water Treatr	nent Chemi	cals @ \$1.50/	KW-Yr		\$501,750	
C.	Maintenance	Capital Cost of New Eq Annual Percent of Capi Annual Maintenace Cos	Based on th uipment (se tal Cost sts ( both ma	e capital cost o e estimate) aterials & labor	of added e )	quipment.	\$33,643,656 1.0% \$336,437	
D.	Increased Por	wer Requirements (plan Load Cooling Tower Pumps Makeup Water Pumps Cooling Tower Fans Miscellaneous	nt auxiliary Units 2 1 14 1	load) Kw/Unit 1,285 250 207 50	C.F. 0.75 0.75 0.75 0.75 0.75 Subtotal	\$/Kwh \$0.030 \$0.030 \$0.030 \$0.030	Annual Cost \$506,547 \$49,275 \$571,196 \$9,855 \$1,136,873	
E.	Decreased Ra	ating or Net Output of the Load Overall Plant Percent of Capacity	h <b>e Plant (at</b> Units 1	the generator Kw/Unit 0 0.00%	r <b>terminal</b> C.F. 0.75	<b>s)</b> \$/Kwh \$0.030	Annual Cost \$0	
F.	<b>Fixed Annual</b> (100% Operate	O & M Costs ors and 1/2 of Maint)		\$183,218	or	\$411	per MW	
G.	Variable O & (50% Maint &	M Costs 100% Supplies & 100% /	Aux Load ar	\$1,806,841 nd 100% Decre	or eased Rati	\$0.617 ng)	per MWh	
Н.	Dispatch Pen	alty - One Time During Load	Construction	on Kw/Unit	C.F.	\$/Kwh \$0.030	Annual Cost	
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	Parsons Corporation Client:_U.S. D Project Propo	OOE NETL sed Section 316b Coolin	g Tower Ret	rofits			Date: Proj. No.	1/31/2002 50802
	O & M COST	ESTIMATE	2	2002 Dollars			Conceptual	
	Big Bend Coa	I Fired Power Plant - Uni	t #2 - 446 M	W		446	MW	
Α.	Operators	Туре	No - FTE	\$/ Yr	Burden	ОН	Annual Cost	
		Unskilled	0.25	\$20,000	0.5	0.25	\$9,375	
		Skilled	0.1	\$30,000	0.5	0.25	\$5,625	
		Supv	0	\$40,000	0.5	0.25	\$0	
		Admin	0	\$20,000	0.5	0.25	\$0	
					Subtotal		15,000	
В.	Supplies	Makeup & Water Treat	ment Chemio	cals @ \$1.50/	KW-Yr		\$501,750	
C.	Maintenance	Capital Cost of New Ec Annual Percent of Capi	Based on th juipment (see	e capital cost ( e estimate)	of added e	equipment.	\$33,643,656 1.0%	
		Annual Maintenace Co	sts ( both ma	aterials & labor	)		\$336,437	
D.	Increased Po	wer Requirements (pla Load Cooling Tower Pumps Makeup Water Pumps Cooling Tower Fans Miscellaneous	nt auxiliary Units 2 1 14 14 1	load) Kw/Unit 1,285 250 207 50	C.F. 0.75 0.75 0.75 0.75 0.75 Subtotal	\$/Kwh \$0.030 \$0.030 \$0.030 \$0.030	Annual Cost \$506,547 \$49,275 \$571,196 \$9,855 \$1,136,873	
Е.	Decreased Ra	ating or Net Output of t	he Plant (at	the generato	r terminal	s)		
		Load	Units	Kw/Unit	C.F.	\$/Kwh	Annual Cost	
		Overall Plant Percent of Capacity	1	0 0.00%	0.75	\$0.030	\$0	
F.	Fixed Annual (100% Operat	O & M Costs ors and 1/2 of Maint)		\$183,218	or	\$411	per MW	
G.	Variable O & (50% Maint &	<b>M Costs</b> 100% Supplies & 100%	Aux Load ar	\$1,806,841 nd 100% Decre	or eased Rati	\$0.617 ng)	′ per MWh	
н.	Dispatch Pen	alty - One Time During	Constructio	on Kw/llpit	C F	¢/Kwb	Annual Cost	
			0	446 000	0.75	\$0.030		
			-	.,				Dogo 7
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	Parsons Corporation Client:_U.S. D Project Propos	OE NETL sed Section 316b Cooling	g Tower Ret	trofits			Date: Proj. No.	1/31/2002 50802
	O & M COST	ESTIMATE	:	2002 Dollars			Conceptual	
	Big Bend Coal	Fired Power Plant - Unit	: #3 - 446 M	W		446	MW	
Α.	Operators	Туре	No - FTE	\$/ Yr	Burden	ОН	Annual Cost	
		Unskilled	0.25	\$20,000	0.5	0.25	\$9,375	
		Skilled	0.1	\$30,000	0.5	0.25	\$5,625	
		Supv	0	\$40,000	0.5	0.25	\$0 \$0	
		Admin	0	\$20,000	0.5	0.25	\$0	
					Subtotal		15,000	
В.	Supplies	Makeup & Water Treatr	nent Chemi	cals @ \$1.50/	KW-Yr		\$501,750	
C.	Maintenance	Capital Cost of New Eq	Based on th	e capital cost o	of added e	quipment.	\$34.309.656	
		Annual Percent of Capit	al Cost	· · · · · ,			1.0%	
		Annual Maintenace Cos	sts ( both ma	aterials & labor	)		\$343,097	
D.	Increased Po	wer Requirements (plan	nt auxiliary	load)	C F	¢/Kwb	Appuel Cost	
		Load Cooling Tower Dumps	onits	1 265	0.75	\$/KWII		
		Makeun Water Pumps	∠ 1	250	0.75	\$0.030 \$0.030	φ030,003 \$40,275	
		Cooling Tower Fans	15	207	0.75	\$0.030 \$0.030	\$611 996	
		Miscellaneous	1	50	0.75	\$0.030	\$9.855	
					Subtotal	• • • • •	\$1,209,209	
E.	Decreased Ra	ating or Net Output of th	ne Plant (at	the generator	r terminal	s)		
		Load	Units	Kw/Unit	C.F.	\$/Kwh	Annual Cost	
		Overall Plant	1	0	0.75	\$0.030	\$0	
		Percent of Capacity		0.00%				
F.	Fixed Annual (100% Operate	O & M Costs ors and 1/2 of Maint)		\$186,548	or	\$418	8 per MW	
G.	Variable O & (50% Maint &	<b>M Costs</b> 100% Supplies & 100% /	Aux Load ar	\$1,882,507 nd 100% Decre	or eased Rati	\$0.642 ng)	2 per MWh	
н.	Dispatch Pen	alty - One Time During	Construction	on Kw/Unit	C.F.	\$/Kwh	Annual Cost	
		Overall Plant	0	446,000	0.75	\$0.030	\$0	
								Page 8

	Parsons Corporation							
	Client:_U.S. D Project Propos	OOE NETL sed Section 316b Coolin	g Tower Re	trofits			Date: Proj. No.	1/31/2002 50802
	O & M COST	ESTIMATE		2002 Dollars			Conceptual	
	Big Bend Coal	l Fired Power Plant - Unit	t #4 - 486 M	W		486	MW	
Α.	Operators	Туре	No - FTE	\$/ Yr	Burden	ОН	Annual Cost	
		Unskilled	0.25	\$20,000	0.5	0.25	\$9,375	
		Skilled	0.1	\$30,000	0.5	0.25	\$5,625	
		Supv	0	\$40,000	0.5	0.25	\$0	
		Admin	0	\$20,000	0.5	0.25	\$0	
					Subtotal		15,000	
В.	Supplies	Makeup & Water Treatr	ment Chemi	cals @ \$1.50/	KW-Yr		\$546,750	
C.	Maintenance		Based on th	e capital cost	of added e	quipment.		
		Capital Cost of New Eq	uipment (se	e estimate)			\$34,975,656	
		Annual Percent of Capit	tal Cost				1.0%	
		Annual Maintenace Cos	sts ( both ma	aterials & labor	·)		\$349,757	
	In an and Day			le e d				
D.	Increased Po	wer Requirements (plai	Int auxiliary	load) Kw/Lloit	CE	¢/Kwb	Annual Cost	
		Cooling Tower Pumps	2	1 450	0.75	\$0.030	\$571.500	
		Makeun Water Pumps	1	250	0.75	\$0.030	\$49 275	
		Cooling Tower Fans	16	207	0.75	\$0.030	\$652,795	
		Miscellaneous	1	50	0.75	\$0.030	\$9,855	
			•		Subtotal		\$1,283,515	
Е.	Decreased Ra	ating or Net Output of t	he Plant (at	the generato	r terminal	s)		
		Load	Units	Kw/Unit	C.F.	\$/Kwh	Annual Cost	
		Overall Plant	1	500	0.75	\$0.030	\$24,638	
		Percent of Capacity		0.10%				
F.	Fixed Annual	O & M Costs		\$189,878	or	\$391	per MW	
	(100% Operate	ors and 1/2 of Maint)						
•		N 0 (.		¢0.000.704		<b>\$0,000</b>		
G.	(50% Maint &	100% Supplies & 100%	Aux Load ar	52,029,781 nd 100% Decre	eased Rati	ა0.630 ng)	per www	
Н.	Dispatch Pen	alty - One Time During	Constructio	on Kw/Llpit	C F	¢/Kwb	Annual Cost	
			NOTION	446.000	0.75	\$0.020		
			0	440,000	0.75	φ0.030	<b>4</b> 0	
								Page 9

	Parsons Corporation Client:_U.S. D Project Propos	OE NETL sed Section 316b Coolin	g Tower Ret	rofits			Date: Proj. No.	1/31/2002 50802
	O & M COST	ESTIMATE	:	2002 Dollars			Conceptual	
	Big Bend Coal Unit #1, #2, #3	Fired Power Plant - Unit 3 @ 446 MW & #4 @ 486	t #3 - 446 M 6 MW	W		1,824	MW	
Α.	Operators	Туре	No - FTE	\$/ Yr	Burden	OH	Annual Cost	
		Unskilled	1	\$20,000	0.5	0.25	\$37,500	
		Skilled	0.4	\$30,000	0.5	0.25	\$22,500	
		Supv	0	\$40,000	0.5	0.25	\$U \$0	
		Aumin	0	φ20,000	Subtotal	0.25	φ0 000 03	
					Cubiola		00,000	
В.	Supplies	Makeup & Water Treatr	ment Chemi	cals @ \$1.50/	KW-Yr		\$2,052,000	
C.	Maintenance	Capital Cost of New Eq	Based on th uipment (se	e capital cost ( e estimate)	of added e	quipment.	\$136,572,624	
		Annual Percent of Capi	tal Cost				1.0%	
		Annual Maintenace Cos	sts ( both ma	aterials & labor	)		\$1,365,726	
D.	Increased Por	wer Requirements (plat Load Cooling Tower Pumps Makeup Water Pumps Cooling Tower Fans Miscellaneous	nt auxiliary Units 8 4 59 4	load) Kw/Unit 1,346 250 207 50	C.F. 0.75 0.75 0.75 0.75 Subtotal	\$/Kwh \$0.030 \$0.030 \$0.030 \$0.030	Annual Cost \$2,122,767 \$197,100 \$2,407,182 \$39,420 \$4,766,469	
E.	Decreased Ra	ating or Net Output of the	ne Plant (at	the generato		S) ¢/kwb	Annual Cost	
		Overall Plant	1	500	0.75	\$0.030	\$24 638	
		Percent of Capacity	I	0.03%	0.10	φ0.000	φ24,000	
F.	Fixed Annual (100% Operate	O & M Costs ors and 1/2 of Maint)		\$742,863	or	\$407	per MW	
G.	Variable O & (50% Maint &	<b>M Costs</b> 100% Supplies & 100% .	Aux Load ar	\$7,525,970 nd 100% Decre	or eased Rati	\$0.628 ng)	s per MWh	
н.	Dispatch Pen	alty - One Time During	Construction	on Kw/Llnit	C F	\$/Kwh	Annual Cost	
		Overall Plant	0	1,824,000	0.75	\$0.030	\$0	
								Page 10

	Parsons Corporation Client:U.S. Project:Prop	DOE NETL osed Section 316b Coolin	ng Tower Ret	rofits			Date: Proj. No.	1/31/2002 50802
	O & M COST E	STIMATE	2	2002 Dollars			Conceptual	
	Barney Davis G	as Fired Power Plant - Un	iit #1 - 353 N	IW		353	MW	
Α.	Operators	Туре	No - FTE	\$/ Yr	Burden	OH	Annual Cost	
		Unskilled	0.2	\$20,000	0.5	0.25	\$7,500	
		Skilled	0.1	\$30,000	0.5	0.25	\$5,625	
		Supv	0	\$40,000	0.5	0.25	\$U \$0	
		Admin	0	\$20,000	0.5	0.25	\$0	
					Subtotal		13,125	
В.	Supplies	Makeup & Water Treatm	nent Chemic	als @ \$1.50/	′KW-Yr		\$397,125	
C.	Maintenance	Capital Cost of New Equ	Based on t uipment (see	he capital co estimate)	st of added	l equipme	ent. \$23,560,416	
		Annual Percent of Capita	al Cost				1.0%	
		Annual Maintenace Cos	ts ( both mat	erials & labo	or)		\$235,604	
D.	Increased Pow	er Requirements (plant a Load Cooling Tower Pumps Makeup Water Pumps Cooling Tower Fans Miscellaneous	auxiliary loa Units 2 1 12 1 Plant (at the	d) <u>Kw/Unit</u> 955 250 207 50 e generator	C.F. 0.75 0.75 0.75 0.75 Subtotal	\$/Kwh \$0.030 \$0.030 \$0.030 \$0.030	Annual Cost \$376,461 \$49,275 \$489,596 \$9,855 \$925,187	
		Load	Units	Kw/Unit	C.F. ,	\$/Kwh	Annual Cost	
		Overall Plant Percent of Capacity	1	75 0.02%	0.75	\$0.030	\$3,696	
F.	Fixed Annual C (100% Operator	<b>8 M Costs</b> s and 1/2 of Maint)		\$130,927	or	\$371	per MW	
G.	Variable O & M (50% Maint & 10	Costs 00% Supplies & 100% Au:	x Load and <sup>2</sup>	\$1,443,810 100% Decrea	or ased Rating	\$0.623 g)	per MWh	
н.	Dispatch Penal	ty - One Time During Co	onstruction	Kw/l Init	C F	¢/Kwb	Annual Cost	
		Overall Plant	0	353,000	0.75	\$0.030	\$0	
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	Parsons Corporation Client:U.S. Project:Prop	DOE NETL losed Section 316b Coolir	ng Tower Ret	trofits			Date: Proj. No.	1/31/2002 50802
	O & M COST E	STIMATE	2	2002 Dollars			Conceptual	
	Barney Davis G	as Fired Power Plant - Ur	nit #2 - 351 M	1W		351	MW	
Α.	Operators	Туре	No - FTE	\$/ Yr	Burden	ОН	Annual Cost	
		Unskilled	0.2	\$20,000	0.5	0.25	\$7,500	
		Skilled	0.1	\$30,000	0.5	0.25	\$5,625	
		Supv	0	\$40,000	0.5	0.25	\$0	
		Admin	0	\$20,000	0.5	0.25	\$0	
					Subtotal		13,125	
В.	Supplies	Makeup & Water Treatn	nent Chemic	als @ \$1.50/	′ KW-Yr		\$394,875	
C.	Maintenance	Capital Cost of New Equ	Based on t uipment (see	he capital co estimate)	st of adde	d equipme	ent. \$23,560,416 1.0%	
		Annual Maintenace Cos	ts ( hoth mot	torials & labo	ur)		\$225 604	
		Annual Maintenace Cos			<i>'')</i>		φ233,004	
D.	Increased Pow	rer Requirements (plant Load Load Cooling Tower Pumps Makeup Water Pumps Cooling Tower Fans Miscellaneous	auxiliary loa Units 2 1 12 1	ad) Kw/Unit 955 250 207 50	C.F. 0.75 0.75 0.75 0.75 0.75 Subtotal	\$/Kwh \$0.030 \$0.030 \$0.030 \$0.030	Annual Cost \$376,461 \$49,275 \$489,596 \$9,855 \$925,187	
E.	Decreased Rat	ing or Net Output of the	Plant (at the	e generator	terminals	) • • // < h		
		Load	Units	KW/Unit	0.F.	\$/KWN	Annual Cost	
		Overall Plant Percent of Capacity	1	75 0.02%	0.75	\$0.030	\$3,696	
F.	Fixed Annual C (100% Operator	<b>D &amp; M Costs</b> rs and 1/2 of Maint)		\$130,927	or	\$373	8 per MW	
G.	<b>Variable O &amp; M</b> (50% Maint & 1	<b>l Costs</b> 00% Supplies & 100% Au	x Load and <sup>2</sup>	\$1,441,560 100% Decrea	or ased Rating	\$0.625 g)	öper MWh	
Н.	Dispatch Pena	Ity - One Time During Co	onstruction	Kw/Upit	0.5	¢/Kwb	Annual Coat	
			IVIOLITIUS	1.W/UIII	0.5.	φ/Γ\WΠ ΦΟ 020	Annual Cost	
		Overall Plant	U	353,000	0.75	<b>Ф</b> 0.030	\$0	
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O & M COST ESTIMATE     2002 Dollars     Conceptual       Barney Davis Gas Fired Power Plants - Unit 4* 109 333 MW & 428 251 MW     704     MW       A     Operators     Type     No -FTE     S/Yr     Burden     OH     Annual Cost       Unskilled     0.2     \$30,000     0.5     0.25     \$15,000       Skilled     0.2     \$30,000     0.5     0.25     \$00       Admin     0     \$20,000     0.5     0.25     \$00       Colling Tower Plants     Contrastructure (See estimate)     \$10%     \$171,208       Di Increased Power Requirements (plant auxillary load)     \$471,20,83     \$1,9%     \$471,20,85       Di Increased Power Requirements (plant auxillary load)     \$10%     Annual Cost     \$1,9%       Cooling Tower Fams     2     260     0.75     \$0,030     \$93,550       Cooling Tower Fams     2     207     0.75		Parsons Corporation Client:U.S. Project:Prop	DOE NETL osed Section 316b Coolin	ng Tower Re	trofits			Date: Proj. No.	1/31/2002 50802
Barney Davis Gas Fired Power Plants       7.4 MW         • Unit #1 @ 353 MW & #2 @ 351 MW       The *T to		O & M COST ESTIMATE 2002 Dollars						Conceptual	
A.         Operators         Type         No-FTE         S/Yr         Burden         OH         Annual Cost           Unskilled         0.4         \$20,000         0.5         0.25         \$15,000           Supy         0         \$40,000         0.5         0.25         \$30,000           Admin         0         \$20,000         0.5         0.25         \$30,000           Admin         0         \$20,000         0.5         0.25         \$30,000           Admin         0         \$20,000         0.5         0.25         \$30,000           Supplies         Makeup & Water Treatment Chemicals @ \$1.50/ KW-Yr         \$792,000         \$47,120,832           Annual Percent of Capital Cost of New Equipment (see estimate)         \$47,120,832         \$47,120,832           Annual Percent of Capital Cost         1.0%         \$471,208           D.         Increased Power Requirements (plant auxiliary load)         \$471,208           Cooling Tower Pumps         2         250         0.75         \$0.030         \$397,193           Miscellaneous         2         50         0.75         \$0.030         \$397,193           Miscellaneous         2         50         0.75         \$0.030         \$37,391		Barney Davis Gas Fired Power Plants         704           - Unit #1 @ 353 MW & #2 @ 351 MW         704						MW	
Unskilled       0.4       \$20,000       0.5       0.25       \$15,000         Skilled       0       \$20,000       0.5       0.25       \$12,250         Admin       0       \$20,000       0.5       0.25       \$30         B. Supplies       Makeup & Water Treatment Chemicals @ \$1.50 / KW-Yr       \$792,000         C. Maintenance       Based on the capital cost of added equipment.         Capital Cost of New Equipment (see estimate)       \$47,120,832         Annual Percent of Capital Cost       1.0%         Annual Maintenace Costs ( both materials & labor)       \$471,120,832         D. Increased Power Requirements (plant auxiliary load)       \$471,208         Cooling Tower Pumps 2       250       0.75       \$0.030       \$979,193         Miscellaneous       2       207       0.75       \$0.030       \$979,193         Miscellaneous       2       50       0.75       \$0.030       \$19,710         Subtotal       1       150       0.75       \$0.030       \$19,710         Subtotal       2       0.75       \$0.030       \$19,710         Subtotal       51,854       or       \$372,991       \$1,850,375         E.       Decreased Rating or Net Output of the Plant (at the generator te	Α.	Operators	Туре	No - FTE	\$/ Yr	Burden	OH	Annual Cost	
Skilled       0.2       \$30,000       0.5       0.25       \$11,250         Admin       0       \$20,000       0.5       0.25       \$0         Subtotal       26,250         B. Supplies       Makeup & Water Treatment Chemicals @ \$1.50/ KW-Yr       \$792,000         C. Maintenance       Based on the capital cost of added equipment. Capital Cost of New Equipment (see estimate)       \$47,120,832         Annual Percent of Capital Cost       1.0%       Annual Percent of Capital Cost       1.0%         Annual Maintenace Costs (both materials & labor)       \$471,208       \$471,208         D. Increased Power Requirements (plant auxiliary load)         \$471,208         Makeup Water Pumps       2       250       0.75       \$0.030       \$979,193         Miscellaneous       2       50       0.75       \$0.030       \$979,193         Miscellaneous       2       50       0.75       \$0.030       \$979,193         Miscellaneous       2       50       0.75       \$0.030       \$97,193         Miscellaneous       2       0.75       \$0.030       \$97,193         Miscellaneous       2       0.75       \$0.030       \$7,391         Subtotal       0       0.75       \$0			Unskilled	0.4	\$20,000	0.5	0.25	\$15,000	
Supp       0       \$40,000       0.5       0.25       \$0         Admin       0       \$20,000       0.5       0.25       \$0         B. Supplies       Makeup & Water Treatment Chemicals @ \$1.50/ KW-Yr       \$792,000         C. Maintenance       Based on the capital cost of added equipment. Capital Cost of New Equipment (see estimate)       \$471,120,832         Annual Percent of Capital Cost       1.0%         Annual Maintenace Costs (both materials & labor)       \$471,120,832         D. Increased Power Requirements (plant auxiliary load)       \$471,208         D. Increased Power Requirements (plant auxiliary load)       \$471,208         Makeup Water Pumps       2       250       0.75       \$0.030       \$979,193         Makeup Tower Pares       2       200       0.75       \$0.030       \$979,193         Miscellaneous       2       50       0.75       \$0.030       \$979,193         Subtotal       1       0.02%       \$1,850,375       \$1,850,375         E. Decreased Rating or Net Output of the Plant (at the generator terminals)       \$1,080,375         Percent of Capacity       0.02%       \$372 per MW         (100% Operators and 1/2 of Maint)       \$2,885,370       or       \$372 per MWh         (50% Maint & 100% Supplies & 100			Skilled	0.2	\$30,000	0.5	0.25	\$11,250	
Admin       0       \$20,000       0.5       0.25       30         Subtotal       26,250         B. Supplies       Makeup & Water Treatment Chemicals @ \$1.50/ KW-Yr       \$792,000         C. Maintenance       Based on the capital cost of added equipment. Capital Cost of New Equipment (see estimate)       \$47,120,832         Annual Maintenace       Cost of New Equipment (see estimate)       \$47,120,832         Annual Maintenace Costs ( both materials & labor)       \$47,120,832         D. Increased Power Requirements (plant auxiliary load)       Cooling Tower Pumps 2       250       0.75       \$0,030       \$9752,922         Makeup Water Pumps 2       250       0.75       \$0,030       \$979,193         Miscellaneous       2       250       0.75       \$0,030       \$979,193         Miscellaneous       2       207       0.75       \$0,030       \$979,193         Miscellaneous       2       207       0.75       \$0,030       \$19,710         Subtotal       0       0.75       \$0,030			Supv	0	\$40,000	0.5	0.25	\$0	
Subtotal     26,250       B. Supplies     Makeup & Water Treatment Chemicals @ \$1.50/ KW-Yr     \$792,000       C. Maintenance     Based on the capital cost of added equipment. Capital Cost of New Equipment (see estimate)     \$47,120,832 1.0% Annual Percent of Capital Cost       D. Increased Power Requirements (plant auxiliary load)     \$471,208       D. Increased Power Requirements (plant auxiliary load)     \$471,208       Cooling Tower Pumps     4     955     0.75     \$0.030     \$752,922       Makeup Water Pumps     2     250     0.75     \$0.030     \$98,550       Subtotal     Cooling Tower Fans     24     207     0.75     \$0.030     \$775,922       Miscellaneous     2     50     0.75     \$0.030     \$98,550       Subtotal     \$1,850,375     \$19,710     \$14,850,375       E. Decreased Rating or Net Output of the Plant (at the generator terminals)     \$1,850,375       Qiverall Plant     1     150     \$0.75     \$0.030     \$7,391       Percent of Capacity     0.02%     \$372 per MW       (100% Operators and 1/2 of Maint)     \$2,885,370     or     \$372 per MW       (50% Maint & 100% Supplies & 100% Aux Load and 100% Decreased Rating)     \$0.624 per MWh       (50% Maint & 100% Supplies & 100% Aux Load and 100% Decreased Rating)     \$0.030     \$0			Admin	0	\$20,000	0.5	0.25	\$0	
8. Supples       Makeup & Water Treatment Chemicals @ \$1.50 / KW-Yr       \$792,000         9. Maintenance       Capital Cost of New Equipment (see estimate)       \$47,120,832         Annual Maintenace Costs ( both materials & labor)       \$471,208         9. Increased Power Requirements (plant auxiliary load)       \$471,208         9. Increased Power Requirements (plant auxiliary load)       \$303,003         9. Increased Power Requirements (plant auxiliary load)       \$303,003         9. Increased Reting or Net Output of the Plant (at the generator terminals)       \$303,003         9. Makeup Water Pumps       2       250       0.75       \$0.030       \$\$98,550         9. Cooling Tower Fans       24       207       0.75       \$0.030       \$\$97,193         Makeup Water Pumps       2       250       0.75       \$0.030       \$\$91,910         9. Decreased Rating or Net Output of the Plant (at the generator terminals)       \$1,850,375         9. Orreall Plant       1       150       0.75       \$0.030       \$7,391         9. Percent of Capacity       0.02%       \$372 per MW       (00% Maint & 100% Supplies & 100% Aux Load and 100% Decreased Rating)         9. Variable O & M Costs       \$2,885,370       or       \$0.624 per MWh       (50% Maint & 100% Supplies & 100% Aux Load and 100% Decreased Rating)         <						Subtotal		26,250	
1. Mintenace       Based on the capital cost of added equipment.	В.	Supplies	Makeup & Water Treatm	nent Chemic	als @ \$1.50/	′ KW-Yr		\$792,000	
Annual Percent of Capital Cost Annual Maintenace Costs (both materials & labor)       1.0% \$471,208         D. Increased Power Requirements (plant auxiliary load) <ul> <li></li></ul>	C.	Maintenance	Capital Cost of New Equ	Based on t uipment (see	he capital co estimate)	st of addec	d equipme	ent. \$47,120,832	
Annual Maintenace Costs ( both materials & labor)       \$471,208         D. Increased Power Requirements (plant auxiliary load) <ul> <li></li></ul>			Annual Percent of Capit	al Cost				1.0%	
9. Increased Power Requirements (plant auxiliary load) <u>             Load             <u>             Units             <u>             Wubitit             <u>             V.5             <u>             S0.030             <u>             S998,550             S0.030             <u>             S979,193             </u> <u> </u></u></u></u></u></u></u></u></u></u></u>			Annual Maintenace Cos	ts ( both ma	terials & labo	or)		\$471,208	
Cooling Tower Pans       24       207       0.75       \$0.030       \$19,710         Miscellaneous       2       50       0.75       \$0.030       \$19,710         Subtotal       \$1,850,375         E. Decreased Rating or Net Output of the Plant (at the generator terminals) <u>Load</u> Units       Kw/Unit       C.F.       \$/Kwh       Annual Cost <u>Overall Plant</u> 1       150       0.75       \$0.030       \$7,391            Percent of Capacity       0.02%        0.02%        \$261,854       or       \$372 per MW             (100% Operators and 1/2 of Maint)           \$2,885,370       or       \$0.624 per MWh             (50% Maint & 100% Supplies & 100% Aux Load and 100% Decreased Rating)               S/Kwh       Annual Cost             H. Dispatch Penalty - One Time During Construction <u>Load</u> Months          Kw/Unit          C.F.          S/Kwh       Annual Cost             Overall Plant       0       704,000       0.75          S0.030          \$0	D.	Increased Pow	er Requirements (plant a Load Cooling Tower Pumps Makeup Water Pumps	auxiliary loa Units 4 2	ad) Kw/Unit 955 250	C.F. 0.75 0.75	\$/Kwh \$0.030 \$0.030	Annual Cost \$752,922 \$98,550	
Miscellaneous       2       50       0.75       \$0.030       \$19,710         Subtotal       Subtotal       \$1,850,375         E.       Decreased Rating or Net Output of the Plant (at the generator terminals)         Load       Units       Kw/Unit       C.F.       \$/Kwh       Annual Cost         Overall Plant       1       150       0.75       \$0.030       \$7,391         Percent of Capacity       0.02%         F.       Fixed Annual O & M Costs       \$261,854       or       \$372 per MW         (100% Operators and 1/2 of Maint)       \$2,885,370       or       \$0.624 per MWh         G.       Variable O & M Costs       \$2,885,370       or       \$0.624 per MWh         (50% Maint & 100% Supplies & 100% Aux Load and 100% Decreased Rating)       H.       Dispatch Penalty - One Time During Construction         Load       Months       Kw/Unit       C.F.       \$/Kwh       Annual Cost         Overall Plant       0       704,000       0.75       \$0.030       \$0			Cooling Tower Fans	24	207	0.75	\$0.030	\$979,193	
Subtotal       \$1,850,375         E.       Decreased Rating or Net Output of the Plant (at the generator terminals) <u>Load</u> Units       Kw/Unit       C.F.       \$/Kwh       Annual Cost <u>Overall Plant</u> 1       150       0.75       \$0.030       \$7,391         Percent of Capacity       0.02%         F.       Fixed Annual O & M Costs       \$261,854       or       \$372 per MW         (100% Operators and 1/2 of Maint)       \$2,885,370       or       \$0.624 per MWh         (50% Maint & 100% Supplies & 100% Aux Load and 100% Decreased Rating)       H.       Dispatch Penalty - One Time During Construction <u>Load</u> Months       Kw/Unit       C.F.       \$/Kwh       Annual Cost            Overall Plant       0       704,000       0.75       \$0.030       \$0			Miscellaneous	2	50	0.75	\$0.030	\$19,710	
<ul> <li>E. Decreased Rating or Net Output of the Plant (at the generator terminals) <ul> <li> <ul> <li> <ul> <li> <ul> <li> <li> <ul> <li> <li> <li> <li> <li> <li> <li> <l< th=""><th></th><th></th><th></th><th></th><th></th><th>Subtotal</th><th></th><th>\$1,850,375</th><th></th></l<></li></li></li></li></li></li></li></ul></li></li></ul></li></ul></li></ul></li></ul></li></ul>						Subtotal		\$1,850,375	
Load         Units         Kw/Unit         C.F.         \$/Kwh         Annual Cost           Overall Plant         1         150         0.75         \$0.030         \$7,391           Percent of Capacity         0.02%         0.02%         \$261,854         or         \$372 per MW           G. Variable O & M Costs (100% Operators and 1/2 of Maint)         \$2,885,370         or         \$0.624 per MWh           G. Variable O & M Costs (50% Maint & 100% Supplies & 100% Aux Load and 100% Decreased Rating)         \$0.624 per MWh           H. Dispatch Penalty - One Time During Construction Load         Months         Kw/Unit         C.F.         \$/Kwh         Annual Cost           Overall Plant         0         704,000         0.75         \$0.030         \$0	E.	Decreased Rati	ing or Net Output of the	Plant (at the	e generator	terminals)	)		
Overall Plant         1         150         0.75         \$0.030         \$7,391           Percent of Capacity         0.02%         0.02%         \$261,854         or         \$372 per MW           F. Fixed Annual O & M Costs         \$261,854         or         \$372 per MW           (100% Operators and 1/2 of Maint)         \$2,885,370         or         \$0.624 per MWh           G. Variable O & M Costs         \$2,885,370         or         \$0.624 per MWh           (50% Maint & 100% Supplies & 100% Aux Load and 100% Decreased Rating)         H.         Dispatch Penalty - One Time During Construction           Load         Months         Kw/Unit         C.F.         \$/Kwh         Annual Cost           Overall Plant         0         704,000         0.75         \$0.030         \$0			Load	Units	Kw/Unit	C.F.	\$/Kwh	Annual Cost	
F. Fixed Annual O & M Costs (100% Operators and 1/2 of Maint)       \$261,854 or       \$372 per MW         G. Variable O & M Costs (50% Maint & 100% Supplies & 100% Aux Load and 100% Decreased Rating)       \$0.624 per MWh         H. Dispatch Penalty - One Time During Construction Dverall Plant       C.F.       \$/Kwh       Annual Cost         0       704,000       0.75       \$0.030       \$0			Overall Plant Percent of Capacity	1	150 0.02%	0.75	\$0.030	\$7,391	
<ul> <li>G. Variable O &amp; M Costs \$2,885,370 or \$0.624 per MWh (50% Maint &amp; 100% Supplies &amp; 100% Aux Load and 100% Decreased Rating)</li> <li>H. Dispatch Penalty - One Time During Construction Load Months Kw/Unit C.F. \$/Kwh Annual Cost Overall Plant 0 704,000 0.75 \$0.030 \$0</li> </ul>	F.	Fixed Annual C (100% Operator	<b>) &amp; M Costs</b> is and 1/2 of Maint)		\$261,854	or	\$372	e per MW	
Load       Months       Kw/Unit       C.F.       \$/Kwh       Annual Cost         Overall Plant       0       704,000       0.75       \$0.030       \$0	G.	Variable O & M (50% Maint & 10	Costs 00% Supplies & 100% Au	x Load and <sup>-</sup>	\$2,885,370 100% Decrea	or ased Rating	\$0.624 g)	per MWh	
Overall Plant 0 704,000 0.75 \$0.030 \$0	н.	Dispatch Penal	<b>Ity - One Time During Co</b> Load	onstruction Months	Kw/Unit	C.F.	\$/Kwh	Annual Cost	
Page 6			Overall Plant	0	704,000	0.75	\$0.030	\$0	
1 dge e									Page 6

	Parsons Corporatio	n							
	Client: 11.5						Date:	1/31/2002	
	Project: Pro	nosed Section 316h C	ooling Tow	er Retrofits			Proi No	50802	
	FIOJECI. FIO	posed Section STOD C	ooning row	el Kellonis			F10j. NO.	50002	
	0 & M COST	ESTIMATE		2002 Dollars			Conceptual		
			-	LOOZ Donaro			Conceptual		
	Hudson Gas Fired Power Plant - Unit #1 - 455 MW 455 MW								
		_							
Α.	Operators	Туре	NO - FTE	<u>\$/ Yr</u>	Burden	OH	Annual Cost		
		Unskilled	0.25	\$20,000	0.5	0.25	\$9,375		
		Skilled	0.1	\$30,000	0.5	0.25	\$5,625		
		Supv	0	\$40,000	0.5	0.25	\$0		
		Admin	0	\$20,000	0.5	0.25	\$0		
					Subtotal		15,000		
В.	Supplies	Makeup & Water Trea	atment Che	emicals @ \$1	.50/ KW-Y	r	\$511,875		
C.	Maintenance	9	Based on	the capital co	ost of adde	d equipme	nt.		
		Capital Cost of New E	Equipment	(see estimate	e)		\$30,716,453		
		Annual Percent of Ca	pital Cost				1.0%		
		Annual Maintenace C	costs ( both	materials & I	labor)		\$307,165		
D.	Increased P	ower Requirements (	plant auxil	iary load)					
		Load	Units	Kw/Unit	C.F.	\$/Kwh	Annual Cost		
		Cooling Tower Pump	£ 2	955	0.75	\$0.030	\$376,461		
		Makeup Water Pump	: 1	250	0.75	\$0.030	\$49,275		
		Cooling Tower Fans	12	207	0.75	\$0.030	\$489,596		
		Miscellaneous	1	50	0.75	\$0.030	\$9,855		
					Subtotal		\$925,187		
Ε.	Decreased F	Rating or Net Output	of the Plan	t (at the gen	erator terr	ninals)			
		Load	Units	Kw/Unit	C.F.	\$/Kwh	Annual Cost		
		Overall Plant	1	500	0.75	\$0.030	\$24,638		
		Percent of Capacity		0.11%					
F.	Fixed Annua	al O & M Costs		\$168,582	or	\$371	per MW		
	(100% Opera	ators and 1/2 of Maint)							
		,							
G.	Variable O 8	M Costs		\$1,615,282	or	\$0.540	per MWh		
	(50% Maint &	& 100% Supplies & 100	)% Aux Loa	ad and 100%	Decreased	d Rating)			
н.	Dispatch Pe	nalty - One Time Duri	ing Constr	uction					
		Load	Months	Kw/Unit	C.F.	\$/Kwh	Annual Cost		
		Overall Plant	0	455,000	0.75	\$0.030	\$0		
							7 -		
								_	
								Page 4	

	Parsons Corporatio	n						
	Client:U.S	DOE NETL		or Potrofito			Date:	1/31/2002
	FIUJECI. FIU	posed Section 5100 C	Jooning Tow	el Relionis			Proj. No.	50602
	0 & M COS1	ESTIMATE	2	2002 Dollars			Conceptual	
	Hudson Coal	Fired Power Plant - U	MW					
Α.	Operators	Туре	No - FTE	\$/ Yr	Burden	ОН	Annual Cost	
		Unskilled	0.25	\$20,000	0.5	0.25	\$9,375	
		Skilled	0.1	\$30,000	0.5	0.25	۵,625 مع	
		Admin	0	\$20,000	0.5	0.25	\$0 \$0	
			Ū	<i><b>Q</b>20,000</i>	Subtotal	0.20	15.000	
В.	Supplies	Makeup & Water Tre	atment Che	emicals @ \$1	.50/ KW-Yı	r	\$742,500	
C.	Maintenance	9	Based on	the capital co	ost of adde	d equipme	nt.	
		Capital Cost of New	Equipment	(see estimate	e)		\$42,807,816	
		Annual Percent of Ca	apital Cost				1.0%	
		Annual Maintenace C	Costs ( both	materials &	labor)		\$428,078	
_								
D.	Increased P	ower Requirements (	plant auxil	liary load)	C F	¢/Kuch	Annual Coat	
		Load Cooling Tower Pump	Units	1.400	0.F.	\$/KWII	Annual Cost	
		Makeun Water Pump	י: ∠ אי 1	250	0.75	\$0.030	\$49 275	
		Cooling Tower Fans	, i 19	207	0.75	\$0.030	\$775.194	
		Miscellaneous	1	50	0.75	\$0.030	\$9,855	
					Subtotal		\$1,421,682	
E.	Decreased F	Rating or Net Output	of the Plan	t (at the gen	erator terr	ninals)		
		Load	Units	Kw/Unit	C.F.	\$/Kwh	Annual Cost	
		Overall Plant	1	800	0.75	\$0.030	\$39,420	
		Percent of Capacity		0.12%				
F.	Fixed Annua	al O & M Costs		\$229,039	or	\$347	per MW	
	(100% Opera	ators and 1/2 of Maint)						
G.	Variable O 8 (50% Maint 8	& <b>M Costs</b> & 100% Supplies & 10	0% Aux Loa	\$2,417,641 ad and 100%	or Decreased	\$0.558 d Rating)	per MWh	
н.	Dispatch Pe	nalty - One Time Dur	ing Constr Months	ruction Kw/LInit	CF	\$/Kwh	Annual Cost	
		Overall Plant	0	455,000	0.75	\$0.030	\$0	
			2	,			40	
								Page 5

	<b>D</b> 0 "							
	Client: US						Data	1/31/2002
	Dreiset: Dro	DUE NETL	oling Tow	or Dotrofito			Dale.	F0902
	Project: Pro	posed Section 316b CC	oling Tow	er Retronts			Proj. No.	50802
	0 % M COST	ECTIMATE	<u> </u>	002 Dellara			Concentual	
		ESTIMATE	2	002 Dollars			Conceptual	
	Hudson Pow	er Plants				1,115	MW	
	- Unit #1 Gas	@ 455 MW & #2 Coal	@ 660 M\	N		.,e		
Δ	Operators	Type	No - FTF	\$/ Yr	Burden	он	Annual Cost	
7.0	oporatoro	l Inskilled	0.5	\$20,000	0.5	0.25	\$18,750	
		Skilled	0.2	\$30,000	0.5	0.25	\$11,250	
		Supy	0.2	\$40,000	0.5	0.25	¢11,200 \$0	
		Admin	0	\$20,000 \$20,000	0.5	0.25	0¢ 02	
		Aumin	0	φ20,000	0.5 Subtotal	0.25	ψ0 20.000	
					Subiolai		30,000	
_							• · · · · ·	
В.	Supplies	Makeup & Water Trea	tment Che	micals @ \$1	.50/ KW-Yı	r	\$1,254,375	
C.	Maintenance	e	Based on t	the capital co	ost of added	d equipmer	nt.	
		Capital Cost of New E	4	1,539			\$73,524,269	
		Annual Percent of Ca	1	250			1.0%	
		Annual Maintenace C	48	171			\$735,243	
							. ,	
П	Increased P	ower Requirements (n	lant auxil	iary load)				
	moreaceury	hoad	l Inite	Kw/Linit	CE	\$/Kwh	Annual Cost	
		Cooling Tower Dumps	4	1 222	0.75	\$0.020	¢062 910	
		Cooling Tower Pump:	4	1,223	0.75	\$0.030 ¢0.030	\$903,019	
		Makeup Water Pump	2	250	0.75	\$0.030	\$98,550	
		Cooling Tower Fans	31	207	0.75	\$0.030	\$1,264,791	
		Miscellaneous	2	50	0.75	\$0.030	\$19,710	
					Subtotal		\$2,346,870	
Ε.	Decreased F	Rating or Net Output o	f the Plan	t (at the gen	erator tern	ninals)		
		Load	Units	Kw/Unit	C.F.	\$/Kwh	Annual Cost	
		Overall Plant	1	1.300	0.75	\$0.030	\$64.058	
		Percent of Capacity		0 12%			*- ,	
		r crocint of Oupdoity		0.1270				
F	Fixed Annua			¢207 624	<b></b>	¢057	DOT MAA	
г.		al U & IVI COSIS		\$397,021	OI	\$30 <i>1</i>	per www	
	(100% Opera	ators and 1/2 of Maint)						
-				• · · · · · · · · ·		<b>.</b>		
G.	Variable O 8	M Costs		\$4,032,924	or	\$0.551	per MWh	
	(50% Maint 8	& 100% Supplies & 100	% Aux Loa	ad and 100%	Decreased	d Rating)		
Н.	Dispatch Pe	nalty - One Time Durii	ng Constr	uction				
		Load	Months	Kw/Unit	C.F.	\$/Kwh	Annual Cost	
		Overall Plant	0	1,115,000	0.75	\$0.030	\$0	
								Page 6

# **APPENDIX C**

# JANUARY 22, 2003 ADDENDUM

**Addendum to Report** 

# "An Investigation Site-Specific Factors for Retrofitting Recirculating Cooling Towers at Existing Power Plants"

January 22, 2003

Prepared by

The United States Department of Energy National Energy Technology Laboratory

### **Executive Summary**

### Background

This addendum updates a report prepared by Parsons Corporation (Parsons) for the Department of Energy/Office of Fossil Energy's National Energy Technology Laboratory (DOE/NETL). The purpose of the addendum is to provide further information on the critical role that site-specific factors can have on the cost and feasibility of retrofitting cooling towers on thermoelectric power plants that currently employ once-through cooling.

The Parsons report was commissioned during the relatively brief interagency review period for the Environmental Protection Agency's §316(b) Phase II proposed rule for existing power plants. One of the Agency's regulatory options under consideration at that time was to require that over fifty (50) existing thermoelectric power plants retrofit from once-through cooling systems to wet recirculating towers. The Parsons analysis focused on the feasibility of implementing such a requirement on four existing steam-condensing power plants taking into consideration site-specific factors. DOE/NETL used the results of the analysis to provide input to EPA during the proposal's public comment period on the impacts that site-specific factors could have on retrofitting once-through plants with recirculating cooling towers.

The Parsons report was intended to provide a preliminary assessment -- a "30,000-foot view"-- of how site-specific factors might affect the cost of installation of cooling towers and ancillary equipment and any resultant economic and energy impacts on plant operations. Parsons was tasked with completing the study in four weeks and was instructed not to contact the utilities that owned the four plants since the interagency review process was ongoing. Therefore, Parsons was not able to obtain the requisite plant data from the plant operators that would typically be used to generate a detailed site-specific analysis. Nevertheless, while using only publicly available information and aerial photographs, the Parsons study concluded that the retrofit of closed-loop cooling systems at the four existing power plants would impose significant capital cost burdens and loss of net generation output.

Subsequent to the issuance of the Parsons report, DOE/NETL had discussions with each of the four utilities that own the power plants evaluated in the study. These discussions focused on actual site-specific concerns expressed by these utilities. We also sought comment about design parameters selected in the study and input on other issues that would affect the installation and operation of cooling towers at these and similar plants that DOE/NETL was unable to obtain during the interagency review. The subject addendum summarizes the supplementary information that was provided by the four utilities and presents a discussion of the impact of this new information on the cost and feasibility of retrofitting wet cooling towers on the four power plants.

The overall conclusion based on DOE/NETL analysis of the supplemental site-specific information is that cooling towers can be more difficult, and more costly, to retrofit than
one would assume based solely on publicly available information. Based on this additional information, we believe that it is critical that EPA recognizes in its rulemaking process that the cost and operational impacts of retrofitting once-through cooling systems must be evaluated on a case-by-case basis. The additional site-specific information also makes it clear that adverse environmental impacts (AEI) beyond those associated with impingement and entrainment and beyond water quality in general, would be caused by a requirement to retrofit to wet cooling towers. The other AEI include endangered species issues, visibility issues, noise pollution, salt corrosion, increased air emissions, and increased waste, and would impact cooling tower retrofit options.

### **General Issues**

### Siting

Parsons utilized publicly available aerial photographs to recommend locations for the installation of cooling towers at each of the plants. Additional site-specific information provided by the utilities has shown that most of the locations suggested in the report would not be feasible due to factors unknown at the time of the Parson's study. These factors include the presence of existing landfills, desalinization plants, railroad tracks, and other facilities, as well as commitments to use the targeted location for other purposes. The result of the actual site-specific information is that *three* of the four sites would require a more remote placement of the towers that would result in higher costs and possibly longer outage times.

### Plume Abatement

One of the four plants investigated by the Parsons report was deemed to require plume abatement. Additional information provided by the utilities indicates that at least *three* of the four plants would likely require plume abatement due to local factors that were not known at the time of the Parsons study. Plume abatement measures would double the capital cost of the resulting cooling tower and result in other AEI.

# Salt Drift

Even with optimum drift control there will be particulate emissions of salt from cooling towers employing salt water. These will have corrosive impacts within the power plant and may have adverse environmental impacts outside the plant boundaries. The consequences of adequately addressing salt emissions from the cooling towers include adding additional cost for salt drift reduction at three of the four plants and recognition of other AEI. At one of the plants it is likely that the State and Federal air quality standards for particulate emissions would be exceeded and a variance for the wet tower would be extremely unlikely.

### Noise Abatement

Due to the need to re-site several of the wet towers based on new actual plant-specific information, the new locations close to urban areas would require some amount of noise abatement technologies. These would both increase the original Parsons' cost estimates and create additional AEI.

### Local Uses Related to Cooling Water Intake and Discharge

At the nuclear facility that was evaluated the intake canal and pumps are also used for emergency cooling. In addition, at one of the fossil-fuel-fired plants, the discharge canal is used to dilute brine discharge from a desalination plant as well as to provide a warm water sanctuary for manatees, an endangered species. While these site-specific considerations were not included in the initial Parsons study they clearly would limit the practicality of reducing cooling water flow rates at these plants that would result from the installation of a closed-loop system.

### Outage Times

The Parsons study assumed conservatively that all of the construction required for retrofitting the cooling tower systems could be performed while the plant is on line, thereby minimizing cost and energy impacts due to plant outages. Based on the input provided by the site operators, it appears that an extended outage would be required by two of the four plants resulting in losses in revenue. The impact of the loss of generating capacity - aside from the loss of revenue attributable to the plant - from these units during retrofit would need to be evaluated based on the historical records and projections of future dispatch for each plant.

### Energy Penalty

The Parsons study used nearby wet bulb temperatures that were lower than temperatures actually experienced at some plant sites. This would result in an increase in actual energy penalty. Furthermore, the Parsons study is based on a 2 percentile of maximum wet-bulb incidence rather than the 1 percentile normally used to calculate the impacts on electricity generation during the times of peak summer demand. The 1 percentile of maximum wet-bulb temperature is typically a few degrees higher than the 2 percentile. For a given cooling tower design, an increase in wet-bulb temperature translates directly to increases in condenser temperature, with corresponding increases in turbine back pressure and the resultant energy penalty.

# Revenue Loss

In terms of lost revenues, Parsons assumed a conservative replacement cost of electricity based on the average annual price of electricity of \$0.03/kWh. However, the greatest loss in energy output from plants with cooling towers would be on the hottest, most humid days of the year when market prices for electricity are far greater than \$0.03/kWh. The value of lost revenue could be calculated more accurately by looking at historical records of each plant and the specific price of power in each region, a level of detail that was

neither feasible, nor in the scope of the Parsons study. Nevertheless, this lost revenue could be significant in some cases.

# **General Conclusions**

The Parsons report highlighted the critical importance of site-specific factors such as those discussed above in the final determination of the costs and impacts of retrofitting to recirculating cooling towers in existing power plants. At the plants considered in this study, the incorporation of additional actual and more detailed site-specific information had the impact of increasing cooling tower capital cost estimates by as much as 100 percent. More importantly, other uses or beneficial impacts of the existing cooling water systems suggest that some cooling tower projects that seem workable as a general proposition are impractical at any cost when these site-specific uses are considered.

The opportunity to consult with the utility companies has demonstrated that the issue of retrofitting cooling towers is even more complex than shown in the report. Therefore, DOE/NETL reiterates its strong preference for a site-specific approach to implementation of §316b regulations. In addition, the finding that non-water related adverse environmental impacts will almost certainly result from installation of cooling towers at some, if not most, sites leads us to conclude that all AEI should be considered in a regulation that contemplates measures such as retrofitting cooling towers.

# **Plant Specific Issues and Responses**

Subsequent to the issuance of the Parsons report, DOE/NETL obtained site-specific information from the electric-utility companies that operated the four plants included in the Parsons report that was not available at the time the report was prepared. Input was provided from America Electric Power (AEP) Company Inc., owner of the Barney M. Davis plant, Tampa Electric Company (TECO) Inc., owner of the Big Bend Station, PSEG Fossil LLC, owners of the Hudson Generating Station, and Dominion Virginia Power Inc., owner of the Surry Power Station.

The following presents a discussion of the comments received and DOE/NETL's assessment of those comments that would significantly impact the general conclusions reached in the Parsons report.

# **Big Bend Station**

# Siting Issues

The Parsons report sited the "conceptual" cooling tower on land that is unavailable. Part of the "conceptual" cooling tower is located on land that is occupied by a 25 million gallon per day seawater desalination plant that is under construction at the Big Bend power station.

An alternative possibility would be to construct a cooling tower south of the plant at a site currently used for byproduct management operations (beneficial use of waste to produce gypsum). The land is adjacent to the Apollo Beach residential community and proximate to an undeveloped coastal area covered with sensitive vegetation. Major modifications to the design of the cooling tower system, if sited at this location, would likely be required to minimize adverse environmental impacts and accommodate local permitting requirements. These modifications would require significantly higher costs. Furthermore, the existing byproduct management activities would have to be relocated and changed, thus requiring a detailed alternative analysis to minimize the impact on byproduct handling.

### Plume Abatement Issues

The Parsons report does not include plume abatement technology in the cost estimate for the closed-loop, wet cooling tower retrofit at the Big Bend Station site. However, the Big Bend site is located adjacent to the Apollo Beach residential community. Although the need for plume abatement technology at the Big Bend Station site would not be determined until the actual permitting process was completed, the inclusion of such technology would likely be needed and would double the cooling towers' capital costs and significantly increase their annual operating and maintenance costs.

### Adverse Environmental Impact Issues

The Parsons report does not include several potential adverse environmental impact issues associated with installation of a cooling tower system as defined in their conceptual study. The adverse environmental impacts that would need to be considered, and potential remedies sought include: (1) impact on endangered species such as the manatee that live in warmer waters created from the Big Bend discharge during the winter months; (2) increased air pollution emissions from power production due to loss in power plant efficiency; (3) visibility concerns from cooling tower plume; and (4) increased particulate emissions from cooling tower exhaust.

The Big Bend Station cooling water discharge provides a warm water refuge for manatees in the winter season and the discharge canal has been designated by the State of Florida as a Manatee Sanctuary. This benefit would be lost if the Big Bend Station were to retrofit their once-through cooling system with a recirculating cooling tower system.

The best available location for siting a cooling tower requires relocation of gypsum handling and raises the potential for salt contamination. A careful analysis and design would be required to determine if saleable gypsum can still be produced or if alternative disposition would be required.

Remedies to mitigate or avoid these potential adverse environmental impacts are sitespecific and would require a detailed assessment of alternative measures.

### Lost Revenue Issues

Big Bend Station currently has a salable byproduct, gypsum, with annual revenue of \$2 million. If the chloride level of the gypsum were raised above acceptable limits from exposure to salt drift, these revenues would be lost. Alternative utilization paths for the gypsum would have to be explored. Soil stabilization and trail construction are two potential uses. If alternative beneficial uses cannot be found, gypsum disposal costs would likely be an order of magnitude higher than current gypsum sales resulting in a total annual net revenue loss of about \$20 million.

### Outage Time

It is likely that tie-in of a cooling tower system would be scheduled concurrent with a major outage for the power plant. Since the cooling tower tie-in would need to accommodate connections with the condenser and the desalination plant, it is likely that the cooling tower tie-in outage would significantly exceed a scheduled outage. Given the substantial congestion amongst above and underground facilities and the complexities associated with new lines and sumps for the desalination plant at the Big Bend Station, DOE/NETL believes that the cooling tower tie-in outage time would require a detailed engineering analysis estimate.

### Energy Penalty

The energy penalty estimated in the study for the cooling tower retrofit probably underestimated the actual energy penalty for the following reasons: (1) the temperature rise across the condensers is designed for a 17 degree rise rather than the 15 degree rise assumed in the Parsons report; (2) Big Bend Station rejects 70 percent of the rated steam flow rather than the 65 percent rejection rate assumed in the Parsons report; (3) turbine configurations for 2 of the 4 units at Big Bend Power Station were different than assumed in the Parsons report; and (4) the wet bulb temperature and summer average water temperature at the Big Bend Station are higher than estimated in the Parsons report.

The steam turbine exhaust physical design parameters coupled with condensing steam flow rates have a significant impact on steam turbine generator electric output and plant efficiency. Changes in turbine configuration from those used in the Parsons study could have a significant impact on the predicted change in generation output. Seasonal average values for cooling water and ambient wet bulb temperature do not reflect the extreme hot summer weather, which is coincident with highest demand for power and the highest cost for replacement power. The combination of factors listed above will increase the energy penalty estimated in the Parsons report. A more detailed study, beyond the scope of the "conceptual" estimate, is required to provide a more accurate estimate of energy penalty.

### Economic Issues

The desalination plant begins operation this year and was not pictured on the aerial photo used by Parsons. Neglecting the existence of the desalination plant significantly reduces

plant cost associated with installation of a cooling tower at the Big Bend Station. The desalination plant is currently configured to dilute brine discharge with water discharged from the once through cooling system. The reduced water discharge associated with a cooling tower would require an alternative strategy to be developed for the disposal of brine concentrate. Tampa Electric Company considered one other option that entailed discharging the brine concentrate via pipeline into the center of Tampa Bay. That study indicated that the plant would not be economically feasible if a mid-bay discharge were included. Since the current rulemaking could result in installation of such a discharge system 5 or more years after the desalination system is in operation and when it's capacity will be more than four times the initial capacity, DOE/NETL is unable to determine the magnitude of the potential cost impact on this project.

In addition to cost increases related to providing dilution for the desalination brine, siting issues associated with the cooling tower in a less convenient location than assumed in the Parsons report would significantly increase capital and operating costs at the power plant. There is also a potential annual loss in revenue of \$20 million if gypsum byproduct sales are lost due to higher chloride content of the gypsum from salt drift deposition and more difficult management of gypsum because of encroachment of the cooling tower at the gypsum treatment area.

Revenues lost from extended outage time to tie-in the cooling tower system are expected to be significant. It is not possible to quantify lost revenues without a detailed engineering study.

The capital cost of the cooling tower situated on available land is estimated to be twice the capital cost estimated in the Parsons conceptual estimate. The major reason for this cost increase is the likely need to install plume abatement technology. If a cooling tower system were to be installed at Big Bend Station there would also likely be a need to have an extensive review of adverse environmental impacts that would increase the normal time needed to secure local, State, and Federal permits.

### **Hudson Generating Station**

### Siting Issues

Due to local sensitivity to a fatal Conrail train accident that occurred several years ago, it would be politically unacceptable to locate the cooling towers in proximity to the railroad tracks as they are shown in the Parsons design. That is, even a plume abated cooling tower under some conditions of weather could produce a low hanging plume that would obscure the visibility of any trains and its drift could ice the tracks.

In addition, planned modifications to the New Jersey Turnpike will physically interfere with the cooling tower location as proposed in the Parsons report. The SCRs and scrubbers that PSEG is obligated to regulatory agencies to install in 2006 and 2007 would prevent location closer to the powerhouse.

A more suitable location, further away from the power house, would entail considerably higher construction costs and pumping power requirements. This location, toward the North, would be on the other side of the Conrail railroad tracks and in the case of Unit 2, also across Penhorn Creek.

In that location, a full evaluation of the capital costs would require adding expensive bridging and tunneling of large diameter pipes to and from the towers to traverse these barriers. The stream crossings would also be subject to large permitting costs because of the environmental issues involved. This difference is reflected in the site-specific cost estimate PSEG prepared in 1997 (see below), which budgets \$35,067,804 for pumps and piping systems, versus the total cost of \$11,918,000 estimated for the same items in the Parsons report.

# Noise Issues

Because the design is very open, noise abatement features on a wet-dry tower are generally a necessity, particularly if the tower is to be located near an urban environment, as would be the case at Hudson. The capital costs of noise abatement attenuation on cooling towers are usually very significant. The resulting operating costs can also be much greater. This aspect of the application of a wet-dry cooling tower design is neglected in total and thus these costs are not reflected in the Parsons report.

### Energy Penalty Issues

PSEG identified several assumptions in the Parsons report that would tend to underestimate the energy penalty associated with the installation of wet-dry cooling towers at the Hudson site.

- The study is based on a circulating cooling water flow that is 20,000 gallons per minute lower than the actual value. This means that the tower size and pumping power needed may have been underestimated by approximately 9 percent in the report.
- The study is based on a 2 percentile of maximum wet bulb incidence rather than the 1 normally used. This means that the lower corresponding wet-bulb temperature (74°F) selected in the study instead of the higher 1 percentile wet bulb of 76°F. This change would mean a 2 degrees F increase in condenser temperature, with corresponding increases in turbine back pressure and associated energy penalty.
- The adverse impacts of using brackish water in a cooling tower, as regards lower evaporation potential, lower thermodynamic properties, and extra pumping power requirements due to greater density were not included in the Parsons report.

# Salt Drift Issues

Compliance with State and Federal air quality regulations would likely not be possible for particulate emissions (PM) from mechanical draft cooling towers at Hudson Generation Station. Predicted PM emissions due to salt drift from the mechanical draft tower on Unit No. 2 exceed the maximum allowable rate of 30 pounds per hour and thus a variance from these regulations would be required. Due to the urban setting of the site, PSEG believes that obtaining this variance would be difficult or impossible.

### Cooling Tower Blowdown Issues

Water quality regulations are strict in New Jersey and require treating the cooling tower blowdown water. Both the temperature and pollutant levels of any returning water must achieve regulatory permit compliance.

PSEG's detailed site-specific study, made in 1997 (see below), estimates that treating the cooling tower blowdown water at Hudson to meet these regulatory requirements would require a \$5,508,000 treatment facility. This treatment facility was not included in the Parsons estimate.

#### Outage Issues

The Parsons report assumes that retrofit work would fit into the normal spring or fall outage timeframe. However, a more likely scenario is that an extended scheduled outage would be required for the final tie-ins, intake modifications, existing CW piping modifications, services, start-up and testing. This outage construction period was estimated by the PSEG engineering study to be from 2 to 3 months for Hudson Station.

#### Permitting Issues

PSEG has recently obtained licenses and permits for the installation of a new, combined cycle unit with recirculating cooling towers at its Linden Generating Station. Based on this experience, PSEG estimates that it would take at least one year to acquire the four Federal, eight State, one county, and four municipal permits required for the retrofit of Hudson station with closed cycle cooling. This significant permitting effort was not included in the Parsons estimate for the proposed conversion.

### Differences in Construction Cost Estimates

In 1997 PSEG obtained turnkey budget pricing from three respected cooling tower manufacturers based on a specification derived from a detailed site-specific engineering study defining the requirements for the potential conversion of Hudson Station to closed-cycle cooling.

• Based on the lowest of those vendor quotes, that turnkey tower cost of \$48,580,000 (in 1997 dollars) was approximately twice the corresponding \$24,800,000 (in 2002 dollars) tower cost estimated by Parsons.

- The total estimated project cost for the conversion of Hudson units 1 and 2 to wet-dry towers was \$168,250,250 (in 1997 dollars), and was more than double the corresponding \$73,524,000 (in 2002 dollars) total project cost estimated by Parsons.
- The significant difference in costs between the vendor quotes and PSEG's estimated project cost and the costs estimated by Parsons further highlights the need for site-specific information in determining the economic feasibility of retrofitting once-through power plants with closed-loop systems.

# **Surry Power Station**

### Plume Abatement Issues

The Parsons report did not include plume abatement technology in the cost estimate for the closed-loop wet cooling tower retrofit at the Surry Power Station site. However, based on the relatively close proximity of Colonial Williamsburg (8 miles) and Busch Gardens (7.5 miles) to the Surry Power Station, plume abatement technology could be required. Although the need for plume abatement technology at the Surry Power Station site would not be determined until the actual permitting process was completed, the inclusion of such technology would double the cooling towers' capital costs and significantly increase their annual operating and maintenance costs.

### Emergency Services Issues

Dominion expressed concern with respect to maintaining the integrity of operation of the Surry Power Station's Emergency Service Water pumps under the proposed wet cooling tower retrofit design. Preserving the integrity and operation of the Surry Power Station's Emergency Service Water pumps is a significant safety issue. Dominion's concern is valid and serves to underscore how the understanding of truly site-specific issues is critically important to the retrofit design process.

# Lost Revenue Issues

The Parsons report assumed that lost power could be replaced at an average annual electricity cost of \$0.03/kWh. The greatest loss in energy output from plants with cooling towers would be on the hottest, most humid days of the year when market prices are far greater than \$0.03/kWh. The value of lost revenue could be calculated more accurately by looking at historical records of each plant and the specific price of power in each region, a level of detail that was neither feasible, nor in the scope of the Parsons study. Nevertheless, this lost revenue could be significant in some cases and also serves to underscore the site-specific nature of retrofitting with cooling towers.

### Energy Penalty Issues

Dominion Virginia Power presents data in support of their position that the Parsons study may underestimate the energy penalty that is attributable to the warmer cooling water

temperatures associated with the installation of cooling towers at the Surry Power Station site. The issue of lost revenue, from the preceding paragraph, becomes more significant as the actual energy penalty becomes larger.

### **Barney M. Davis**

### Salt Drift

There are several research facilities that lease space on the Barney M. Davis property. These facilities are located between 500 to 1000 feet downwind from the site of the proposed cooling towers. Based on this information and considering the corrosivity of the drift, some type of drift abatement might be required. Salt drift control is a site-specific issue and if it should be required at the Barney M. Davis site, it would increase the proposed cooling towers' capital and annual operating and maintenance costs over that which was reported in the Parsons study and cause other AEI.

### Capital Cost Issues

AEP Inc. secured a cooling tower budget estimate, using actual Barney M. Davis plant operating conditions, from the Marley Cooling Technologies Company. AEP's cooling tower material and labor costs, using a wet-bulb temperature of 77 °F, an 8 °F approach temperature, an 180,000 gallon per minute flow rate, and a 20 °F condenser range, was between \$5.2 and \$5.5 million per tower. The Parsons material and labor estimate using the same wet-bulb and approach temperatures, but with a 215,000 gallon per minute flow rate and a 15 °F condenser range, was \$4.8 million. In this manner, the Parsons report may have underestimated the material and labor costs for a wet cooling tower retrofit at the Barney M.Davis plant by between 8 and 15 percent. Cooling water flow rate and the coolant temperature range through the condenser are two site-specific operating parameters that directly affect the proposed cooling towers' costs and the potential energy penalties associated with their retrofit to once-through cooled facilities.